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SOLUBILITY DATA SERIES

Volume 2

KRYPTON, XENON AND RADON — *Gas Solubilities*

## SOLUBILITY DATA SERIES

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# SOLUBILITY DATA SERIES

Volume 2

KRYPTON, XENON AND RADON — *Gas Solubilities*

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FOREWORD

*If the knowledge is  
undigested or simply wrong,  
more is not better*

How to communicate and disseminate numerical data effectively in chemical science and technology has been a problem of serious and growing concern to IUPAC, the International Union of Pure and Applied Chemistry, for the last two decades. The steadily expanding volume of numerical information, the formulation of new interdisciplinary areas in which chemistry is a partner, and the links between these and existing traditional subdisciplines in chemistry, along with an increasing number of users, have been considered as urgent aspects of the information problem in general, and of the numerical data problem in particular.

Among the several numerical data projects initiated and operated by various IUPAC commissions, the *Solubility Data Project* is probably one of the most ambitious ones. It is concerned with preparing a comprehensive critical compilation of data on solubilities in all physical systems, of gases, liquids and solids. Both the basic and applied branches of almost all scientific disciplines require a knowledge of solubilities as a function of solvent, temperature and pressure. Solubility data are basic to the fundamental understanding of processes relevant to agronomy, biology, chemistry, geology and oceanography, medicine and pharmacology, and metallurgy and materials science. Knowledge of solubility is very frequently of great importance to such diverse practical applications as drug dosage and drug solubility in biological fluids, anesthesiology, corrosion by dissolution of metals, properties of glasses, ceramics, concretes and coatings, phase relations in the formation of minerals and alloys, the deposits of minerals and radioactive fission products from ocean waters, the composition of ground waters, and the requirements of oxygen and other gases in life support systems.

The widespread relevance of solubility data to many branches and disciplines of science, medicine, technology and engineering, and the difficulty of recovering solubility data from the literature, lead to the proliferation of published data in an ever increasing number of scientific and technical primary sources. The sheer volume of data has overcome the capacity of the classical secondary and tertiary services to respond effectively.

While the proportion of secondary services of the review article type is generally increasing due to the rapid growth of all forms of primary literature, the review articles become more limited in scope, more specialized. The disturbing phenomenon is that in some disciplines, certainly in chemistry, authors are reluctant to treat even those limited-in-scope reviews exhaustively. There is a trend to preselect the literature, sometimes under the pretext of reducing it to manageable size. The crucial problem with such preselection - as far as numerical data are concerned - is that there is no indication as to whether the material was excluded by design or by a less than thorough literature search. We are equally concerned that most current secondary sources, critical in character as they may be, give scant attention to numerical data.

On the other hand, tertiary sources - handbooks, reference books, and other tabulated and graphical compilations - as they exist today, are comprehensive but, as a rule, uncritical. They usually attempt to cover whole disciplines, thus obviously are superficial in treatment. Since they command a wide market, we believe that their service to advancement of science is at least questionable. Additionally, the change which is taking place in the generation of new and diversified numerical data, and the rate at which this is done, is not reflected in an increased third-level service. The emergence of new tertiary literature sources does not parallel the shift that has occurred in the primary literature.

With the status of current secondary and tertiary services being as briefly stated above, the innovative approach of the *Solubility Data Project* is that its compilation and critical evaluation work involve consolidation and reprocessing services when both activities are based on intellectual and scholarly reworking of information from primary sources. It comprises compact compilation, rationalization and simplification, and the fitting of isolated numerical data into a critically evaluated general framework.

The *Solubility Data Project* has developed a mechanism which involves a number of innovations in exploiting the literature fully, and which contains new elements of a more imaginative approach for transfer of reliable information from primary to secondary/tertiary sources. *The fundamental trend of the Solubility Data Project is toward integration of secondary and tertiary services with the objective of producing in-depth critical analysis and evaluation which are characteristic to secondary services, in a scope as broad as conventional tertiary services.*

Fundamental to the philosophy of the project is the recognition that the basic element of strength is the active participation of career scientists in it. Consolidating primary data, producing a truly critically-evaluated set of numerical data, and synthesizing data in a meaningful relationship are demands considered worthy of the efforts of top scientists. Career scientists, who themselves contribute to science by their involvement in active scientific research, are the backbone of the project. The scholarly work is commissioned to recognized authorities, involving a process of careful selection in the best tradition of IUPAC. This selection in turn is the key to the quality of the output. These top experts are expected to view their specific topics dispassionately, paying equal attention to their own contributions and to those of their peers. They digest literature data into a coherent story by weeding out what is wrong from what is believed to be right. To fulfill this task, the evaluator must cover *all* relevant open literature. No reference is excluded by design and every effort is made to detect every bit of relevant primary source. Poor quality or wrong data are mentioned and explicitly disqualified as such. In fact, it is only when the reliable data are presented alongside the unreliable data that proper justice can be done. The user is bound to have incomparably more confidence in a succinct evaluative commentary and a comprehensive review with a complete bibliography to both good and poor data.

It is the standard practice that any given solute-solvent system consists of two essential parts: I. Critical Evaluation and Recommended Values, and II. Compiled Data Sheets.

The Critical Evaluation part gives the following information:

- (i) a verbal text of evaluation which discusses the numerical solubility information appearing in the primary sources located in the literature. The evaluation text concerns primarily the quality of data after consideration of the purity of the materials and their characterization, the experimental method employed and the uncertainties in control of physical parameters, the reproducibility of the data, the agreement of the worker's results on accepted test systems with standard values, and finally, the fitting of data, with suitable statistical tests, to mathematical functions;
- (ii) a set of recommended numerical data. Whenever possible, the set of recommended data includes weighted average and standard deviations, and a set of smoothing equations derived from the experimental data endorsed by the evaluator;
- (iii) a graphical plot of recommended data.

The compilation part consists of data sheets of the best experimental data in the primary literature. Generally speaking, such independent data sheets are given only to the best and endorsed data covering the known range of experimental parameters. Data sheets based on primary sources where the data are of a lower precision are given only when no better data are available. Experimental data with a precision poorer than considered acceptable are reproduced in the form of data sheets when they are the only known data for a particular system. Such data are considered to be still suitable for some applications, and their presence in the compilation should alert researchers to areas that need more work.

The typical data sheet carries the following information:

- (i) components - definition of the system - their names, formulas and Chemical Abstracts registry numbers;
- (ii) reference to the primary source where the numerical information is reported. In cases when the primary source is a less common periodical or a report document, published though of limited availability, abstract references are also given;
- (iii) experimental variables;
- (iv) identification of the compiler;
- (v) experimental values as they appear in the primary source. Whenever available, the data may be given both in tabular and graphical form. If auxiliary information is available, the experimental data are converted also to SI units by the compiler.

Under the general heading of Auxiliary Information, the essential experimental details are summarized:

- (vi) experimental method used for the generation of data;
- (vii) type of apparatus and procedure employed;
- (viii) source and purity of materials;
- (ix) estimated error;
- (x) references relevant to the generation of experimental data as cited in the primary source.

This new approach to numerical data presentation, developed during our four years of existence, has been strongly influenced by the diversity of background of those whom we are supposed to serve. We thus deemed it right to preface the evaluation/compilation sheets in each volume with a detailed discussion of the principles of the accurate determination of relevant solubility data and related thermodynamic information.

Finally, the role of education is more than corollary to the efforts we are seeking. The scientific standards advocated here are necessary to strengthen science and technology, and should be regarded as a major effort in the training and formation of the next generation of scientists and engineers. Specifically, we believe that there is going to be an impact of our project on scientific-communication practices. The quality of consolidation adopted by this program offers down-to-earth guidelines, concrete examples which are bound to make primary publication services more responsive than ever before to the needs of users. The self-regulatory message to scientists of 15 years ago to refrain from unnecessary publication has not achieved much. The literature is still, in 1978, cluttered with poor-quality articles. The Weinberg report (in "Reader in Science Information", Eds. J. Sherrod and A. Hodina, Microcard Editions Books, Indian Head, Inc., 1973, p. 292) states that "admonition to authors to restrain themselves from premature, unnecessary publication can have little effect unless the climate of the entire technical and scholarly community encourages restraint..." We think that projects of this kind translate the climate into operational terms by exerting pressure on authors to avoid submitting low-grade material. The type of our output, we hope, will encourage attention to quality as authors will increasingly realize that their work will not be suited for permanent retrievability unless it meets the standards adopted in this project. It should help to dispel confusion in the minds of many authors of what represents a permanently useful bit of information of an archival value, and what does not.

If we succeed in that aim, even partially, we have then done our share in protecting the scientific community from unwanted and irrelevant, wrong numerical information.

A. S. Kertes

December, 1978



## PREFACE

The users of this volume will find (1) the available experimental solubility data of krypton, xenon, and radon gas in liquids as reported in the scientific literature, (2) tables of smoothed mole fraction solubility data for the systems which were studied over a temperature interval and (3) tables of either tentative or recommended solubility data when two or more laboratories reported solubility data over the same range of temperature and pressure for a system. Users have the option of using the experimental values, either directly, or in their own smoothing equations, or of using the smoothed values prepared by the compilers and evaluators. The goal was to cover the literature thoroughly enough so that the user need not do a detailed literature search for krypton, xenon, and radon solubility data prior to 1978.

Some words of explanation are required with respect to units, corrections, smoothing equations, auxiliary data and data sources, nomenclature, and other points. The experimental data are presented in the units found in the original paper. In addition the original data are often converted to other units, especially mole fraction. Temperatures have been converted to Kelvin. In evaluations of solubility data, S.I. units are used.

Only in the past 10 to 15 years have experimental methods for the determination of the solubility of gases in liquids developed to the point where 0.5 percent or better accuracy is attained. Only a small fraction of the literature's gas solubility data are accurate to 0.5 percent. The corrections for non-ideal gas behavior and for expansion of the liquid phase on dissolution of the gas are small and well within the normal experimental error. Thus such corrections were not made for the krypton and xenon gas solubility data at low pressure. For radon gas solubility data the real gas volume of  $22,290 \text{ cm}^3 \text{ mol}^{-1}$  at standard conditions was used in the calculation of mole fraction.

Small, often unknown partial pressures, of radioactive krypton, xenon and radon are frequently used in the measurement of Ostwald coefficients. Bunsen coefficients and mole fraction gas solubilities at 101.325 kPa (1 atm) were calculated from the Ostwald coefficient, assuming that the Ostwald coefficient was independent of pressure. This is a reasonable often made assumption. However, it is an assumption, and the Bunsen coefficients and mole fraction solubilities calculated from Ostwald coefficients measured at low unknown partial pressures of radioactive gas should be accepted with caution.

The lack of high accuracy is also the reason that only a two-constant equation is used to smooth and evaluate most of the gas solubility data. A Gibbs energy of solution equation linear in temperature is used

$$\Delta G^\circ / \text{J mol}^{-1} = -RT \ln X_1 = A + BT$$

or in alternate form

$$\ln X_1 = -\Delta G^\circ / RT = -(A/R)/T - (B/R)$$

where A is  $\Delta H^\circ$ , B is  $-\Delta S^\circ$ ,  $X_1$  is the mole fraction solubility at a gas partial pressure of 101.325 kPa (1 atm), and R is  $8.31433 \text{ J K}^{-1} \text{ mol}^{-1}$ . The constants A and B require five digits to reproduce the mole fraction solubility to three significant figures. Although the constants are given to five digits it is not intended to imply that the values of the changes in enthalpy and entropy of solution are significant to more than two or three digits.

An inconsistency, which we believe is justified, is found with respect to the solubility data in water. Much time and effort was expended in evaluating the solubility data of each gas in water. A recommended equation and table of values are presented. However, for systems which contain water and other solvent compounds such as electrolytes or water miscible polar organic compounds, the experimental gas solubility in water from that paper is given, even when it is at variance with our recommended values. These data of sometimes poorer quality are presented because the author's ratio of gas solubility in water to solubility in the aqueous solution may be more accurate than the solubility itself. This may be especially true of some of the solubility data in aqueous electrolyte solutions.

Solvent density data were often required in making solubility unit conversions. The density data were not directly referenced. The main sources of density data are

Circular 461 of the U.S. National Bureau of Standards  
American Petroleum Research Project 44 Publications  
The International Critical Tables, Volume III (E.W. Washburn, Editor)  
McGraw-Hill Co., 1931  
Smow Table, Pure and Applied Chemistry 1976, 45, 1-9  
Thermodynamic Properties of Aliphatic Alcohols, R. C. Wilhoit and  
B. J. Zwolinski, J. Phys. Chem. Ref. Data 1973, 2, Supplement No. 1  
Organic Solvents, J. A. Riddick and W. B. Bunger (Technique of Chemistry, Volume II, A. Weissberger, Editor) Wiley-Interscience, New York, 1970, 3rd Ed.

The solubility data are supplemented with partial molal volume and calorimetric enthalpy of solution data when they are available.

Chemical Abstracts recommended names and registry numbers were used throughout. Common names are cross referenced to Chemical Abstract recommended names in the index.

The Editor would appreciate users calling errors and omissions to his attention.

The Editor gratefully acknowledges the advice and comments of members of the IUPAC Commission on Equilibrium Data and the Subcommittee on Solubility Data; the cooperation and hard work of the Evaluators and compilers; and the untiring efforts of the typists Peggy Tyler, Carolyn Dowie, and Lesley Flanagan.

Acknowledgment is made to the Donors of the Petroleum Research Fund, administered by the American Chemical Society, for partial support of the compilation and evaluation of the gas solubility data.

H. Lawrence Clever

Atlanta, GA  
December, 1978

## THE SOLUBILITY OF GASES IN LIQUIDS

C. L. Young, R. Battino, and H. L. Clever

INTRODUCTION

The Solubility Data Project aims to make a comprehensive search of the literature for data on the solubility of gases, liquids and solids in liquids. Data of suitable accuracy are compiled into data sheets set out in a uniform format. The data for each system are evaluated and where data of sufficient accuracy are available values recommended and in some cases a smoothing equation suggested to represent the variation of solubility with pressure and/or temperature. A text giving an evaluation and recommended values and the compiled data sheets are published on consecutive pages.

DEFINITION OF GAS SOLUBILITY

The distinction between vapor-liquid equilibria and the solubility of gases in liquids is arbitrary. It is generally accepted that the equilibrium set up at 300K between a typical gas such as argon and a liquid such as water is gas-liquid solubility whereas the equilibrium set up between hexane and cyclohexane at 350K is an example of vapor-liquid equilibrium. However, the distinction between gas-liquid solubility and vapor-liquid equilibrium is often not so clear. The equilibria set up between methane and propane above the critical temperature of methane and below the critical temperature of propane may be classed as vapor-liquid equilibrium or as gas-liquid solubility depending on the particular range of pressure considered and the particular worker concerned.

The difficulty partly stems from our inability to rigorously distinguish between a gas, a vapor, and a liquid, which has been discussed in numerous textbooks. We have taken a fairly liberal view in these volumes and have included systems which may be regarded, by some workers, as vapor-liquid equilibria.

UNITS AND QUANTITIES

The solubility of gases in liquids is of interest to a wide range of scientific and technological disciplines and not solely to chemistry. Therefore a variety of ways for reporting gas solubility have been used in the primary literature and inevitably sometimes, because of insufficient available information, it has been necessary to use several quantities in the compiled tables. Where possible, the gas solubility has been quoted as a mole fraction of the gaseous component in the liquid phase. The units of pressure used are bar, pascal, millimeters of mercury and atmosphere. Temperatures are reported in Kelvin.

EVALUATION AND COMPILATION

The solubility of comparatively few systems is known with sufficient accuracy to enable a set of recommended values to be presented. This is true both of the measurement near atmospheric pressure and at high pressures. Although a considerable number of systems have been studied by at least two workers, the range of pressures and/or temperatures is often sufficiently different to make meaningful comparison impossible.

Occasionally, it is not clear why two groups of workers obtained very different sets of results at the same temperature and pressure, although both sets of results were obtained by reliable methods and are internally consistent. In such cases, sometimes an incorrect assessment has been given. There are several examples where two or more sets of data have been classified as tentative although the sets are mutually inconsistent.

Many high pressure solubility data have been published in a smoothed form. Such data are particularly difficult to evaluate, and unless specifically discussed by the authors, the estimated error on such values can only be regarded as an "informed guess".

Many of the high pressure solubility data have been obtained in a more general study of high pressure vapor-liquid equilibrium. In such cases a note is included to indicate that additional vapor-liquid equilibrium data are given in the source. Since the evaluation is for the compiled data, it is possible that the solubility data are given a classification which is better than that which would be given for the complete vapor-liquid data (or vice versa). For example, it is difficult to determine coexisting liquid and vapor compositions near the critical point of a mixture using some widely used experimental techniques which yield accurate high pressure solubility data. For example, conventional methods of analysis may give results with an expected error which would be regarded as sufficiently small for vapor-liquid equilibrium data but an order of magnitude too large for acceptable high pressure gas-liquid solubility.

It is occasionally possible to evaluate data on mixtures of a given substance with a member of a homologous series by considering all the available data for the given substance with other members of the homologous series. In this study the use of such a technique has been very limited.

The estimated error is often omitted in the original article and sometimes the errors quoted do not cover all the variables. In order to increase the usefulness of the compiled tables estimated errors have been included even when absent from the original article. If the error on *any* variable has been inserted by the compiler this has been noted.

#### PURITY OF MATERIALS

The purity of materials has been quoted in the compiled tables where given in the original publication. The solubility is usually more sensitive to impurities in the gaseous component than to liquid impurities in the liquid component. However, the most important impurities are traces of a gas dissolved in the liquid. Inadequate degassing of the absorbing liquid is probably the most often overlooked serious source of error in gas solubility measurements.

#### APPARATUS AND PROCEDURES

In the compiled tables brief mention is made of the apparatus and procedure. There are several reviews on experimental methods of determining gas solubilities and these are given in References 1-7.

#### METHODS OF EXPRESSING GAS SOLUBILITIES

Because gas solubilities are important for many different scientific and engineering problems, they have been expressed in a great many ways:

##### The Mole Fraction, X(g)

The mole fraction solubility for a binary system is given by:

$$X(g) = \frac{n(g)}{n(g) + n(l)}$$

$$= \frac{W(g)/M(g)}{\{W(g)/M(g)\} + \{W(l)/M(l)\}}$$

here  $n$  is the number of moles of a substance (an *amount* of substance),  $W$  is the mass of a substance, and  $M$  is the molecular mass. To be unambiguous, the partial pressure of the gas (or the total pressure) and the temperature of measurement must be specified.

##### The Weight Per Cent Solubility, wt%

For a binary system this is given by

$$\text{wt\%} = 100 W(g) / \{W(g) + W(l)\}$$

where W is the weight of substance. As in the case of mole fraction, the pressure (partial or total) and the temperature must be specified. The weight per cent solubility is related to the mole fraction solubility by

$$X(g) = \frac{\text{wt\%/M}(g)}{\text{wt\%/M}(g) + \{(100 - \text{wt\%})/\text{M}(l)\}}$$

#### The Weight Solubility, $C_w$

The weight solubility is the number of moles of dissolved gas per gram of solvent when the partial pressure of gas is 1 atmosphere. The weight solubility is related to the mole fraction solubility at one atmosphere partial pressure by

$$X(g) \text{ (partial pressure 1 atm)} = \frac{C_w M(l)}{1 + C_w M(l)}$$

where  $M(l)$  is the molecular weight of the solvent.

#### The Moles Per Unit Volume Solubility, $n$

Often for multicomponent systems the density of the liquid mixture is not known and the solubility is quoted as moles of gas per unit volume of liquid mixture. This is related to the mole fraction solubility by

$$X = \frac{n v^{\circ}(l)}{1 + n v^{\circ}(l)}$$

where  $v^{\circ}(l)$  is the molar volume of the liquid component.

#### The Bunsen Coefficient, $\alpha$

The Bunsen coefficient is defined as the volume of gas reduced to 273.15K and 1 atmosphere pressure which is absorbed by unit volume of solvent (at the temperature of measurement) under a partial pressure of 1 atmosphere. If ideal gas behavior and Henry's law is assumed to be obeyed,

$$\alpha = \frac{V(g) \ 273.15}{V(l) \ T}$$

where  $V(g)$  is the volume of gas absorbed and  $V(l)$  is the original (starting) volume of absorbing solvent. The mole fraction solubility  $X$  is related to the Bunsen coefficient by

$$X \text{ (1 atm)} = \frac{\alpha}{\alpha + \frac{273.15}{T} \frac{v^{\circ}(g)}{v^{\circ}(l)}}$$

where  $v^{\circ}(g)$  and  $v^{\circ}(l)$  are the molar volumes of gas and solvent at a pressure of one atmosphere. If the gas is ideal,

$$X = \frac{\alpha}{\alpha + \frac{273.15R}{v^{\circ}(l)}}$$

Real gases do not follow the ideal gas law and it is important to establish the real gas law used for calculating  $\alpha$  in the original publication and to make the necessary adjustments when calculating the mole fraction solubility.

#### The Kuenen Coefficient, $S$

This is the volume of gas, reduced to 273.15K and 1 atmosphere pressure, dissolved at a partial pressure of gas of 1 atmosphere by 1 gram of solvent.

### The Ostwald Coefficient, L

The Ostwald coefficient, L, is defined as the ratio of the volume of gas absorbed to the volume of the absorbing liquid, all measured at the same temperature:

$$L = \frac{V(g)}{V(l)}$$

If the gas is ideal and Henry's Law is applicable, the Ostwald coefficient is independent of the partial pressure of the gas. It is necessary, in practice, to state the temperature and total pressure for which the Ostwald coefficient is measured. The mole fraction solubility, X, is related to the Ostwald coefficient by

$$X = \left[ \frac{RT}{P(g) L v^O(l)} + 1 \right]^{-1}$$

where P is the partial pressure of gas. The mole fraction solubility will be at a partial pressure of P(g).

### The Absorption Coefficient, $\beta$

There are several "absorption coefficients", the most commonly used one being defined as the volume of gas, reduced to 273.15K and 1 atmosphere, absorbed per unit volume of liquid when the total pressure is 1 atmosphere.  $\beta$  is related to the Bunsen coefficient by

$$\beta = \alpha(1-P(l))$$

where P(l) is the partial pressure of the liquid in atmosphere.

### The Henry's Law Constant

A generally used formulation of Henry's Law may be expressed as

$$P(g) = K_H X$$

where  $K_H$  is the Henry's Law constant and X the mole fraction solubility. Other formulations are

$$P(g) = K_2 C(l)$$

or

$$C(g) = K_C C(l)$$

where  $K_2$  and  $K_C$  are constants, C the concentration, and (l) and (g) refer to the liquid and gas phases. Unfortunately,  $K_H$ ,  $K_2$  and  $K_C$  are all sometimes referred to as Henry's Law constants. Henry's Law is a limiting law but can sometimes be used for converting solubility data from the experimental pressure to a partial gas pressure of 1 atmosphere, provided the mole fraction of the gas in the liquid is small, and that the difference in pressures is small. Great caution must be exercised in using Henry's Law.

### The Mole Ratio, N

The mole ratio, N, is defined by

$$N = n(g)/n(l)$$

Table 1 contains a presentation of the most commonly used inter-conversions not already discussed.

For gas solubilities greater than about 0.01 mole fraction at a partial pressure of 1 atmosphere there are several additional factors which must be taken into account to unambiguously report gas solubilities. Solution densities or the partial molar volume of gases must be known. Corrections should be made for the possible non-ideality of the gas or the non-applicability of Henry's Law.

TABLE 1 Interconversion of parameters used for reporting solubility

$$L = \alpha(T/273.15)$$

$$C_w = \alpha/v_o \rho$$

$$K_H = \frac{17.033 \times 10^6 \rho_{\text{soln}}}{\alpha M(l)} + 760$$

$$L = C_w v_{t,\text{gas}} \rho$$

where  $v_o$  is the molal volume of the gas in  $\text{cm}^3 \text{mol}^{-1}$  at  $0^\circ\text{C}$ ,  $\rho$  the density of the solvent at the temperature of the measurement,  $\rho_{\text{soln}}$  the density of the solution at the temperature of the measurement, and  $v_{t,\text{gas}}$  the molal volume of the gas ( $\text{cm}^3 \text{mol}^{-1}$ ) at the temperature of the measurement.

### SALT EFFECTS

The effect of a dissolved salt in the solvent on the solubility of a gas is often studied. The activity coefficient of a dissolved gas is a function of the concentration of all solute species (see ref. 8). At a given temperature and pressure the logarithm of the dissolved gas activity coefficient can be represented by a power series in  $C_s$ , the electrolyte concentration, and  $C_i$ , the nonelectrolyte solute gas concentration

$$\log f_i = \sum_{m,n} k_{mn} C_s^m C_i^n$$

It is usually assumed that only the linear terms are important for low  $C_s$  and  $C_i$  values when there is negligible chemical interaction between solute species.

$$\log f_i = k_s C_s + k_i C_i$$

where  $k_s$  is the salt effect parameter and  $k_i$  is the solute-solute gas interaction parameter. The dissolved gas activity is the same in the pure solvent and a salt solution in that solvent for a given partial pressure and temperature

$$a_1 = f_i S_i = f_i^o S_i^o \quad \text{and} \quad f_1 = f_1^o \frac{S_1^o}{S_1}$$

where  $S_i$  and  $S_i^o$  are the gas solubility in the salt solution and in the pure solvent, respectively, and the  $f$ 's are the corresponding activity coefficients. It follows that  $\log \frac{f_1}{f_1^o} = \log \frac{S_1^o}{S_1} = k_s C_s + k_i (S_i - S_i^o)$ . When the

quantity  $(S_i - S_i^o)$  is small the second term is negligible even though  $k_s$  and  $k_i$  may be of similar magnitude. This is generally the case for gas solubilities and the equation reduces to

$$\log \frac{f_i}{f_i^o} = \log \frac{S_i^o}{S_i} = k_s C_s$$

which is the form of the empirical Setschenow equation in use since the 1880's. A salt that increases the activity coefficient of the dissolved gas is said to salt-out and a salt that decreases the activity coefficient of the dissolved gas is said to salt-in.

Although salt effect studies have been carried out for many years, there appears to be no common agreement of the units for either the gas solubility or the salt concentration. Both molar ( $\text{mol dm}^{-3}$ ) and molal ( $\text{mol kg}^{-1}$ ) are used for the salt concentration. The gas solubility ratio  $S_i^o/S_i$  is given as Bunsen coefficient ratio and Ostwald coefficient ratio,

which would be the same as a molar ratio; Kueunen coefficient ratio, volume dissolved in 1 g or 1 kg of solvent which would be a molal ratio; and mole fraction ratio. Recent theoretical treatments use salt concentration in  $\text{mol dm}^{-3}$  and  $S_i^0/S_i$  ratio as mole fraction ratio with each salt ion acting as a mole. Evaluations which compare the results of several workers are made in the units most compatible with present theory.

#### TEMPERATURE DEPENDENCE OF GAS SOLUBILITY

In a few cases it has been found possible to fit the mole fraction solubility at various temperatures using an equation of the form

$$\ln x = A + B / (T/100K) + C \ln (T/100K) + DT/100K$$

It is then possible to write the thermodynamic functions  $\overline{\Delta G}_1^0$ ,  $\overline{\Delta H}_1^0$ ,  $\overline{\Delta S}_1^0$  and  $\overline{\Delta C}_{P1}^0$  for the transfer of the gas from the vapor phase at

101,325 Pa partial pressure to the (hypothetical) solution phase of unit mole fraction as:

$$\overline{\Delta G}_1^0 = -RAT - 100 RB - RCT \ln (T/100) - RDT^2/100$$

$$\overline{\Delta S}_1^0 = RA + RC \ln (T/100) + RC + 2 RDT/100$$

$$\overline{\Delta H}_1^0 = -100 RB + RCT + RDT^2/100$$

$$\overline{\Delta C}_{P1}^0 = RC + 2 RDT/100$$

In cases where there are solubilities at only a few temperatures it is convenient to use the simpler equations

$$\overline{\Delta G}_1^0 = -RT \ln x = A + BT$$

in which case  $A = \overline{\Delta H}_1^0$  and  $-B = \overline{\Delta S}_1^0$ .

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8. Long, F. A.; McDevit, W. F. Chem. Rev. 1952, 51, 119.



APPENDIX I. Conversion Factors  $k$  and  $k^{-1}$ 

Non-SI Unit	$k$ 1 (non-SI Unit) = $k$ (SI Unit)	$k^{-1}$ 1 (SI Unit) = $k^{-1}$ (non-SI Unit)
<b>LENGTH</b>		
		SI Unit, m
Å (angstrom)	$1 \times 10^{-10}$ (*)	$1 \times 10^{-10}$ (*)
cm (centimeter)	$1 \times 10^{-2}$ (*)	$1 \times 10^{-2}$ (*)
in (inch)	$254 \times 10^{-4}$ (*)	$3\,937\,008 \times 10^{-5}$
ft (foot)	$3\,048 \times 10^{-4}$ (*)	$3\,280\,840 \times 10^{-6}$
<b>AREA</b>		
		SI Unit, m <sup>2</sup>
cm <sup>2</sup>	$1 \times 10^{-4}$ (*)	$1 \times 10^{-4}$ (*)
in <sup>2</sup>	$64\,516 \times 10^{-8}$ (*)	$1\,550\,003 \times 10^{-3}$
ft <sup>2</sup>	$9\,290\,304 \times 10^{-8}$ (*)	$1\,076\,391 \times 10^{-5}$
<b>VOLUME</b>		
		SI Unit, m <sup>3</sup>
cm <sup>3</sup>	$1 \times 10^{-6}$ (*)	$1 \times 10^{-6}$ (*)
in <sup>3</sup>	$16\,387\,064 \times 10^{-12}$ (*)	$6\,102\,374 \times 10^{-2}$
ft <sup>3</sup>	$2\,831\,685 \times 10^{-8}$	$3\,531\,467 \times 10^{-5}$
l (litre)	$1 \times 10^{-3}$ (*)	$1 \times 10^{-3}$ (*)
UKgal (UK gallon)	$45\,461 \times 10^{-7}$	$21\,997 \times 10^{-2}$
USgal (US gallon)	$37\,854 \times 10^{-7}$	$26\,417 \times 10^{-2}$
<b>MASS</b>		
		SI Unit, kg
g (gram)	$1 \times 10^{-3}$ (*)	$1 \times 10^{-3}$ (*)
t (tonne)	$1 \times 10^3$ (*)	$1 \times 10^3$ (*)
lb (pound)	$45\,359\,237 \times 10^{-8}$ (*)	$2\,204\,623 \times 10^{-6}$
<b>DENSITY</b>		
		SI Unit, kg m <sup>-3</sup>
g cm <sup>-3</sup>	$1 \times 10^3$ (*)	$1 \times 10^3$ (*)
g l <sup>-1</sup>	1 (*)	1 (*)
lb in <sup>-3</sup>	$2\,767\,991 \times 10^{-2}$	$3\,612\,728 \times 10^{-11}$
lb ft <sup>-3</sup>	$1\,601\,847 \times 10^{-5}$	$6\,242\,795 \times 10^{-8}$
lb UKgal <sup>-1</sup>	$99\,776 \times 10^{-3}$	$100\,224 \times 10^{-7}$
lb USgal <sup>-1</sup>	$1\,198\,264 \times 10^{-4}$	$8\,345\,406 \times 10^{-9}$
<b>PRESSURE</b>		
		SI Unit, Pa (pascal, kg m <sup>-1</sup> s <sup>-2</sup> )
dyn cm <sup>-2</sup>	$1 \times 10^{-1}$ (*)	$1 \times 10^{-1}$ (*)
at (kgf cm <sup>-2</sup> )	$980\,665 \times 10^{-1}$ (*)	$1\,019\,716 \times 10^{-11}$
atm (atmosphere)	101 325 (*)	$9\,869\,233 \times 10^{-12}$
bar	$1 \times 10^5$ (*)	$1 \times 10^5$ (*)
lbf in <sup>-2</sup> (p.s.i.)	$6\,894\,757 \times 10^{-3}$	$1\,450\,377 \times 10^{-10}$
lbf ft <sup>-2</sup>	$47\,880 \times 10^{-3}$	$20\,886 \times 10^{-6}$
inHg (inch of mercury)	$3\,386\,388 \times 10^{-3}$	$2\,952\,999 \times 10^{-10}$
mmHg (millimeter of mercury, torr)	$1\,333\,224 \times 10^{-4}$	$7\,500\,617 \times 10^{-9}$

APPENDIX I. Conversion Factors  $k$  and  $k^{-1}$ 

Non-SI Unit	$k$ 1 (non-SI Unit) = $k$ (SI Unit)	$k^{-1}$ 1 (SI Unit) = $k^{-1}$ (non-SI Unit)
ENERGY		Unit, J (joule, $\text{kg m}^2\text{s}^{-2}$ )
erg	$1 \times 10^{-7}$ (*)	$1 \times 10^7$ (*)
cal <sub>IT</sub> (I.T. calorie)	$41\,868 \times 10^{-4}$ (*)	$2\,388\,459 \times 10^{-7}$
cal <sub>th</sub> (thermochemical calorie)	$4\,184 \times 10^{-3}$ (*)	$2\,390\,057 \times 10^{-7}$
kW h (kilowatt hour)	$36 \times 10^5$ (*)	$2\,777\,778 \times 10^{-13}$
l atm	$101\,325 \times 10^{-3}$ (*)	$9\,869\,233 \times 10^{-9}$
ft lbf	$1\,355\,818 \times 10^{-6}$	$7\,375\,622 \times 10^{-7}$
hp h (horse power hour)	$2\,684\,519$	$3\,725\,062 \times 10^{-13}$
Btu (British thermal unit)	$1\,055\,056 \times 10^{-3}$	$9\,478\,172 \times 10^{-10}$

An asterisk (\*) denotes an exact relationship

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>1. Krypton; Kr; 7439-90-9</li> <li>2. Water; H<sub>2</sub>O; 7732-18-5</li> </ol>	<p>EVALUATOR:</p> <p>Rubin Battino, Department of Chemistry, Wright State University Dayton, Ohio, 45431 U.S.A. June 1978</p>
<p>CRITICAL EVALUATION:</p> <p>The experimental solubility data produced by three workers was considered to be of sufficient reliability to use for the smoothing equation. In fitting the data to the equation those points which were different by about two standard deviations or more from the smoothed values were rejected. Most of the low temperature values of Morrison and Johnstone were thrown out, but since they had the only higher temperature data these were retained. The transition between their high temperature data and the more reliable low temperature data of the other two workers was smooth. We used 30 points for the final smoothing and they were obtained as follows (reference - number of data points used from that reference): 1-8; 2-6; 3-16. The fitting equation used was</p> $\ln x_1 = A + B/(T/100K) + C \ln (T/100K) + DT/100K \quad (1)$ <p>where <math>x_1</math> is the mole fraction solubility of krypton at 101,325 Pa (1 atm) partial pressure of gas. The fit in <math>\ln x_1</math> gave a standard deviation of 0.32% taken at the middle of the temperature range. Table 1 gives the smoothed values of the mole fraction solubility (at 101,325 Pa partial pressure of gas) and the Ostwald coefficient at 5K intervals.</p> <p>Table 1 also gives the thermodynamic functions <math>\Delta \bar{G}_1^\circ</math>, <math>\Delta \bar{H}_1^\circ</math>, <math>\Delta \bar{S}_1^\circ</math>, <math>\Delta \bar{C}_{P1}^\circ</math> for the transfer of gas from the vapor phase at 101,325 Pa partial gas pressure to the (hypothetical) solution phase of unit mole fraction. These thermodynamic properties were calculated from the smoothing equation according to the following equations:</p> $\Delta \bar{G}_1^\circ = - RAT - 100RB - RCT \ln (T/100) - RDT^2/100 \quad (2)$ $\Delta \bar{S}_1^\circ = RA + RC \ln (T/100) + RC + 2RDT/100 \quad (3)$ $\Delta \bar{H}_1^\circ = - 100RB + RCT + RDT^2/100 \quad (4)$ $\Delta \bar{C}_{P1}^\circ = RC + 2RDT/100 \quad (5)$ <p>The best fit for the 30 data points gave the following equation</p> $\ln x_1 = -66.9928 + 91.0166/(T/100K) + 24.2207 \ln (T/100K) \quad (6)$ <p>The data from six other workers were rejected for the following reasons. Yeh and Peterson's values (4) were 3 to 4 per cent low. Antropoff's data (5) were very far off, being all much too low. König's results (6) were also low, being off by about 4 to 12 per cent. The two values by Van Liempt (7) were rather imprecise. Kitani (8) determined the solubility of krypton-85 in water, saline, lipids and blood at 37°C by a radiochemical technique. Seventeen determinations at the one temperature were reproducible to + 4% and were 5% lower than the selected values in this section. Wood and Caputi (9) determined the solubilities from 1 to 48°C in water and sea water, but their results are 2 to 5% high.</p>	

<b>COMPONENTS:</b>  1. Krypton; Kr; 7439-90-9  2. Water; H <sub>2</sub> O; 7732-18-5	<b>EVALUATOR:</b> Rubin Battino Department of Chemistry Wright State University Dayton, Ohio 45431 U.S.A.  June 1978
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**CRITICAL EVALUATION:**

Table 1. Smoothed values of the solubility of krypton in water and thermodynamic functions<sup>a</sup> at 5K intervals using equation 6 at 101,325 Pa partial pressure of krypton.

T/K	Mol Fraction $X_1 \times 10^5$	Ostwald Coefficient $L \times 10^2$	$\Delta\bar{G}_1^b/\text{KJ mol}^{-1}$	$\Delta\bar{H}_1/\text{KJ mol}^{-1}$	$\Delta\bar{S}_1/\text{JK}^{-1}\text{mol}^{-1}$
273.15	8.842	11.000	21.20	-20.67	-153
278.15	7.537	9.550	21.95	-19.66	-150
283.15	6.511	8.396	22.69	-18.65	-146
288.15	5.696	7.470	23.41	-17.65	-142
293.15	5.041	6.720	24.12	-16.64	-139
298.15	4.512	6.109	24.80	-15.63	-136
303.15	4.079	5.609	25.47	-14.63	-132
308.15	3.725	5.197	26.13	-13.62	-129
313.15	3.432	4.858	26.76	-12.61	-126
318.15	3.190	4.578	27.39	-11.61	-123
323.15	2.990	4.348	27.99	-10.60	-119
328.15	2.823	4.160	28.58	-9.59	-116
333.15	2.686	4.007	29.15	-8.58	-113
338.15	2.572	3.885	29.71	-7.58	-110
343.15	2.480	3.790	30.26	-6.57	-107
348.15	2.405	3.718	30.79	-5.56	-104
353.15	2.346	3.668	31.30	-4.56	-102

<sup>a</sup> $\Delta\bar{C}_{P1}^\circ$  was independent of temperature and has the value  $201 \text{ JK}^{-1}\text{mol}^{-1}$ .

<sup>b</sup> $\text{cal}_{th} = 4.184 \text{ joule}$ .

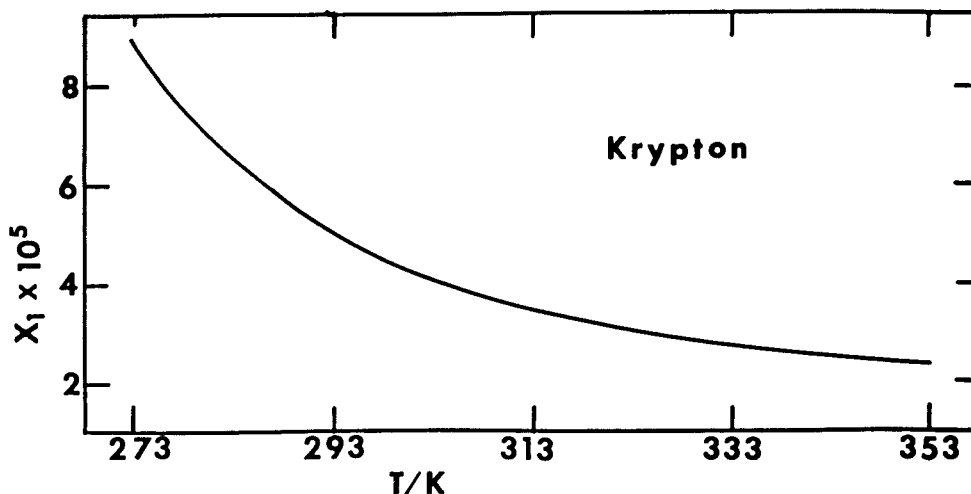


FIGURE 1. The mole fraction solubility of krypton in water at a krypton partial pressure of 101.325 kPa (1 atm).

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>1. Krypton; Kr; 7439-90-9</li> <li>2. Water; H<sub>2</sub>O; 7732-18-5</li> </ol>	<p>EVALUATOR:</p> <p>Rubin Battino  Department of Chemistry  Wright State University  Dayton, Ohio 45431  U.S.A.</p> <p>June 1978</p>												
<p>CRITICAL EVALUATION:</p> <p>Anderson, Keeler, and Klach (10) measured the solubility of krypton + krypton-85 between 373 and 573K at partial pressures of 1.5 to <math>60 \times 10^{-4}</math> psia in the presence of oxygen gas at pressures between 270 and 1930 psia. The mole fraction solubility calculated at 101.325 kPa krypton partial pressure appears to be a consistent extension of the krypton solubilities below 353K. The combined data indicates the minimum solubility is at 380 K. See the data sheets for the Anderson, Keeler and Klach paper for additional information.</p> <p>Alexander (11) made seven determinations of the heat of solution of krypton in water at 298.15 K. He obtained an enthalpy of solution of <math>-(15.8_2 \pm 0.6_8) \text{ kJ mol}^{-1}</math>. The value agrees well with the value of <math>-15.63 \text{ kJ mol}^{-1}</math> derived from the solubility data.</p> <p>Popov and Drakin (12, 13) measured the apparent molar volume of krypton dissolved in water under a krypton partial pressure of 4.7 to 20.1 atm at 298.15 K by a density method.</p> <table border="0" data-bbox="161 885 1156 970"> <tr> <td>p/atm</td> <td>4.70</td> <td>12.00</td> <td>15.20</td> <td>18.27</td> <td>20.10</td> </tr> <tr> <td><math>\bar{V}/\text{cm}^3 \text{ mol}^{-1}</math></td> <td><math>38 \pm 5</math></td> <td><math>32 \pm 2</math></td> <td><math>31.2 \pm 1.4</math></td> <td><math>31.4 \pm 1.2</math></td> <td><math>31.3 \pm 1.1</math></td> </tr> </table> <p>They recommended a value of <math>31.3 \text{ cm}^3 \text{ mol}^{-1}</math>.</p> <p><u>References</u></p> <ol style="list-style-type: none"> <li>1. Morrison, T. J.; Johnstone, N. B. <u>J. Chem. Soc.</u> 1954, 3441.</li> <li>2. Benson, B. B.; Krause, D. <u>J. Chem. Phys.</u> 1976, <u>64</u>, 689.</li> <li>3. Weiss, R. F.; Kyser, T. K. <u>J. Chem. Eng. Data</u> 1978, <u>23</u>, 69.</li> <li>4. Yeh, S-Y.; Peterson, R. E. <u>J. Pharm. Sci.</u> 1964, <u>53</u>, 822.</li> <li>5. Antropoff, A. <u>Proc. Roy. Soc. (London)</u> 1910, <u>83</u>, 474; <u>Z. Elektrochem.</u> 1919, <u>25</u>, 269.</li> <li>6. König, H. <u>Z. Naturforsch.</u> 1963, <u>18a</u>, 363.</li> <li>7. van Liempt, J. A. M.; van Wijk, W. <u>Rec. Trav. Chim.</u> 1937, <u>56</u>, 632.</li> <li>8. Kitani, K. <u>Scand. J. Clinical Lab. Invest.</u> 1972, <u>29</u>, 167.</li> <li>9. Wood, D.; Caputi, R. <u>AD631557</u>, Avail. CFSTI, 1966, 17 pp.</li> <li>10. Anderson, C. J.; Keeler, R. A.; Klach, S. J. <u>J. Chem. Eng. Data</u> 1962, <u>7</u>, 290.</li> <li>11. Alexander, D. M. <u>J. Phys. Chem.</u> 1959, <u>63</u>, 994.</li> <li>12. Popov, G. A.; Drakin, S. I. <u>Moskov. Khimiko-technol. Inst. Trudy</u> 1972, <u>71</u>, 43.</li> <li>13. Popov, G. A.; Drakin, S. I. <u>Zh. Fiz. Khim.</u> 1974, <u>48</u>, 631.</li> </ol> <p>The last three paragraphs of the evaluation were added by the Editor.</p>		p/atm	4.70	12.00	15.20	18.27	20.10	$\bar{V}/\text{cm}^3 \text{ mol}^{-1}$	$38 \pm 5$	$32 \pm 2$	$31.2 \pm 1.4$	$31.4 \pm 1.2$	$31.3 \pm 1.1$
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<b>VARIABLES:</b> T/K: 279.75 - 348.05	<b>PREPARED BY:</b> R. Battino																																																																		
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="145 532 1188 889"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^5</math></th> <th>Kunenen Coefficient <math>S_0 \times 10^3</math></th> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^5</math></th> <th>Kunenen Coefficient <math>S_0 \times 10^3</math></th> </tr> </thead> <tbody> <tr><td>279.75</td><td>6.591</td><td>82.0</td><td>319.15</td><td>3.110</td><td>38.3</td></tr> <tr><td>281.15</td><td>6.382</td><td>79.4</td><td>325.05</td><td>2.923*</td><td>35.9</td></tr> <tr><td>285.75</td><td>5.589</td><td>69.5</td><td>331.05</td><td>2.719*</td><td>33.3</td></tr> <tr><td>288.65</td><td>5.277</td><td>65.6</td><td>332.95</td><td>2.681*</td><td>32.8</td></tr> <tr><td>291.35</td><td>4.966</td><td>61.7</td><td>337.85</td><td>2.590*</td><td>31.6</td></tr> <tr><td>294.35</td><td>4.687</td><td>58.2</td><td>340.65</td><td>2.520*</td><td>30.7</td></tr> <tr><td>297.85</td><td>4.312</td><td>53.5</td><td>344.65</td><td>2.444*</td><td>29.7</td></tr> <tr><td>303.35</td><td>3.948</td><td>48.9</td><td>347.05</td><td>2.431*</td><td>29.5</td></tr> <tr><td>308.55</td><td>3.582</td><td>44.3</td><td>348.05</td><td>2.416*</td><td>29.3</td></tr> <tr><td>314.55</td><td>3.290</td><td>40.6</td><td></td><td></td><td></td></tr> </tbody> </table> <p>*Solubility values which were used in the final smoothing equation for the recommended solubility values in the critical evaluation.</p> <p>The authors reported the solubility at cm<sup>3</sup> at 273.15 K and 101.325 kPa (1 atm) per Kg water. We have labeled it Kunenen coefficient <math>\times 10^3</math>.</p> <p>The mole fraction solubility of gas at 101.325 kPa (1 atm) partial pressure of Krypton was calculated by the compiler.</p>		T/K	Mol Fraction $x_1 \times 10^5$	Kunenen Coefficient $S_0 \times 10^3$	T/K	Mol Fraction $x_1 \times 10^5$	Kunenen Coefficient $S_0 \times 10^3$	279.75	6.591	82.0	319.15	3.110	38.3	281.15	6.382	79.4	325.05	2.923*	35.9	285.75	5.589	69.5	331.05	2.719*	33.3	288.65	5.277	65.6	332.95	2.681*	32.8	291.35	4.966	61.7	337.85	2.590*	31.6	294.35	4.687	58.2	340.65	2.520*	30.7	297.85	4.312	53.5	344.65	2.444*	29.7	303.35	3.948	48.9	347.05	2.431*	29.5	308.55	3.582	44.3	348.05	2.416*	29.3	314.55	3.290	40.6			
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<b>METHOD:</b> Flowing the previously degassed liquid in a thin film through the gas in an absorption spiral. Volume changes are measured in burets. See ref. 1.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton. 99-100% pure; the residue being xenon. 2. Water. no comments made by authors.																																																																		
<b>APPARATUS/PROCEDURE:</b> Apparatus of Morrison and Billett (1) used. The authors smoothing equation is $\log_{10} S_0 = -60.434 + (3410)/(T/K)$	<b>ESTIMATED ERROR:</b> Some data at lower temperatures are several per cent low. <b>REFERENCES:</b> 1. Morrison, T. J.; Billett, F. <u>J. Chem. Soc.</u> 1952, 3819.																																																																		

<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Water; H <sub>2</sub> O; 7732-18-5	<b>ORIGINAL MEASUREMENTS:</b> Benson, B. B.; Krause, D. <u>J. Chem. Phys.</u> 1976, <u>64</u> , 689 - 709.																											
<b>VARIABLES:</b> T/K: 273.151 - 318.154	<b>PREPARED BY:</b> R. Battino																											
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<p>VARIABLES:</p> <p>T/K: 373.15 - 573.15</p> <p>Kr P/kPa: <math>1.0135 \times 10^{-3}</math> - <math>41.8 \times 10^{-3}</math> (<math>1.47 \times 10^{-4}</math> - <math>60.6 \times 10^{-4}</math> psia)</p>	<p>PREPARED BY:</p> <p>A.L. Cramer H.L. Clever</p>																																																																											
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<p>METHOD/APPARATUS/PROCEDURE:</p> <p>A Kr/<math>^{85}\text{Kr}</math> stock mixture and <math>\text{O}_2</math> are added separately to a thermostated stainless steel vessel containing about 275 ml of water. Equilibration time varied from 1.5 to 22 hours without appreciable difference in results (one run went for 64 hours). At equilibrium both liquid and vapor were sampled and the krypton in each phase was determined by counting the <math>^{85}\text{Kr}</math> tag.</p> <p>Henry's law constant is linear in temperature. The authors give</p> $K = (p/\text{psia})/X_1 = (0.126 - 0.0263(t/^\circ\text{C})) \times 10^5$ <p>with a standard deviation of <math>0.218 \times 10^5</math>.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>ESTIMATED ERROR:</p> <p>At the 95% confidence level the uncertainty in K is</p> $\pm 0.471 \times 10^5 (0.0677 - (T - 202)^2 / 75334)$ <p><math>\delta T/K = 0.1</math></p>																																																																											

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Smoothed data: A graph of the krypton mole fraction solubility at a partial krypton pressure of 101.325 kPa was constructed using the solubility data at temperatures between 273 and 348 K used in the critical evaluation of krypton + water, as well as the data from this paper. The data give a single smooth curve with a minimum near 380 K.

The thirty data points used in the critical evaluation of krypton solubility at temperature below 348 K and the 15 data points from the present paper were combined in a linear regression to obtain the equation

$$\ln X_1 = -61.52677 + 82.72769/(T/100) + 21.7672 \ln (T/100)$$

The equation is a tentative equation for use between 373.15 and 573.15 K. It is not recommended for use at lower temperatures. It gives a mole fraction solubility at 273.15 K that is 3.3% lower, at 293.15 K 0.02% lower, and 348.15 K 2.5% higher than the recommended equation for that temperature interval.

Smoothed values of the mole fraction solubility, Ostwald coefficients, Gibbs energy, enthalpy and entropy of solution at 25 K intervals between 373.15 and 573.15 K are given in Table 1. A comparison of the two equations and the data from this paper is given in Figure 1.

TABLE 1. Tentative values of the solubility of krypton in water at a krypton partial pressure of 101.325 kPa and values of the thermodynamic properties on solution between 373.15 and 573.15 K.

T/K	Mol Fraction $X_1 \times 10^5$	Ostwald Coefficient L	$\Delta G^\circ/\text{kJ mol}^{-1}$	$\Delta H^\circ/\text{kJ mol}^{-1}$	$\Delta S^\circ/\text{J K}^{-1}\text{mol}^{-1}$
373.15	2.27	0.0370	33.18	-1.25	-92.3
398.15	2.31	0.0394	35.33	+3.27	-80.5
423.15	2.55	0.0451	37.21	+7.80	-69.5
448.15	2.99	0.0545	38.81	+12.3	-59.1
473.15	3.68	0.0684	40.17	+16.8	-49.3
498.15	4.69	0.0884	41.28	+21.4	-40.0
523.15	6.16	0.116	42.17	+25.9	-31.1
548.15	8.27	0.155	42.84	+30.4	-22.7
573.15	11.3	0.207	43.31	+34.9	-14.6

$\Delta C_p^\circ$  is constant with a value of 181. J K<sup>-1</sup> mol<sup>-1</sup>.

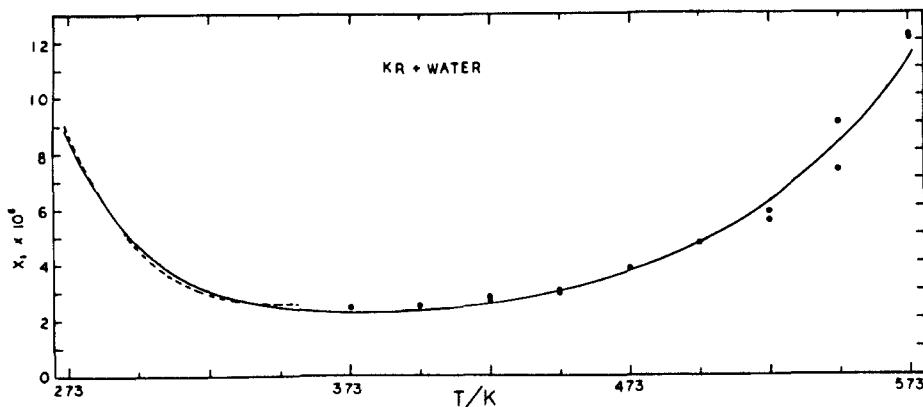


FIGURE 1. The mole fraction solubility of krypton in water at a krypton partial pressure of 101.325 kPa (1 atm). Recommended low temperature equation ----, tentative high temperature equation \_\_\_\_\_.

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>1. Krypton; Kr; 7439-90-9</li> <li>2. Sea Water</li> </ol>	<p>EVALUATOR:</p> <p>H. L. Clever          Chemistry Department          Emory University          Atlanta, GA 30322          U.S.A.</p>
<p>CRITICAL EVALUATION:</p> <p>There are three reports of the solubility of krypton in sea water. König (1) reports krypton solubility values at eight temperatures between 273.15 and 297.15 K. Wood and Caputi (2) report krypton solubility values at three temperatures between 274.45 and 321.25 K. Weiss and Kyser (3) report three to five krypton solubility values at each of seven temperatures between 273.23 and 313.25 K.</p> <p>Weiss and Kyser appear to have carried out the most reliable work and we recommend use of their values. Weiss and Kyser corrected these data for the real molar value of krypton and for the fugacity of the krypton. Their equation for the Bunsen solubility coefficient of krypton, corrected for nonideal behavior, is given by the equation</p> $\ln[\text{Bunsen}] = -57.2596 + 87.4242(100/T) + 22.9332 \ln(T/100) + S\%[-0.008723 - 0.002793(T/100) + 0.0012398(T/100)^2]$ <p>where T is the absolute temperature and S% is the salinity in parts per thousand.</p> <p>Weiss and Kyser give equations for the solubility of krypton from moist air at 101.325 kPa (1 atm) total pressure in units of <math>\text{cm}^3 \text{ Kr(STP) dm}^{-3}</math> sea water and <math>\text{cm}^3 \text{ Kr(STP) kg}^{-1}</math> sea water assuming that krypton mole fraction in dry air is <math>1.141 \times 10^{-6}</math> (4). The equations are</p> $\ln[\text{cm}^3 \text{ Kr(STP) dm}^{-3}] = -109.9320 + 149.8152(100/T) + 72.8393 \ln(T/100) - 9.9217(T/100) + S\%[-0.006953 - 0.004085(T/100) + 0.0014759(T/100)^2]$ <p>and</p> $\ln[\text{cm}^3 \text{ Kr(STP) kg}^{-1}] = -112.6840 + 153.5817(100/T) + 74.4690 \ln(T/100) - 10.0189(T/100) + S\%[-0.011213 - 0.001844(T/100) + 0.0011201(T/100)^2]$ <p>Extensive tables of krypton Bunsen coefficients and <math>\text{cm}^3 \text{ Kr(STP) kg}^{-1}</math> as a function of temperature and salinity as calculated from the above equations are given in the original paper.</p> <p>Weiss and Kyser compare the earlier work with their results. They show that the König data are as much as 14 per cent lower at low temperatures and that the Wood and Caputi data averages 1.9 percent lower than their own data at 274.45 and 299.55 K. Data sheets follow for both the Weiss and Kyser and the Wood and Caputi solubility values. The Wood and Caputi values extend the temperature range another seven degrees.</p> <ol style="list-style-type: none"> <li>1. König, H. <u>Z. Naturforsch.</u> 1963, 18a, 363.</li> <li>2. Wood, D.; Caputi, R. <u>USNRDL-TR-988</u>, Feb. 1966.</li> <li>3. Weiss, R. F.; Kyser, T. K. <u>J. Chem. Eng. Data</u>, 1978, 23, 69.</li> <li>4. Glueckauf, E.; Kitt, G. A. <u>Proc. Roy. Soc. London</u>, 1956, 234A, 557.</li> </ol>	

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Krypton; Kr; 7439-90-9</li> <li>Sea Water</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Weiss, R. F.; Kyser, T. K.</p> <p><u>J. Chem. Eng. Data</u> 1978, <u>23</u>, 69 - 72.</p>																																																																																																																																																						
<p>VARIABLES:</p> <p>T/K: 273.22 - 313.25          Kr P/kPa: 101.325 (1 atm)          Salinity/mil<sup>-1</sup>: 0 - 36.595</p>	<p>PREPARED BY:</p> <p>A. L. Cramer</p>																																																																																																																																																						
<p>EXPERIMENTAL VALUES: <span style="float: right;">Salinity/‰</span></p> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th colspan="2" style="text-align: center;">0.0</th> <th colspan="2" style="text-align: center;">19.046</th> <th colspan="2" style="text-align: center;">36.595</th> </tr> <tr> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Bunsen/α</th> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Bunsen/α</th> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Bunsen/α</th> </tr> </thead> <tbody> <tr><td>273.74</td><td>0.10778</td><td></td><td></td><td>273.24</td><td>0.08451</td></tr> <tr><td>273.72</td><td>0.10778</td><td></td><td></td><td>273.22</td><td>0.08438</td></tr> <tr><td>273.72</td><td>0.10790</td><td></td><td></td><td>273.24</td><td>0.08442</td></tr> <tr><td>273.73</td><td>0.10786</td><td></td><td></td><td>273.23</td><td>0.08444</td></tr> <tr><td></td><td></td><td>278.05</td><td>0.08200</td><td>278.47</td><td>0.07198</td></tr> <tr><td>283.48</td><td>0.07981</td><td>278.05</td><td>0.08212</td><td>278.46</td><td>0.07204</td></tr> <tr><td>283.47</td><td>0.07985</td><td>278.05</td><td>0.08220</td><td>278.47</td><td>0.07193</td></tr> <tr><td>283.47</td><td>0.07979</td><td></td><td></td><td>283.57</td><td>0.06273</td></tr> <tr><td>293.39</td><td>0.06222</td><td></td><td></td><td>283.57</td><td>0.06276</td></tr> <tr><td>293.39</td><td>0.06220</td><td></td><td></td><td>283.56</td><td>0.06270</td></tr> <tr><td>293.40</td><td>0.06227</td><td></td><td></td><td>288.25</td><td>0.05566</td></tr> <tr><td>293.39</td><td>0.06221</td><td></td><td></td><td>288.25</td><td>0.05547</td></tr> <tr><td>293.40</td><td>0.06226</td><td></td><td></td><td>288.25</td><td>0.05554</td></tr> <tr><td></td><td></td><td></td><td></td><td>293.49</td><td>0.04920</td></tr> <tr><td>304.12</td><td>0.04953</td><td></td><td></td><td>293.49</td><td>0.04933</td></tr> <tr><td>304.13</td><td>0.04957</td><td></td><td></td><td>293.49</td><td>0.04935</td></tr> <tr><td>304.13</td><td>0.04955</td><td>303.23</td><td>0.04525</td><td>303.11</td><td>0.04084</td></tr> <tr><td>304.12</td><td>0.04961</td><td>303.23</td><td>0.04510</td><td>303.12</td><td>0.04093</td></tr> <tr><td></td><td></td><td>303.23</td><td>0.04517</td><td>303.11</td><td>0.04085</td></tr> <tr><td></td><td></td><td>303.23</td><td>0.04532</td><td>313.25</td><td>0.03475</td></tr> <tr><td>313.24</td><td>0.04215</td><td></td><td></td><td>313.25</td><td>0.03469</td></tr> <tr><td>313.25</td><td>0.04218</td><td></td><td></td><td>313.25</td><td>0.03481</td></tr> <tr><td>313.25</td><td>0.04216</td><td></td><td></td><td>313.24</td><td>0.03475</td></tr> </tbody> </table>		0.0		19.046		36.595		T/K	Bunsen/α	T/K	Bunsen/α	T/K	Bunsen/α	273.74	0.10778			273.24	0.08451	273.72	0.10778			273.22	0.08438	273.72	0.10790			273.24	0.08442	273.73	0.10786			273.23	0.08444			278.05	0.08200	278.47	0.07198	283.48	0.07981	278.05	0.08212	278.46	0.07204	283.47	0.07985	278.05	0.08220	278.47	0.07193	283.47	0.07979			283.57	0.06273	293.39	0.06222			283.57	0.06276	293.39	0.06220			283.56	0.06270	293.40	0.06227			288.25	0.05566	293.39	0.06221			288.25	0.05547	293.40	0.06226			288.25	0.05554					293.49	0.04920	304.12	0.04953			293.49	0.04933	304.13	0.04957			293.49	0.04935	304.13	0.04955	303.23	0.04525	303.11	0.04084	304.12	0.04961	303.23	0.04510	303.12	0.04093			303.23	0.04517	303.11	0.04085			303.23	0.04532	313.25	0.03475	313.24	0.04215			313.25	0.03469	313.25	0.04218			313.25	0.03481	313.25	0.04216			313.24	0.03475
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<p>METHOD: Solubility determinations by the Scholander microgasometric technique as used by Douglas (1), with minor modification by Weiss (2).</p> <p>Real krypton molar volume at STP was used and a fugacity correction was applied.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>Krypton. Matheson Gas Products. &gt; 99.995 % pure. Gas chromatographic checks showed <math>\leq 0.01</math> % air.</li> <li>Sea Water. Collected from surface, evaporated to increase salinity <math>\sim 2\%</math>, passed through 0.45 <math>\mu</math> millipore filter and poisoned with 1 mg/l of HgCl<sub>2</sub>.</li> </ol>																																																																																																																																																						
<p>APPARATUS/PROCEDURE: An equilibrium chamber, containing pure gas saturated with water vapor, is separated by mercury from a closed side chamber containing degassed water. The apparatus is tipped on its side, allowing degassed water to flow into the equilibrium chamber. Dissolution is aided by mechanical shaking.</p>	<p>ESTIMATED ERROR:</p> <p><math>\delta T/K = 0.01</math>  <math>\delta \text{salinity} = 0.004</math></p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>Douglas, E. <u>J. Phys. Chem.</u> 1964, <u>68</u>, 169.  <u>ibid.</u> 1965, <u>69</u>, 2608.</li> <li>Weiss, R. F. <u>J. Chem. Eng. Data</u> 1971, <u>16</u>, 235-241.</li> </ol>																																																																																																																																																						

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1. Krypton; Kr; 7439-90-9 2. Sea Water		Wood, D.; Caputi, R.  U.S.N.R.D.L.-TR-988, 27 Feb. 1966 <u>Chem. Abstr.</u> 1967, 66, 118693u.			
VARIABLES:		PREPARED BY:			
T/K: 274.45 - 320.95 P/kPa: 101.325 (1 atm)		A. L. Cramer			
EXPERIMENTAL VALUES:					
T/K	Henry's Constant $K = (P_1/\text{mmHg})/X_1$	Percent Error*	Number of Determinations	Mol Fraction $X_1 \times 10^3$	Bunsen Coefficient $\alpha$
Water; H <sub>2</sub> O; 7732-18-5					
274.45	$0.866 \times 10^7$	0.3	3	0.0878	0.1098
298.15	$1.653 \times 10^7$	0.4	2	0.0450	0.0571
320.95	$2.340 \times 10^7$	2.1	4	0.0325	0.0400
Artificial Sea Water(1); S% = 34.727					
274.45	$1.181 \times 10^7$	0.3	2	0.0644	0.0803
299.55	$2.163 \times 10^7$	0.1	2	0.0351	0.0435
320.35	$2.792 \times 10^7$	0.3	2	0.0272	0.0335
<p>* Percent error is the maximum spread in Henry's constant times 100 divided by average Henry's constant.</p> <p>The mole fractions were calculated by the compiler from the average Henry's constant. The Bunsen coefficients were calculated by the compiler from the mole fractions using a solvent mean molecular weight of 18.4823 and sea water densities from the International Critical Tables.</p>					
AUXILIARY INFORMATION					
METHOD/APPARATUS/PROCEDURE:			SOURCE AND PURITY OF MATERIALS:		
<p>Degassed water was introduced into an evacuated apparatus (&lt; 50 <math>\mu</math> Hg) and gas bled into burette. After the system was isolated, gas was admitted to equilibrium column and the water was circulated through the column, flowing over packing of 4 mm Berl saddles at 110 ml/min for 4-5 hr.</p> <p>Dissolved gas was reclaimed and measured by evacuating the system <math>\rightarrow</math> &lt; 1 <math>\mu</math> Hg and allowing water to distill and condense in a cold trap. Water was melted and refrozen until all the gas was recovered. Gas was then transferred to a gas burette and the pressure was measured with a Hg manometer. Purity was checked by gas chromatography.</p>			1. Krypton. AIRCO. Certified 0.015% Xe. Air contamination 0.0001 determined by gas chromatography.  2. Water. Distilled three times before degassing. Sea Water. Artificial, modified from (1).		
			ESTIMATED ERROR: $\delta T/K = 0.1, 0.005, 0.03$ (as T increases) $\delta P/P = 0.001$ $\delta H/H = 0.005$ (author's error analysis)		
			REFERENCES:		
			1. Lyman, J.; Fleming, R. H. <u>J. Mar. Res.</u> 1940, <u>3</u> , 134.		

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>1. Krypton; Kr; 7439-90-9</li> <li>2. Water; H<sub>2</sub>O; 7732-18-5</li> <li>3. Electrolyte</li> </ol>	<p>EVALUATOR:</p> <p>H. L. Clever          Chemistry Department          Emory University          Atlanta, GA 30322          U. S. A.</p> <p>September 1978</p>
<p>CRITICAL EVALUATION:</p> <p>The solubility of krypton in aqueous electrolyte solutions.</p> <p>The results of studies of the solubility of krypton in aqueous salt solution can be classified as no better than tentative. Körösy (1) reports a solubility of krypton in aqueous 20 weight per cent CaCl<sub>2</sub> solution which is of dubious value. Morrison and Johnstone (2) report Setschenow salt effect parameters for 13 aqueous electrolyte solutions. All of their values are based on only one measurement in a one molal salt solution. Although Morrison and Johnstone's Setschenow parameter values for other gases usually accord well with the results of more extensive studies of other workers, their values based on only one measurement in an electrolyte solution must be classed as tentative.</p> <p>Yeh and Peterson (3), Kitani (4), and Kirk, Parrish and Morken (5) have measured the solubility of krypton in 0.9 weight percent NaCl solution. Kirk <i>et al.</i> did not report a krypton solubility in water so it is not possible to convert their solubility value to a Setschenow parameter. The Setschenow salt effect parameters for krypton in aqueous NaCl solutions from the data of Morrison and Johnstone, Yeh and Peterson, and Kitani do not agree well (Table 1). The values based on Yeh and Peterson's data appear to be high and somewhat erratic as a function of temperature. The values of Morrison and Johnstone and of Kitani are probably more reliable.</p> <p>Anderson, Keeler and Klach (6) measured the solubility of krypton in water, and in aqueous solution containing UO<sub>2</sub>SO<sub>4</sub>, CuSO<sub>4</sub> and H<sub>2</sub>SO<sub>4</sub> at temperatures between 373 and 573 K. They found no statistical difference in the Henry's constant of krypton in water and in a solution that was 0.02 mol dm<sup>-3</sup> UO<sub>2</sub>SO<sub>4</sub>, 0.005 mol dm<sup>-3</sup> CuSO<sub>4</sub> and 0.005 mol dm<sup>-3</sup> H<sub>2</sub>SO<sub>4</sub>. There were differences in the Henry's constant for krypton in water and in a little more concentrated solution containing 0.04 mol dm<sup>-3</sup> UO<sub>2</sub>SO<sub>4</sub>, 0.01 mol dm<sup>-3</sup> CuSO<sub>4</sub> and 0.01 mol dm<sup>-3</sup> H<sub>2</sub>SO<sub>4</sub>.</p>	

COMPONENTS:			EVALUATOR:			
1. Krypton; Kr; 7439-90-9			H. L. Clever			
2. Water; H <sub>2</sub> O; 7732-18-5			Chemistry Department			
3. Electrolyte			Emory University			
			Atlanta, GA 30322			
			U. S. A.			
			September 1978			
CRITICAL EVALUATION:						
Electrolyte	T/K	mol salt Kg <sup>-1</sup> H <sub>2</sub> O	k <sub>s</sub> = (1/m) log (S <sup>o</sup> /S)	K <sub>sx</sub> = (1/m) log (X <sup>o</sup> /X)	Ref.	
NH <sub>4</sub> Cl	298.15	1.0	0.065	0.080	2	
(CH <sub>3</sub> ) <sub>4</sub> NI	298.15	1.0	-0.016	-0.001	2	
(C <sub>2</sub> H <sub>5</sub> ) <sub>4</sub> NBr	298.15	1.0	-0.032	-0.017	2	
HCl	298.15	1.0	0.028	0.043	2	
HNO <sub>3</sub>	298.15	1.0	-0.003	0.012	2	
BaCl <sub>2</sub>	298.15	1.0	0.151	0.174	2	
LiCl	298.15	1.0	0.116	0.131	2	
NaCl	298.15	1.0	0.146	0.161	2	
	298.15	0.155	0.195	0.210	3	
	303.15	0.155	0.216	0.231	3	
	310.15	0.155	0.224	0.239	3	
	310.15	0.155	0.137	0.152	4	
	310.15	0.155	*	--	5	
	318.15	0.155	0.197		3	
Na <sub>2</sub> SO <sub>4</sub>	298.15	1.0	0.203	0.226	2	
Na <sub>3</sub> PO <sub>4</sub> **	298.15	0.066	0.266	--	3	
	303.15	0.066	0.287	--	3	
	310.15	0.066	0.265	--	3	
	318.15	0.066	0.368	--	3	
KCl	298.15	1.0	0.124	0.139	2	
KBr	298.15	1.0	0.120	0.135	2	
KI	298.15	1.0	0.120	0.135	2	
KNO <sub>3</sub>	298.15	1.0	0.093	0.108	2	
UO <sub>2</sub> SO <sub>4</sub>	373-573	0.02-0.04	--	--	6	
*k <sub>s</sub> ranges between 0.05 and 0.20 depending on the value of water solubility used.						
** The Na <sub>3</sub> PO <sub>4</sub> concentration in mol dm <sup>-3</sup> solution.						
REFERENCES						
1. Korossy, F. <u>Trans. Faraday Soc.</u> 1937, <u>33</u> , 416.						
2. Morrison, T. J.; Johnstone, N. B. B. <u>J. Chem. Soc.</u> 1955, 3655.						
3. Yeh, S. Y.; Peterson, R. E. <u>J. Pharm. Sci.</u> 1964, <u>53</u> , 822.						
4. Kitani, K. <u>Scand. J. Clin. Lab. Invest.</u> 1972, <u>29</u> , 167.						
5. Kirk, W. P.; Parish, P. W.; Morken, D. A. <u>Health Physics</u> 1975, <u>28</u> , 249.						
6. Anderson, C. J.; Keeler, R. A.; Klach, S. S. <u>J. Chem. Eng. Data</u> 1962, <u>7</u> , 290.						

<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Water; H <sub>2</sub> O; 7732-18-5 3. Ammonium Chloride; NH <sub>4</sub> Cl; 12125-02-9	<b>ORIGINAL MEASUREMENTS:</b> Morrison, T.J.; Johnstone, N.B.B.  <u>J. Chem. Soc.</u> 1955, 3655-3659.						
<b>VARIABLES:</b> T/K: 298.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> T.D. Kittredge H.L. Clever						
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="306 506 1079 610"> <thead> <tr> <th>T/K</th> <th><math>k_s = (1/m) \log (S^0/S)</math></th> <th><math>k_{sX} = (1/m) \log (X^0/X)</math></th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>0.065</td> <td>0.080</td> </tr> </tbody> </table> <p>The value of the Setschenow salt effect parameter, <math>k_s</math>, was apparently determined from only two solubility measurements. They were the solubility of krypton in pure water, <math>S^0</math>, and the solubility of krypton in a near one equivalent of salt per kg of water solution, <math>S</math>. No solubility values are given in the paper. The <math>S^0/S</math> ratio was referenced to a solution containing one kg of water. The compiler calculated the salt effect parameter <math>k_{sX}</math> from the mole fraction solubility ratio <math>X^0/X</math>. The electrolyte was assumed to be 100 per cent dissociated and both cation and anion were used in the mole fraction calculation.</p>		T/K	$k_s = (1/m) \log (S^0/S)$	$k_{sX} = (1/m) \log (X^0/X)$	298.15	0.065	0.080
T/K	$k_s = (1/m) \log (S^0/S)$	$k_{sX} = (1/m) \log (X^0/X)$					
298.15	0.065	0.080					
<b>AUXILIARY INFORMATION</b>							
<b>METHOD:</b> Gas absorption in a flow system.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton. British Oxygen Co. Ltd. 2. Water. No information given. 3. Electrolyte. No information given.						
<b>APPARATUS/PROCEDURE:</b> The previously degassed solvent flows in a thin film down an absorption spiral containing Kr gas plus solvent vapor at a total pressure of one atm. The volume of gas absorbed is measured in attached calibrated burets (1).	<b>ESTIMATED ERROR:</b> $\delta k_s = 0.010$  <b>REFERENCES:</b> 1. Morrison, T.J.; Billett, F. <u>J. Chem. Soc.</u> 1952, 3819.						



<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Water; H <sub>2</sub> O; 7732-18-5 3. Ammonium Type Salts	<b>ORIGINAL MEASUREMENTS:</b> Morrison, T.J.; Johnstone, N.B.B.  <u>J. Chem. Soc.</u> 1955, 3655-3659.															
<b>VARIABLES:</b> T/K: 298.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> T.D. Kittredge H.L. Clever															
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<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Water; H <sub>2</sub> O; 7732-18-5 3. Acids	<b>ORIGINAL MEASUREMENTS:</b> Morrison, T.J.; Johnstone, N.B.B.  J. Chem. Soc. 1955, 3655-3659.															
<b>VARIABLES:</b> T/K: 298.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> T.D. Kittredge H.L. Clever															
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<p>VARIABLES:</p> <p>T/K: 373.15 - 578.15 Kr P/psia: 0.407 - 36.680 (0.59 - 53.2 x <math>10^{-4}</math> psia)</p>	<p>PREPARED BY:</p> <p>A.L. Cramer H.L. Clever</p>																																																									
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<table border="1"> <thead> <tr> <th rowspan="2">T/K</th> <th colspan="2">Pressure/psia</th> <th rowspan="2">Henry's Constant <math>K = (p/\text{psia})/x_1</math> <math>K \times 10^{-5}</math></th> <th rowspan="2">Mol Fraction <math>x_1 \times 10^5</math> at 101.325 kPa Kr</th> </tr> <tr> <th>Total <math>\text{O}_2 + \text{H}_2\text{O} + \text{Kr}</math></th> <th>Partial x <math>10^4</math> Kr</th> </tr> </thead> <tbody> <tr> <td></td> <td>0.02 mol <math>\text{dm}^{-3}</math> <math>\text{UO}_2\text{SO}_4</math>,</td> <td>0.005 mol <math>\text{dm}^{-3}</math> <math>\text{CuSO}_4</math> and</td> <td>0.005 mol <math>\text{dm}^{-3}</math> <math>\text{H}_2\text{SO}_4</math></td> <td></td> </tr> <tr> <td>373.15</td> <td>115 365</td> <td>0.93 5.03</td> <td>6.37 6.66</td> <td>2.31 2.21</td> </tr> <tr> <td>398.15</td> <td>110 350</td> <td>0.59 33.9</td> <td>5.78 5.93</td> <td>2.54 2.48</td> </tr> <tr> <td>423.15</td> <td>125 315</td> <td>0.40 28.2</td> <td>5.1 5.20</td> <td>2.88 2.83</td> </tr> <tr> <td>523.15</td> <td>1120 1165 1310 1330 1495</td> <td>15.0 15.0 6.20 7.20 39.0</td> <td>2.60 2.70 2.80 2.60 2.38</td> <td>5.65 5.44 5.25 5.65 6.18</td> </tr> <tr> <td>524.15</td> <td>1095</td> <td>53.2</td> <td>2.08</td> <td>7.07</td> </tr> <tr> <td>543.15</td> <td>1235</td> <td>44.1</td> <td>1.75</td> <td>8.40</td> </tr> <tr> <td>548.15</td> <td>1340 1485 1565 1715</td> <td>11.0 4.20 6.00 42.9</td> <td>1.9 1.8 2.0 1.90</td> <td>7.74 8.17 7.35 7.74</td> </tr> <tr> <td>573.15</td> <td>1577 1665 1736 1870 2015</td> <td>7.0 9.1 3.0 4.5 3.77</td> <td>1.0 1.1 1.20 1.3 1.49</td> <td>14.7 13.4 12.3 11.3 9.87</td> </tr> <tr> <td>578.15</td> <td>1625</td> <td>2.5</td> <td>1.01</td> <td>14.55</td> </tr> </tbody> </table>		T/K	Pressure/psia		Henry's Constant $K = (p/\text{psia})/x_1$ $K \times 10^{-5}$	Mol Fraction $x_1 \times 10^5$ at 101.325 kPa Kr	Total $\text{O}_2 + \text{H}_2\text{O} + \text{Kr}$	Partial x $10^4$ Kr		0.02 mol $\text{dm}^{-3}$ $\text{UO}_2\text{SO}_4$ ,	0.005 mol $\text{dm}^{-3}$ $\text{CuSO}_4$ and	0.005 mol $\text{dm}^{-3}$ $\text{H}_2\text{SO}_4$		373.15	115 365	0.93 5.03	6.37 6.66	2.31 2.21	398.15	110 350	0.59 33.9	5.78 5.93	2.54 2.48	423.15	125 315	0.40 28.2	5.1 5.20	2.88 2.83	523.15	1120 1165 1310 1330 1495	15.0 15.0 6.20 7.20 39.0	2.60 2.70 2.80 2.60 2.38	5.65 5.44 5.25 5.65 6.18	524.15	1095	53.2	2.08	7.07	543.15	1235	44.1	1.75	8.40	548.15	1340 1485 1565 1715	11.0 4.20 6.00 42.9	1.9 1.8 2.0 1.90	7.74 8.17 7.35 7.74	573.15	1577 1665 1736 1870 2015	7.0 9.1 3.0 4.5 3.77	1.0 1.1 1.20 1.3 1.49	14.7 13.4 12.3 11.3 9.87	578.15	1625	2.5	1.01	14.55
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<p>METHOD /APPARATUS/PROCEDURE:</p> <p>A Kr/<math>^{85}\text{Kr}</math> stock mixture and <math>\text{O}_2</math> are added separately to a thermostated stainless steel vessel containing about 275 ml of solution. Equilibration time varied from 1.5 to 22 hours without appreciable difference in results (one run went for 64 hours). At equilibrium both liquid and vapor were sampled and the krypton in each phase was determined by counting the <math>^{85}\text{Kr}</math> tag.</p> <p>Henry's law constant is linear in temperature. The authors give <math>K = (9.188 - 0.0267t/^\circ\text{C}) \times 10^5 \text{ psia } x_1^{-1}</math> with a standard deviation about the line of <math>0.170 \times 10^5</math>.</p> <p>The solubility of Kr in water and in the uranyl sulfate solution above appears to be the same. The Henry's constant for the two sets of data pooled for one equation is <math>K = (9.162 - 0.0265t/^\circ\text{C}) \times 10^5 \text{ psia } x_1^{-1}</math></p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>No information</p> <p>ESTIMATED ERROR: The 95% confidence limits are given by <math>K \pm 0.357 \times 10^5 \left[ 0.05 + \frac{(t-230)^2}{130,000} \right]^{1/2}</math></p> <p>REFERENCES:</p> <p>*The mole fraction solubility at a krypton partial pressure of 101.325 kPa was calculated by the compilers.</p>																																																									

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VARIABLES:		PREPARED BY:		
T/K: 373.15 - 573.15 Kr P/pa: 2.261 - 50-332 (3.28 - 73.0 x 10 <sup>-4</sup> psia)		A.L. Cramer H.L. Clever		
EXPERIMENTAL VALUES:				
T/K	Pressure/psia		Henry's Constant K = (p/psia)/X <sub>1</sub>	Mol Fraction X <sub>1</sub> x 10 <sup>5</sup> at 101.325 kPa Kr
	Total O <sub>2</sub> + H <sub>2</sub> O + Kr	Partial x 10 <sup>4</sup> Kr		
	0.04 mol dm <sup>-3</sup>	UO <sub>2</sub> SO <sub>4</sub> , 0.01 mol dm <sup>-3</sup>	CuSO <sub>4</sub> , 0.01 mol dm <sup>-3</sup>	H <sub>2</sub> SO <sub>4</sub>
373.15	355 350 380	29.8 7.25 68.0	6.31 6.20 5.96	2.33 2.37 2.47
423.15	400 410 445	27.6 6.93 73.0	5.19 5.73 5.18	2.83 2.57 2.84
523.15	825 860 860 905	43.7 5.02 25.1 55.7	1.90 2.03 2.20 2.11	7.74 7.24 6.68 6.97
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Henry's law constant is not linear in temperature as it appears to be for water and the more dilute uranyl sulfate solution.		ESTIMATED ERROR:		
The mean values of K at the four temperatures are		REFERENCES:		
T/K	K/psia X <sub>1</sub> <sup>-1</sup> x 10 <sup>-5</sup>			
373.15	(6.16 ± 0.26)			
423.15	(5.36 ± 0.26)			
473.15	(2.06 ± 0.23)			
523.15	(1.09 ± 0.23)			

<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Water; H <sub>2</sub> O; 7732-18-5 3. Barium Chloride; BaCl <sub>2</sub> ; 10361-37-2	<b>ORIGINAL MEASUREMENTS:</b> Morrison, T.J.; Johnstone, N.B.B.  <u>J. Chem. Soc.</u> 1955, 3655-3659.						
<b>VARIABLES:</b> T/K: 298.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> T.D. Kittredge H.L. Clever						
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<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Water; H <sub>2</sub> O; 7732-18-5 3. Sodium Chloride; NaCl; 7647-14-5	<b>ORIGINAL MEASUREMENTS:</b> Yeh, S.Y.; Peterson, R.E.  <u>J. Pharm. Sci.</u> 1964, <u>53</u> , 822 - 824.																				
<b>VARIABLES:</b> T/K: 298.15 - 318.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> H.L. Clever																				
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="302 514 1072 725"> <thead> <tr> <th>T/K</th> <th>Ostwald Coefficient L</th> <th><math>\Delta H^\circ/\text{cal mol}^{-1}</math></th> <th><math>\Delta S^\circ/\text{cal K}^{-1} \text{mol}^{-1}</math></th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>0.0542</td> <td>-5017</td> <td>-28.9</td> </tr> <tr> <td>303.15</td> <td>0.0499</td> <td>-4252</td> <td>-26.4</td> </tr> <tr> <td>310.15</td> <td>0.0444</td> <td>-3181</td> <td>-22.9</td> </tr> <tr> <td>318.15</td> <td>0.0411</td> <td>-1957</td> <td>-19.0</td> </tr> </tbody> </table> <p>For comparison, the authors' Ostwald coefficients in water were 0.0581, 0.0539, 0.0481 and 0.0441 at the four temperatures.</p> <p>The sodium chloride solution is 0.9 weight percent which is about 0.155 mole NaCl kg<sup>-1</sup> water.</p> <p>Each solubility value is the average of three or four measurements. The standard deviation of each measurement closely approximates 1.0 per cent.</p> <p>The thermodynamic changes are for the transfer of one mole of krypton from the gas phase at a concentration of one mole dm<sup>-3</sup> to the solution at a concentration of one mole dm<sup>-3</sup>.</p>		T/K	Ostwald Coefficient L	$\Delta H^\circ/\text{cal mol}^{-1}$	$\Delta S^\circ/\text{cal K}^{-1} \text{mol}^{-1}$	298.15	0.0542	-5017	-28.9	303.15	0.0499	-4252	-26.4	310.15	0.0444	-3181	-22.9	318.15	0.0411	-1957	-19.0
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<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Water; H <sub>2</sub> O; 7732-18-5 3. Alkali Halides	<b>ORIGINAL MEASUREMENTS:</b> Morrison, T.J.; Johnstone, N.B.B.  <u>J. Chem. Soc.</u> 1955, 3655-3659.																																	
<b>VARIABLES:</b> T/K: 298.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> T.D. Kittredge H.L. Clever																																	
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<b>VARIABLES:</b> T/K: 298.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> T.D. Kittredge H.L. Clever						
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<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Water; H <sub>2</sub> O; 7732-18-5 3. Sodium Phosphate (phosphate buffer); Na <sub>3</sub> PO <sub>4</sub> ; 7601-54-9	<b>ORIGINAL MEASUREMENTS:</b> Yeh, S-Y.; Peterson, R.E.  J. <u>Pharm. Sci.</u> 1964, <u>53</u> , 822 - 824.																				
<b>VARIABLES:</b> T/K: 298.15 - 318.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b>  H.L. Clever																				
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<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Pentane; C <sub>5</sub> H <sub>12</sub> ; 109-66-0	<b>ORIGINAL MEASUREMENTS:</b> Makranczy, J.; Megyery-Balog, K.; Rusz, L.; Patyi, L.  <u>Hung. J. Ind. Chem.</u> 1976, <u>4</u> , 269-280.								
<b>VARIABLES:</b> T/K: 298.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> S.A. Johnson								
<b>EXPERIMENTAL VALUES:</b>  <table border="1" data-bbox="170 522 1130 687"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>7.85</td> <td>1.528</td> <td>1.668</td> </tr> </tbody> </table>  The mole fraction and Bunsen coefficient were calculated by the compiler.		T/K	Mol Fraction $x_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	298.15	7.85	1.528	1.668
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<b>METHOD:</b> Volumetric method. The apparatus of Bodor, Bor, Mohai, and Sipos (1) was used.	<b>SOURCE AND PURITY OF MATERIALS:</b> Both the gas and liquid were analytical grade reagents of Hungarian or foreign origin. No further information.								
<b>APPARATUS/PROCEDURE:</b>	<b>ESTIMATED ERROR:</b> $\delta X_1 / X_1 = 0.03$  <b>REFERENCES:</b> 1. Bodor, E.; Bor, Gy.; Mohai, B.; Sipos, G. Veszpremi Vegyip. Egy. Kozl. 1957, <u>1</u> , 55. <u>Chem. Abstr.</u> 1961, <u>55</u> , 3175h.								

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>1. Krypton; Kr; 7439-90-9</li> <li>2. Hexane; C<sub>6</sub>H<sub>14</sub>; 110-54-3</li> </ol>	<p>EVALUATOR:</p> <p>H. L. Clever            Chemistry Department            Emory University            Atlanta, GA 30322            U.S.A.</p>																																				
<p>CRITICAL EVALUATION:</p> <p>The solubility of krypton in hexane at 101.325 kPa was measured in three laboratories. Clever, Battino, Saylor and Gross (1) report three solubilities between 289.30 and 313.75 K. Steinberg and Manowitz (2) report solubilities at 183.15 and 298.15 K. Makranczy, Megyery-Balog, Ruzs, and Patyi (3) report a solubility at 298.15. The solubility values near 298.15 K from the three laboratories differ by about 30 percent.</p> <p>Clever <i>et al.</i> probably used materials of better purity than the materials used by Steinberg and Manowitz. The single value of Makranczy <i>et al.</i> is difficult to judge, but their results tend to scatter for other gases dissolved in hydrocarbons. The values of Clever <i>et al.</i> are to be preferred for the 288.15 - 313.15 K temperature range. The smoothed data is given on the Clever <i>et al.</i> data sheet which follows this page.</p> <p>The 183.15 K solubility value of Steinberg and Manowitz and the three solubility values of Clever <i>et al.</i> were combined in a linear least squares fit to an equation for the Gibbs energy of solution as a function of temperature. The result is a highly tentative equation for the 183.15 - 313.15 K temperature interval.</p> <p>The tentative values for the transfer of one mole of krypton from the gas at a pressure of 101.325 kPa to the hypothetical unit mole fraction solution are</p> $\Delta G^\circ/\text{J mol}^{-1} = -RT \ln X_1 = -3,340.9 + 52.564 T$ <p>Std. Dev. <math>\Delta G^\circ = 63</math>,      Coef. Corr. = 0.9998</p> $\Delta H^\circ/\text{J mol}^{-1} = -3,340.9, \Delta S^\circ/\text{J K}^{-1} \text{ mol}^{-1} = -52.564$ <p>The tentative solubility values and the Gibbs energy of solution at 101.325 kPa as a function of temperature are in Table 1.</p> <p>TABLE 1. Solubility of krypton in hexane. Tentative values of the mole fraction solubility and Gibbs energy at 101.325 kPa (1 atm) as a function of temperature.</p> <table border="1" data-bbox="400 1320 960 1663"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> x 10<sup>3</sup></th> <th><math>\Delta G^\circ/\text{J mol}^{-1}</math></th> </tr> </thead> <tbody> <tr><td>183.15</td><td>16.1</td><td>6,286.3</td></tr> <tr><td>203.15</td><td>13.0</td><td>7,337.6</td></tr> <tr><td>223.15</td><td>10.9</td><td>8,388.9</td></tr> <tr><td>243.15</td><td>9.38</td><td>9,440.2</td></tr> <tr><td>263.15</td><td>8.27</td><td>10,491</td></tr> <tr><td>273.15</td><td>7.82</td><td>11,017</td></tr> <tr><td>283.15</td><td>7.42</td><td>11,543</td></tr> <tr><td>293.15</td><td>7.07</td><td>12,068</td></tr> <tr><td>298.15</td><td>6.91</td><td>12,331</td></tr> <tr><td>303.15</td><td>6.76</td><td>12,594</td></tr> <tr><td>313.15</td><td>6.48</td><td>13,120</td></tr> </tbody> </table> <ol style="list-style-type: none"> <li>1. Clever, H. L.; Battino, R.; Saylor, J. H.; Gross, P. M. <i>J. Phys. Chem.</i> 1957, <u>61</u>, 1078.</li> <li>2. Steinberg, M.; Manowitz, B. <i>Ind. Eng. Chem.</i> 1959, <u>51</u>, 47.</li> <li>3. Makranczy, J.; Megyery-Balog, K.; Ruzs, L.; Patyi, L. <i>Hung. J. Ind. Chem.</i> 1976, <u>4</u>, 269.</li> </ol>		T/K	Mol Fraction X <sub>1</sub> x 10 <sup>3</sup>	$\Delta G^\circ/\text{J mol}^{-1}$	183.15	16.1	6,286.3	203.15	13.0	7,337.6	223.15	10.9	8,388.9	243.15	9.38	9,440.2	263.15	8.27	10,491	273.15	7.82	11,017	283.15	7.42	11,543	293.15	7.07	12,068	298.15	6.91	12,331	303.15	6.76	12,594	313.15	6.48	13,120
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<b>VARIABLES:</b> T/K: 183.15 - 298.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> H.L. Clever A.L. Cramer												
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298.15	5.73	0.995	1.05										
<b>AUXILIARY INFORMATION</b>													
<b>METHOD / APPARATUS / PROCEDURE:</b> Absorption coefficient determined by a modified McDaniel method (1).	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton. Matheson Co. Technical grade. 2. Hexane. Technically or chemically pure.  <b>ESTIMATED ERROR:</b> $\delta\beta/\beta = 0.05 - 0.10$  <b>REFERENCES:</b> 1. Furman, N.H. "Scott's Standard Methods of Chemical Analysis" Van Nostrand Co., NY, 1939, 5th ed., Vol. II, p. 2587.												

<p>COMPONENTS:</p> <p>1. Krypton; Kr; 7439-90-9</p> <p>2. Hexane; C<sub>6</sub>H<sub>14</sub>; 110-54-3</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Makranczy, J.; Megyery-Balog, K.; Rusz, L.; Patyi, L.</p> <p><u>Hung. J. Ind. Chem.</u> 1976, 4, 269-280.</p>								
<p>VARIABLES:</p> <p>T/K: 298.15</p> <p>P/kPa: 101.325 (1 atm)</p>	<p>PREPARED BY:</p> <p>S.A. Johnson</p>								
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<p>METHOD/APPARATUS/PROCEDURE:</p> <p>Volumetric method. The apparatus of Bodor, Bor, Mohai, and Sipos (1) was used.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>Both the gas and liquid were analytical grade reagents of Hungarian or foreign origin. No further information.</p> <p>ESTIMATED ERROR:</p> <p><math>\delta x_1/x_1 = 0.03</math></p> <p>REFERENCES:</p> <p>1. Bodor, E.; Bor, Gy.; Mohai, B.; Sipos, G. <u>Veszpremi Vegyip. Egy. Kozl.</u> 1957, 1, 55. <u>Chem. Abstr.</u> 1961, 55, 3175h.</p>								

<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Heptane; C <sub>7</sub> H <sub>16</sub> ; 142-82-5	<b>ORIGINAL MEASUREMENTS:</b> Clever, H.L.; Battino, R.; Saylor, J.H.; Gross, P.M.  J. <u>Phys. Chem.</u> 1957, <u>61</u> , 1078-1083																								
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313.65	6.54	0.899	1.032																																						
T/K	Mol Fraction $X_1 \times 10^3$	$\Delta G^\circ/\text{J mol}^{-1}$																																							
288.15	7.48	11730																																							
293.15	7.27	12002																																							
298.15	7.07	12275																																							
303.15	6.88	12548																																							
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<b>VARIABLES:</b> T/K: 289.25 - 313.75 Total P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> P.L. Long																																								
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<p>COMPONENTS:</p> <p>1. Krypton; Kr; 7439-90-9</p> <p>2. Octane; C<sub>8</sub>H<sub>18</sub>; 111-65-9</p> <p>Decane; C<sub>10</sub>H<sub>22</sub>; 124-18-5</p>	<p>EVALUATOR:</p> <p>H. L. Clever  Chemistry Department  Emory University  Atlanta, GA 30322  U. S. A.</p> <p>October 1978</p>
<p>CRITICAL EVALUATION:</p> <p>Solubilities in the octane + krypton and decane + krypton systems were reported from three laboratories. Clever, Battino, Saylor and Gross (1) reported solubility values at three temperatures between 289 and 313 K. Both Makranczy, Megyery-Balog, Rusz and Patyi (2) and Wilcock, Battino, Danforth and Wilhelm (3) report one value at or very near 298.15 K.</p> <p>Octane + Krypton</p> <p>The solubility values of krypton in octane from the three laboratories at 298.15 K shows a range of values of 3.8 per cent. The value of Wilcock, <u>et al.</u> (3), determined with improved apparatus for degassing and solubility measurement, should be the most reliable value. However, since they report a solubility at only one temperature, we recommend as the tentative values the data of Clever, <u>et al.</u> (2) (Page 36) with the reservation that the smoothed value at 298.15 K may be about one percent high.</p> <p>Decane + Krypton</p> <p>The solubility values for krypton in decane at 298.15 K from the three laboratories shows a 4.3 per cent range. The average value from the three laboratories agrees within 0.2 per cent of the value of Clever, <u>et al.</u> (2). We recommend as the tentative solubility values the smoothed data of Clever, <u>et al.</u> (2) (Page 40). The single value of Wilcock, <u>et al.</u> (3) at 298.16 K is 2 per cent higher and may be the most reliable experimental value.</p> <p>REFERENCES</p> <ol style="list-style-type: none"> <li>1. Clever, H. L.; Battino, R.; Saylor, J. H.; Gross, P. M. <u>J. Phys. Chem.</u> 1957, <u>61</u>, 1078.</li> <li>2. Makranczy, J.; Megyery-Balog, K.; Rusz, L.; Patyi, L. <u>Hung. J. Ind. Chem.</u> 1976, <u>4</u>, 269.</li> <li>3. Wilcock, R. J.; Battino, R.; Danforth, W. F; Wilhelm, E. <u>J. Chem. Thermodyn.</u> 1978, <u>10</u>, 817.</li> </ol>	

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<p>VARIABLES:</p> <p>T/K: 298.15 P/kPa: 101.325 (1 atm)</p>	<p>PREPARED BY:</p> <p>S.A. Johnson</p>								
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<p>METHOD /APPARATUS/PROCEDURE:</p> <p>Volumetric method. The apparatus of Bodor, Bor, Mohai, and Sipos (1) was used.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>Both the gas and liquid were analytical grade reagents of Hungarian or foreign origin. No further information.</p>								
<p>APPARATUS/PROCEDURE:</p>	<p>ESTIMATED ERROR:</p> <p><math>\delta X_1/X_1 = 0.03</math></p> <p>REFERENCES:</p> <p>1. Bodor, E.; Bor, Gy.; Mohai, B.; Sipos, G. Veszpremi Vegyip. Egy. Kozl. 1957, 1, 55. Chem. Abstr. 1961, 55, 3175h.</p>								

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<b>VARIABLES:</b> T/K: 298.18 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b>  A.L. Cramer								
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<b>METHOD / APPARATUS / PROCEDURE:</b> <p>The solubility apparatus is based on the design of Morrison and Billett (1) and the version used is described by Battino, Evans, and Danforth (2). The degassing apparatus is that described by Battino, Banzhof, Bogan, and Wilhelm (3).</p> <p>Degassing. Up to 500 cm<sup>3</sup> of solvent is placed in a flask of such size that the liquid is about 4 cm deep. The liquid is rapidly stirred, and vacuum is applied intermittently through a liquid N<sub>2</sub> trap until the permanent gas residual pressure drops to 5 microns.</p> <p>Solubility Determination. The degassed solvent is passed in a thin film down a glass spiral tube containing solute gas plus the solvent vapor at a total pressure of one atm. The volume of gas absorbed is found by difference between the initial and final volumes in the buret system. The solvent is collected in a tared flask and weighed.</p>	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton. The Matheson Co., Inc., or Air Products and Chemicals. Purest commercially available.  2. Octane. Phillips Petroleum Co. 99 mol per cent minimum.								
<b>ESTIMATED ERROR:</b> $\delta T/K = 0.03$ $\delta P/\text{mmHg} = 0.5$ $\delta X_1/X_1 = 0.005$									
<b>REFERENCES:</b> 1. Morrison, T.J.; Billett, F. <u>J. Chem. Soc.</u> 1948, 2033. 2. Battino, R.; Evans, F.D.; Danforth, W.F. <u>J. Am. Oil Chem. Soc.</u> 1968, <u>45</u> , 830. 3. Battino, R.; Banzhof, M.; Bogan, M.; Wilhelm, E. <u>Anal. Chem.</u> 1971, <u>43</u> , 806.									



<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Krypton; Kr; 7439-90-9</li> <li>Nonane; C<sub>9</sub>H<sub>20</sub>; 111-84-2</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Clever, H.L.; Battino, R.; Saylor, J.H.; Gross, P.M.</p> <p><u>J. Phys. Chem.</u> 1957, <u>61</u>, 1078-1083.</p>																								
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<p>Smoothed Data: <math>\Delta G^\circ/\text{J mol}^{-1} = -RT \ln X_1 = -4544.4 + 56.358 T</math></p> <p>Std. Dev. <math>\Delta G^\circ = 14.0</math>, Coef. Corr. = 0.9998</p> <p><math>\Delta H^\circ/\text{J mol}^{-1} = -4544.4</math>, <math>\Delta S^\circ/\text{J K}^{-1} \text{ mol}^{-1} = -56.358</math></p>																									
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<p>APPARATUS/PROCEDURE:</p> <p>The apparatus is a modification of that of Morrison and Billett (1). The modifications include the addition of a spiral storage for the solvent, a manometer for a constant reference pressure, and an extra buret for highly soluble gases. The solvent is degassed by a modification of the method of Baldwin and Daniel (2).</p>	<p>ESTIMATED ERROR:</p> <p><math>\delta T/\text{K} = 0.05</math> <math>\delta P/\text{mmHg} = 3</math> <math>\delta X_1/X_1 = 0.03</math></p>																								
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<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Decane. C <sub>10</sub> H <sub>22</sub> ; 124-18-5	<b>ORIGINAL MEASUREMENTS:</b> Clever, H.L.; Battino, R.; Saylor, J.H.; Gross, P.M.  J. Phys. Chem. 1957, <u>61</u> , 1078-1083.																																								
<b>VARIABLES:</b> T/K: 289.75 - 313.35 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> P.L. Long																																								
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="336 504 1008 705"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th>Bunsen Coefficient α</th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>289.75</td> <td>7.59</td> <td>0.883</td> <td>0.937</td> </tr> <tr> <td>298.15</td> <td>7.22</td> <td>0.832</td> <td>0.908</td> </tr> <tr> <td>313.35</td> <td>6.53</td> <td>0.740</td> <td>0.849</td> </tr> </tbody> </table> <p>Smoothed Data: <math>\Delta G^\circ/\text{J mol}^{-1} = -RT \ln X_1 = -4853.9 + 57.311 T</math>            Std. Dev. <math>\Delta G^\circ = 8.9</math>, Coef. Corr. = 0.9999  <math>\Delta H^\circ/\text{J mol}^{-1} = -4853.9</math>, <math>\Delta S^\circ/\text{J K}^{-1} \text{ mol}^{-1} = -57.311</math></p> <table border="1" data-bbox="456 826 940 1108"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th><math>\Delta G^\circ/\text{J mol}^{-1}</math></th> </tr> </thead> <tbody> <tr> <td>288.15</td> <td>7.70</td> <td>11660</td> </tr> <tr> <td>293.15</td> <td>7.43</td> <td>11947</td> </tr> <tr> <td>298.15</td> <td>7.19</td> <td>12233</td> </tr> <tr> <td>303.15</td> <td>6.96</td> <td>12520</td> </tr> <tr> <td>308.15</td> <td>6.75</td> <td>12806</td> </tr> <tr> <td>313.15</td> <td>6.55</td> <td>13093</td> </tr> <tr> <td>318.15</td> <td>6.36</td> <td>13380</td> </tr> </tbody> </table> <p>The solubility values were adjusted to a partial pressure of krypton of 101.325 kPa (1 atm) by Henry's law.            The Bunsen coefficients were calculated by the compiler.</p>		T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	Bunsen Coefficient α	Ostwald Coefficient L	289.75	7.59	0.883	0.937	298.15	7.22	0.832	0.908	313.35	6.53	0.740	0.849	T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	$\Delta G^\circ/\text{J mol}^{-1}$	288.15	7.70	11660	293.15	7.43	11947	298.15	7.19	12233	303.15	6.96	12520	308.15	6.75	12806	313.15	6.55	13093	318.15	6.36	13380
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<b>METHOD / APPARATUS / PROCEDURE:</b> Solvent was degassed by a modification of the method of Baldwin and Daniel (1). Saturation apparatus was that of Morrison and Billett (2), modified to include spiral storage for the solvent, a manometer for constant reference pressure, and an extra buret. Solvent was saturated with gas as it flowed through an 8 mm x 180 cm glass spiral attached to a buret.  For an evaluation of the krypton + decane system see page 35.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton. Linde Air Products Co. Pure. 2. Decane. Humphrey-Wilkinson, Inc. Shaken with H <sub>2</sub> SO <sub>4</sub> , washed, dried over Na.  <b>ESTIMATED ERROR:</b> $\delta T/\text{K} = 0.05$ $\delta P/\text{mmHg} = 3$ $\delta X_1/X_1 = 0.03$  <b>REFERENCES:</b> 1. Baldwin, R.R.; Daniel, S.G. J. Appl. Chem. 1952, <u>2</u> , 161. 2. Morrison, T.J.; Billett, F. J. Chem. Soc. 1948, 2033; <u>ibid.</u> 1952, 3819.																																								

<p>COMPONENTS:</p> <p>1. Krypton; Kr; 7439-90-9</p> <p>2. Decane; C<sub>10</sub>H<sub>22</sub>; 124-18-5</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Makranczy, J.; Megyery-Balog, K.; Rusz, L.; Patyi, L.</p> <p><u>Hung. J. Ind. Chem.</u> 1976, <u>4</u>, 269-280.</p>								
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<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="323 498 993 632"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>7.05</td> <td>0.812</td> <td>0.886</td> </tr> </tbody> </table> <p>The mole fraction and Bunsen coefficient were calculated by the compiler.</p> <p>See the evaluation of the krypton + decane system on page 35 for the recommended Gibbs energy equation and smoothed solubility values.</p>		T/K	Mol Fraction $X_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	298.15	7.05	0.812	0.886
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<p>VARIABLES:</p> <p>T/K: 298.16 P/kPa: 101.325 (1 atm)</p>	<p>PREPARED BY:</p> <p>A. L. Cramer</p>								
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<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Undecane; C <sub>11</sub> H <sub>24</sub> ; 1120-21-4	<b>ORIGINAL MEASUREMENTS:</b> Makranczy, J.; Megyery-Balog, K.; Rusz, L.; Patyi, L.  <u>Hung. J. Ind. Chem.</u> 1976, <u>4</u> , 269-280.								
<b>VARIABLES:</b> T/K: 298.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> S.A. Johnson								
<b>EXPERIMENTAL VALUES:</b>  <table border="1" data-bbox="175 546 1112 713"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>7.10</td> <td>0.756</td> <td>0.825</td> </tr> </tbody> </table>  The mole fraction and Bunsen coefficient were calculated by the compiler.		T/K	Mol Fraction $x_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	298.15	7.10	0.756	0.825
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<b>APPARATUS/PROCEDURE:</b> The apparatus is a modification of the apparatus of Morrison and Billett (1). The modifications include the addition of a helical storage for the solvent, a manometer for a reference pressure, and an extra buret for highly soluble gases. The solvent is degassed by a modification of the method of Baldwin and Daniel (2).	<b>ESTIMATED ERROR:</b> $\delta T/K = 0.05$ $\delta P/\text{mmHg} = 3$ $\delta X_1/X_1 = 0.03$  <b>REFERENCES:</b> 1. Morrison, T.J.; Billett, F. <u>J. Chem. Soc.</u> 1948, 2033; <u>ibid.</u> 1952, 3819. 2. Baldwin, R.R.; Daniel, S.G. <u>J. Appl. Chem.</u> 1952, <u>2</u> , 161.																																					

<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Dodecane; C <sub>12</sub> H <sub>26</sub> ; 112-40-3	<b>ORIGINAL MEASUREMENTS:</b> Steinberg, M.; Manowitz, B.  <u>Ind. Eng. Chem.</u> 1959, <u>51</u> , 47-51.								
<b>VARIABLES:</b> T/K: 298.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> H.L. Clever A.L. Cramer								
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="312 504 985 624"> <thead> <tr> <th>T/K</th> <th>Mol Fraction x<sub>1</sub> x 10<sup>3</sup></th> <th>Bunsen Coefficient α</th> <th>Absorption Coefficient β</th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>7.8</td> <td>0.78</td> <td>0.82</td> </tr> </tbody> </table> <p>The authors define the Absorption coefficient as the volume of gas, corrected to 288.15 K and 101.325 kPa, absorbed under a total system pressure of 101.325 kPa per unit volume of solvent at 288.15 K.</p> <p>The mole fraction solubilities and Bunsen coefficients were calculated by the compiler.</p> <p>For an evaluation note on the krypton + dodecane system see page 44.</p>		T/K	Mol Fraction x <sub>1</sub> x 10 <sup>3</sup>	Bunsen Coefficient α	Absorption Coefficient β	298.15	7.8	0.78	0.82
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<b>AUXILIARY INFORMATION</b>									
<b>METHOD /APPARATUS/PROCEDURE:</b> Absorption coefficient determined by a modified McDaniel method (1).	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton. Technical grade. The Matheson Co. 2. Dodecane. Technically or chemically pure.  <b>ESTIMATED ERROR:</b> $\delta\beta/\beta = 0.05 - 0.10$  <b>REFERENCES:</b> 1. Furman, N.H. "Scott's Standard Methods of Chemical Analysis" Van Nostrand Co., NY, 1939, 5th ed., Vol. II, p. 2587.								

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<b>VARIABLES:</b> T/K: 298.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> S.A. Johnson								
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<b>AUXILIARY INFORMATION</b>									
<b>METHOD /APPARATUS/PROCEDURE:</b> Volumetric method. The apparatus of Bodor, Bor, Mohai, and Sipos (1) was used.	<b>SOURCE AND PURITY OF MATERIALS:</b> Both the gas and liquid were analytical grade reagents of Hungarian or foreign origin. No further information.  <b>ESTIMATED ERROR:</b> $\delta X_1 / X_1 = 0.03$  <b>REFERENCES:</b> 1. Bodor, E.; Bor, Gy.; Mohai, B.; Sipos, G. <u>Veszpremi Vegyip. Egy. Kozl.</u> 1957, <u>1</u> , 55. <u>Chem. Abstr.</u> 1961, <u>55</u> , 3175h.								



<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Tridecane; C <sub>13</sub> H <sub>28</sub> ; 629-50-5	<b>ORIGINAL MEASUREMENTS:</b> Makranczy, J.; Megyery-Balog, K.; Rusz, L.; Patyi, L.  <u>Hung. J. Ind. Chem.</u> 1976, 4, 269-280.								
<b>VARIABLES:</b> T/K: 298.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> S.A. Johnson								
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="164 516 1125 685"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>6.96</td> <td>0.641</td> <td>0.700</td> </tr> </tbody> </table> <p>The mole fraction and Bunsen coefficient were calculated by the compiler.</p>		T/K	Mol Fraction $x_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	298.15	6.96	0.641	0.700
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<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Tetradecane; C <sub>14</sub> H <sub>30</sub> ; 629-59-4	<b>ORIGINAL MEASUREMENTS:</b> Clever, H.L.; Battino, R.; Saylor, J.H.; Gross, P.M.  <u>J. Phys. Chem.</u> 1957, <u>61</u> , 1078-1083.																								
<b>VARIABLES:</b> T/K: 289.15 - 313.45 Total P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> P.L. Long																								
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<b>APPARATUS/PROCEDURE:</b> The apparatus is a modification of that of Morrison and Billett (1). The modifications include the addition of a spiral storage for the solvent, a manometer for a constant reference pressure, and an extra buret for highly soluble gases. The solvent is degassed by a modification of the method of Baldwin and Daniel (2).	<b>ESTIMATED ERROR:</b> $\delta T / K = 0.05$ $\delta P / \text{mmHg} = 3$ $\delta X_1 / X_1 = 0.03$																								
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<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Pentadecane; C <sub>15</sub> H <sub>32</sub> ; 629-62-9 or Hexadecane; C <sub>16</sub> H <sub>34</sub> ; 544-76-3	<b>ORIGINAL MEASUREMENTS:</b> Makranczy, J.; Megyery-Balog, K.; Ruzs, L.; Patyi, L.  <u>Hung. J. Ind. Chem.</u> 1976, <u>4</u> , 269-280.																				
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<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="153 532 1141 878"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td colspan="4" style="text-align: center;">Pentadecane; C<sub>15</sub>H<sub>32</sub>; 629-62-9</td> </tr> <tr> <td>298.15</td> <td>7.04</td> <td>0.573</td> <td>0.625</td> </tr> <tr> <td colspan="4" style="text-align: center;">Hexadecane; C<sub>16</sub>H<sub>34</sub>; 544-76-3</td> </tr> <tr> <td>298.15</td> <td>6.96</td> <td>0.534</td> <td>0.583</td> </tr> </tbody> </table> <p data-bbox="98 1017 1155 1045">The mole fraction and Bunsen coefficient were calculated by the compiler.</p>		T/K	Mol Fraction $x_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	Pentadecane; C <sub>15</sub> H <sub>32</sub> ; 629-62-9				298.15	7.04	0.573	0.625	Hexadecane; C <sub>16</sub> H <sub>34</sub> ; 544-76-3				298.15	6.96	0.534	0.583
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<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Propene; C <sub>3</sub> H <sub>6</sub> ; 74-98-6			<b>ORIGINAL MEASUREMENTS:</b> Orobinsky, N. A., Blagoy, Yu. P. and Semyannikova, E. L., <i>Ukr. Fiz. Zhur.</i> , <u>1968</u> , 13, 372.		
<b>VARIABLES:</b> Temperature, pressure			<b>PREPARED BY:</b> C. L. Young		
<b>EXPERIMENTAL VALUES:</b>					
T/K	P/bar	Mole fraction of krypton in liquid, $x_{Kr}$	T/K	P/bar	Mole fraction of krypton in liquid, $x_{Kr}$
130	1.10	0.291	150	4.95	0.669
	1.30	0.417		5.34	0.763
	1.47	0.530		5.83	0.854
	1.64	0.663		5.98	0.873
	1.81	0.784		6.28	0.958
	1.91	0.865	160	2.40	0.133
	1.96	0.925		2.57	0.147
140	1.11	0.121		4.30	0.302
	1.32	0.177		4.69	0.345
	1.89	0.355		5.42	0.411
	2.37	0.426		6.23	0.503
	2.55	0.506		6.96	0.578
	2.82	0.569		7.45	0.635
	3.06	0.679		8.92	0.820
	3.29	0.785		9.32	0.889
	3.33	0.785		9.66	0.935
	3.51	0.887	170	2.70	0.103
	3.73	0.948		5.52	0.278
150	1.91	0.172		7.13	0.387
	2.89	0.310		8.48	0.455
	3.46	0.378		9.12	0.474
	3.66	0.425		9.84	0.550
	4.10	0.515		10.59	0.588
	4.63	0.605		13.53	0.828
	4.83	0.667		14.22	0.904
<b>AUXILIARY INFORMATION</b>					
<b>METHOD/APPARATUS/PROCEDURE:</b> Recirculating vapor flow apparatus fitted with magnetic pump. Temperature measured with platinum resistance thermometer; pressure measured with Bourdon gauge. Samples of liquid phase analysed by gas chromatography.			<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Sample purity 99.97 mole per cent. 2. Purified sample contained about 0.02 mole per cent nitrogen, oxygen and carbon dioxide and less than 0.5 mole per cent hydrocarbon impurity.		
			<b>ESTIMATED ERROR:</b> $\delta T/K = \pm 0.03$ ; $\delta P/\text{bar} = \pm 0.4\%$ $\delta x_{Kr} = \pm 0.5\%$ .		
			<b>REFERENCES:</b>		

## COMPONENTS:

- (1) Krypton; Kr; 7439-90-9  
 (2) Propene; C<sub>3</sub>H<sub>6</sub>; 74-98-6

## ORIGINAL MEASUREMENTS:

Orobinsky, N. A., Blagoy, Yu. P.  
 and Semyarnikova, E. L., *Ukr. Fiz.*  
*Zhur.*, 1968, 13, 372.

## EXPERIMENTAL VALUES:

T/K	P/bar	Mole fraction of krypton in liquid, $x_{Kr}$	T/K	P/bar	Mole fraction of krypton in liquid, $x_{Kr}$	
180	2.78	0.086	190	11.13	0.307	
	3.66	0.110		14.42	0.403	
	6.62	0.234		16.5	0.477	
	9.12	0.355		17.3	0.510	
	10.84	0.404		21.5	0.656	
	12.61	0.495		22.8	0.724	
	14.42	0.579		23.5	0.760	
	14.57	0.590		200	4.90	0.097
	17.46	0.744			7.97	0.160
	17.7	0.769			12.32	0.255
	18.3	0.799			16.5	0.333
	19.3	0.865			17.8	0.351
	19.3	0.865			23.3	0.503
190	2.78	0.063	29.4	0.693		
	7.33	0.189				

COMPONENTS:	EVALUATOR:																								
1. Krypton; Kr; 7439-90-9 2. Cyclohexane; C <sub>6</sub> H <sub>12</sub> ; 110-82-7	H.L. Clever Chemistry Department Emory University Atlanta, GA 30322 U.S.A.																								
<p><b>CRITICAL EVALUATION:</b>            The solubility of krypton in cyclohexane at 101.325 kPa was measured in two laboratories. Clever, Battino, Saylor and Gross (1) report three values between 289.15 and 313.65 K. Dymond (2) reports four values between 293.50 and 309.35 K. Each data set was fitted to a Gibbs energy equation linear in temperature by the method of least squares. The smoothed data agreed within 1.7 per cent at 293.15 K and 0.5 per cent at 313.15 K, with the Dymond solubility values being the higher values over the temperature range. The two data sets agree well within experimental error.</p> <p>The seven solubility values from the two laboratories were combined and fitted to a Gibbs energy equation linear in temperature by the method of least squares to obtain the recommended equation.</p> <p>The recommended thermodynamic values for the transfer of krypton from the gas at 101.325 kPa (1 atm) to the hypothetical unit mole fraction solution are</p> $\Delta G^{\circ}/J \text{ mol}^{-1} = -RT \ln X_1 = -3,576.0 + 56.557 T$ $\text{Std. Dev. } \Delta G^{\circ} = 15, \text{ Coef. Corr.} = 0.9995$ $\Delta H^{\circ}/J \text{ mol}^{-1} = -3,576.0, \Delta S^{\circ}/J \text{ K}^{-1} \text{ mol}^{-1} = -56.557$ <p>The recommended values of the mole fraction solubility at 101.325 kPa and the Gibbs energy of solution as a function of temperature are given in Table 1.</p>																									
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<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>1. Krypton; Kr; 7439-90-9</li> <li>2. Cyclohexane; C<sub>6</sub>H<sub>12</sub>; 110-82-7</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Clever, H.L.; Battino, R.; Saylor, J.H.; Gross, P.M.</p> <p><u>J. Phys. Chem.</u> 1957, <u>61</u>, 1078-1083.</p>																
<p>VARIABLES:</p> <p>T/K: 289.15 - 313.65 P/kPa: 101.325 (1 atm)</p>	<p>PREPARED BY:</p> <p>P.L. Long</p>																
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="319 498 998 691"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>289.15</td> <td>4.98</td> <td>1.021</td> <td>1.081</td> </tr> <tr> <td>298.15</td> <td>4.67</td> <td>0.967</td> <td>1.055</td> </tr> <tr> <td>313.65</td> <td>4.36</td> <td>0.885</td> <td>1.016</td> </tr> </tbody> </table> <p>Smoothed Data: <math>\Delta G^\circ = -RT \ln x_1 = -3465.1 + 56.239 T</math> Std. Dev. <math>\Delta G^\circ = 0.6</math>, Coef. Corr. = .9999</p> <p>For an evaluation of the krypton + cyclohexane system see page 53 with a recommendation of a Gibbs energy equation and solubility values.</p> <p>The solubility values were adjusted to a partial pressure of krypton of 101.325 kPa (1 atm) by Henry's law. The Bunsen coefficients were calculated by the compiler.</p>		T/K	Mol Fraction $x_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	289.15	4.98	1.021	1.081	298.15	4.67	0.967	1.055	313.65	4.36	0.885	1.016
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<p>AUXILIARY INFORMATION</p>																	
<p>METHOD / APPARATUS / PROCEDURE:</p> <p>Solvent was degassed by a modification of the method of Baldwin and Daniel (1). Saturation apparatus was that of Morrison and Billett (2), modified to include spiral storage for the solvent, a manometer for constant reference pressure, and an extra buret. Solvent was saturated with gas as it flowed through an 8mm x 180 cm glass spiral attached to a buret.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>1. Krypton. Linde Air Products Co. Pure.</li> <li>2. Cyclohexane. Phillips Petroleum Co. Used as received.</li> </ol> <p>ESTIMATED ERROR:</p> <p><math>\delta T/K = 0.05</math> <math>\delta P/\text{mmHg} = 3</math> <math>\delta x_1/x_1 = 0.03</math></p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>1. Baldwin, R.R.; Daniel, S.G. <u>J. Appl. Chem.</u> 1952, <u>2</u>, 161.</li> <li>2. Morrison, T.J.; Billett, F. <u>J. Chem. Soc.</u> 1948, 2033; <u>ibid.</u> 1952, 3819.</li> </ol>																

<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Cyclohexane; C <sub>6</sub> H <sub>12</sub> ; 110-82-7	<b>ORIGINAL MEASUREMENTS:</b> Dymond, J. H.  <u>J. Phys. Chem.</u> 1967, <u>71</u> , 1829 - 1831.																				
<b>VARIABLES:</b> T/K: 293.50 - 309.35 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> M. E. Derrick																				
<b>EXPERIMENTAL VALUES:</b>  <table border="1" data-bbox="336 540 1094 735"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> x 10<sup>3</sup></th> <th>Bunsen Coefficient α</th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>293.50</td> <td>4.85</td> <td>1.01</td> <td>1.08</td> </tr> <tr> <td>298.15</td> <td>4.73</td> <td>0.979</td> <td>1.07</td> </tr> <tr> <td>304.75</td> <td>4.57</td> <td>0.939</td> <td>1.05</td> </tr> <tr> <td>309.35</td> <td>4.47</td> <td>0.909</td> <td>1.03</td> </tr> </tbody> </table> <p data-bbox="134 756 1012 836">           Smoothed Data: <math>\Delta G^\circ/\text{J mol}^{-1} = -RT \ln X_1 = -3893.4 + 57.572 T</math>            Std. Dev. <math>\Delta G^\circ = 0.8</math>,      Coef. Corr. = 0.9999         </p> <p data-bbox="134 876 1145 977">           See the evaluation of krypton + cyclohexane for the recommended Gibbs energy equation and smoothed solubility values.            The Bunsen and Ostwald coefficients were calculated by the compiler.         </p>		T/K	Mol Fraction X <sub>1</sub> x 10 <sup>3</sup>	Bunsen Coefficient α	Ostwald Coefficient L	293.50	4.85	1.01	1.08	298.15	4.73	0.979	1.07	304.75	4.57	0.939	1.05	309.35	4.47	0.909	1.03
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<b>AUXILIARY INFORMATION</b>																					
<b>METHOD:</b> Saturation of liquid with gas at partial pressure of gas equal to 1 atm.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton. Matheson Co., dried. 2. Cyclohexane. Matheson, Coleman, and Bell, chromatography reagent. Dried and fractionally frozen. m.p. 6.45° C.																				
<b>APPARATUS/PROCEDURE:</b> Dymond-Hildebrand apparatus (1) using an all-glass pumping system to spray slugs of degassed solvent into the gas. Amount of gas dissolved calculated from initial and final gas pressures.	<b>ESTIMATED ERROR:</b> $\delta X_1/X_1 = 0.01$  <b>REFERENCES:</b> 1. Dymond, J.; Hildebrand, J. H. <u>Ind. Eng. Chem. Fundam.</u> 1967, <u>6</u> , 130.																				



<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Methylcyclohexane; C <sub>7</sub> H <sub>14</sub> ; 108-87-2	<b>ORIGINAL MEASUREMENTS:</b> Clever, H.L.; Saylor, J.H.; Gross, P.M.  J. <u>Phys. Chem.</u> 1958, <u>62</u> , 89-91.																																								
<b>VARIABLES:</b> T/K: 289.15 - 316.25 Total P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> P.L. Long																																								
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="305 498 981 687"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>289.15</td> <td>6.14</td> <td>1.086</td> <td>1.15</td> </tr> <tr> <td>303.15</td> <td>5.56</td> <td>0.971</td> <td>1.078</td> </tr> <tr> <td>316.25</td> <td>5.02</td> <td>0.863</td> <td>0.999</td> </tr> </tbody> </table> <p>Smoothed Data: <math>\Delta G^\circ/J \text{ mol}^{-1} = -RT \ln X_1 = -5652.1 + 61.865 T</math>            Std. Dev. <math>\Delta G^\circ = 13.5</math>, Coef. Corr. = 0.9999  <math>\Delta H^\circ/J \text{ mol}^{-1} = -5652.1</math>, <math>\Delta S^\circ/J \text{ K}^{-1} \text{ mol}^{-1} = -61.865</math></p> <table border="1" data-bbox="425 817 907 1089"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^3</math></th> <th><math>\Delta G^\circ/J \text{ mol}^{-1}</math></th> </tr> </thead> <tbody> <tr> <td>288.15</td> <td>6.21</td> <td>12,174</td> </tr> <tr> <td>293.15</td> <td>5.96</td> <td>12,484</td> </tr> <tr> <td>298.15</td> <td>5.74</td> <td>12,793</td> </tr> <tr> <td>303.15</td> <td>5.53</td> <td>13,102</td> </tr> <tr> <td>308.15</td> <td>5.33</td> <td>13,412</td> </tr> <tr> <td>313.15</td> <td>5.14</td> <td>13,721</td> </tr> <tr> <td>318.15</td> <td>4.97</td> <td>14,030</td> </tr> </tbody> </table> <p>The solubility values were adjusted to a partial pressure of krypton of 101.325 kPa (1 atm) by Henry's law.            The Bunsen coefficients were calculated by the compiler.</p>		T/K	Mol Fraction $X_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	289.15	6.14	1.086	1.15	303.15	5.56	0.971	1.078	316.25	5.02	0.863	0.999	T/K	Mol Fraction $X_1 \times 10^3$	$\Delta G^\circ/J \text{ mol}^{-1}$	288.15	6.21	12,174	293.15	5.96	12,484	298.15	5.74	12,793	303.15	5.53	13,102	308.15	5.33	13,412	313.15	5.14	13,721	318.15	4.97	14,030
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<b>METHOD:</b> Volumetric. The apparatus (1) is a modification of that used by Morrison and Billett (2). Modifications include the addition of a spiral solvent storage tubing, a manometer for constant reference pressure, and an extra gas buret for highly soluble gases.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton. Matheson Co., Inc. Both standard and research grades were used. 2. Methylcyclohexane. Eastman Kodak Co., white label. Dried over Na and distilled; corrected b.p. 100.95 to 100.97°, lit. b.p. 100.93°C.																																								
<b>APPARATUS/PROCEDURE:</b> (a) Degassing. 700 ml of solvent is shaken and evacuated while attached to a cold trap, until no bubbles are seen; solvent is then transferred through a 1 mm capillary tubing, released as a fine mist into a continuously evacuated flask. (b) Solvent is saturated with gas as it flows through 8 mm x 180 cm of tubing attached to a gas buret. Pressure is maintained at 1 atm as the gas is absorbed.	<b>ESTIMATED ERROR:</b> $\delta T/K = 0.05$ $\delta P/\text{mmHg} = 3$ $\delta X_1/X_1 = 0.03$  <b>REFERENCES:</b> 1. Clever, H.L.; Battino, R.; Saylor, J.H.; Gross, P.M. <u>J. Phys. Chem.</u> 1957, <u>61</u> , 1078. 2. Morrison, T.J.; Billett, F. <u>J. Chem. Soc.</u> 1948, 2033; <u>ibid.</u> 1952, 3819.																																								

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>1. Krypton; Kr; 7439-90-9</li> <li>2. Cyclooctane; C<sub>8</sub>H<sub>16</sub>; 292-64-8</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Wilcock, R.J.; Battino, R.; Wilhelm, E.</p> <p><u>J. Chem. Thermodyn.</u> 1977, <u>9</u>, 111-115.</p>								
<p>VARIABLES:</p> <p>T/K: 298.26 P/kPa: 101.325</p>	<p>PREPARED BY:</p> <p>H.L. Clever</p>								
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="375 512 1064 683"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>298.26</td> <td>3.442</td> <td>0.5727</td> <td>0.6254</td> </tr> </tbody> </table> <p>The solubility values were adjusted to a partial pressure of krypton of 101.325 kPa (1 atm) by Henry's law. The Bunsen coefficients were calculated by the compiler.</p>		T/K	Mol Fraction $X_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	298.26	3.442	0.5727	0.6254
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<p>METHOD/APPARATUS/PROCEDURE:</p> <p>The apparatus is based on the design by Morrison and Billett (1) and the version used is described by Battino, Evans, and Danforth (2). Degassing. Up to 500 cm<sup>3</sup> of solvent is placed in a flask of such size that the liquid is about 4 cm deep. The liquid is rapidly stirred and vacuum is applied intermittently through a liquid N<sub>2</sub> trap until the permanent gas residual pressure drops to 5 microns. Solubility Determination. The degassed solvent passes in a thin film down a glass spiral containing the solute gas and solvent vapor at a total pressure of one atm. The volume of gas absorbed is measured in the attached gas buret, and the solvent is collected in a tared flask and weighed.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>1. Krypton. Matheson Co., Inc. Minimum purity 99.995 mol per cent.</li> <li>2. Cyclooctane. Chemical Samples Co. 99 mol per cent, fractionally distilled, <math>n(\text{Na D}, 298.15 \text{ K}) = 1.4562</math>.</li> </ol> <p>ESTIMATED ERROR:</p> <p><math>\delta T/K = 0.03</math> <math>\delta P/\text{mmHg} = 0.5</math> <math>\delta X_1/X_1 = 0.03</math></p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>1. Morrison, T.J.; Billett, F. <u>J. Chem. Soc.</u> 1948, 2033.</li> <li>2. Battino, R.; Evans, F.D.; Danforth, W.F. <u>J. Am. Oil Chem. Soc.</u> 1968, <u>45</u>, 830.</li> </ol>								

<p>COMPONENTS:</p> <p>1. Krypton; Kr; 7439-90-9</p> <p>2. <i>cis</i>-1,2-Dimethylcyclohexane; C<sub>8</sub>H<sub>16</sub>; 2207-01-4</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Geller, E.B.; Battino, R.; Wilhelm, E.</p> <p><i>J. Chem. Thermodyn.</i> 1976, <b>8</b>, 197-202.</p>								
<p>VARIABLES:</p> <p>T/K: 297.92 P/kPa: 101.325 (1 atm)</p>	<p>PREPARED BY:</p> <p>H.L. Clever</p>								
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<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. <u>trans</u> -1,2-Dimethylcyclohexane; $C_8H_{16}$ ; 6876-23-9	<b>ORIGINAL MEASUREMENTS:</b> Geller, E.B.; Battino, R.; Wilhelm, E.  <u>J. Chem. Thermodyn.</u> 1976, <u>8</u> , 197-202.								
<b>VARIABLES:</b> T/K: 297.91 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> H.L. Clever								
<b>EXPERIMENTAL VALUES:</b>  <table border="1" data-bbox="371 518 1048 687"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>297.91</td> <td>5.972</td> <td>0.9270</td> <td>1.011</td> </tr> </tbody> </table> The solubility values were adjusted to a partial pressure of krypton of 101.325 kPa (1 atm) by Henry's law. The Bunsen coefficients were calculated by the compiler.		T/K	Mol Fraction $x_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	297.91	5.972	0.9270	1.011
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<b>METHOD / APPARATUS / PROCEDURE:</b> The apparatus is based on the design by Morrison and Billett (1) and the version used is described by Battino, Evans, and Danforth (2). See krypton + 1,2 dimethylcyclohexane data sheet for more detail.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton. Either Air Products & Chemicals Inc., or Matheson Co., Inc., 99 mol % or better. 2. <u>trans</u> -1,2-Dimethylcyclohexane. Chemical Samples Co., fractionally distilled and stored in dark. $n_D(298.15)$ 1.4248.  <b>ESTIMATED ERROR:</b> $\delta T/K = 0.03$ $\delta P/mmHg = 0.5$ $\delta x_1/x_1 = 0.02$  <b>REFERENCES:</b> 1. Morrison, T.J.; Billett, F. <u>J. Chem. Soc.</u> 1948, 2033. 2. Battino, R.; Evans, F.D.; Danforth, W.F. <u>J. Am. Oil Chem. Soc.</u> 1968, <u>45</u> , 830.								

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>1. Krypton; Kr; 7439-90-9</li> <li>2. <u>cis</u>-1,3-Dimethylcyclohexane, 59 mol %; C<sub>8</sub>H<sub>16</sub>; 638-04-0</li> <li>3. <u>trans</u>-1,3-Dimethylcyclohexane, 41 mol %; C<sub>8</sub>H<sub>16</sub>; 2207-03-6</li> </ol>	<p>ORIGINAL MEASUREMENTS: Geller, E.B.; Battino, R.; Wilhelm, E.</p> <p><u>J. Chem. Thermodyn.</u> 1976, <u>8</u>, 197-202.</p>								
<p>VARIABLES:</p> <p>T/K: 298.21 P/kPa: 101.325 (1 atm)</p>	<p>PREPARED BY:</p> <p>H.L. Clever</p>								
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<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. <u>cis</u> -1,4-Dimethylcyclohexane, 70 mol %; C <sub>8</sub> H <sub>16</sub> ; 624-29-3 3. <u>trans</u> -1,4-Dimethylcyclohexane, 30 mol %; C <sub>8</sub> H <sub>16</sub> ; 2207-04-7	<b>ORIGINAL MEASUREMENTS:</b> Geller, E.B.; Battino, R.; Wilhelm, E.  <u>J. Chem. Thermodyn.</u> 1976, <u>8</u> , 197-202.								
<b>VARIABLES:</b> T/K: 298.35 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b>  H.L. Clever								
<b>EXPERIMENTAL VALUES:</b>  <table border="1" data-bbox="374 546 1044 717"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>298.35</td> <td>6.005</td> <td>0.9320</td> <td>1.018</td> </tr> </tbody> </table> <p>The solubility value was adjusted to a partial pressure of krypton of 101.325 kPa (1 atm) by Henry's law.</p> <p>The Bunsen coefficient was calculated by the compiler.</p>		T/K	Mol Fraction $X_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	298.35	6.005	0.9320	1.018
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<b>METHOD/APPARATUS/PROCEDURE:</b>  The apparatus is based on the design by Morrison and Billett (1) and the version used is described by Battino, Evans, and Danforth (2). See krypton + 1,2 dimethylcyclohexane data sheet for more detail.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton. Either Air Products & Chemicals, Inc., or Matheson Co., Inc. 99 mol % or better. 2. <u>cis</u> -1,4-Dimethylcyclohexane. Chemical Samples Co., binary mixture, analysed by R. I. by authors, used as received. 3. <u>trans</u> -1,4-Dimethylcyclohexane. Chemical Samples Co., binary mixture, analysed by R. I. by authors, used as received.  <b>ESTIMATED ERROR:</b> $\delta T/K = 0.03$ $\delta P/mmHg = 0.5$ $\delta X_1/X_1 = 0.02$  <b>REFERENCES:</b> 1. Morrison, T.J.; Billett, F. <u>J. Chem. Soc.</u> 1948, 2033. 2. Battino, R.; Evans, F.D.; Danforth, W.F. <u>J. Am. Oil Chem. Soc.</u> 1968, <u>45</u> , 830.								

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Krypton; Kr; 7439-90-9</li> <li>1,2,3,4-Tetrahydronaphthalene (Tetralin); C<sub>10</sub>H<sub>12</sub>; 119-64-2</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Körösy, F.</p> <p><u>Trans. Faraday Soc.</u> 1937, <u>33</u>, 416-425.</p>								
<p>VARIABLES:</p> <p>T/K: 297.15 P/kPa: 101.325 (1 atm)</p>	<p>PREPARED BY:</p> <p>H.L. Clever</p>								
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="322 512 991 671"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>297.15</td> <td>2.7</td> <td>0.45</td> <td>0.49</td> </tr> </tbody> </table> <p>The mole fraction solubility and the Bunsen coefficient were calculated by the compiler. It was assumed that gas behavior is ideal, the Ostwald coefficient is independent of pressure, and that Henry's law is obeyed.</p>		T/K	Mol Fraction $X_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	297.15	2.7	0.45	0.49
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<p>METHOD:</p> <p>The apparatus and method of Winkler (1) were used. However, the apparatus was usually not thermostated, and degassing was by evacuating and shaking the solvent, not by evacuating and boiling the solvent as was done by Winkler.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>Krypton. Source not given. The gas contained 5% xenon and 1% non-inert gases.</li> <li>1,2,3,4-Tetrahydronaphthalene. No information.</li> </ol>								
<p>APPARATUS/PROCEDURE:</p>	<p>ESTIMATED ERROR:</p> $\delta X_1 / X_1 = 0.05$ <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>Winkler, L.W. <u>Ber.</u> 1891, <u>24</u>, 89.</li> </ol>								

<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Benzene; C <sub>6</sub> H <sub>6</sub> ; 71-43-2	<b>ORIGINAL MEASUREMENTS:</b> Clever, H.L.; Battino, R.; Saylor, J.H.; Gross, P.M.  <u>J. Phys. Chem.</u> 1957, <u>61</u> , 1078-1083.																																								
<b>VARIABLES:</b> T/K: 289.35 - 313.45 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> P.L. Long																																								
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="367 524 1045 711"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>289.35</td> <td>2.81</td> <td>0.714</td> <td>0.756</td> </tr> <tr> <td>298.35</td> <td>2.73</td> <td>0.685</td> <td>0.748</td> </tr> <tr> <td>313.45</td> <td>2.64</td> <td>0.654</td> <td>0.750</td> </tr> </tbody> </table> <p>Smoothed Data: <math>\Delta G^\circ/\text{J mol}^{-1} = -RT \ln x_1 = -1926.5 + 55.517 T</math>            Std. Dev. <math>\Delta G^\circ = 6.2</math>, Coef. Corr. = .9999  <math>\Delta H^\circ/\text{J mol}^{-1} = -1926.5</math>, <math>\Delta S^\circ/\text{J K}^{-1} \text{ mol}^{-1} = -55.517</math></p> <table border="1" data-bbox="485 842 971 1109"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^3</math></th> <th><math>\Delta G^\circ/\text{J mol}^{-1}</math></th> </tr> </thead> <tbody> <tr> <td>288.15</td> <td>2.81</td> <td>14071</td> </tr> <tr> <td>293.15</td> <td>2.78</td> <td>14348</td> </tr> <tr> <td>298.15</td> <td>2.74</td> <td>14626</td> </tr> <tr> <td>303.15</td> <td>2.70</td> <td>14903</td> </tr> <tr> <td>308.15</td> <td>2.67</td> <td>15181</td> </tr> <tr> <td>313.15</td> <td>2.64</td> <td>15458</td> </tr> <tr> <td>318.15</td> <td>2.61</td> <td>15736</td> </tr> </tbody> </table> <p>The solubility values were adjusted to a partial pressure of krypton of 101.325 kPa (1 atm) by Henry's law.            The Bunsen coefficients were calculated by the compiler.</p>		T/K	Mol Fraction $x_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	289.35	2.81	0.714	0.756	298.35	2.73	0.685	0.748	313.45	2.64	0.654	0.750	T/K	Mol Fraction $x_1 \times 10^3$	$\Delta G^\circ/\text{J mol}^{-1}$	288.15	2.81	14071	293.15	2.78	14348	298.15	2.74	14626	303.15	2.70	14903	308.15	2.67	15181	313.15	2.64	15458	318.15	2.61	15736
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<b>METHOD / APPARATUS / PROCEDURE:</b> Solvent was degassed by a modification of the method of Baldwin and Daniel (1). Saturation apparatus was that of Morrison and Billett (2), modified to include spiral storage for the solvent, a manometer for constant reference pressure, and an extra buret. Solvent was saturated with gas as it flowed through an 8 mm x 180 cm glass spiral attached to a buret.  NOTE: F. Körösy <u>Trans. Faraday Soc.</u> 1937, <u>33</u> , 416 reports an Ostwald coefficient of 0.97 (mole fraction $3.55 \times 10^{-3}$ ) at 295.15 K. Van Liempt and van Wijk <u>Recl. trav. Chim. Pays-Bas</u> 1937, <u>56</u> , 632 report a Bunsen coefficient of 0.67 (mole fraction $2.65 \times 10^{-3}$ ) at 292.15 K. Neither of the solubility of krypton in benzene values were considered in the smoothed data fit given above.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton. Linde Air Products Co. Pure. 2. Benzene. Jones & Laughlin Steel Co. Shaken with H <sub>2</sub> SO <sub>4</sub> , water washed, dried over Na, distilled.  <b>ESTIMATED ERROR:</b> $\delta T/K = 0.05$ $\delta P/\text{mmHg} = 3$ $\delta x_1/x_1 = 0.03$  <b>REFERENCES:</b> 1. Baldwin, R.R.; Daniel, S.G. <u>J. Appl. Chem.</u> 1952, <u>2</u> , 161. 2. Morrison, T.J.; Billett, F. <u>J. Chem. Soc.</u> 1948, 2033; <u>ibid.</u> 1952, 3819.																																								



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<b>VARIABLES:</b> T/K: 303.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> C.E. Edelman A.L. Cramer								
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="326 512 1001 646"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>303.15</td> <td>3.81</td> <td>0.687</td> <td>0.762</td> </tr> </tbody> </table> <p>The solubility value was adjusted to a partial pressure of krypton of 101.325 kPa (1 atm) by Henry's law.</p> <p>The Bunsen coefficient was calculated by the compiler.</p>		T/K	Mol Fraction $X_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	303.15	3.81	0.687	0.762
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<b>METHOD:</b> Volumetric. The solvent is saturated with gas as it flows through an 8 mm x 180 cm glass helix attached to a gas buret. The total pressure of solute gas plus solvent vapor is maintained at 1 atm as the gas is absorbed.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton. Linde Air Products Co. 2. 1,4-Dimethylbenzene. Eastman Kodak white label. Fractionally crystallized twice, dried over Na, distilled, b.p. 138.0-138.2°C.								
<b>APPARATUS/PROCEDURE:</b> The apparatus is a modification of the apparatus of Morrison and Billett (1). The modifications include the addition of a helical storage for the solvent, a manometer for a reference pressure, and an extra buret for highly soluble gases. The solvent is degassed by a modification of the method of Baldwin and Daniel (2).	<b>ESTIMATED ERROR:</b> $\delta T/K = 0.05$ $\delta P/mmHg = 3$ $\delta X_1/X_1 = 0.03$  <b>REFERENCES:</b> 1. Morrison, T.J.; Billett, F. <u>J. Chem. Soc.</u> 1948, 2033; <u>ibid.</u> 1952, 3819. 2. Baldwin, R.R.; Daniel, S.G. <u>J. Appl. Chem.</u> 1952, <u>2</u> , 161.								

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<b>VARIABLES:</b> T/K: 298.14 - 298.27 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> H.L. Clever																												
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<b>METHOD:</b> The apparatus is based on the design by Morrison and Billett (1) and the version used is described by Battino, Evans, and Danforth (2).	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton. Either Air Products & Chemicals, Inc., or Matheson Co., Inc. 99 mol % or better. 2. 1,4-Dimethylbenzene. Phillips Petroleum Co., pure grade.																												
<b>APPARATUS/PROCEDURE:</b> Degassing. Up to 500 cm <sup>3</sup> of solvent is placed in a flask of such size that the liquid is about 4 cm deep. The liquid is rapidly stirred, and vacuum is applied intermittently through a liquid N <sub>2</sub> trap until the permanent gas residual pressure drops to 5 microns. Solubility Determination. The degassed solvent passes in a thin film down a glass spiral tube containing the solute gas plus the solvent vapor at a total pressure of one atm. The volume of gas absorbed is found by difference between the initial and final gas volume in the buret system. The solvent is collected in a tared flask and weighed.	<b>ESTIMATED ERROR:</b> $\delta T/K = 0.03$ $\delta P/mmHg = 0.5$ $\delta x_1/x_1 = 0.02$  <b>REFERENCES:</b> 1. Morrison, T.J.; Billett, F. <u>J. Chem. Soc.</u> 1948, 2033. 2. Battino, R.; Evans, F.D.; Danforth, W.F. <u>J. Am. Oil Chem. Soc.</u> 1968, <u>45</u> , 830.																												

<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Industrial Hydrocarbons	<b>ORIGINAL MEASUREMENTS:</b> van Liempt, J.A.M.; van Wijk, W.  <u>Rec. Trav. Chim. Pays-Bas</u> 1937, <u>56</u> , 632 - 634.																					
<b>VARIABLES:</b> T/K: 291.65 - 293.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> H. L. Clever																					
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<b>AUXILIARY INFORMATION</b>																						
<b>METHOD:</b> The apparatus appears to be similar to the Winkler type apparatus used by Körösy (1).	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton. Source not given. Contained 5 % xenon. 2. Solvents. No information given.																					
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<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Krypton; Kr; 7439-90-9</li> <li>Hydrocarbons</li> </ol>	<p>ORIGINAL MEASUREMENTS: Steinberg, M.; Manowitz, B.</p> <p><u>Ind. and Eng. Chem.</u>, 1959, <u>51</u>, 47-50.</p>								
<p>VARIABLES:</p> <p>T/K: 296.15 - 298.65 P/kPa: 101.325 (1 atm)</p>	<p>PREPARED BY: H.L. Clever, P.L. Long, A.L. Cramer</p>								
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="301 526 1079 904"> <thead> <tr> <th>T/K</th> <th>Absorption Coefficient*</th> </tr> </thead> <tbody> <tr> <td>296.15</td> <td>"Ultrasene" (paraffins 80 wt %, naphthenes 20 wt %) 0.58</td> </tr> <tr> <td>298.65</td> <td>1,3,5-Trimethylbenzene (Mesitylene); C<sub>9</sub>H<sub>12</sub>; 108-67-8 0.63</td> </tr> <tr> <td>298.15</td> <td>Diphenylbenzene (Terphenyl); C<sub>18</sub>H<sub>14</sub>; 26140-60-3 0.30</td> </tr> </tbody> </table> <p>*Volume of gas (corrected to 288.15 K and 1 atm) absorbed under a total system pressure of 1 atm, per unit volume of solvent (corrected to 288.15 K).</p>		T/K	Absorption Coefficient*	296.15	"Ultrasene" (paraffins 80 wt %, naphthenes 20 wt %) 0.58	298.65	1,3,5-Trimethylbenzene (Mesitylene); C <sub>9</sub> H <sub>12</sub> ; 108-67-8 0.63	298.15	Diphenylbenzene (Terphenyl); C <sub>18</sub> H <sub>14</sub> ; 26140-60-3 0.30
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<p>AUXILIARY INFORMATION</p>									
<p>METHOD/APPARATUS/PROCEDURE: Modified McDaniel (1) method.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>Krypton. Matheson Co. Technically pure.</li> <li>Ultrasene. Atlantic Refining Co. Mesitylene. No source. Technical grade. Terphenyl. No source. Technical grade.</li> </ol> <p>ESTIMATED ERROR: <math>\delta\beta/\beta = 0.05 - 0.10.</math></p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>Furman, N.H., 1939 "Scott's Standard Methods of Chemical Analysis" II, 5th Ed., Van Nostrand Co., N.Y., p. 2587.</li> </ol>								

<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Amsco 123-15	<b>ORIGINAL MEASUREMENTS:</b> Steinberg, M.; Manowitz, B.  <u>Ind. Eng. Chem.</u> 1959, <u>51</u> , 47-50.																																							
<b>VARIABLES:</b> T/K: 218.15 - 423.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b>  H.L. Clever																																							
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<b>METHOD/APPARATUS/PROCEDURE:</b> <p>The absorption coefficient at one atm krypton was measured by modified McDaniel method (1).</p> <p>The Henry's constant (<math>K = (P/\text{atm})/X_1</math>) at low concentration of krypton was measured by static and dynamic tracer techniques.</p> <p>The authors state that log (Absorption Coefficient) vs <math>1/T</math> is linear and gives an enthalpy of solution of <math>-1700 \text{ cal mol}^{-1}</math>.</p>	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton. Matheson Co., Inc. Technical grade. 2. Amsco 123-15. American Mineral Spirits Co. No. 140. Paraffin 59.6 wt %, naphthene 27.3 wt %, aromatics 13.2 wt %.  <b>ESTIMATED ERROR:</b> $\delta K/K = 0.05 - 0.10$ (McDaniel method) $\delta K/K = 0.18$ (Tracer methods)  <b>REFERENCES:</b> 1. Furman, N.H. "Scott's Standard Methods of Chemical Analysis" Van Nostrand Co., NY 1939, 5th ed., Vol. II, p. 2587.																																							



COMPONENTS: 1. Krypton; Kr; 7439-90-9 2. Methanol; CH <sub>4</sub> O; 64-56-1	EVALUATOR: H. L. Clever Chemistry Department Emory University Atlanta, GA 30322 USA  May 1978
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## CRITICAL EVALUATION:

The solubility of krypton in methanol was measured in several laboratories. Only one laboratory reports krypton in methanol solubility values at more than one temperature. Thus, it is not possible to intercompare data from the different laboratories and recommend a set of solubility values and thermodynamic parameters for the system.

Van Liempt and van Wijk (1) report a Bunsen coefficient of 0.52 (mole fraction  $0.94 \times 10^{-3}$ ) at 291.15 K. Steinberg and Manowitz (2) report an absorption coefficient (volume of gas corrected to 288.15 K and 101.325 kPa absorbed under a total system pressure of 101.325 kPa per unit volume of solvent calculated at 288.15 K) of 1.06 at 144.15 to 153.15 K in the methanol + water eutectic (83 weight percent methanol). Komarenko and Manzhelii (3) report five solubility values between 176.15 and 213.15 K measured at a krypton pressure of 26.664 kPa (200 mmHg). The compiler has recalculated these at 101.325 kPa assuming Henry's law is obeyed.

It is not possible to judge the reliability of the single solubility values of van Liempt and van Wijk and of Steinberg and Manowitz. Data sheets on them are not included. Both the methanol and the krypton used by Komarenko and Manzhelii are of exceptional purity. Their degassing technique is thorough. The solubility method appears reliable, and their data should be of good quality. The Komarenko and Manzhelii solubility values were fitted to a three constant equation by the method of least squares. The smoothed solubility values at 101.325 kPa and the values of the thermodynamic changes for the transfer of krypton from the gas at 101.325 kPa to the hypothetical unit mole fraction solution for the temperature interval of 173.15 to 213.15 K are given on the data sheet which follows.

Although recommended solubility of krypton in methanol values are not given, a tentative set of values based on the five low temperature values of Komarenko and Manzhelii and the single room temperature value of von Liempt and van Wijk is given. This set of values should be used with extreme caution until more work is done on the system. The solubility equation is

$$\ln X_1 = -12.625 + 11.868/(T/100) + 1.4776 \ln (T/100)$$

Solubility values and values of thermodynamic parameters are given in Tables 1 and 2.

TABLE 1. Tentative values of the solubility of krypton in methanol at 101.325 kPa.

T/K	Mol Fraction $X_1 \times 10^3$	T/K	Mol Fraction $X_1 \times 10^3$
173.15	7.01	243.15	1.61
183.15	5.24	253.15	1.41
193.15	4.05	263.15	1.25
203.15	3.23	273.15	1.12
213.15	2.63	283.15	1.01
223.15	2.20	293.15	0.92
233.15	1.87		

TABLE 2. Tentative values for the transfer of one mole of krypton from the gas at 101.325 kPa to the hypothetical unit mole fraction solution.

T/K	$\Delta G^\circ/\text{J mol}^{-1}$	$\Delta H^\circ/\text{J mol}^{-1}$	$\Delta S^\circ/\text{JK}^{-1}\text{mol}^{-1}$	$\Delta C_p/\text{JK}^{-1}\text{mol}^{-1}$
193.15	8,845	-7,494	-84.60	12.29
293.15	17,031	-6,266	-79.47	12.29

- van Liempt, J.A.M.; von Wijk, W. *Rec. Trav. Chim. Pays-Bas* 1937, **56**, 632.
- Steinberg, M.; Manowitz, B. *Ind. Eng. Chem.* 1959, **51**, 47.
- Komarenko, V.G.; Manzhelii, V.G. *Ukr. Fiz. Zh. (Ukr. Ed.)* 1968, **13**, 387.

<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Methanol; CH <sub>4</sub> O; 64-56-1	<b>ORIGINAL MEASUREMENTS:</b> Komarenko, V.G.; Manzhelii, V.G.  Ukr. Fiz. Zh. (Ukr. Ed.) 1968, 13, 387-391. Ukr. Phys. J. 1968, 13, 273-276.																																				
<b>VARIABLES:</b> T/K: 176.15 - 213.15 P/kPa: 26.664 (200 mmHg)	<b>PREPARED BY:</b> T.D. Kittredge																																				
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<p>CRITICAL EVALUATION:</p> <p>Komarenko and Manzhelii (1) report eight values of the solubility of krypton in ethanol at 26.664 kPa (200 mmHg) between 159.15 and 223.15 K. We are not aware of any other measurements of the solubility of krypton in pure ethanol. However, van Liempt and van Wijk (2) report a Bunsen coefficient of 0.51 at 292.15 K in 96 per cent ethanol and 0.67 in 97½ per cent ethanol. Krestov and Nedelko (4) have calculated the solubility and the thermodynamic properties of krypton in ethanol + water mixtures over the 303 to 343 K temperature range by a comparative method using argon data as the reference. We have not been able to obtain a copy of their paper.</p> <p>Komarenko and Manzhelii used krypton and ethanol of exceptional purity. Their degassing technique is thorough, the solubility method appears reliable, and their data should be of good quality. The Komarenko and Manzhelii values were fitted to a three constant equation by the method of least squares. The equation, the smoothed solubility values at 101.325 kPa, and the values of the Thermodynamic parameters for the transfer of one mole of krypton from the gas at 101.325 kPa to the hypothetical unit mole fraction solution are given on the Komarenko and Manzhelii data sheet which follows.</p> <ol style="list-style-type: none"> <li>1. Komarenko, V.G.; Manzhelii, V.G. <u>Ukr. Fiz. Zh.</u> (Ukr. Ed.) 1968, <u>13</u>, 387.</li> <li>2. van Liempt, J.A.M.; van Wijk, W. <u>Rec. Trav. Chim. Pays-Bas</u> 1937, <u>56</u>, 632.</li> <li>3. Körösy, F. <u>Trans. Faraday Soc.</u> 1937, <u>33</u>, 416.</li> <li>4. Krestov, G.A.; Nedelko, B.E. <u>Tr. Ivanov. Khim. Tekhnol. Inst.</u> 1970, No. 12, 38. <u>Chem. Abstr.</u> 1972, <u>77</u>, 93469n; 1974, <u>80</u>, 7706v.</li> </ol>	

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VARIABLES: T/K: 163.15 - 243.15 P/kPa: 26.664 (200 mmHg)		PREPARED BY:  T.D. Kittredge			
EXPERIMENTAL VALUES:					
	T/K	Mol Fraction P/mmHg 200 $X_1 \times 10^3$	Mol Fraction P/mmHg 760 $X_1 \times 10^3$		
	163.15	4.84	18.4		
	173.15	3.64	13.8		
	183.15	2.79	10.6		
	193.15	2.18	8.28		
	203.15	1.775	6.745		
	213.15	1.473	5.597		
	223.15	1.240	4.712		
	233.15	1.064	4.043		
	243.15	0.983	3.73		
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163.15	18.4	5.422	-6.457	-72.81	-49.31
173.15	13.8	6.163	-6.859	-75.21	-31.27
183.15	10.6	6.923	-7.083	-76.47	-13.24
193.15	8.33	7.689	-7.125	-76.70	+4.79
203.15	6.705	8.453	-6.987	-76.00	22.83
213.15	5.544	9.206	-6.668	-74.48	40.86
223.15	4.711	9.940	-6.169	-72.19	58.90
233.15	4.115	10.65	-5.490	-69.22	76.93
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<b>COMPONENTS:</b>  1. Krypton; Kr; 7439-90-9  2. 2-Methyl-1-propanol; C <sub>4</sub> H <sub>10</sub> O; 78-83-1	<b>ORIGINAL MEASUREMENTS:</b>  Battino, R.; Evans, F. D.; Danforth, W. F.; Wilhelm, E.  <u>J. Chem. Thermodyn.</u> 1971, <u>3</u> , 743-751.																																											
<b>VARIABLES:</b>  T/K: 282.93 - 308.44 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b>  H. L. Clever																																											
<b>EXPERIMENTAL VALUES:</b>  <table border="1" data-bbox="333 516 1038 679"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th>Bunsen Coefficient α</th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>282.93</td> <td>2.90</td> <td>0.711</td> <td>0.737</td> </tr> <tr> <td>297.89</td> <td>2.57</td> <td>0.622</td> <td>0.678</td> </tr> <tr> <td>308.44</td> <td>2.34</td> <td>0.559</td> <td>0.632</td> </tr> </tbody> </table> Smoothed Data: $\Delta G^\circ = -RT \ln X_1 = -6,078.0 + 70.039 T$ Std. Dev. $\Delta G^\circ = 11.0$ , Coef. Corr. = 0.9999 $\Delta H^\circ/\text{J mol}^{-1} = -6078.0$ , $\Delta S^\circ/\text{J K}^{-1} \text{ mol}^{-1} = -70.039$  <table border="1" data-bbox="408 878 935 1149"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th><math>\Delta G^\circ/\text{J mol}^{-1}</math></th> </tr> </thead> <tbody> <tr><td>278.15</td><td>3.04</td><td>13,403</td></tr> <tr><td>283.15</td><td>2.90</td><td>13,754</td></tr> <tr><td>288.15</td><td>2.78</td><td>14,104</td></tr> <tr><td>293.15</td><td>2.66</td><td>14,454</td></tr> <tr><td>298.15</td><td>2.55</td><td>14,804</td></tr> <tr><td>303.15</td><td>2.45</td><td>15,154</td></tr> <tr><td>308.15</td><td>2.35</td><td>15,505</td></tr> <tr><td>313.15</td><td>2.27</td><td>15,855</td></tr> </tbody> </table> The solubility values were adjusted to a partial pressure of krypton of 101.325 kPa (1 atm) by Henry's law. The Bunsen coefficients were calculated by the compiler.		T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	Bunsen Coefficient α	Ostwald Coefficient L	282.93	2.90	0.711	0.737	297.89	2.57	0.622	0.678	308.44	2.34	0.559	0.632	T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	$\Delta G^\circ/\text{J mol}^{-1}$	278.15	3.04	13,403	283.15	2.90	13,754	288.15	2.78	14,104	293.15	2.66	14,454	298.15	2.55	14,804	303.15	2.45	15,154	308.15	2.35	15,505	313.15	2.27	15,855
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<b>METHOD:</b>  A. Degasser (1). B. Absorption of gas in a thin film of liquid (2,3)  <b>APPARATUS/PROCEDURE:</b>  Degassing. The solvent is sprayed into an evacuated chamber of an all glass apparatus; it is stirred and heated until the pressure drops to the vapor pressure of the liquid. Solubility Determination. The degassed liquid passes in a thin film down a glass spiral tube at a total pressure of one atm of solute gas plus solvent vapor. The gas absorbed is measured in the attached buret system, and the solvent is collected in a tared flask and weighed.	<b>SOURCE AND PURITY OF MATERIALS:</b>  1. Krypton. Air Products & Chemicals. Research grade. Greater than 99 mol %.  2. 2-Methyl-1-propanol. Fisher Scientific Co. Certified (99 mol %).  <b>ESTIMATED ERROR:</b>  $\delta T/K = 0.03$ $\delta P/\text{mmHg} = 0.5$ $\delta X_1/X_1 = 0.015$  <b>REFERENCES:</b> 1. Battino, R.; Evans, F.D. <u>Anal. Chem.</u> 1966, <u>38</u> , 1627. 2. Morrison, T. J.; Billet, F. <u>J. Chem. Soc.</u> 1948, 2033. 3. Clever, H. L.; Battino, R.; Saylor, J. H.; Gross, P. M. <u>J. Phys. Chem.</u> 1957, <u>61</u> , 1078.																																											

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>1. Krypton; Kr; 7439-90-9</li> <li>2. 1-Pentanol (Amyl Alcohol); C<sub>5</sub>H<sub>12</sub>O; 71-41-0</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>van Liempt, J. A. M.; van Wijk, W.</p> <p><u>Rec. Trav. Chim. Pays-Bas</u> 1937, <u>56</u> 632-634.</p>								
<p>VARIABLES:</p> <p>T/K: 296.15 P/kPa: 101.325 (1 atm)</p>	<p>PREPARED BY:</p> <p>H. L. Clever</p>								
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296.15	3.18	0.66	0.72						
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<p>METHOD:</p> <p>The apparatus appears to be similar to the Winkler type apparatus used by Körösy (1).</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>1. Krypton. Source not given. Contained 5 % xenon.</li> <li>2. Amyl Alcohol. No information.</li> </ol>								
<p>APPARATUS/PROCEDURE:</p>	<p>ESTIMATED ERROR:</p> <p><math>\delta X_1/X_1 = 0.10</math> (Compiler)</p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>1. Körösy, F. <u>Trans. Faraday Soc.</u> 1937, <u>33</u>, 416.</li> </ol>								



<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>1. Krypton; Kr; 7439-90-9</li> <li>2. 1-Octanol; C<sub>8</sub>H<sub>18</sub>O; 111-87-5</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Wilcock, R. J.; Battino, R.; Danforth, W. F.; Wilhelm, E.</p> <p><u>J. Chem. Thermodyn.</u> 1978, <u>10</u>, 817 - 822.</p>								
<p>VARIABLES:</p> <p>T/K: 298.06 P/kPa: 101.325 (1 atm)</p>	<p>PREPARED BY:</p> <p>A.L. Cramer</p>								
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="330 512 1005 681"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>298.06</td> <td>3.773</td> <td>0.5349</td> <td>0.5837</td> </tr> </tbody> </table> <p>A preliminary account of this work appeared in <u>Conf. Int. Thermodyn. Chim. (C.R.)</u> 4th 1975, <u>6</u>, 122-128.</p> <p>The solubility value was adjusted to a krypton partial pressure of 101.325 kPa (1 atm) by Henry's law.</p> <p>The Bunsen coefficient was calculated by the compiler.</p>		T/K	Mol Fraction $x_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	298.06	3.773	0.5349	0.5837
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<p>METHOD /APPARATUS/PROCEDURE:</p> <p>The solubility apparatus is based on the design of Morrison and Billett (1) and the version used is described by Battino, Evans, and Danforth (2). The degassing apparatus is that described by Battino, Banzhof, Bogan, and Wilhelm (3). See Krypton + Octane data sheet for more detail.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>1. Krypton. The Matheson Co., Inc., or Air Products and Chemicals. Purest commercially available.</li> <li>2. 1-Octanol. Eastman Organic Chemicals. Distilled until refractive index equals the value recommended by Wilhoit, R.C.; Zwolinski, B. J. <u>J. Phys. Chem. Ref. Data</u> 1973, <u>2</u> (Suppl. No. 1), 1-212 and 1-278.</li> </ol> <p>ESTIMATED ERROR:</p> <p><math>\delta T/K = 0.03</math> <math>\delta P/\text{mmHg} = 0.5</math> <math>\delta x_1/x_1 = 0.005</math></p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>1. Morrison, T.J.; Billett, F. <u>J. Chem. Soc.</u> 1948, 2033.</li> <li>2. Battino, R.; Evans, F.D.; Danforth, W.F. <u>J. Am. Oil Chem. Soc.</u> 1968, 45, 830.</li> <li>3. Battino, R.; Banzhof, M.; Bogan, M.; Wilhelm, E. <u>Anal. Chem.</u> 1971, <u>43</u>, 806.</li> </ol>								

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>1. Krypton; Kr; 7439-90-9</li> <li>2. 1-Decanol; C<sub>10</sub>H<sub>22</sub>O; 112-30-1</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Wilcock, R. J.; Battino, R.; Danforth, W. F.; Wilhelm, E.</p> <p><u>J. Chem. Thermodyn.</u> 1978, <u>10</u>, 817 - 822.</p>								
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<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Krypton; Kr; 7439-90-9</li> <li>1,2,3-Propanetriol (Glycerol); C<sub>3</sub>H<sub>8</sub>O<sub>3</sub>; 56-81-5</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Körösy, F.</p> <p><u>Trans. Faraday Soc.</u> 1937, <u>33</u>, 416-425.</p>								
<p>VARIABLES:</p> <p>T/K: 293.15 P/kPa: 101.325 (1 atm)</p>	<p>PREPARED BY:</p> <p>H.L. Clever</p>								
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<p>METHOD:</p> <p>The apparatus and method of Winkler (1) were used. However, the apparatus was usually not thermostated, and degassing was by evacuating and shaking the solvent, not by evacuating and boiling the solvent as was done by Winkler.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>Krypton. Source not given. The gas contained 5% xenon and 1% non-inert gases.</li> <li>1,2,3-Propanetriol. No information.</li> </ol>								
<p>APPARATUS/PROCEDURE:</p>	<p>ESTIMATED ERROR:</p> <p><math>\delta x_1/x_1 = 0.05</math></p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>Winkler, L.W. <u>Ber.</u> 1891, <u>24</u>, 89.</li> <li>van Liempt, J.A.M.; van Wijk, W. <u>Rec. Trav. Chim. Pays-Bas</u> 1937, <u>56</u>, 632.</li> </ol>								

<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Cyclohexanol; C <sub>6</sub> H <sub>12</sub> O; 108-93-0	<b>ORIGINAL MEASUREMENTS:</b> Körösy, F.  <u>Trans. Faraday Soc.</u> 1937, <u>33</u> , 416-425.								
<b>VARIABLES:</b> T/K: 295.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> H.L. Clever								
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<b>APPARATUS/PROCEDURE:</b>	<b>ESTIMATED ERROR:</b> $\delta x_1/x_1 = 0.05$ <b>REFERENCES:</b> 1. Winkler, L.W. <u>Ber.</u> 1891, <u>24</u> , 89.								

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>1. Krypton; Kr; 7439-90-9</li> <li>2. 2-Propanone (Acetone); C<sub>3</sub>H<sub>6</sub>O; 67-64-1</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Körösy, F.</p> <p><u>Trans. Faraday Soc.</u> 1937, <u>33</u>,416-425.</p>																				
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<p>APPARATUS/PROCEDURE:</p>	<p>ESTIMATED ERROR:</p> <p><math>\delta X_1/X_1 = 0.05</math></p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>1. Winkler, L.W. <u>Ber.</u> 1891, <u>24</u>, 89.</li> </ol>																				

<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Acetic Acid, Glacial; C <sub>2</sub> H <sub>4</sub> O <sub>2</sub> ; 64-19-7	<b>ORIGINAL MEASUREMENTS:</b> Körösy, F.  Trans. <u>Faraday Soc.</u> 1937, <u>33</u> , 416-425.								
<b>VARIABLES:</b> T/K: 295.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> H.L. Clever								
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COMPONENTS: 1. Krypton; Kr; 7439-90-9 2. Esters	ORIGINAL MEASUREMENTS: Körösy, F.  <u>Trans. Faraday Soc.</u> 1937, <u>33</u> , 416-425.																				
VARIABLES: T/K: 293.15 P/kPa: 101.325 (1 atm)	PREPARED BY: H.L. Clever																				
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<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Undecafluoro(trifluoromethyl)-cyclohexane (Perfluoromethyl-cyclohexane); C <sub>7</sub> F <sub>14</sub> ; 355-02-2	<b>ORIGINAL MEASUREMENTS:</b> Clever, H.L.; Saylor, J.H.; Gross, P.M.  J. Phys. Chem. 1958, 62, 89-91.																																								
<b>VARIABLES:</b> T/K: 289.15 - 316.25 Total P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> P.L. Long																																								
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="349 504 1021 695" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>289.15</td> <td>9.06</td> <td>1.058</td> <td>1.12</td> </tr> <tr> <td>303.15</td> <td>8.08</td> <td>0.925</td> <td>1.027</td> </tr> <tr> <td>316.25</td> <td>7.77</td> <td>0.872</td> <td>1.01</td> </tr> </tbody> </table> <p>Smoothed Data: <math>\Delta G^\circ/J \text{ mol}^{-1} = -RT \ln X_1 = -4302.3 + 54.078 T</math>            Std. Dev. <math>\Delta G^\circ = 46.1</math>, Coef. Corr. = 0.9980  <math>\Delta H^\circ/J \text{ mol}^{-1} = -4302.3</math>, <math>\Delta S^\circ/J \text{ K}^{-1} \text{ mol}^{-1} = -54.078</math></p> <table border="1" data-bbox="463 826 940 1098" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^3</math></th> <th><math>\Delta G^\circ/J \text{ mol}^{-1}</math></th> </tr> </thead> <tbody> <tr> <td>288.15</td> <td>9.02</td> <td>11,280</td> </tr> <tr> <td>293.15</td> <td>8.75</td> <td>11,551</td> </tr> <tr> <td>298.15</td> <td>8.49</td> <td>11,821</td> </tr> <tr> <td>303.15</td> <td>8.25</td> <td>12,091</td> </tr> <tr> <td>308.15</td> <td>8.03</td> <td>12,362</td> </tr> <tr> <td>313.15</td> <td>7.81</td> <td>12,632</td> </tr> <tr> <td>318.15</td> <td>7.61</td> <td>12,903</td> </tr> </tbody> </table> <p>The solubility values were adjusted to a partial pressure of krypton of 101.325 kPa (1 atm) by Henry's law.            The Bunsen coefficients were calculated by the compiler.</p>		T/K	Mol Fraction $X_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	289.15	9.06	1.058	1.12	303.15	8.08	0.925	1.027	316.25	7.77	0.872	1.01	T/K	Mol Fraction $X_1 \times 10^3$	$\Delta G^\circ/J \text{ mol}^{-1}$	288.15	9.02	11,280	293.15	8.75	11,551	298.15	8.49	11,821	303.15	8.25	12,091	308.15	8.03	12,362	313.15	7.81	12,632	318.15	7.61	12,903
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<b>METHOD:</b> Volumetric. The apparatus (1) is a modification of that used by Morrison and Billett (2). Modifications include the addition of a spiral solvent storage tubing, a manometer for constant reference pressure, and an extra gas buret for highly soluble gases.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton. Matheson Co., Inc. Both standard and research grades were used. 2. Perfluoromethylcyclohexane. du Pont FCS-326, shaken with concentrated H <sub>2</sub> SO <sub>4</sub> , washed, dried over Drierite and distilled. b.p. 75.95 to 76.05° at 753 mm., lit. b.p. 76.14 at 760 mm.																																								
<b>APPARATUS/PROCEDURE:</b> (a) Degassing. 700 ml of solvent is shaken and evacuated while attached to a cold trap, until no bubbles are seen; solvent is then transferred through a 1 mm capillary tubing, released as a fine mist into a continuously evacuated flask. (b) Solvent is saturated with gas as it flows through 8 mm x 180 cm of tubing attached to a gas buret. Pressure is maintained at 1 atm as the gas is absorbed.	<b>ESTIMATED ERROR:</b> $\delta T/K = 0.05$ $\delta P/\text{mmHg} = 3$ $\delta X_1/X_1 = 0.03$  <b>REFERENCES:</b> 1. Clever, H.L.; Battino, R.; Saylor, J.H.; Gross, P.M. J. Phys. Chem. 1957, 61, 1078. 2. Morrison, T.J.; Billett, F. J. Chem. Soc. 1948, 2033; <i>ibid.</i> 1952, 3819.																																								



<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Dichlorodifluoromethane (Freon-12); $\text{CCl}_2\text{F}_2$ ; 75-71-8		<b>ORIGINAL MEASUREMENTS:</b> Steinberg, M.; Manowitz, B.; Pruzansky, J. US AEC BNL-542 (T-140). Chem. Abstr. 1959, <u>53</u> , 21242g.			
<b>VARIABLES:</b> T/K: 190.15 - 273.15		<b>PREPARED BY:</b> H.L. Clever			
<b>EXPERIMENTAL VALUES:</b>					
T/K	Absorption Coefficient	Henry's Constant K/atm	Mol Fraction $X_1 \times 10^2$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L
190.15	13.9	--	4.32	13.2	9.2
193.15	12.6	--	3.76	11.9	8.4
197.65	11.3	--	3.42	10.7	7.7 <sub>5</sub>
203.15	--	32.5	3.08	--	--
244.15	5.1	--	1.72	4.8	4.3
260.85	--	86	1.16	--	--
273.15	2.4	108	$\begin{cases} 0.925 \\ 0.89 \end{cases}$	2.3	2.3
Smoothed Data: $\Delta G^\circ/\text{J mol}^{-1} = -RT \ln X_1 = -7772.6 + 67.346 T$ Std. Dev. $\Delta G^\circ = 69.5$ , Coef. Corr. = 0.9997 $\Delta H^\circ/\text{J mol}^{-1} = -7,772.6$ , $\Delta S^\circ/\text{J K}^{-1} \text{ mol}^{-1} = 0.9997$					
T/K	Mol Fraction $X_1 \times 10^2$	$\Delta G^\circ/\text{J mol}^{-1}$			
193.15	3.84	5,235.4			
203.15	3.02	5,908.8			
213.15	2.44	6,582.3			
223.15	2.00	7,225.8			
233.15	1.67	7,929.2			
243.15	1.41	8,602.7			
253.15	1.22	9,276.2			
263.15	1.06	9,949.7			
273.15	0.93	10,623			
<b>AUXILIARY INFORMATION</b>					
<b>METHOD/APPARATUS/PROCEDURE:</b> Dynamic tracer technique (1). The Henry's constant is $K = (P/\text{atm})/X_1.$ The Henry's constants are probably from data smoothed by the authors. The report is discussed further in a later paper (2).			<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton. 2. Dichlorodifluoromethane.		
			<b>ESTIMATED ERROR:</b> $\delta X/X = 0.03 - 0.05$ (Compiler)		
			<b>REFERENCES:</b> 1. Steinberg, M.; Manowitz, B. <u>Ind. Eng. Chem.</u> 1959, <u>51</u> , 47. 2. Steinberg, M. US AEC TID-7593, 1959, 217-218. <u>Chem. Abstr.</u> 1961, <u>55</u> , 9083e.		

<p>COMPONENTS:</p> <p>1. Krypton; Kr; 7439-90-9</p> <p>2. Halogenated Methanes</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Körösy, F.</p> <p><u>Trans. Faraday Soc.</u> 1937, <u>33</u>, 416-425.</p>																																				
<p>VARIABLES:</p> <p>T/K: 273.15 - 295.15</p> <p>P/kPa: 101.325 (1 atm)</p>	<p>PREPARED BY:</p> <p>H.L. Clever</p>																																				
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<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Krypton; Kr; 7439-90-9</li> <li>Fluorobenzene; C<sub>6</sub>H<sub>5</sub>F; 462-06-6</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Saylor, J.H.; Battino, R.</p> <p><u>J. Phys. Chem.</u> 1958, <u>62</u>, 1334-1337.</p>																																																		
<p>VARIABLES:</p> <p>T/K: 288.15 - 328.15 P/kPa: 101.325 (1 atm)</p>	<p>PREPARED BY:</p> <p>H.L. Clever, A.L. Cramer</p>																																																		
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<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Hexafluorobenzene; C <sub>6</sub> F <sub>6</sub> ; 392-56-3	<b>ORIGINAL MEASUREMENTS:</b> Evans, F. D.; Battino, R.  <u>J. Chem. Thermodyn.</u> 1971, <u>3</u> , 753-760.																																						
<b>VARIABLES:</b> T/K: 282.91 - 297.92 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> H. L. Clever																																						
<b>EXPERIMENTAL VALUES:</b>  <table border="1" data-bbox="377 528 1077 721"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th>Bunsen Coefficient α</th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr><td>282.91</td><td>6.45</td><td>1.286</td><td>1.332</td></tr> <tr><td>283.09</td><td>6.42</td><td>1.279</td><td>1.326</td></tr> <tr><td>297.76</td><td>5.92</td><td>1.155</td><td>1.259</td></tr> <tr><td>297.92</td><td>5.89</td><td>1.148</td><td>1.252</td></tr> </tbody> </table> Smoothed Data: $\Delta G^\circ/\text{J mol}^{-1} = -RT \ln X_1 = -4,063.6 + 56.302 T$ Std. Dev. $\Delta G^\circ = 4.9$ , Coef. Corr. = 0.9999 $\Delta H^\circ/\text{J mol}^{-1} = -4063.6$ , $\Delta S^\circ/\text{J K}^{-1} \text{ mol}^{-1} = -56.302$  <table border="1" data-bbox="463 876 990 1078"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th><math>\Delta G^\circ/\text{J mol}^{-1}</math></th> </tr> </thead> <tbody> <tr><td>278.15</td><td>6.64</td><td>11,597</td></tr> <tr><td>283.15</td><td>6.44</td><td>11,878</td></tr> <tr><td>288.15</td><td>6.25</td><td>12,160</td></tr> <tr><td>293.15</td><td>6.07</td><td>12,441</td></tr> <tr><td>298.15</td><td>5.90</td><td>12,723</td></tr> </tbody> </table> The solubility values were adjusted to a partial pressure of krypton of 101.325 kPa (1 atm) by Henry's law. The Bunsen coefficients were calculated by the compiler.		T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	Bunsen Coefficient α	Ostwald Coefficient L	282.91	6.45	1.286	1.332	283.09	6.42	1.279	1.326	297.76	5.92	1.155	1.259	297.92	5.89	1.148	1.252	T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	$\Delta G^\circ/\text{J mol}^{-1}$	278.15	6.64	11,597	283.15	6.44	11,878	288.15	6.25	12,160	293.15	6.07	12,441	298.15	5.90	12,723
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<b>METHOD /APPARATUS/PROCEDURE:</b> The solubility apparatus is based on the design of Morrison and Billett (1) and the version used is described by Battino, Evans, and Danforth (2). The degassing apparatus is that described by Battino, Banzhof, Bogan, and Wilhelm (3). Degassing. Up to 500 cm <sup>3</sup> of solvent is placed in a flask of such size that the liquid is about 4 cm deep. The liquid is rapidly stirred and the vacuum is applied intermittently through a liquid N <sub>2</sub> trap until the permanent gas residual pressure drops to 5 microns. Solubility Determination. The degassed solvent is passed in a thin film down a glass spiral tube containing solute gas plus the solvent vapor at a total pressure of one atm. The volume of gas absorbed is found by difference between the initial and final volumes in the buret system. The solvent is collected in a tared flask and weighed.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton. Either Air Products & Chemicals or Matheson. Better than 99 mol % (usually 99.9+) 2. Hexafluorobenzene. Imperial Smelting Co., Avonmouth, U.K. GC purity 99.7%, density at 25° C 1.60596 g cm <sup>-3</sup> . Purified by method in <u>Anal. Chem.</u> 1968, <u>40</u> , 224.  <b>ESTIMATED ERROR:</b> $\delta T/K = 0.03$ $\delta P/\text{mmHg} = 0.5$ $\delta X_1/X_1 = 0.015$  <b>REFERENCES:</b> 1. Morrison, T. J.; Billett, F. <u>J. Chem. Soc.</u> 1948, 2033. 2. Battino, R.; Evans, F. D.; Danforth, W. F. <u>J. Am. Oil Chem. Soc.</u> 1968, <u>45</u> , 830. 3. Battino, R.; Banzhof, M.; Bogan, M.; Wilhelm, E. <u>Anal. Chem.</u> 1971, <u>43</u> , 806.																																						

<p>COMPONENTS:</p> <p>1. Krypton; Kr; 7439-90-9</p> <p>2. Chlorobenzene; C<sub>6</sub>H<sub>5</sub>Cl; 108-90-7</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Saylor, J.H.; Battino, R.</p> <p><u>J. Phys. Chem.</u> 1958, <u>62</u>, 1334-1337.</p>																																																		
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<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="342 493 1021 715"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr><td>288.15</td><td>2.84</td><td>0.629</td><td>0.664</td></tr> <tr><td>298.15</td><td>2.75</td><td>0.604</td><td>0.659</td></tr> <tr><td>313.15</td><td>2.56</td><td>0.553</td><td>0.634</td></tr> <tr><td>328.15</td><td>2.44</td><td>0.520</td><td>0.625</td></tr> </tbody> </table> <p>Smoothed Data: <math>\Delta G^\circ/\text{J mol}^{-1} = -RT \ln X_1 = -3079.8 + 59.412 T</math>  Std. Dev. <math>\Delta G^\circ = 13.8</math>, Coef. Corr. = .9999  <math>\Delta H^\circ/\text{J mol}^{-1} = -3079.8</math>, <math>\Delta S^\circ/\text{J K}^{-1} \text{ mol}^{-1} = -59.412</math></p> <table border="1" data-bbox="464 836 949 1139"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^3</math></th> <th><math>\Delta G^\circ/\text{J mol}^{-1}</math></th> </tr> </thead> <tbody> <tr><td>288.15</td><td>2.85</td><td>14,040</td></tr> <tr><td>293.15</td><td>2.79</td><td>14,337</td></tr> <tr><td>298.15</td><td>2.73</td><td>14,634</td></tr> <tr><td>303.15</td><td>2.67</td><td>14,931</td></tr> <tr><td>308.15</td><td>2.62</td><td>15,228</td></tr> <tr><td>313.15</td><td>2.57</td><td>15,525</td></tr> <tr><td>318.15</td><td>2.53</td><td>15,822</td></tr> <tr><td>323.15</td><td>2.48</td><td>16,119</td></tr> <tr><td>328.15</td><td>2.44</td><td>16,416</td></tr> </tbody> </table> <p>Solubility values were adjusted to a partial pressure of krypton of 101.325 kPa (1 atm) by Henry's law. Bunsen coefficients were calculated by the compiler.</p>		T/K	Mol Fraction $X_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	288.15	2.84	0.629	0.664	298.15	2.75	0.604	0.659	313.15	2.56	0.553	0.634	328.15	2.44	0.520	0.625	T/K	Mol Fraction $X_1 \times 10^3$	$\Delta G^\circ/\text{J mol}^{-1}$	288.15	2.85	14,040	293.15	2.79	14,337	298.15	2.73	14,634	303.15	2.67	14,931	308.15	2.62	15,228	313.15	2.57	15,525	318.15	2.53	15,822	323.15	2.48	16,119	328.15	2.44	16,416
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<p>VARIABLES:</p> <p>T/K: 303.15 P/kPa: 101.325 (1 atm) 1,4-Dichlorobenzene/X<sub>3</sub>: 0 - 0.455</p>	<p>PREPARED BY:</p> <p>C. E. Eddelman A. L. Cramer</p>																						
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<p>METHOD:</p> <p>Volumetric. The solvent is saturated with gas as it flows through an 8 mm x 180 cm glass helix attached to a gas buret. The total pressure of solute gas plus solvent vapor is maintained at 1 atm as the gas is absorbed.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>1. Krypton. Linde Air Products Co.</li> <li>2. 1,4-Dimethylbenzene. Eastman Kodak white label. Distilled.</li> <li>3. 1,4-Dichlorobenzene. Eastman Kodak white label. Recrystallized twice from methanol, dried in air.</li> </ol>																						
<p>APPARATUS/PROCEDURE:</p> <p>The apparatus is a modification of the apparatus of Morrison and Billett (1). The modifications include the addition of a helical storage for the solvent, a manometer for a reference pressure, and an extra buret for highly soluble gases. The solvent is degassed by a modification of the method of Baldwin and Daniel (2).</p>	<p>ESTIMATED ERROR:</p> <p>δT/K = 0.05 δP/mmHg = 3 δX<sub>1</sub>/X<sub>1</sub> = 0.03</p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>1. Morrison, T.J.; Billett, F. <u>J. Chem. Soc.</u> 1948, 2033; <u>ibid.</u> 1952, 3819.</li> <li>2. Baldwin, R.R.; Daniel, S.G. <u>J. Appl. Chem.</u> 1952, <u>2</u>, 161.</li> </ol>																						

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<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Iodobenzene; C <sub>6</sub> H <sub>5</sub> I; 591-50-4	<b>ORIGINAL MEASUREMENTS:</b> Saylor, J.H.; Battino, R.  <u>J. Phys. Chem.</u> 1958, <u>62</u> , 1334-1337.																																																		
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<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: left;">T/K</th> <th style="text-align: center;">Mol Fraction <math>X_1 \times 10^3</math></th> <th style="text-align: center;">Bunsen Coefficient <math>\alpha</math></th> <th style="text-align: center;">Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr><td>288.15</td><td style="text-align: center;">1.73</td><td style="text-align: center;">0.349</td><td style="text-align: center;">0.368</td></tr> <tr><td>298.15</td><td style="text-align: center;">1.70</td><td style="text-align: center;">0.339</td><td style="text-align: center;">0.370</td></tr> <tr><td>313.15</td><td style="text-align: center;">1.63</td><td style="text-align: center;">0.322</td><td style="text-align: center;">0.369</td></tr> <tr><td>328.15</td><td style="text-align: center;">1.58</td><td style="text-align: center;">0.309</td><td style="text-align: center;">0.371</td></tr> </tbody> </table> <p>Smoothed Data: <math>\Delta G^\circ/\text{J mol}^{-1} = -RT \ln X_1 = -1841.9 + 59.241 T</math>            Std. Dev. <math>\Delta G^\circ = 8.8</math>, Coef. Corr. = .9999  <math>\Delta H^\circ/\text{J mol}^{-1} = -1841.9</math>, <math>\Delta S^\circ/\text{J K}^{-1} \text{ mol}^{-1} = -59.241</math></p> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: left;">T/K</th> <th style="text-align: center;">Mol Fraction <math>X_1 \times 10^3</math></th> <th style="text-align: center;"><math>\Delta G^\circ/\text{J mol}^{-1}</math></th> </tr> </thead> <tbody> <tr><td>288.15</td><td style="text-align: center;">1.74</td><td style="text-align: center;">15,228</td></tr> <tr><td>293.15</td><td style="text-align: center;">1.71</td><td style="text-align: center;">15,525</td></tr> <tr><td>298.15</td><td style="text-align: center;">1.69</td><td style="text-align: center;">15,821</td></tr> <tr><td>303.15</td><td style="text-align: center;">1.67</td><td style="text-align: center;">16,117</td></tr> <tr><td>308.15</td><td style="text-align: center;">1.65</td><td style="text-align: center;">16,413</td></tr> <tr><td>313.15</td><td style="text-align: center;">1.63</td><td style="text-align: center;">16,709</td></tr> <tr><td>318.15</td><td style="text-align: center;">1.61</td><td style="text-align: center;">17,006</td></tr> <tr><td>323.15</td><td style="text-align: center;">1.60</td><td style="text-align: center;">17,302</td></tr> <tr><td>328.15</td><td style="text-align: center;">1.58</td><td style="text-align: center;">17,598</td></tr> </tbody> </table> <p>Solubility values were adjusted to a partial pressure of krypton of 101.325 kPa (1 atm) by Henry's law. Bunsen coefficients were calculated by the compiler.</p>		T/K	Mol Fraction $X_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	288.15	1.73	0.349	0.368	298.15	1.70	0.339	0.370	313.15	1.63	0.322	0.369	328.15	1.58	0.309	0.371	T/K	Mol Fraction $X_1 \times 10^3$	$\Delta G^\circ/\text{J mol}^{-1}$	288.15	1.74	15,228	293.15	1.71	15,525	298.15	1.69	15,821	303.15	1.67	16,117	308.15	1.65	16,413	313.15	1.63	16,709	318.15	1.61	17,006	323.15	1.60	17,302	328.15	1.58	17,598
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<b>METHOD /APPARATUS/PROCEDURE:</b> The solvent was degassed by evacuating the space above it, shaking, and then passing it as a fine mist into another evacuated container. The degassed liquid was saturated as it passed as a thin film inside a glass helix which contained the solute gas plus solvent vapor at a total pressure of 1 atm (1,2). The volume of liquid and the volume of gas absorbed are determined in a system of burets.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton. Linde Air Products Co. 2. Iodobenzene. Eastman Kodak white label. Shaken with aq. Na <sub>2</sub> S <sub>2</sub> O <sub>3</sub> , dried over P <sub>4</sub> O <sub>10</sub> , distilled. b.p. 77.40 - 77.60°C (20 mmHg).																																																		
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<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. 1,4-Dimethylbenzene (p-Xylene); $C_8H_{10}$ ; 106-42-3 3. 1,4-Diiodobenzene; $C_6H_4I_2$ ; 624-38-4	<b>ORIGINAL MEASUREMENTS:</b> Clever, H.L.  <u>J. Phys. Chem.</u> 1957, <u>61</u> , 1082-1083.															
<b>VARIABLES:</b> T/K: 303.15 P/kPa: 101.325 (1 atm) 1,4-Diiodobenzene/ $X_3$ : 0-0.078	<b>PREPARED BY:</b> C.E. Eddleman A.L. Cramer															
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="262 512 1153 687"> <thead> <tr> <th>T/K</th> <th>1,4-Diiodo- benzene Mol Fraction <math>X_3</math></th> <th>Mol Fraction <math>X_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>303.15</td> <td>0.0</td> <td>3.81</td> <td>0.687</td> <td>0.762</td> </tr> <tr> <td></td> <td>0.078</td> <td>3.48</td> <td>0.626</td> <td>0.695</td> </tr> </tbody> </table> <p>The solubility values were adjusted to a partial pressure of krypton of 101.325 kPa (1 atm) by Henry's law.</p> <p>The Bunsen coefficients were calculated by the compiler.</p>		T/K	1,4-Diiodo- benzene Mol Fraction $X_3$	Mol Fraction $X_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	303.15	0.0	3.81	0.687	0.762		0.078	3.48	0.626	0.695
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<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Krypton; Kr; 7439-90-9</li> <li>1,1,2,2,3,3,4,4,4-nonafluoro-N, N-bis (nonafluorobutyl)-1-butanamine (Perfluorotributylamine); (C<sub>4</sub>F<sub>9</sub>)<sub>3</sub>N; 311-89-7</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Powell, R.J.</p> <p><u>J. Chem. Eng. Data</u> 1972, <u>17</u>, 302-304.</p>																
<p>VARIABLES:</p> <p>T/K: 298.15 P/kPa: 101.325 (1 atm)</p>	<p>PREPARED BY:</p> <p>P.L. Long</p>																
<p>EXPERIMENTAL VALUES:</p> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Mol Fraction <math>x_1 \times 10^3</math></th> <th style="text-align: center;">Bunsen Coefficient <math>\alpha</math></th> <th style="text-align: center;">Ostwald Coefficient L</th> <th style="text-align: center;"><math>R \frac{\Delta \log x_1}{\Delta \log T} = N</math></th> </tr> </thead> <tbody> <tr> <td style="text-align: center;">298.15</td> <td style="text-align: center;">11.15</td> <td style="text-align: center;">0.708</td> <td style="text-align: center;">0.773</td> <td style="text-align: center;">-3.30</td> </tr> </tbody> </table>		T/K	Mol Fraction $x_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	$R \frac{\Delta \log x_1}{\Delta \log T} = N$	298.15	11.15	0.708	0.773	-3.30						
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<p>The author implies that solubility measurements were made between 288.15 and 318.15 K, but only the solubility at 298.15 was given in the paper. The slope <math>R(\Delta \log x_1 / \Delta \log T)</math> was given. The smoothed data below were calculated by the compiler from the slope in the form:</p> $\log x_1 = \log(11.15 \times 10^{-3}) + (-3.30/R) \log(T/298.15)$ <p>with <math>R = 1.9872 \text{ cal K}^{-1} \text{ mol}^{-1}</math>.</p> <p>Smoothed Data:</p> <table border="1" style="margin-left: auto; margin-right: auto; border-collapse: collapse;"> <thead> <tr> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Mol Fraction <math>x_1 \times 10^3</math></th> </tr> </thead> <tbody> <tr><td style="text-align: center;">288.15</td><td style="text-align: center;">11.81</td></tr> <tr><td style="text-align: center;">293.15</td><td style="text-align: center;">11.47</td></tr> <tr><td style="text-align: center;">298.15</td><td style="text-align: center;">11.15</td></tr> <tr><td style="text-align: center;">303.15</td><td style="text-align: center;">10.85</td></tr> <tr><td style="text-align: center;">308.15</td><td style="text-align: center;">10.55</td></tr> <tr><td style="text-align: center;">313.15</td><td style="text-align: center;">10.28</td></tr> <tr><td style="text-align: center;">318.15</td><td style="text-align: center;">10.01</td></tr> </tbody> </table>		T/K	Mol Fraction $x_1 \times 10^3$	288.15	11.81	293.15	11.47	298.15	11.15	303.15	10.85	308.15	10.55	313.15	10.28	318.15	10.01
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<p>METHOD / APPARATUS / PROCEDURE:</p> <p>Solvent is degassed by freezing and pumping, then boiling under reduced pressure. The Dymond and Hildebrand (1) apparatus, with all glass pumping system, is used to spray slugs of degassed solvent into the krypton. Amount of gas dissolved is calculated from the initial and final gas pressure.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>Krypton. No source. Manufacturer's research grade, dried over CaCl<sub>2</sub> before use.</li> <li>Perfluorotributylamine. Minnesota Mining &amp; Mfg. Co. Column distilled, used portion with b.p. = 447.85 - 448.64K, &amp; single peak GC.</li> </ol>																
	<p>ESTIMATED ERROR:</p> $\delta N / \text{cal K}^{-1} \text{ mol}^{-1} = 0.1$ $\delta x_1 / x_1 = 0.002$																
	<p>REFERENCES:</p> <ol style="list-style-type: none"> <li>Dymond, J.; Hildebrand, J.H. <u>Ind. Eng. Chem. Fundam.</u> 1967, <u>6</u>, 130.</li> </ol>																

<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 $^{85}\text{Kr}$ ; 13983-27-2 2. Carbon Dioxide; $\text{CO}_2$ ; 124-38-9	<b>ORIGINAL MEASUREMENTS:</b> Notz, K. J.; Meservey, A. B.  ORNL-5121, June 1976 <u>Chem. Abstr.</u> 1977, <u>86</u> , 61170c, 79549t																																												
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<b>METHOD:</b> Tracer technique. Collimated counter with equilibrated gas-liquid samples. Krypton gas was 5 per cent $^{85}\text{Krypton}$ and 95 per cent stable Kr. The total pressure of the system was the equilibrium pressure of liquid $\text{CO}_2$ + the Kr pressure.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton. Cryogenic Rare Gas Labs. Ultra high purity grade. Krypton-85. Isotopes Div., ORNL. 2. Carbon dioxide. Matheson Co., Inc. Research grade.																																												
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<b>EXPERIMENTAL VALUES:</b>  Smoothed Data: $\ln X_1 = 41.5327 - 65.4529/(T/100) - 67.2463 \ln (T/100) + 16.4072 (T/100)$  Std. error about regression line $5.429 \times 10^{-3}$ .																																																													
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<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Carbon Disulfide; CS <sub>2</sub> ; 75-15-0	<b>ORIGINAL MEASUREMENTS:</b> Powell, R.J.  <u>J. Chem. Eng. Data</u> 1972, <u>17</u> , 302-304.																
<b>VARIABLES:</b> T/K: 298.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> P.L. Long																
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<p>The author implies that solubility measurements were made between 273.15 and 308.15 K, but only the solubility at 298.15 was given in the paper. The slope <math>R(\Delta \log x_1 / \Delta \log T)</math> was given. The smoothed data below were calculated by the compiler from the slope in the form:</p> $\log x_1 = \log(1.756 \times 10^3) + (-7.30/R) \log(T/298.15)$ <p>with <math>R = 1.9872 \text{ cal K}^{-1} \text{ mol}^{-1}</math>.</p>																	
<b>Smoothed Data:</b>	<table border="1" data-bbox="542 915 830 1179"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^3</math></th> </tr> </thead> <tbody> <tr><td>273.15</td><td>2.422</td></tr> <tr><td>278.15</td><td>2.266</td></tr> <tr><td>283.15</td><td>2.122</td></tr> <tr><td>288.15</td><td>1.980</td></tr> <tr><td>293.15</td><td>1.868</td></tr> <tr><td>298.15</td><td>1.756</td></tr> <tr><td>303.15</td><td>1.652</td></tr> </tbody> </table>	T/K	Mol Fraction $x_1 \times 10^3$	273.15	2.422	278.15	2.266	283.15	2.122	288.15	1.980	293.15	1.868	298.15	1.756	303.15	1.652
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<b>METHOD / APPARATUS / PROCEDURE:</b> <p>Solvent is degassed by freezing and pumping, then boiling under reduced pressure. The Dymond and Hildebrand (1) apparatus, with all glass pumping system, is used to spray slugs of degassed solvent into the krypton. Amount of gas dissolved is calculated from the initial and final gas pressures.</p>	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton. No source. Manufacturer's research grade, dried over CaCl <sub>2</sub> before use. 2. Carbon disulfide. No source given. Manufacturer's spectrochemical grade.  <b>ESTIMATED ERROR:</b> $\delta N / \text{cal K}^{-1} \text{ mol}^{-1} = 0.1$ $\delta x_1 / x_1 = 0.002$  <b>REFERENCES:</b> 1. Dymond, J.; Hildebrand, J.H. <u>Ind. Eng. Chem. Fundam.</u> 1967, <u>6</u> , 130.																

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Krypton, Kr; 7439-90-9</li> <li>Sulfinylbismethane (Dimethyl Sulfoxide); C<sub>2</sub>H<sub>6</sub>OS (CH<sub>3</sub>SOCH<sub>3</sub>); 67-68-5</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Dymond, J. H.</p> <p><u>J. Phys. Chem.</u> 1967, <u>71</u>, 1829-1831.</p>								
<p>VARIABLES:</p> <p>T/K: 298.15 P/kPa: 101.325 (1 atm)</p>	<p>PREPARED BY:</p> <p>M. E. Derrick</p>								
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<p>AUXILIARY INFORMATION</p>									
<p>METHOD /APPARATUS/PROCEDURE:</p> <p>The liquid is saturated with the gas at a gas partial pressure of 1 atm.</p> <p>The apparatus is that described by Dymond and Hildebrand (1). The apparatus uses an all-glass pumping system to spray slugs of degassed solvent into the gas. The amount of gas dissolved is calculated from the initial and final gas pressure.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>Krypton. Matheson Co. Dried.</li> <li>Dimethyl Sulfoxide. Matheson, Coleman, and Bell Co. Spectro-quality reagent, dried, and a fraction frozen out. Melting pt. 18.37° C.</li> </ol> <p>ESTIMATED ERROR:</p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>Dymond, J.; Hildebrand, J. H. <u>Ind. Eng. Chem. Fundam.</u> 1967, <u>6</u>, 130.</li> </ol>								

<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Nitrous Oxide; N <sub>2</sub> O; 10024-97-2		<b>ORIGINAL MEASUREMENTS:</b> Steinberg, M.; Manowitz, B.; Pruzansky, J.  US AEC BNL-542 (T-140). <u>Chem. Abstr.</u> 1959, <u>53</u> , 21242g.			
<b>VARIABLES:</b>  T/K: 190.15 - 243.65		<b>PREPARED BY:</b>  H. L. Clever			
<b>EXPERIMENTAL VALUES:</b>					
T/K	Absorption Coefficient	Henry's Constant K/atm	Mol Fraction X <sub>1</sub> × 10 <sup>2</sup>	Bunsen Coefficient α	Ostwald Coefficient L
190.15	8.7	-	1.30	8.2	5.7
193.15	8.5	-	1.30	8.1	5.7
201.15	-	88	1.14	-	-
215.15	5.0	-	0.79 <sub>5</sub>	4.7	3.7
236.15	3.8	-	0.64 <sub>5</sub>	3.6	3.1
240.15	-	155	0.64 <sub>5</sub>	-	-
243.65	-	165	0.60 <sub>5</sub>	-	-
Smoothed Data: $\Delta G^{\circ}/J \text{ mol}^{-1} = -RT \ln X_1 = -5,741.0 + 66.134 T$ Std. Dev. $\Delta G^{\circ} = 85.4$ , Coef. Corr. = 0.9984 $\Delta H^{\circ}/J \text{ mol}^{-1} = -5,741.0$ , $\Delta S^{\circ}/J \text{ K}^{-1} \text{ mol}^{-1} = -66.134$					
T/K	Mol Fraction X <sub>1</sub> × 10 <sup>2</sup>	$\Delta G^{\circ}/J \text{ mol}^{-1}$			
193.15	1.25	7,032.8			
203.15	1.05	7,694.1			
213.15	0.896	8,355.4			
223.15	0.775	9,016.8			
233.15	0.679	9,678.1			
243.15	0.601	10,339			
<b>AUXILIARY INFORMATION</b>					
<b>METHOD/APPARATUS/PROCEDURE:</b> Dynamic tracer technique (1).  The Henry's constant is  $K = (P/\text{atm})/X_1$  The Henry's constants may be from data smoothed by the authors.  The report is discussed further in a later paper (2).			<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton. 2. Nitrous oxide.  No information on either component.		
			<b>ESTIMATED ERROR:</b>  $\delta X/X = 0.03 - 0.05$ (Compiler)		
			<b>REFERENCES:</b> 1. Steinberg, M.; Manowitz, B. <u>Ind. Eng. Chem.</u> 1959, <u>51</u> , 47. 2. Steinberg, M. US AEC TID-7593, 1959, 217-218. <u>Chem. Abstr.</u> 1961, <u>55</u> , 9083e.		



<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Nitromethane; CH <sub>3</sub> NO <sub>2</sub> ; 75-52-5	<b>ORIGINAL MEASUREMENTS:</b> Friedman, H.L.  J. Am. Chem. Soc. 1954, <u>76</u> , 3294-3297.												
<b>VARIABLES:</b> T/K: 298.00 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> P.L. Long												
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="347 502 1021 691" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">T/K</th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Mol Fraction <math>X_1 \times 10^3</math></th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Bunsen Coefficient <math>\alpha</math></th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td style="border-bottom: 1px solid black;">298.00</td> <td style="border-bottom: 1px solid black;"></td> <td style="border-bottom: 1px solid black;"></td> <td style="border-bottom: 1px solid black;">0.381 0.378</td> </tr> <tr> <td style="border-bottom: 1px solid black;"></td> <td style="border-bottom: 1px solid black;">0.838</td> <td style="border-bottom: 1px solid black;">0.348</td> <td style="border-bottom: 1px solid black;">0.380 av.</td> </tr> </tbody> </table> <p>The author reports Ostwald coefficients measured at about 700 mmHg. The Bunsen coefficient and the mole fraction solubility at 101.325 kPa (1 atm) were calculated by the compiler with the assumptions that the gas is ideal, that Henry's law is obeyed, and that the Ostwald coefficient is independent of pressure.</p>		T/K	Mol Fraction $X_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	298.00			0.381 0.378		0.838	0.348	0.380 av.
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<b>AUXILIARY INFORMATION</b>													
<b>METHOD:</b> Gas absorption. The method was essentially that employed by Eucken and Herzberg (1). Modifications included a magnetic stirring device instead of shaking the saturation vessel, and balancing the gas pressure against a column of mercury with electrical contacts instead of balancing the gas pressure against the atmosphere.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton. Air Reduction Co. Reagent grade, 99.8 per cent pure by mass spectroscopy. 2. Nitromethane. Source not given. Distilled, dried by filtering at 253 K.												
<b>APPARATUS/PROCEDURE:</b> The solvent was degassed by vacuum. The procedure, repeated 5-10 times, was to alternate 5-15 s evacuation and rapid stirring to produce cavitation. In the solubility measurement, gas, pre-saturated with solvent vapor, was brought into contact with about 80 ml of solvent in the saturation vessel. Initial conditions were established by a time extrapolation. Solubility equilibrium was approached from both under- and supersaturation by varying the rate.	<b>ESTIMATED ERROR:</b> $\delta T/K = 0.05$ $\delta P/\text{mmHg} = 0.3$ $\delta L/L = 0.03$  <b>REFERENCES:</b> 1. Eucken, A.; Herzberg, G. <u>Z. Phys. Chem.</u> 1950, <u>195</u> , 1.												

<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Nitrobenzene; C <sub>6</sub> H <sub>5</sub> NO <sub>2</sub> ; 98-95-3	<b>ORIGINAL MEASUREMENTS:</b> Saylor, J.H.; Battino, R.  <u>J. Phys. Chem.</u> 1958, <u>62</u> , 1334-1337.																																																		
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<b>METHOD/APPARATUS/PROCEDURE:</b> <p>The solvent was degassed by evacuating the space above it, shaking, and then passing it as a fine mist into another evacuated container. The degassed liquid was saturated as it passed as a thin film inside a glass helix which contained the solute gas plus solvent vapor at a total pressure of 1 atm (1,2). The volume of the liquid and the volume of gas absorbed were determined in a system of burets.</p>	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton. Linde Air Products Co. 2. Nitrobenzene. Eastman Kodak white label. Distilled from P <sub>4</sub> O <sub>10</sub> , b.p. 81.0 - 81.2°C (10 mmHg).  <b>ESTIMATED ERROR:</b> $\delta T / \text{K} = 0.03$ $\delta P / \text{mmHg} = 1.0$ $\delta X_1 / X_1 = 0.005$ (authors)  <b>REFERENCES:</b> 1. Morrison, T.J.; Billett, F. <u>J. Chem. Soc.</u> 1948, 2033. 2. Clever, H.L.; Battino, R.; Saylor, J.H.; Gross, P.M. <u>J. Phys. Chem.</u> 1957, <u>61</u> , 1078.																																																		

<p>COMPONENTS:</p> <p>1. Krypton; Kr; 7439-90-9</p> <p>2. Ammonia; NH<sub>3</sub>; 7664-41-7</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Michels, A., Dumoulin, E. and Van Dijk, J. J. Th., <i>Physica</i>, <u>1959</u>, 25, 840.</p>																						
<p>VARIABLES:</p> <p>Temperature, pressure</p>	<p>PREPARED BY:</p> <p>C. L. Young</p>																						
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="85 497 699 854"> <thead> <tr> <th>T/K</th> <th>P/bar</th> <th>Mole fraction of krypton in liquid, <math>x_{Kr}</math></th> </tr> </thead> <tbody> <tr> <td rowspan="3">253.05</td> <td>25.414</td> <td>0.0066</td> </tr> <tr> <td>50.702</td> <td>0.0120</td> </tr> <tr> <td>101.421</td> <td>0.0182</td> </tr> <tr> <td rowspan="4">268.05</td> <td>203.103</td> <td>0.0239</td> </tr> <tr> <td>25.447</td> <td>0.0067</td> </tr> <tr> <td>50.741</td> <td>0.0147</td> </tr> <tr> <td>101.421</td> <td>0.0259</td> </tr> <tr> <td></td> <td>177.405</td> <td>0.0330</td> </tr> </tbody> </table>		T/K	P/bar	Mole fraction of krypton in liquid, $x_{Kr}$	253.05	25.414	0.0066	50.702	0.0120	101.421	0.0182	268.05	203.103	0.0239	25.447	0.0067	50.741	0.0147	101.421	0.0259		177.405	0.0330
T/K	P/bar	Mole fraction of krypton in liquid, $x_{Kr}$																					
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<p>AUXILIARY INFORMATION</p>																							
<p>METHOD / APPARATUS / PROCEDURE:</p> <p>One pass flow method. Ammonia added to equilibrium cell. Krypton passed through liquid ammonia for many hours. Sample of gas and liquid analysed at atmospheric pressure by adsorbing ammonia in sulfuric acid. Details in source.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>No details given.</p> <p>ESTIMATED ERROR:  <math>\delta T/K = \pm 0.1</math>; <math>\delta P/\text{bar} = \pm 0.005</math>;  <math>\delta x_{Ar} = \delta y_{Ar} = \pm 0.5\%</math>.</p> <p>REFERENCES:</p>																						

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>1. Krypton; Kr; 7439-90-9</li> <li>2. Phosphoric Acid, Tris(methyl phenyl) Ester (Tricresyl Phosphate); <math>C_{21}H_{21}O_4P</math>; 1330-78-5</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Körösy, F.</p> <p><u>Trans. Faraday Soc.</u> 1937, <u>33</u>,416-425.</p>								
<p>VARIABLES:</p> <p>T/K: 295.15 P/kPa: 101.325 (1 atm)</p>	<p>PREPARED BY:</p> <p>H. L. Clever</p>								
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="397 514 1077 675"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>295.15</td> <td>3.3</td> <td>0.21</td> <td>0.23</td> </tr> </tbody> </table> <p>The mole fraction solubility and the Bunsen coefficient were calculated by the compiler. It was assumed that gas behavior is ideal, the Ostwald coefficient is independent of pressure, and that Henry's law is obeyed.</p> <p>An average density of the tricresyl phosphate isomers was used for the mole fraction solubility calculation.</p>		T/K	Mol Fraction $x_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	295.15	3.3	0.21	0.23
T/K	Mol Fraction $x_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L						
295.15	3.3	0.21	0.23						
<p>AUXILIARY INFORMATION</p>									
<p>METHOD:</p> <p>The apparatus and method of Winkler (1) were used. However, the apparatus was usually not thermostated, and degassing was by evacuating and shaking the solvent, not by evacuating and boiling the solvent as was done by Winkler.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>1. Krypton. Source not given. The gas contained 5 % xenon and 1 % non-inert gases.</li> <li>2. Tris (methylphenyl) ester of phosphoric acid. Source not given. Technical grade.</li> </ol>								
<p>APPARATUS/PROCEDURE:</p>	<p>ESTIMATED ERROR:</p> <p><math>\delta x_1/x_1 = 0.05</math></p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>1. Winkler, L. W. <u>Ber.</u> 1891, <u>24</u>, 89.</li> </ol>								

<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Octamethylcyclotetrasiloxane; $C_8H_{24}O_4Si_4$ ; 556-67-2	<b>ORIGINAL MEASUREMENTS:</b> Wilcock, R.J.; McHale, J.L.; Battino, B.; Wilhelm, E.  <u>Fluid Phase Equil.</u> 1978, <u>2</u> , 225-230.								
<b>VARIABLES:</b> T/K: 298.35 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> H.L. Clever								
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="348 493 1016 622"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>298.35</td> <td>12.43</td> <td>0.9019</td> <td>0.9851</td> </tr> </tbody> </table> <p>The solubility value was adjusted to a gas partial pressure of 101.325 kPa by Henry's law.</p> <p>The Bunsen coefficient was calculated by the compiler.</p>		T/K	Mol Fraction $X_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	298.35	12.43	0.9019	0.9851
T/K	Mol Fraction $X_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L						
298.35	12.43	0.9019	0.9851						
<b>AUXILIARY INFORMATION</b>									
<b>METHOD /APPARATUS/PROCEDURE:</b> <p>The apparatus is based on the design of Morrison and Billett (1), and the version used is described by Battino, Evans, and Danforth (2). The degassing apparatus and procedure are described by Battino, Banzhof, Bogan, and Wilhelm (3).</p> <p>Degassing. Up to 500 cm<sup>3</sup> of solvent is placed in a flask of such size that the liquid is about 4 cm deep. The liquid is rapidly stirred, and vacuum is applied intermittently through a liquid N<sub>2</sub> trap until the permanent gas residual pressure drops to 5 microns.</p> <p>Solubility Determination. The degassed solvent is passed in a thin film down a glass spiral tube containing the solute gas plus the solvent vapor at a total pressure of one atm. The volume of gas absorbed is found by difference between the initial and final volumes in the buret system. The solvent is collected in a tared flask and weighed.</p>	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton. Matheson Co., Inc. Minimum per cent purity 99.995. 2. Octamethylcyclotetrasiloxane. General Electric Co. Distilled density of 298.15 K was 0.9500 g cm <sup>-3</sup> .  <b>ESTIMATED ERROR:</b> $\delta T/K = 0.03$ $\delta P/mmHg = 0.5$ $\delta X_1/X_1 = 0.01$  <b>REFERENCES:</b> 1. Morrison, T.J.; Billett, F. J. Chem. Soc. 1948, 2033. 2. Battino, R.; Evans, F.D.; Danforth, W.F. J. Am. Oil Chem. Soc. 1968, 45, 830. 3. Battino, R.; Banzhof, M.; Bogan, M.; Wilhelm, E. Anal. Chem. 1971, 43, 806.								

<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Olive Oil	<b>EVALUATOR:</b> H. L. Clever Chemistry Department Emory University Atlanta, GA 30322 U.S.A.  August 1978
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**CRITICAL EVALUATION:**

The solubility of krypton in olive oil was measured by Lawrence, Loomis, Tobias and Turpin (1) at 295.15 and 310.15 K, by Yeh and Peterson (2) at 298.15, 303.15, 310.15 and 318.15 K, and at 310.15 K by Masson and Taylor (3) and by Kitani (4).

The data were converted to a mole fraction solubility at a partial pressure of krypton of 101.325 kPa (1 atm) assuming that olive oil is 1,2,3-propanetriyl ester of Z-9-octadecenoic acid, or triolein, of molecular weight 885.46. The data from the four laboratories shows considerable scatter. Yeh and Peterson made direct volumetric measurements at atmospheric pressure while the other workers used radiochemical techniques at low krypton partial pressures in the presence of air which can be subject to greater errors than the volumetric method. The data of Yeh and Peterson are internally self-consistent. It was decided to accept the Yeh and Peterson data as the basis of a tentative set of solubility data for krypton in olive oil.

The Yeh and Peterson data were used in a linear regression of a Gibbs energy equation linear in temperature. The tentative values of the thermodynamic changes for the transfer of one mole of krypton from the gas at 101.325 kPa (1 atm) to the hypothetical unit mole fraction solution are

$$\Delta G^{\circ}/J \text{ mol}^{-1} = -RT \ln X_1 = -4,690.4 + 48.782 T$$

$$\text{Std. Dev.} = 5.4, \text{ Coef. Corr.} = 0.9999$$

$$\Delta H^{\circ}/J \text{ mol}^{-1} = -4,690.4, \Delta S^{\circ}/J \text{ K}^{-1} \text{ mol}^{-1} = -48.782$$

A table of tentative mole fraction solubility and Gibbs energy values as a function of temperature appears below.

TABLE 1. The solubility of krypton in olive oil. The tentative values of the mole fraction solubility at a krypton partial pressure of 101.325 kPa (1 atm) and the Gibbs energy change as a function of temperature.

T/K	Mol Fraction $X_1 \times 10^2$	$\Delta G^{\circ}/J \text{ mol}^{-1}$
293.15	1.94	9,610.0
295.15	1.91	9,707.6
298.15	1.88	9,854.0
303.15	1.82	10,098
308.15	1.76 <sub>5</sub>	10,341
310.15	1.74 <sub>5</sub>	10,439
313.15	1.71 <sub>5</sub>	10,586
318.15	1.67 <sub>5</sub>	10,830

Continued on next page.

COMPONENTS: 1. Krypton; Kr; 7439-90-9 2. Olive Oil	EVALUATOR: H. L. Clever Chemistry Department Emory University Atlanta, GA 30322 U.S.A.  August 1978
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## CRITICAL EVALUATION:

Figure 1 shows the per cent deviation of all of the reported mole fraction solubility data from the smoothed data of Yeh and Peterson. Since olive oil is a natural product that may vary somewhat in composition and thus show variation in its solvent capacity, the data sheets on all the workers are included.

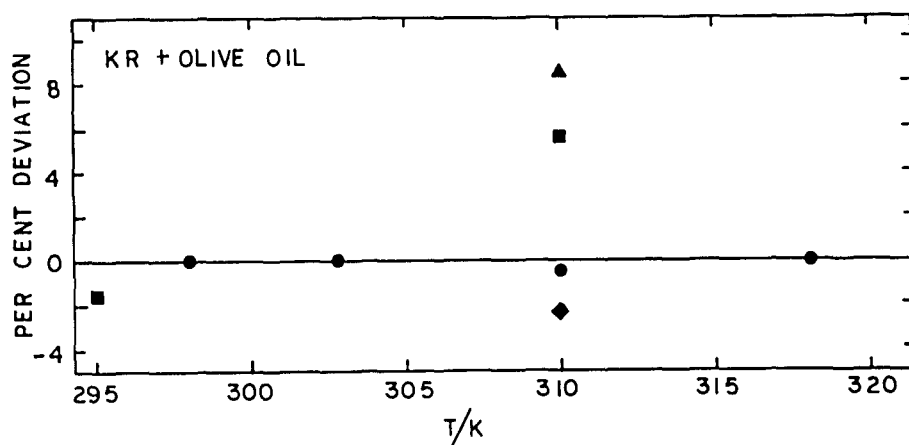


FIGURE 1. Solubility of krypton in olive oil. Percent deviation from regression equation fitted to data of Yeh and Peterson.

● Yeh and Peterson, ■ Lawrence *et al.*,  
 ▲ Masson and Taylor, and ◆ Kitani

## REFERENCES

- Lawrence, J.H.; Loomis, W.F.; Tobias, C.A.; Turpin, F.H. J. Physiol 1946, 105, 197.
- Yeh, S.-Y.; Peterson, R.E. J. Pharm. Sci. 1963, 52, 453.
- Masson, M.B.R.; Taylor, K. Phys. Med. Biol. 1967, 12, 93.
- Kitani, K. Scand. J. Clin. Lab. Invest. 1972, 29, 167.

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Krypton; Kr; 7439-90-9</li> <li>Olive oil</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Lawrence, J. H.; Loomis, W. F.; Tobias, C. A.; Turpin, F. H.</p> <p><u>J. Physiol.</u> 1946, <u>105</u>, 197-204.</p>												
<p>VARIABLES:</p> <p>T/K: 295.15 - 310.15</p>	<p>PREPARED BY:</p> <p>H. L. Clever A. L. Cramer</p>												
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="400 508 1105 677"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^2</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>295.15</td> <td>1.88</td> <td>0.44</td> <td>0.47<sub>5</sub></td> </tr> <tr> <td>310.15</td> <td>1.85</td> <td>0.43</td> <td>0.49<sub>5</sub></td> </tr> </tbody> </table> <p>The mole fraction solubility and Ostwald coefficients were calculated by the compiler.</p> <p>The molecular weight of olive oil was taken to be 885 and the density was calculated from <math>\rho = 0.9152 - 0.000468t/^{\circ}\text{C}</math> (1) for the mole fraction calculation.</p> <p>See the evaluation sheet for the solubility in olive oil for more information.</p>		T/K	Mol Fraction $X_1 \times 10^2$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	295.15	1.88	0.44	0.47 <sub>5</sub>	310.15	1.85	0.43	0.49 <sub>5</sub>
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<p>AUXILIARY INFORMATION</p>													
<p>METHOD /APPARATUS/PROCEDURE:</p> <p>Radiochemical method. No details of the method given, but authors state they used an isotope of half life 34 hours. Possibly the isotope was krypton-79.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>No information given.</p> <p>ESTIMATED ERROR:</p> <p><math>\delta\alpha/\alpha = 0.05</math> (Compiler)</p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>Battino, R.; Evans, F. D.; Danforth, W. F. <u>J. Am. Oil Chem. Soc.</u> 1968, <u>45</u>, 830.</li> </ol>												



<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Olive Oil (1)	<b>ORIGINAL MEASUREMENTS:</b> Yeh, S.Y.; Peterson, R.E.  <u>J. Pharm. Sci.</u> 1963, <u>52</u> , 453-458.																				
<b>VARIABLES:</b> T/K: 298.15 - 318.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> H.L. Clever																				
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<p>The Bunsen coefficients are the average of three measurements. The Ostwald coefficients were fitted by the method of least squares to the equation <math>\log L = A/T + B</math> by the authors. The same line fitted olive oil and the fats. From the slope and intercept they obtained</p>																					
$\Delta H^\circ = (-1185 \pm 46) \text{ cal mol}^{-1} \text{ and } \Delta S^\circ = (-5.6 \pm 0.1) \text{ cal K}^{-1} \text{ mol}^{-1}$																					
<p>The thermodynamic values are for the standard state transfer of one mole of krypton from the gas phase at a concentration of one mole <math>\text{dm}^{-3}</math> to the solution at a concentration of one mole <math>\text{dm}^{-3}</math>. See the evaluation of the krypton + olive oil system on pages 108-109 for the thermodynamic values of the standard state transfer on one mole of krypton from the gas phase at a partial pressure of one atm to the hypothetical unit mole fraction solution.</p>																					
<b>AUXILIARY INFORMATION</b>																					
<b>METHOD / APPARATUS / PROCEDURE:</b> <p>Oil was dried and degassed by stirring under vacuum at 80°C for about 12 hr. A 50 ml. sample was placed in an absorption flask attached to a Geffken gas buret (1). The oil was constantly stirred and equilibrated with increments of gas until no change was observed in a differential oil manometer for <math>\frac{1}{2}</math> hr. Difference between initial and final buret readings indicated amount of gas absorbed. Absorption at successively lower temperatures was determined. The authors also measured the viscosity and surface tension of the liquid.</p>	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton. Matheson Co., Research grade, maximum impurity 0.04 mole per cent $\text{N}_2$ and Xe. 2. Olive Oil. Magnus, Mabee and Raynard Co., U.S.P.  <b>ESTIMATED ERROR:</b> $\delta T/K = 0.05$ $\delta P/\text{mmHg} = 0.5$ $\delta \alpha/\alpha = 0.005$  <b>REFERENCES:</b> 1. Geffken, G. <u>Z. Physik Chem.</u> 1904, <u>49</u> , 257.																				

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Krypton-85; <math>^{85}\text{Kr}</math>; 13983-27-2</li> <li>Olive oil</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Masson, M. B. R.; Taylor, K.</p> <p><u>Phys. Med. Biol.</u> 1967, <u>12</u>, 93-98.</p>										
<p>VARIABLES:</p> <p>T/K: 310.15</p>	<p>PREPARED BY:</p> <p>A.L. Cramer</p>										
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="285 506 1218 654"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^2</math></th> <th>Bunsen Coefficient <math>\alpha \pm \text{Std Dev}</math></th> <th>Number of Determinations</th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>310.15</td> <td>1.90</td> <td>0.440 <math>\pm</math> 0.004</td> <td>14</td> <td>0.500</td> </tr> </tbody> </table> <p>The mole fraction solubility and Ostwald coefficient were calculated by the compiler.</p> <p>The molecular weight of olive oil was taken to be 885 and the density was calculated from <math>\rho = 0.9152 - 0.000468t/^\circ\text{C}</math> (1) for the mole fraction calculation.</p> <p>See the evaluation sheet for the solubility in olive oil for more information.</p>		T/K	Mol Fraction $X_1 \times 10^2$	Bunsen Coefficient $\alpha \pm \text{Std Dev}$	Number of Determinations	Ostwald Coefficient L	310.15	1.90	0.440 $\pm$ 0.004	14	0.500
T/K	Mol Fraction $X_1 \times 10^2$	Bunsen Coefficient $\alpha \pm \text{Std Dev}$	Number of Determinations	Ostwald Coefficient L							
310.15	1.90	0.440 $\pm$ 0.004	14	0.500							
<p>AUXILIARY INFORMATION</p>											
<p>METHOD /APPARATUS/PROCEDURE:</p> <p>The olive oil was sprayed into a circulating mixture of krypton-85 and air. The difference between the count rate before and after the solvent was sprayed equals the amount absorbed by the olive oil. The measurement was checked by replacing the radioactive gas by air, recirculating the olive oil and measurement of the increase of radioactivity in the gas phase, which was compared with the original decrease.</p> <p>The sensor was a thallium activated sodium iodide crystal, behind a thin beryllium window.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>Krypton-85. Radiochemical Centre, Amersham, UK.</li> <li>Olive oil. No information given.</li> </ol> <p>ESTIMATED ERROR:</p> <p><math>\delta\alpha/\alpha = 0.03</math> (Compiler)</p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>Battino, R.; Evans, F.D. Danforth, W.F. <u>J. Am. Oil Chem. Soc.</u> 1968, <u>45</u>, 830.</li> </ol>										

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Krypton-85; <math>^{85}\text{Kr}</math>; 13983-27-2</li> <li>Olive Oil</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Kitani, K.</p> <p><u>Scand. J. Clin. Lab. Invest.</u> 1972, <u>29</u>, 167-172.</p>										
<p>VARIABLES:</p> <p>T/K: 310.15</p>	<p>PREPARED BY:</p> <p>P.L. Long A.L. Cramer</p>										
<p>EXPERIMENTAL VALUES:</p>											
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T/K	Mol Fraction $x_1 \times 10^2$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L $\pm$ Std Dev	Number of Determinations							
310.15	1.71	0.397	0.451 $\pm$ 0.015	19							
<p>AUXILIARY INFORMATION</p>											
<p>METHOD /APPARATUS/PROCEDURE:</p> <p>Glass cuvettes were filled with the solvent. One-third was replaced by the radioactive gas and air. The sealed cuvette was rotated for two hours in a water bath at <math>37^\circ\text{C}</math>. The total pressure was adjusted to one atm by means of a thin needle. Samples from both the liquid and gas phase were counted by a scintillation detector and a Phillips pulse-height analyzer at the energy peak. Corrections for self absorption and scatter were made.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>Krypton-85. Radiochemical Centre, Amersham, UK.</li> <li>Olive oil. Commercial sample.</li> </ol> <p>ESTIMATED ERROR:</p> <p style="text-align: center;"><math>\delta L/L = 0.03</math></p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>Battino, R.; Evans, F.D.; Danforth, W.F. <u>J. Am. Oil Chem. Soc.</u> 1968, <u>45</u>, 830.</li> </ol>										

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>1. Krypton; Kr; 7439-90-9</li> <li>2. Biological Systems</li> </ol>	<p>EVALUATOR:</p> <p>H. L. Clever  Chemistry Department  Emory University  Atlanta, GA 30322  U.S.A.</p> <p>September 1978</p>
<p>CRITICAL EVALUATION:</p> <p>The solubility of krypton in biological fluids and tissues.</p> <p>There are several factors that make it difficult to compare and evaluate the solubility of krypton in biological systems. First, the material from biological specimens may show a natural variation in properties which affects the solubility. Second, workers have used quite different experimental techniques to measure the solubility. Some have used classical volumetric methods with the krypton at a partial pressure near atmospheric pressure, many have used radiochemical techniques either with natural krypton tagged with radioactive krypton at a total pressure near atmospheric or with a small unknown partial pressure of radioactive krypton. In neither of the radiochemical techniques is it necessary to know the total pressure to obtain an Ostwald coefficient. However, to compare the results of krypton solubility determinations by the volumetric method and by the radiochemical techniques one must assume the Ostwald coefficient is independent of pressure. This may not be true, especially if the gas associates with one or more components of the biological fluid. In these systems the solubility data are classed as tentative. Below are comments, which compare rather than evaluate, the solubility data in several types of biological systems.</p> <p><b>Fat.</b> Yeh and Peterson (1) found little difference in the solubility of krypton in olive oil, human fat, dog fat and rat fat by a volumetric method. Masson and Taylor (2) used a radiochemical method and obtained solubility values that were eight per cent higher in olive oil and three per cent higher in human fat than Yeh and Peterson's results. The Masson and Taylor method, although elegant, appears to be more subject to error than the Yeh and Peterson technique. The results of the two laboratories probably agree within experimental error. Kirk, Parrish and Morken's (3) results with guinea pig fat are reported on a weight basis. They appear to be of similar magnitude to the solubility found in other fats.</p> <p><b>Blood and blood components.</b> Several studies showed that the solubility of krypton and other gases varies linearly with the percent of either red blood cells, serum albumin, or hemoglobin in blood and in other fluids. The results of these studies are sometimes extrapolated to 100% blood component to obtain the solubility of the gas in that component. Both Hardewig, Rochester and Briscoe (4) and Kitani (5) report a value of the Ostwald coefficient of krypton in human red blood cells. The values agree within 5 per cent. Yeh and Peterson (1) show that 0.075 mole of krypton associates with a mole of human hemoglobin and that 0.2 to 0.05 mole of krypton associate with a mole of human serum albumin at temperatures of 298.15 and 310.15 K respectively. Muehlbaecher, DeBon and Featherstone (6) carried out qualitative experiments that showed that bovine hemoglobin associates with krypton while bovine gamma-globulin and serum albumin apparently do not associate. Kirk, Parrish and Morken (3) reported the solubility of krypton in dog, cat, hamster and guinea pig blood and Strang (7) reported the solubility of krypton in rabbit blood.</p> <p><b>Tissues.</b> The distribution of krypton between the gas phase and the tissue can be measured either with homogenized tissue in a saline or other solution, with solid tissue, or with tissue from an animal sacrificed after breathing air containing krypton. It is likely that the structured tissue interacts somewhat differently with the gas than does the homogenized tissue, but there is not enough data to draw any conclusions about the effect of tissue structure and "solubility". Both Yeh and Peterson (1) and Strang (7) reported on work with rabbit tissues. Kitani (5) reported results with human liver tissues. Kirk, Parrish and Morken (3) reported on a range of guinea pig tissues and guinea pig brain and Yeh and Peterson (1) reported results on beef brain tissues.</p>	

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>1. Krypton; Kr; 7439-90-9</li> <li>2. Biological Systems</li> </ol>	<p>EVALUATOR:</p> <p>H. L. Clever  Chemistry Department  Emory University  Atlanta, GA 30322  U.S.A.</p> <p>September 1978</p>
<p>CRITICAL EVALUATION:</p> <p>In addition there are whole blood tissue coefficients for the partition of krypton between blood and tissue determined incidental to regional blood flow studies. These results could be converted into gas-tissue coefficients using the gas-blood Ostwald coefficients. The tissue-blood partition coefficients for krypton are not given in this compilation. Many are summarized by Kirk, Parrish and Morken (3) from the work of Lassen and Munck (8), Lassen and Ingvar (9), Lassen (10, 11), Ingvar and Lassen (12), Glass and Harper (13), Thornburn, Kopald, Herd, Hollenberg, O'Morchoe, and Barger (14), Friedman, Kopald and Smith (15), Bell and Harper (16), Hollenberg and Dougherty (17), Setchell, Waites and Thorburn (18), and Bell and Battersby (19).</p> <p>REFERENCES</p> <ol style="list-style-type: none"> <li>1. Yeh, S.Y.; Peterson, R.E. <u>J. Pharm. Sci.</u> 1963, <u>52</u>, 453; <u>J. Appl. Physiol.</u> 1965, <u>20</u>, 1041.</li> <li>2. Masson, M.B.R.; Taylor, K. <u>Phys. Med. Biol.</u> 1967, <u>12</u>, 93.</li> <li>3. Kirk, W.P.; Parish, P.W.; Morken, D.A. <u>Health Phys.</u> 1975, <u>28</u>, 249.</li> <li>4. Hardewig, A.; Rochester, D.F.; Briscoe, W.A. <u>J. Appl. Physiol.</u> 1960, <u>15</u>, 723.</li> <li>5. Kitani, K. <u>Scand. J. Clin. Lab. Invest.</u> 1972, <u>29</u>, 167.</li> <li>6. Muehlbaecher, C.; DeBon, F.Z.; Featherstone, R.M. <u>Inst. Anesth. Clinics</u> 1963, <u>1</u>, 937.</li> <li>7. Strang, R. <u>Phys. Med. Biol.</u> 1975, <u>20</u>, 1025.</li> <li>8. Lassen, N.A.; Munck, O. <u>Acta physiol scand.</u> 1955, <u>33</u>, 30.</li> <li>9. Lassen, N.A.; Ingvar, D.H. <u>Experientia</u> 1961, <u>17</u>, 42.</li> <li>10. Lassen, N.A. <u>Minerva Nucl.</u> 1964, <u>8</u>, 211.</li> <li>11. Lassen, N.A. in <u>Radioisotopes in Medical Diagnosis</u>, Belcher, E.H.; Vetter, H. Editors, Appleton-Century-Crofts, 1971.</li> <li>12. Ingvar, D.H.; Lassen, N.A. <u>Acta physiol scand.</u> 1962, <u>54</u>, 325.</li> <li>13. Glass, H.I.; Harper, A.M. <u>Phys. Med. Biol.</u> 1962, <u>7</u>, 335.</li> <li>14. Thornburn, G.D.; Kopald, H.H.; Herd, J.A.; Hollenberg, M.; O'Morchoe, C.C.C.; Barger, A.C. <u>Circulation Res.</u> 1963, <u>13</u>, 290.</li> <li>15. Friedman, E.; Kopald, H.H.; Smith, T.R. <u>Invest. Ophthalmol.</u> 1964, <u>3</u>, 539.</li> <li>16. Bell, G.; Harper, A.M. <u>J. Surg. Res.</u> 1965, <u>5</u>, 382.</li> <li>17. Hollenberg, M.; Dougherty, J. <u>Am. J. Physiol</u> 1966, <u>210</u>, 926.</li> <li>18. Setchell, B.P.; Waites, G.M.H.; Thorburn, G.D. <u>Circulation Res</u> 1966, <u>18</u>, 755.</li> <li>19. Bell, P.R.F.; Battersby, A.C. <u>Surgery</u> 1967, <u>62</u>, 468.</li> </ol>	

COMPONENTS:			ORIGINAL MEASUREMENTS:		
1. Krypton; Kr; 7439-90-9			Yeh, S.Y.; Peterson, R.E.		
2. Human Fat			J. Pharm. Sci. 1963, 52, 453-458.		
VARIABLES:			PREPARED BY:		
T/K: 298.15 - 318.15 P/kPa: 101.325 (1 atm)			H.L. Clever		
EXPERIMENTAL VALUES: Human fat 1			Human fat 2		
T/K	Bunsen Coefficient $\alpha \pm$ Std. Dev.	Ostwald Coefficient L	T/K	Bunsen Coefficient $\alpha \pm$ Std. Dev.	Ostwald Coefficient L
298.15	0.4412 $\pm$ 0.0061	0.4816	298.15	0.4404 $\pm$ 0.0015	0.4807
303.15	0.4258 $\pm$ 0.0012	0.4725	303.15	0.4247 $\pm$ 0.0013	0.4713
310.15	0.4071 $\pm$ 0.0005	0.4626	310.15	0.4062 $\pm$ 0.0004	0.4617
318.15	0.3878 $\pm$ 0.0015	0.4516	318.15	0.3875 $\pm$ 0.0012	0.4513
<p>The Bunsen coefficients are the average of three measurements. The Ostwald coefficients were fitted by the method of least squares to the equation <math>\log L = A/T + B</math> by the authors. The same line fitted olive oil and the fats. From the slope and intercept they obtained</p> $\Delta H^{\circ} = (-1185 \pm 46) \text{ cal mol}^{-1} \text{ and } \Delta S^{\circ} = (-5.6 \pm 0.1) \text{ cal K}^{-1} \text{ mol}^{-1}$ <p>The thermodynamic values are for the transfer of one mole of krypton from the gas phase at a concentration of one mole <math>\text{dm}^{-3}</math> to the solution at a concentration of one mole <math>\text{dm}^{-3}</math>.</p>					
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METHOD /APPARATUS/PROCEDURE:			SOURCE AND PURITY OF MATERIALS:		
<p>Fat was dried and degassed by stirring under vacuum at 80°C for about 12 hr. A 50 ml. sample was placed in an absorption flask attached to a Geffken gas buret (1). The fat was constantly stirred and equilibrated with increments of gas until no change was observed in a differential oil manometer for <math>\frac{1}{2}</math> hr. Difference between initial and final buret readings indicated amount of gas absorbed. Absorption at successively lower temperatures was determined. The authors also measured the viscosity and surface tension of the liquid.</p>			<p>1. Krypton. Matheson Co. Research grade, maximum impurity 0.04 mole per cent <math>\text{N}_2</math> and Xe.</p> <p>2. Human omental fats obtained from two deceased patients (1 and 2). Extracted with petroleum ether (b.p. 309-338 K). The ether was evaporated at 353 K under vacuum for several hours. Stored under refrigeration until use. Fat 2 appeared to have more stearine precipitate than fat 1 at 296 K.</p>		
			ESTIMATED ERROR:		
			$\delta T/K = 0.05$ $\delta P/\text{mmHg} = 0.5$ $\delta \alpha/\alpha = 0.005$		
			REFERENCES:		
			1. Geffken, G. Z. Physik Chem. 1904, 49, 257.		

<b>COMPONENTS:</b> 1. Krypton-85; $^{85}_{36}\text{Kr}$ ; 13983-27-2 2. Human Fat	<b>ORIGINAL MEASUREMENTS:</b> Masson, M.B.R.; Taylor, K.  <u>Phys. Med. Biol.</u> 1967, <u>12</u> , 93-98.															
<b>VARIABLES:</b> T/K: 310.15 Total P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> A.L. Cramer															
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">T/K</th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Bunsen Coefficient <math>\alpha \pm \text{Std. Dev.}</math></th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Number of Determinations</th> </tr> </thead> <tbody> <tr> <td colspan="3" style="text-align: center;">Pooled Fat</td> </tr> <tr> <td style="text-align: center;">310.15</td> <td style="text-align: center;">0.420 <math>\pm</math> 0.006</td> <td style="text-align: center;">16</td> </tr> <tr> <td colspan="3" style="text-align: center;">Abdominal Fat</td> </tr> <tr> <td style="text-align: center;">310.15</td> <td style="text-align: center;">0.414 <math>\pm</math> 0.006</td> <td style="text-align: center;">6</td> </tr> </tbody> </table>		T/K	Bunsen Coefficient $\alpha \pm \text{Std. Dev.}$	Number of Determinations	Pooled Fat			310.15	0.420 $\pm$ 0.006	16	Abdominal Fat			310.15	0.414 $\pm$ 0.006	6
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<b>METHOD / APPARATUS / PROCEDURE:</b> Liquid fat was sprayed into a circulating mixture of $^{85}\text{Kr}$ and air. Difference between count rate in air before and after spraying equals amount absorbed by fat. Then, radioactive gas mixture was replaced by air. The spray pump was re-connected, and increase of count rate in air was compared with original decrease. Sensor was a B-sensitive thallium activated sodium iodide crystal, behind a thin (0.008 in) beryllium window.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton-85. Radiochemical Centre, Amersham, U.K. 2. Fat. Abdominal, perirenal and omental. Heated 50-60°C for 2-3 days; pure lipid filtered off and stored under refrigeration.  <b>ESTIMATED ERROR:</b>  <b>REFERENCES:</b>															

<b>COMPONENTS:</b> 1. Krypton; Kr; 7439-90-9 2. Rat-pooled Fat	<b>ORIGINAL MEASUREMENTS:</b> Yeh, S.Y.; Peterson, R.E.  <u>J. Pharm. Sci.</u> 1963, <u>52</u> , 453-458.															
<b>VARIABLES:</b> T/K: 298.15 - 318.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> H.L. Clever															
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<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Krypton; Kr; 7439-90-9</li> <li>Dog Fat</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Yeh, S.Y.; Peterson, R.E.</p> <p><u>J. Pharm. Sci.</u> 1963, <u>52</u>, 453-458.</p>															
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<p>COMPONENTS:</p> <p>1. Krypton-85; <math>^{85}_{36}\text{Kr}</math>; 13983-27-2</p> <p>2. Blood of Various Animals</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Kirk, W.P.; Parish, P. W.; Morken, D.A.</p> <p><u>Health Phys.</u> 1975, <u>28</u>, 249 - 261.</p>																																																
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<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="387 498 1239 1129"> <thead> <tr> <th>T/K</th> <th>Ostwald Coefficient L <math>\pm</math> Std. Dev.</th> <th>Number of Determinations</th> </tr> </thead> <tbody> <tr> <td colspan="3" style="text-align: center;">Dog blood</td> </tr> <tr> <td>308.65</td> <td>0.0691 <math>\pm</math> 0.0054</td> <td>9</td> </tr> <tr> <td colspan="3" style="text-align: center;">Chinese hamster blood</td> </tr> <tr> <td>310.15</td> <td>0.0822 <math>\pm</math> 0.0014</td> <td>10</td> </tr> <tr> <td colspan="3" style="text-align: center;">Cat blood</td> </tr> <tr> <td>309.15</td> <td>0.0595 <math>\pm</math> 0.0065</td> <td>7</td> </tr> <tr> <td>312.15</td> <td>0.0559 <math>\pm</math> 0.0040</td> <td>8</td> </tr> <tr> <td colspan="3" style="text-align: center;">Guinea pig blood</td> </tr> <tr> <td>309.15</td> <td>0.0546 <math>\pm</math> 0.0076</td> <td>16</td> </tr> <tr> <td>310.15</td> <td>0.0538 <math>\pm</math> 0.0033</td> <td>8</td> </tr> <tr> <td>312.25</td> <td>0.0513 <math>\pm</math> 0.0041</td> <td>8</td> </tr> <tr> <td colspan="3" style="text-align: center;">N,N'-1,2-ethanediy1-bis(N-carboxymethyl)glycine (Ethylenediaminetetraacetic acid or EDTA); <math>\text{C}_{10}\text{H}_{16}\text{N}_2\text{O}_8</math>; 60-00-4. A 10 % solution in water.</td> </tr> <tr> <td>310.15</td> <td>0.0406 <math>\pm</math> 0.0028</td> <td>8</td> </tr> <tr> <td colspan="3" style="text-align: center;">Sodium chloride; NaCl; 7647-14-5. Aqueous soln. 0.9 wt. %</td> </tr> <tr> <td>310.15</td> <td>0.0472 <math>\pm</math> 0.0012</td> <td>4</td> </tr> </tbody> </table> <p>The authors conversion of their experimental data to the Ostwald coefficient assumed that Henry's law is obeyed and the Ostwald coefficient is independent of pressure.</p>		T/K	Ostwald Coefficient L $\pm$ Std. Dev.	Number of Determinations	Dog blood			308.65	0.0691 $\pm$ 0.0054	9	Chinese hamster blood			310.15	0.0822 $\pm$ 0.0014	10	Cat blood			309.15	0.0595 $\pm$ 0.0065	7	312.15	0.0559 $\pm$ 0.0040	8	Guinea pig blood			309.15	0.0546 $\pm$ 0.0076	16	310.15	0.0538 $\pm$ 0.0033	8	312.25	0.0513 $\pm$ 0.0041	8	N,N'-1,2-ethanediy1-bis(N-carboxymethyl)glycine (Ethylenediaminetetraacetic acid or EDTA); $\text{C}_{10}\text{H}_{16}\text{N}_2\text{O}_8$ ; 60-00-4. A 10 % solution in water.			310.15	0.0406 $\pm$ 0.0028	8	Sodium chloride; NaCl; 7647-14-5. Aqueous soln. 0.9 wt. %			310.15	0.0472 $\pm$ 0.0012	4
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<p>APPARATUS/PROCEDURE:</p> <p>The authors fitted the Ostwald coefficients in Guinea pig blood to the equation</p> $\log L = -4.1378 + 889.2/T$ <p>(r = 0.994)</p>	<p>ESTIMATED ERROR:</p> $\delta L/L = 0.02 - 0.14$ <p>REFERENCES:</p>																																																

COMPONENTS:		ORIGINAL MEASUREMENTS:			
1. Krypton; Kr; 7439-90-9		Yeh, S.-Y.; Peterson, R. E.			
2. Water; H <sub>2</sub> O; 7732-18-5		J. <u>Appl. Physiol.</u> 1965, <u>20</u> , 1041-1047.			
3. Sodium Chloride; NaCl; 7647-14-5					
4. Human Albumin; 9048-46-8					
VARIABLES: T/K: 298.15 - 310.15 P/kPa: 101.325 (1 atm) Albumin/wt %: 5.2 - 25.3		PREPARED BY:  A. L. Cramer H. L. Clever			
EXPERIMENTAL VALUES:					
T/K	Albumin wt %	Mol Fraction $X_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L $\pm$ Std. Dev.	Number of Determinations.
298.15	5.2		0.0503	0.0549 $\pm$ 0.0008	6
303.15			0.0446	0.0495 $\pm$ 0.0008	6
310.15			0.0380	0.0431 $\pm$ 0.0008	5
298.15	15.4		0.0504	0.0550 $\pm$ 0.0023	5
303.15			0.0437	0.0485 $\pm$ 0.0015	5
310.15			0.0358	0.0406 $\pm$ 0.0018	5
298.15	25.3		0.0507	0.0553 $\pm$ 0.0006	3
303.15			0.0427	0.0474 $\pm$ 0.0009	3
310.15			0.0336	0.0381 $\pm$ 0.0007	3
298.15	100	161.1	0.0572	0.0624	
303.15		108.7	0.0371	0.0412	
310.15		48.5	0.0172	0.0195	
The Ostwald coefficients in 100 % human albumin were values extrapolated from the values at lower concentration by the authors. The Bunsen coefficients and the mole fraction solubilities were calculated by the compiler. The authors used an albumin molecular weight of 69,000 and a density of 1.0 to calculate the mole ratio of krypton to albumin of 0.192, 0.122, and 0.051 at 298.15, 303.15, and 310.15 K, respectively.					
AUXILIARY INFORMATION					
METHOD:		SOURCE AND PURITY OF MATERIALS:			
A 45 cm <sup>3</sup> sample of albumin in standard saline solution was frozen, evacuated, and melted repeatedly until no bubbles appeared in the liquid under vacuum in the Yeh and Peterson modification (1) of the Geffcken apparatus (2). Equilibration with gas and measurement of the solubility followed.		1. Krypton. The Matheson Co. Research grade with maximum impurity of 0.04 % N <sub>2</sub> and O <sub>2</sub> .			
		2. Serum albumin solution. Cutter Laboratories. A 25 % solution stabilized with 0.02 M sodium caprylate and 0.02 M sodium acetyltryptophanate.			
APPARATUS/PROCEDURE:		ESTIMATED ERROR:			
		$\delta T/K = 0.05$ $\delta P/\text{mmHg} = 0.2$ $\delta L/L = 0.0015$			
		REFERENCES:			
		1. Yeh, S.-Y.; Peterson, R. E. <u>J. Pharm. Sci.</u> 1963, <u>52</u> , 453.			
		2. Geffcken, G. <u>Z. Phys. Chem.</u> 1904, <u>49</u> , 257.			

<b>COMPONENTS:</b> 1. Krypton-85; $^{85}_{36}\text{Kr}$ ; 13983-27-2 2. Rabbit Tissues	<b>ORIGINAL MEASUREMENTS:</b> Strang, R.  <u>Phys. Med. Biol.</u> 1975, <u>20</u> , 1025-1028.																																		
<b>VARIABLES:</b> T/K: 310.15 P/kPa: 101.325 (1 atm) Time/hr: 0.5 - 24	<b>PREPARED BY:</b>  A.L. Cramer																																		
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<b>METHOD:</b> The method of Ladefoged and Anderson (1), modified to exclude rubber stoppers, was used. Tissue was equilibrated with $^{85}\text{Kr}$ at 310.15 K for 0.5, 1, 2, 3, 4, 5, and 24 hours. Radioactivity was determined in a well scintillation counter for tissue samples alone and for sample + gas at the end of equilibration. The uptake of gas did not vary significantly with the time of equilibration. Transfer loss was less than 10%.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton. No information given. 2. Choroid, retina, and sclera. Freshly enucleated eyes dissected under saline to obtain 0.015 - 0.05 g samples.																																		
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<p>METHOD /APPARATUS/PROCEDURE:</p> <p>In Yeh &amp; Peterson (1) modification of Geffcken (2) apparatus, 45 ml of liquid is frozen, evacuated, and melted repeatedly until no bubbles appeared in liquid under vacuum.</p> <p>Equilibration with gas and measurement of solubility followed (1).</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>1. Krypton. The Matheson Co. Research grade, maximum impurity 0.04% nitrogen and/or oxygen.</li> <li>2. Rabbit leg muscle, homogenized with 4x its volume normal saline, and 0.05% "mercury chloride" added as microbial poison.</li> </ol> <p>ESTIMATED ERROR:</p> <p><math>\delta T/K = 0.005</math> <math>\delta P/mmHg = 0.2</math> <math>\delta L/L = 0.05</math></p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>1. Yeh, S-Y.; Peterson, R.E. <u>J. Pharm. Sci.</u> 1963, <u>52</u>, 453.</li> <li>2. Geffcken, G. <u>Z. Physik Chem.</u> 1904, <u>49</u>, 257.</li> </ol>																

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<b>VARIABLES:</b> T/K: 310.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> A.L. Cramer

**EXPERIMENTAL VALUES:**  $^{85}\text{Kr}$  weight partition coefficients for guinea pig tissues.  
**TABLE.** In vivo  $^{85}\text{Kr}$  weight partition coefficients for guinea pig tissues.

T/K	Tissue	Number of Samples	Whole Tissue $L_w \pm \text{Std. Dev.}$	Bloodless Tissue $L_w \pm \text{Std. Dev.}$
310.15	Omental fat	17	0.391 $\pm$ 0.059	0.421 $\pm$ 0.064
	Subcutaneous fat	16	0.380 $\pm$ 0.081	0.405 $\pm$ 0.090
	Lungs (see note (1))	4	0.240 $\pm$ 0.088	0.274 $\pm$ 0.166
	Thymus	6	0.228 $\pm$ 0.114	0.259 $\pm$ 0.132
	Lymph nodes	8	0.126 $\pm$ 0.064	0.138 $\pm$ 0.075
	Bone marrow	15	0.118 $\pm$ 0.093	0.134 $\pm$ 0.119
	Adrenals	18	0.0939 $\pm$ 0.0318	0.102 $\pm$ 0.038
	Thyroid	9	0.0799 $\pm$ 0.0313	0.0829 $\pm$ 0.0373
	Liver	9	0.0713 $\pm$ 0.0214	0.0768 $\pm$ 0.0281
	Large intestine	9	0.0734 $\pm$ 0.0402	0.0744 $\pm$ 0.0423
	Small intestine	9	0.0715 $\pm$ 0.0384	0.0722 $\pm$ 0.0391

Note: (1)  $L_w$  is not a valid measurement in lungs because of  $^{85}\text{Kr}$  in air spaces.

#### AUXILIARY INFORMATION

<b>METHOD / APPARATUS / PROCEDURE:</b> The guinea pig is enclosed in monitored air with $^{85}\text{Kr}$ for 6 hr (1); 15 min before sacrifice, $^{131}\text{I}$ -tagged albumin (2) is injected to indicate the amount of blood in the tissue. Sacrifice, necropsy, and radioactive count at $^{85}\text{Kr}$ level and $^{131}\text{I}$ level determine the uptake of gas in the tissue.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton. No information given. The $^{85}\text{Kr}$ + air mixture had a count of 0.9 $\mu\text{Ci cm}^{-3}$ . 2. Guinea pigs. Duncan-Hartley random bred. 700-1000 g, from commercial suppliers or bred in laboratory.
	<b>ESTIMATED ERROR:</b> $\delta L/L = 0.13$ (blood) - 0.89 (bone marrow)
	<b>REFERENCES:</b> 1. Glass, H.I.; Harper, A.M. <u>Phys. Med. Biol.</u> 1962, <u>7</u> , 335. 2. McCall, M.S.; Camp, M.F. <u>J. Lab. Clin. Med.</u> 1961, <u>58</u> , 772.

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	Uterus	4	0.0426 $\pm$ 0.0125	0.0418 $\pm$ 0.0127																																																			
	Stomach	10	0.0420 $\pm$ 0.0191	0.0415 $\pm$ 0.0206																																																			
	Brain	19	0.0410 $\pm$ 0.0162	0.0405 $\pm$ 0.0167																																																			
	Eyes (whole)	8	0.0404 $\pm$ 0.0127	0.0402 $\pm$ 0.0128																																																			
	Muscle	15	0.0402 $\pm$ 0.0169	0.0396 $\pm$ 0.0173																																																			
	Seminal vesicles	2	0.0374 $\pm$ 0.0066	0.0369 $\pm$ 0.0068																																																			
	Spleen	9	0.0352 $\pm$ 0.0144	0.0365 $\pm$ 0.0090																																																			
	Heart	8	0.0347 $\pm$ 0.0129	0.0300 $\pm$ 0.0148																																																			
<b>Note:</b> (2) Weighted average. The number of samples per animal ranged from 1 to 3. The total number of samples is in parentheses.																																																							
<b>AUXILIARY INFORMATION</b>																																																							
<b>METHOD / APPARATUS / PROCEDURE:</b> See preceding page.	<b>SOURCE AND PURITY OF MATERIALS:</b> See preceding page.  <b>ESTIMATED ERROR:</b> See preceding page.  <b>REFERENCES:</b> See preceding page.																																																						

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Krypton-85; <math>^{85}_{36}\text{Kr}</math>; 13983-27-2</li> <li>Human Liver Tissue</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Kitani, K.; Winkler, K.</p> <p><u>Scand. J. Clin. Lab. Invest.</u> 1972, <u>29</u>, 173-176.</p>
<p>VARIABLES:</p> <p>T/K: 310.15</p>	<p>PREPARED BY:</p> <p>A.L. Cramer</p>
<p>EXPERIMENTAL VALUES:</p> <p>Thirty three measurements of the solubility of krypton-85 were made in liver tissue with triglyceride content varying between 1 and 20 weight per cent. One measurement was made at 50 weight percent triglyceride. The results were given in a graph. The data fitted the regression equation</p> $L = 0.04924 + (0.004072) (\text{triglyceride wt } \%)$ <p>with a regression coefficient of 0.98.</p> <p>The triglyceride weight per cent was calculated as tripalmitin. The tissue solubility was corrected for the water added to the sample. Below a liver triglyceride content of 5 per cent the standard deviation was 0.7 per cent, at higher triglyceride content the standard error increases, and reaches a value of 5 per cent at 25 per cent triglyceride.</p> <p>Tripalmitin is hexadecanoic acid, 1,2,3-propanetriyl ester; <math>\text{C}_{51}\text{H}_{98}\text{O}_6</math>; 555-44-2.</p>	
<p>AUXILIARY INFORMATION</p>	
<p>METHOD /APPARATUS/PROCEDURE:</p> <p>Five g of liver tissue was homogenized at 277 K for 15 m after addition of 5 cm<sup>3</sup> of water. A glass cuvette (1 x 1 x 10 cm) was 2/3 filled with the homogenate, and closed with a rubber stopper. The space above the homogenate was evacuated and filled with air containing krypton-85. The cuvette was rotated for 2 h in a water bath at 310 K. The radioactivity in the homogenate and in the air phase were determined by a scintillation counter placed in a thermostated box at 310 K (1).</p> <p>The triglyceride was determined enzymatically in chloroform-methanol extracts.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>Krypton-85. Radiochemical Centre, Amersham, U.K.</li> <li>Liver tissue. Autopsy material.</li> </ol> <p>ESTIMATED ERROR:</p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>Kitani, K. <u>Scand. J. Clin. Lab. Invest.</u> 1972, <u>29</u>, 167.</li> </ol>

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>1. Krypton; Kr; 7439-90-9</li> <li>2. Water; H<sub>2</sub>O; 7732-18-5</li> <li>3. Sodium chloride, NaCl; 7647-14-5</li> <li>4. Beef brain</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Yeh, S-Y; Peterson, R.E.</p> <p><u>J. Appl. Physiol.</u> 1965, <u>20</u>, 1041-1047.</p>																
<p>VARIABLES:</p> <p>T/K: 298.15 - 310.15</p> <p>P/kPa: 101.325 (1 atm)</p>	<p>PREPARED BY:</p> <p>A.L. Cramer</p>																
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="294 493 1152 685"> <thead> <tr> <th>T/K</th> <th>Absorption Coefficient mean <math>\beta \pm</math> Std. Dev.</th> <th>Number of Determinations</th> <th>cm<sup>3</sup> Kr g<sup>-1</sup> muscle*</th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>0.0572 <math>\pm</math> 0.0017</td> <td>3</td> <td>-</td> </tr> <tr> <td>303.15</td> <td>0.0517 <math>\pm</math> 0.0020</td> <td>3</td> <td>-</td> </tr> <tr> <td>310.15</td> <td>0.0454 <math>\pm</math> 0.0020</td> <td>3</td> <td>0.066 - 0.072</td> </tr> </tbody> </table> <p>*Calculated by the authors. They corrected for dilution with saline solution and assumed a brain specific gravity of 1.04. The range of values reflects the range of lipid, water, and protein content found by analysis of their samples.</p>		T/K	Absorption Coefficient mean $\beta \pm$ Std. Dev.	Number of Determinations	cm <sup>3</sup> Kr g <sup>-1</sup> muscle*	298.15	0.0572 $\pm$ 0.0017	3	-	303.15	0.0517 $\pm$ 0.0020	3	-	310.15	0.0454 $\pm$ 0.0020	3	0.066 - 0.072
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<p>METHOD</p> <p>In Yeh and Peterson (1) modification of Geffcken (2) apparatus, 45 ml of liquid homogenate is frozen, evacuated, and melted repeatedly until no bubbles appear in liquid under vacuum. Equilibration with gas and measurement of solubility follow (1).</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>1. Krypton. The Matheson Co. Research grade; maximum impurity 0.04% nitrogen and/or oxygen.</li> <li>2. Beef brain. Homogenized with 4 x volume normal saline (w/w); then mixed with 0.05% "mercury chloride" added as microbial poison.</li> </ol> <p>ESTIMATED ERROR:</p> <p><math>\delta T/K = 0.05</math></p> <p><math>\delta P/\text{mmHg} = 0.2</math></p> <p><math>\delta L/L = 0.05</math></p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>1. Yeh, S-Y.; Peterson, R.E. <u>J. Pharm. Sci.</u> 1963, <u>52</u>, 453.</li> <li>2. Geffcken, G. <u>Z. Physik Chem.</u> 1904, <u>49</u>, 257.</li> </ol>																



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<b>VARIABLES:</b> T/K: 310.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> A.L. Cramer												
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<b>AUXILIARY INFORMATION</b>													
<b>METHOD/APPARATUS/PROCEDURE:</b> Brain samples were obtained and homogenized under aseptic conditions and diluted 4:1 with sterile 0.9% saline. Penicillin (200 units/ml) and streptomycin (100 $\mu\text{g}/\text{ml}$ ) were added as antibacterial agents. Solubility for 20% brain homogenate in normal saline was determined and Ostwald coefficient for brain was calculated from that value.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Krypton. No information given. The $^{85}\text{Kr}$ + air mixture had a count of 0.9 $\mu\text{Ci cm}^{-3}$ . 2. Guinea pigs. Duncan-Hartley random bred. 700-1000 g, from commercial suppliers or bred in laboratory.												
<b>ESTIMATED ERROR:</b> $\delta\text{L}/\text{L} = 0.36$ (brain) $\delta\text{L}/\text{L} = 0.025$ (saline)													
<b>REFERENCES:</b>													

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Xenon; Xe; 7440-63-3</li> <li>Water; H<sub>2</sub>O; 7732-18-5</li> </ol>	<p>EVALUATOR:</p> <p>Rubin Battino, Department of Chemistry, Wright State University, Dayton, Ohio, 45435 U.S.A.</p> <p>July 1978</p>
<p>CRITICAL EVALUATION:</p> <p>The experimental solubility data of three workers was considered to be of sufficient reliability to use in the smoothing equation. In the process of fitting the data to the smoothing equation any data points which differed from the smooth equation by about two standard deviations or more were rejected. The 20 points used for the final smoothing were obtained as follows (reference - number of data points used from that reference): 1-3; 2-4; 3-11; 4-1; 5-1. The fitting equation used was</p> $\ln x_1 = A + B/(T/100K) + C \ln (T/100K) + DT/100K \quad (1)$ <p>Using T/100K as the variable rather than T/K gives coefficients of approximately equal magnitude. The best fit for the 20 data points was</p> $\ln x_1 = -74.7398 + 105.210/(T/100K) + 27.4664 \ln (T/100K) \quad (2)$ <p>where <math>x_1</math> is the mole fraction solubility of xenon at 101,325 Pa partial pressure of gas. The fit in <math>\ln x_1</math> gave a standard deviation of 0.35% taken at the middle of the temperature range. Table 1 gives smoothed values of the mole fraction solubility at 101,325 Pa partial pressure of gas and the Ostwald coefficient at 5K intervals.</p> <p>Table 1 also gives the thermodynamic functions <math>\Delta\bar{G}_1^\circ</math>, <math>\Delta\bar{H}_1^\circ</math>, <math>\Delta\bar{S}_1^\circ</math>, and <math>\Delta\bar{C}_{P1}^\circ</math> for the transfer of gas from the vapor phase at 101,325 Pa partial gas pressure to the (hypothetical) solution phase of unit mole fraction. These thermodynamic properties were calculated from the smoothing equation according to the following equations:</p> $\Delta\bar{G}_1^\circ = - RAT - 100RB - RCT \ln (T/100) - RDT^2/100 \quad (3)$ $\Delta\bar{S}_1^\circ = RA + RC \ln (T/100) + RC + 2RDT/100 \quad (4)$ $\Delta\bar{H}_1^\circ = - 100RB + RCT + RDT^2/100 \quad (5)$ $\Delta\bar{C}_{P1}^\circ = RC + 2RDT/100 \quad (6)$ <p>The results from five other laboratories were rejected for several reasons. Antropoff's data (6) were very high - being off by as much as 40%. On the other hand, König's data (7) were consistently low by 8 to 22 per cent. Steinberg and Manowitz (8) only crudely measured the solubility and their single value was 6% high. Eucken and Hertzberg's two measurements (9) were both very high (5 to 30%). Wood and Caputi's measurements (10) ranged from 12% high to 3% low although their stated precision was 0.5%.</p> <p>Figure 1 shows the temperature dependence of the solubility of xenon in water. The curve was obtained from the smoothing equation. There is no minimum in the range of the measurements, but the solubility curve flattens out markedly at the higher temperatures. The <math>\ln X</math> equation minimum is 383 K.</p> <p>Alexander (11) made five calorimetric determinations of the xenon enthalpy of solution in water at 298.15 K. He obtained an enthalpy of solution of <math>-17.2 \pm 0.5 \text{ kJ mol}^{-1}</math> which is 11% below the value derived from the temperature coefficient of the solubility values. We have found no reports of the partial molal volume of xenon in water.</p> <p>Ewing and Ionescu (12) determined Henry's constant of xenon in water at three temperatures. Their value at 288.15 K agrees with the recommended value, but their values at 278.15 and 298.15 K are 11.5 and 5 per cent high, respectively.</p>	

<b>COMPONENTS:</b> 1. Xenon; Xe; 7440-63-3 2. Water; H <sub>2</sub> O; 7732-18-5	<b>EVALUATOR:</b> Ruben Battino, Department of Chemistry, Wright State University, Dayton, Ohio, 45435 U.S.A.  July 1978
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**CRITICAL EVALUATION:**

Table 1. Smoothed values of the solubility of xenon in water and thermodynamic functions\* at 5K intervals using equation 2 at 101.325 kPa partial pressure of xenon.

T/K	Mole Fraction $x_1 \times 10^5$	Ostwald Coefficient L x 10 <sup>2</sup>	$\Delta\bar{G}_1^\circ / \text{Jmol}^{-1}$	$\Delta\bar{H}_1^\circ / \text{Jmol}^{-1}$	$\Delta\bar{S}_1^\circ / \text{JK}^{-1}\text{mol}^{-1}$
273.15	17.991	22.384	19.58	-25.10	-163.6
278.15	14.816	18.773	20.39	-23.95	-159.4
283.15	12.393	15.981	21.18	-22.81	-155.4
288.15	10.519	13.795	21.94	-21.67	-151.4
293.15	9.051	12.066	22.69	-20.53	-147.4
298.15	7.890	10.684	23.42	-19.39	-143.6
303.15	6.961	9.571	24.13	-18.25	-139.8
308.15	6.212	8.668	24.82	-17.10	-136.0
313.15	5.604	7.932	25.49	-15.96	-132.4
318.15	5.107	7.329	26.14	-14.82	-128.7
323.15	4.698	6.833	26.78	-13.68	-125.2
328.15	4.362	6.426	27.39	-12.54	-121.7
333.15	4.084	6.093	27.99	-11.39	-118.2
338.15	3.854	5.822	28.58	-10.25	-114.8
343.15	3.666	5.602	29.14	-9.11	-111.5
348.15	3.511	5.429	29.69	-7.97	-108.2

\* $\Delta\bar{C}_{p1}^\circ$  was independent of temperature and has the value  $228 \text{ J K}^{-1} \text{ mol}^{-1}$ .

$\text{cal}_{\text{th}} = 4.184 \text{ joule}$ .

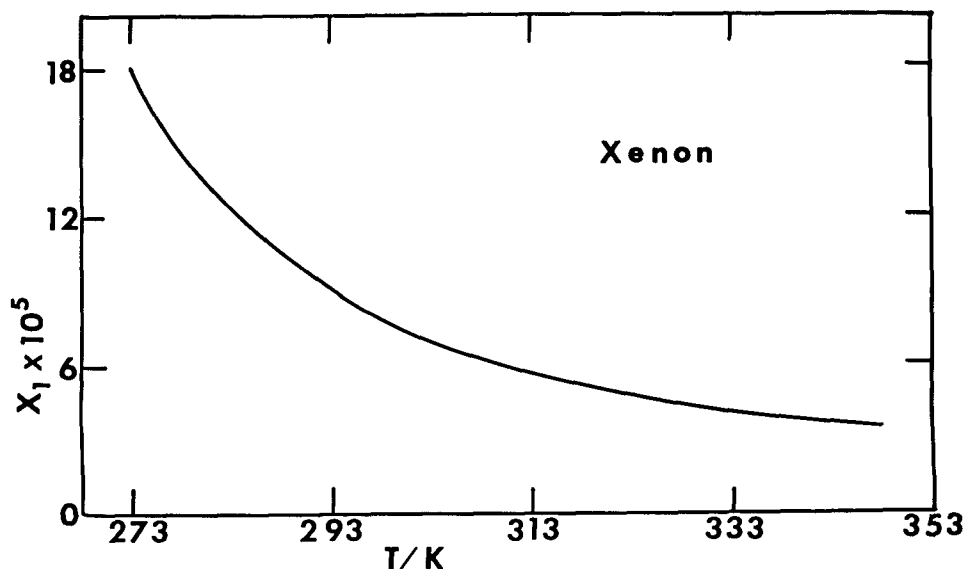


FIGURE 1. The mole fraction solubility of xenon in water at a xenon partial pressure of 101.325 kPa (1 atm).

<p>COMPONENTS:</p> <ol style="list-style-type: none"><li>1. Xenon; Xe; 7440-63-3</li><li>2. Water; H<sub>2</sub>O; 7732-18-5</li></ol>	<p>EVALUATOR:</p> <p>Rubin Battino, Department of Chemistry, Wright State University, Dayton, Ohio, 45435 U.S.A.</p> <p>July 1978</p>
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<b>VARIABLES:</b> T/K: 285.85 - 344.85	<b>PREPARED BY:</b> R. Battino																																	
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="427 493 924 866" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">T/K</th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Mol Fraction <math>X_1 \times 10^5</math></th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Kuenen Coefficient <math>S_o \times 10^3</math></th> </tr> </thead> <tbody> <tr><td>285.85</td><td>10.896</td><td>135.5</td></tr> <tr><td>288.24</td><td>9.943</td><td>123.6</td></tr> <tr><td>288.65</td><td>9.742</td><td>121.1</td></tr> <tr><td>292.75</td><td>8.928</td><td>110.9</td></tr> <tr><td>303.35</td><td>6.821</td><td>84.5</td></tr> <tr><td>313.15</td><td>5.613*</td><td>69.3</td></tr> <tr><td>313.65</td><td>5.493</td><td>67.8</td></tr> <tr><td>321.05</td><td>4.827*</td><td>59.4</td></tr> <tr><td>332.15</td><td>4.150*</td><td>50.8</td></tr> <tr><td>344.85</td><td>3.604*</td><td>43.8</td></tr> </tbody> </table> <p data-bbox="118 886 1163 936">The mole fraction solubility at a partial pressure of xenon of 101.325 kPa was calculated by the compiler.</p> <p data-bbox="104 950 1150 1009">The solubility, <math>S_o</math>, is the cm<sup>3</sup> xenon at 273.15 K and 101.325 kPa per kg of water at a partial gas pressure of 101.325 kPa.</p> <p data-bbox="104 1025 1193 1079">*Solubility values which were used in the final smoothing equation for the recommended solubility values given in the critical evaluation.</p>		T/K	Mol Fraction $X_1 \times 10^5$	Kuenen Coefficient $S_o \times 10^3$	285.85	10.896	135.5	288.24	9.943	123.6	288.65	9.742	121.1	292.75	8.928	110.9	303.35	6.821	84.5	313.15	5.613*	69.3	313.65	5.493	67.8	321.05	4.827*	59.4	332.15	4.150*	50.8	344.85	3.604*	43.8
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<b>METHOD:</b> Flowing the previously degassed liquid in a thin film through the gas in an absorption spiral. Volume changes are measured in burets. See ref. 1.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Xenon-British Oxygen Company, Ltd. Contained about 1% krypton. 2. Water-no comments by authors.																																	
<b>APPARATUS/PROCEDURE:</b> Apparatus of Morrison and Billett used. See ref. 1. The authors used the smoothing equation $\log_{10} S_o = -60.836 + 3605/(T/K).$	<b>ESTIMATED ERROR:</b>  <b>REFERENCES:</b> 1. Morrison, T. J.; Billett, F. <u>J. Chem. Soc.</u> 1952, 3819.																																	

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<b>VARIABLES:</b>  T/K: 298.15 - 318.15	<b>PREPARED BY:</b>  R. Battino															
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<b>AUXILIARY INFORMATION</b>																
<b>METHOD:</b> Used a 125 cm <sup>3</sup> absorption flash in a water bath. The amount of gas absorbed by the degassed liquid is measured on a thermostated gas buret. Details are given in ref. 1.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Xenon-Matheson Co. Maximum impurities of 0.02% nitrogen and 0.05% Krypton. 2. Water-redistilled from glass apparatus.															
<b>APPARATUS/PROCEDURE:</b>	<b>ESTIMATED ERROR:</b> Authors estimate error in solubility to be 1%.															
	<b>REFERENCES:</b> 1. Yeh, S-Y.; Peterson, R. E. J. Pharm. Sci. 1963, <u>52</u> , 453.															

<b>COMPONENTS:</b> 1. Xenon-133; $^{133}_{54}\text{Xe}$ ; 14932-42-4 2. Water; $\text{H}_2\text{O}$ ; 7732-18-5	<b>ORIGINAL MEASUREMENTS:</b> Ladefoged, J.; Andersen, A. M. Phys. Med. Biol. 1967, <u>12</u> , 353-8.						
<b>VARIABLES:</b> T/K: 310.15	<b>PREPARED BY:</b> R. Battino						
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="475 504 973 663" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Mol Fraction <math>x_1 \times 10^5</math></th> <th style="text-align: center;">Ostwald Coefficient <math>L \times 10^2</math></th> </tr> </thead> <tbody> <tr> <td style="text-align: center;">310.15</td> <td style="text-align: center;">5.943*</td> <td style="text-align: center;">8.34</td> </tr> </tbody> </table> <p>The mole fraction solubility at 101.325 Pa (1 atm) was calculated by compiler.</p> <p>*Solubility value which was used in the final smoothing equation for the recommended solubility values which are given in the critical evaluation.</p>		T/K	Mol Fraction $x_1 \times 10^5$	Ostwald Coefficient $L \times 10^2$	310.15	5.943*	8.34
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310.15	5.943*	8.34					
<b>AUXILIARY INFORMATION</b>							
<b>METHOD:</b> An airtight 2 ml vial was half filled with distilled water. Some $^{133}\text{Xe}$ was added to the air in the vial. After 24 hrs equilibration the activity in the aqueous and gas phases was measured in a well-type scintillation counter. The result cited above was the average of 107 observations. Solubility was also measured in saline, olive oil, liquid paraffin, solutions of albumin, and blood at 310.15 K.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Xenon-133. Radiochemical Centre, Amersham. Impurity of other isotopes less than 2%. (Authors) 2. Water. Distilled.						
<b>ESTIMATED ERROR:</b> Result reported by authors as $0.0834 \pm 0.0002$ for 107 observations.							
<b>REFERENCES:</b>							

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Xenon-133; <math>^{133}_{54}\text{Xe}</math>; 14932-42-4</li> <li>Water; <math>\text{H}_2\text{O}</math>; 7732-18-5</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Kitani, K.  <u>Scand. J. Clinical and Lab. Invest.</u>  1972, <u>29</u>, 167-172.</p>						
<p>VARIABLES:</p> <p>T/K: 310.15</p>	<p>PREPARED BY:</p> <p>R. Battino</p>						
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="536 491 1020 658"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^5</math></th> <th>Ostwald Coefficient <math>L \times 10^2</math></th> </tr> </thead> <tbody> <tr> <td>310.15</td> <td>5.914*</td> <td>8.30</td> </tr> </tbody> </table> <p>The mole fraction solubility at 101.325 kPa (1 atm) was calculated by compiler.</p> <p>*Solubility value which was used in the final smoothing equation for the recommended solubility values which are given in the critical evaluation.</p>		T/K	Mol Fraction $X_1 \times 10^5$	Ostwald Coefficient $L \times 10^2$	310.15	5.914*	8.30
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310.15	5.914*	8.30					
<p>AUXILIARY INFORMATION</p>							
<p>METHOD: Liquid was placed in a septum sealed 1 x 1 x 10 cm curette filled two-thirds. The radioactive gas was in air in the other third. After 2 hrs equilibration the middle portion of the liquid and gas phases were counted using a scintillation counter. Solubilities were also measured in saline, lipids, and blood.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>Xenon-133. Radiochemical Centre, Amersham.</li> <li>Water. Distilled.</li> </ol>						
	<p>ESTIMATED ERROR:</p> <p>Temperature control to <math>+ 0.5^\circ\text{C}</math>.  Results reported by author as <math>0.0830 \pm 0.0017</math> (S.D.) for 17 measurements.</p>						
	<p>REFERENCES:</p>						



<b>COMPONENTS:</b> 1. Xenon; Xe; 7440-63-3 2. Water; H <sub>2</sub> O; 7732-18-5	<b>ORIGINAL MEASUREMENTS:</b> Ewing, G. J.; Ionescu, L. G. <u>J. Chem. Eng. Data</u> 1974, <u>19</u> , 367 -369.												
<b>VARIABLES:</b> T/K: 278.15 298.15 P/kPa: 101.325 - 506.625 (1 - 5 atm)	<b>PREPARED BY:</b> H. L. Clever												
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="302 532 1118 719"> <thead> <tr> <th>T/K</th> <th>Henry's Constant <math>K = (P/\text{atm}) / (\text{m/mol Xe kg}^{-1} \text{H}_2\text{O})</math></th> <th>Mol Fraction <math>X_1 \times 10^5</math></th> </tr> </thead> <tbody> <tr> <td>278.15</td> <td>109 ± 10</td> <td>16.5</td> </tr> <tr> <td>288.15</td> <td>171 ± 8</td> <td>10.5</td> </tr> <tr> <td>298.15</td> <td>217 ± 6*</td> <td>8.3</td> </tr> </tbody> </table> <p>*An earlier report from the same laboratory gave a value of 227 (1) at 298.15 K.</p>		T/K	Henry's Constant $K = (P/\text{atm}) / (\text{m/mol Xe kg}^{-1} \text{H}_2\text{O})$	Mol Fraction $X_1 \times 10^5$	278.15	109 ± 10	16.5	288.15	171 ± 8	10.5	298.15	217 ± 6*	8.3
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288.15	171 ± 8	10.5											
298.15	217 ± 6*	8.3											
<b>AUXILIARY INFORMATION</b>													
<b>METHOD:</b> Deionized water was introduced into the reaction vessel, degassed, and then equilibrated with xenon at the desired temperature. Equilibration required up to five hours. The change in pressure of the xenon gas was measured. The moles of xenon absorbed by the water was calculated from the ideal gas equation from the pressure decrease, the gas volume and the temperature. Measurements were made at several pressures up to five atm, and the Henry's law slope determined.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Xenon. J.T.Baker Chemical Co. Stated to contain the impurities Kr 10 ppm, N <sub>2</sub> 50 ppm, O <sub>2</sub> 5 ppm, H <sub>2</sub> 5 ppm, hydrocarbons 15 ppm, and moisture 5 ppm. 2. Water. Deionized.												
<b>ESTIMATED ERROR:</b> $\delta T/K = 0.1$ $\delta P/\text{mmHg} = 0.5$													
<b>REFERENCES:</b> 1. Ewing, G. J.; Maestas, S. <u>J. Phys. Chem.</u> 1970, <u>74</u> , 2341.													

<b>COMPONENTS:</b> 1. Xenon; Xe; 7440-63-3 2. Water; H <sub>2</sub> O; 7732-18-5	<b>ORIGINAL MEASUREMENTS:</b> Benson, B. B.; Krause, D. <u>J. Chem. Phys.</u> 1976, <u>64</u> , 689 - 709.																																										
<b>VARIABLES:</b>  T/K: 274.150 - 318.405	<b>PREPARED BY:</b>  R. Battino																																										
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="473 486 985 903"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^5</math></th> <th>Bunsen Coefficient <math>\alpha \times 10^3</math></th> </tr> </thead> <tbody> <tr><td>274.150</td><td>17.458</td><td>214.578</td></tr> <tr><td>278.157</td><td>14.837*</td><td>182.403</td></tr> <tr><td>283.154</td><td>12.382*</td><td>152.208</td></tr> <tr><td>288.150</td><td>10.498*</td><td>128.398</td></tr> <tr><td>288.150</td><td>10.532*</td><td>129.398</td></tr> <tr><td>293.129</td><td>9.041*</td><td>110.997</td></tr> <tr><td>298.145</td><td>7.875*</td><td>96.573</td></tr> <tr><td>298.148</td><td>7.885*</td><td>96.702</td></tr> <tr><td>298.149</td><td>7.917*</td><td>97.092</td></tr> <tr><td>303.154</td><td>6.966*</td><td>85.320</td></tr> <tr><td>308.155</td><td>6.232*</td><td>76.219</td></tr> <tr><td>313.150</td><td>5.620*</td><td>68.614</td></tr> <tr><td>318.405</td><td>5.134*</td><td>62.584</td></tr> </tbody> </table> <p data-bbox="175 929 1222 976">The mole fraction solubility at 101.325 kPa (1 atm) partial pressure of xenon was calculated by the compiler.</p> <p data-bbox="175 995 1263 1042">*Solubility values which were used in the final smoothing equation for the recommended solubility values given in the critical evaluation.</p>		T/K	Mol Fraction $x_1 \times 10^5$	Bunsen Coefficient $\alpha \times 10^3$	274.150	17.458	214.578	278.157	14.837*	182.403	283.154	12.382*	152.208	288.150	10.498*	128.398	288.150	10.532*	129.398	293.129	9.041*	110.997	298.145	7.875*	96.573	298.148	7.885*	96.702	298.149	7.917*	97.092	303.154	6.966*	85.320	308.155	6.232*	76.219	313.150	5.620*	68.614	318.405	5.134*	62.584
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<b>METHOD/APPARATUS/PROCEDURE:</b> <p data-bbox="156 1315 714 1693">Gas-free water and the pure gas are equilibrated, and volumetric samples of the liquid and gaseous phases are isolated. The gas dissolved in the water is extracted and the number of moles determined on a special mercury manometer. After removal of the water vapor, the number of moles in the sample of the gaseous phase is measured with the same manometer; from which the pressure (and fugacity) above the solution may be calculated. Real gas corrections are made. Predicted maximum error is 0.02%. No drawings of the apparatus are given in the original paper.</p>	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Xenon. No comment by authors. 2. Water. No comment by authors.  <b>ESTIMATED ERROR:</b> Smoothed data were fit to 0.20% rms by the authors. Calculated error in the measurements was 0.02%.  <b>REFERENCES:</b>																																										

COMPONENTS:			ORIGINAL MEASUREMENTS:		
1. Xenon; Xe; 7440-63-3 2. Water; H <sub>2</sub> O; 7732-18-5			Stephan, E. L., Hatfield, N. S., Peoples, R. S. and Pray, H. A. H., <i>Battelle Memorial Institute Report BMI-1067, 1956.</i>		
VARIABLES:			PREPARED BY:		
Temperature, pressure			C. L. Young		
EXPERIMENTAL VALUES:					
T/K	$P^\dagger$ /bar	Mole fraction of xenon in liquid, $x_{\text{Xe}}$	T/K	$P^\dagger$ /bar	Mole fraction of xenon in liquid, $x_{\text{Xe}}$
373.15	9.31	0.000286	533.15	11.8	0.000956
	10.0	0.000281		12.3	0.000932
	16.9	0.000514		14.5	0.00117
	17.9	0.000547		15.0	0.00124
	18.6	0.000555		15.4	0.00120
	20.0	0.000631	574.82	6.48	0.000900
435.93	13.4	0.000498		7.17	0.000932
	14.1	0.000490		7.65	0.000932
	15.4	0.000571		8.20	0.00103
	15.9	0.000579		9.24	0.00108
	16.5	0.000635			
$P^\dagger$ partial pressure of xenon.					
AUXILIARY INFORMATION					
METHOD/APPARATUS/PROCEDURE:			SOURCE AND PURITY OF MATERIALS:		
Static equilibrium apparatus. Gas and liquid equilibrated for 18 hours. Pressure measured with Bourdon gauge and temperature measured with thermocouple. Composition of liquid estimated by volumetric method. Details in source. Partial pressure estimated by subtracting vapor pressure of water from total pressure.			No details given.		
			ESTIMATED ERROR: $\delta T/K = \pm 0.6$ ; $\delta P/\text{bar} = \pm 0.3$ ; $\delta x_{\text{Xe}} = \pm 0.00002$ (estimated by compiler).		
			REFERENCES:		

COMPONENTS:			ORIGINAL MEASUREMENTS:		
1. Xenon; Xe; [7440-63-3]			Franck, E. U.; Lentz, H.; Welsch, H., <i>Z. Phys. Chem., N.F.</i> , <u>1974</u> , 93, 95.		
2. Water; H <sub>2</sub> O; [7732-18-5]					
VARIABLES:			PREPARED BY:		
Temperature, pressure			C. L. Young		
EXPERIMENTAL VALUES:					
T/K	P/bar	Mole fraction of xenon at phase boundary, $x_{Xe}$	T/K	P/bar	Mole fraction of xenon at phase boundary, $x_{Xe}$
627	210	0.030	603	2000	0.187
634	240	0.030	583	200	0.192
635	260	0.030	603	240	0.192
635	270	0.030	617	300	0.192
629	300	0.030	623	350	0.192
575	400	0.030	625	430	0.192
489	600	0.030	615	600	0.192
622	230	0.064	606	850	0.192
633	290	0.064	606	2000	0.192
628	330	0.064	609	2370	0.192
611	420	0.064	612	2700	0.192
573	625	0.064	503	155	0.300
513	1875	0.064	583	250	0.300
604	215	0.096	593	280	0.300
615	240	0.096	609	340	0.300
623	270	0.096	620	420	0.300
629	320	0.096	621	520	0.300
630	340	0.096	616	770	0.300
623	370	0.096	623	1300	0.300
611	500	0.096	527	150	0.495
603	265	0.187	538	175	0.495
617	305	0.187	557	220	0.495
623	340	0.187	571	300	0.495
618	520	0.187	583	370	0.495
603	820	0.187	599	650	0.495 (cont.)
AUXILIARY INFORMATION					
METHOD / APPARATUS / PROCEDURE:			SOURCE AND PURITY OF MATERIALS:		
Small volume static cell with sapphire window. Temperature measured with thermocouple and pressure measured with strain gauge. Phase boundary conditions obtained from discontinuity in isochoric temperature pressure curves for mixtures of fixed composition.			1. Deutsche l'Air Liquide sample, purity 99.998 mole per cent.		
			2. Triple distilled.		
			ESTIMATED ERROR:		
			$\delta T/K = \pm 2$ ; $\delta P/\text{bar} = \pm 1$ ; $\delta x_{Xe} = \pm 0.002$ (estimated by compiler).		
			REFERENCES:		

## COMPONENTS:

1. Xenon; Xe; [7440-63-3]
2. Water; H<sub>2</sub>O; [7732-18-5]

## ORIGINAL MEASUREMENTS:

Franck, E. U.; Lentz, H.; Welsch, H.; *Z. Phys. Chem., N.F.*, 1974, *96*, 95.

## EXPERIMENTAL VALUES:

T/K	P/bar	Mole fraction of xenon at phase boundary, $x_{\text{Xe}}$	T/K	P/bar	Mole fraction of xenon at phase boundary, $x_{\text{Xe}}$
621	1300	0.495	582	450	0.630
528	170	0.625	595	680	0.630
547	240	0.625	496	200	0.771
563	310	0.625	533	260	0.771
579	470	0.625	555	370	0.771
603	1200	0.625	573	520	0.771
613	2600	0.625	588	870	0.771
544	220	0.630	597	1600	0.771
551	260	0.630	598	1820	0.771
563	325	0.630	601	2460	0.771

COMPONENTS:			ORIGINAL MEASUREMENTS:		
1. Xenon; Xe; 7440-63-3 2. Deuterium oxide; D <sub>2</sub> O; 7789-20-0			Stephan, E. L., Hatfield, N. S., Peoples, R. S. and Pray, H. A. H., <i>Battelle Memorial Institute Report</i> BMI-1067, <u>1956</u> .		
VARIABLES:			PREPARED BY:		
Temperature, pressure			C. L. Young		
EXPERIMENTAL VALUES:					
T/K	P <sup>†</sup> /bar	Mole fraction of xenon in liquid, $x_{\text{Xe}}$	T/K	P <sup>†</sup> /bar	Mole fraction of xenon in liquid, $x_{\text{Xe}}$
435.93	10.3	0.000362	533.15	8.9	0.000830
	11.0	0.000436		11.0	0.000972
	12.7	0.000491		11.7	0.001008
	13.4	0.000509		12.3	0.001017
	14.1	0.000495	574.82	6.5	0.000874
533.15	5.8	0.000571		7.2	0.000946
	6.3	0.000589		7.5	0.001088
	6.8	0.000598		8.2	0.001133
	8.2	0.000776		8.9	0.001186
P <sup>†</sup> partial pressure of xenon.					
AUXILIARY INFORMATION					
METHOD /APPARATUS/PROCEDURE:			SOURCE AND PURITY OF MATERIALS:		
Gas and liquid equilibrated for 18 hours. Pressure measured with Bourdon gauge and temperature measured with thermocouple. Composition of liquid estimated by volumetric method. Details in source. Partial pressure estimated by subtracting vapor pressure of deuterium oxide from total pressure.			No details given.		
			ESTIMATED ERROR:		
			$\delta T/K = \pm 0.6$ ; $\delta P/\text{bar} = \pm 0.3$ ; $\delta x_{\text{Xe}} = \pm 2-3\%$ (estimated by compiler).		
			REFERENCES:		

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Xenon; Xe; 7440-63-3</li> <li>Sea Water</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>König, H.</p> <p>Z. <u>Naturforsch.</u> 1963, <u>18a</u>, 363-367.</p>																																			
<p>VARIABLES:</p> <p>T/K: 273.15 - 298.15 P/kPa: 101.325 (1 atm)</p>	<p>PREPARED BY:</p> <p>H. L. Clever A. L. Cramer</p>																																			
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="294 493 1070 765"> <thead> <tr> <th rowspan="2">T/K</th> <th colspan="2">Xenon</th> <th>Bunsen</th> </tr> <tr> <th>cm<sup>3</sup>(STP) kg<sup>-1</sup></th> <th>cm<sup>3</sup>(STP) kg<sup>-1</sup></th> <th>Coefficient <math>\alpha</math></th> </tr> <tr> <td></td> <th>water</th> <th>sea water</th> <th>sea water</th> </tr> </thead> <tbody> <tr> <td>273.15</td> <td>-</td> <td>136</td> <td>0.140</td> </tr> <tr> <td>278.15</td> <td>147</td> <td>115</td> <td>0.118</td> </tr> <tr> <td>283.15</td> <td>128</td> <td>103</td> <td>0.106</td> </tr> <tr> <td>288.15</td> <td>115</td> <td>90.0</td> <td>0.0922</td> </tr> <tr> <td>293.15</td> <td>-</td> <td>80.0</td> <td>0.0818</td> </tr> <tr> <td>298.15</td> <td>96.4</td> <td>70.2</td> <td>0.0717</td> </tr> </tbody> </table> <p>The sea water chlorinity was 19.12%. (Salinity S‰ = 34.54).</p> <p>The Bunsen coefficients were calculated by the compiler using sea water densities from the International Critical Tables.</p>		T/K	Xenon		Bunsen	cm <sup>3</sup> (STP) kg <sup>-1</sup>	cm <sup>3</sup> (STP) kg <sup>-1</sup>	Coefficient $\alpha$		water	sea water	sea water	273.15	-	136	0.140	278.15	147	115	0.118	283.15	128	103	0.106	288.15	115	90.0	0.0922	293.15	-	80.0	0.0818	298.15	96.4	70.2	0.0717
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<p>AUXILIARY INFORMATION</p>																																				
<p>METHOD/APPARATUS/PROCEDURE:</p> <p>The apparatus is a modification of that of Morrison and Billett (1).</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>Xenon. Linde. Greater than 99.9 percent pure.</li> </ol>																																			
<p>APPARATUS/PROCEDURE:</p>	<p>ESTIMATED ERROR:</p> $\delta T/K = 1.0 \begin{matrix} < \\ > \end{matrix} 283.15 \text{ K}$ $= 0.5 \begin{matrix} < \\ > \end{matrix} 298.15 \text{ K}$ <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>Morrison, T. J.; Billett, F. <u>J. Chem. Soc.</u> 1948, 2033; <u>ibid.</u>, 1952, 3821.</li> </ol>																																			

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Xenon; Xe; 7440-63-3</li> <li>Sea Water</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Wood, D.; Caputi, R.</p> <p>U.S.N.R.D.L.-TR-988, 27 Feb. 1966</p> <p>Chem. Abstr. 1967, <u>66</u>, 118693u.</p>																																																						
<p>VARIABLES:</p> <p>T/K: 274.45 - 321.25</p> <p>P/kPa: 101.325 (1 atm)</p>	<p>PREPARED BY:</p> <p>A. L. Cramer</p>																																																						
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<table border="1"> <thead> <tr> <th>T/K</th> <th>Henry's Constant <math>K = (P_1/\text{mmHg})/X_1</math></th> <th>Percent Error*</th> <th>Number of Determinations</th> <th>Mol Fraction <math>X_1 \times 10^2</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> </tr> </thead> <tbody> <tr> <td colspan="6" style="text-align: center;">Water; H<sub>2</sub>O; 7732-18-5</td> </tr> <tr> <td>274.45</td> <td><math>0.425 \times 10^7</math></td> <td>0.5</td> <td>3</td> <td>0.0179</td> <td>0.224</td> </tr> <tr> <td>299.35</td> <td><math>0.987 \times 10^7</math></td> <td>2.0</td> <td>4</td> <td>0.00770</td> <td>0.0955</td> </tr> <tr> <td>320.35</td> <td><math>1.586 \times 10^7</math></td> <td>0.6</td> <td>4</td> <td>0.00479</td> <td>0.0591</td> </tr> <tr> <td colspan="6" style="text-align: center;">Artificial Sea Water (1), S% = 34.727</td> </tr> <tr> <td>274.45</td> <td><math>0.568 \times 10^7</math></td> <td>2.1</td> <td>3</td> <td>0.0134</td> <td>0.167</td> </tr> <tr> <td>300.15</td> <td><math>1.267 \times 10^7</math></td> <td>0.0</td> <td>2</td> <td>0.00600</td> <td>0.0744</td> </tr> <tr> <td>321.25</td> <td><math>1.848 \times 10^7</math></td> <td>2.5</td> <td>4</td> <td>0.00411</td> <td>0.0506</td> </tr> </tbody> </table> <p>*Percent error is the maximum spread in Henry's constant times 100 divided by average Henry's constant.</p> <p>The mole fractions were calculated by the compiler from the average Henry's constant. The Bunsen coefficients were calculated by the compiler from the mole fractions using a solvent mean molecular weight of 18.4823 and sea water densities from the International Critical Tables.</p>		T/K	Henry's Constant $K = (P_1/\text{mmHg})/X_1$	Percent Error*	Number of Determinations	Mol Fraction $X_1 \times 10^2$	Bunsen Coefficient $\alpha$	Water; H <sub>2</sub> O; 7732-18-5						274.45	$0.425 \times 10^7$	0.5	3	0.0179	0.224	299.35	$0.987 \times 10^7$	2.0	4	0.00770	0.0955	320.35	$1.586 \times 10^7$	0.6	4	0.00479	0.0591	Artificial Sea Water (1), S% = 34.727						274.45	$0.568 \times 10^7$	2.1	3	0.0134	0.167	300.15	$1.267 \times 10^7$	0.0	2	0.00600	0.0744	321.25	$1.848 \times 10^7$	2.5	4	0.00411	0.0506
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<p>METHOD /APPARATUS/PROCEDURE:</p> <p>Degassed water was introduced into an evacuated apparatus (&lt; 50 <math>\mu</math> Hg) and gas bled into burette. After the system was isolated, gas was admitted to equilibrium column and the water was circulated through the column, flowing over packing of 4 mm Berl saddles at 110 ml/min for 4-5 hr.</p> <p>Dissolved gas was reclaimed and measured by evacuating the system <math>\rightarrow</math> &lt; 1 <math>\mu</math> Hg and allowing water to distill and condense in a cold trap. Water was melted and refrozen until all the gas was recovered. Gas was then transferred to a gas burette and the pressure was measured with a Hg manometer. Purity was checked by gas chromatography.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>Xenon. AIRCO, Certified 0.0042 impurity, Kr and N<sub>2</sub>. Determined 0.0001 after experiment.</li> <li>Water. Distilled three times before degassing. Sea Water. Artificial, modified from (1).</li> </ol> <p>ESTIMATED ERROR: <math>\delta T/K = 0.1, 0.005, 0.03</math> (as T increases) <math>\delta P/P = 0.001</math> <math>\delta H/H = 0.005</math> (author's error analysis)</p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>Lyman, J.; Fleming, R. H. <u>J. Mar. Res.</u> 1940, <u>3</u>, 134.</li> </ol>																																																						



## COMPONENTS:

1. Xenon; Xe; 7440-63-3
2. Water; H<sub>2</sub>O; 7732-18-5
3. Electrolyte

## EVALUATOR:

H. L. Clever  
Chemistry Department  
Emory University  
Atlanta, GA 30322  
U.S.A.

August 1978

## CRITICAL EVALUATION:

The solubility of xenon in aqueous electrolyte solutions.

There are data on the solubility of xenon in aqueous NaCl, KI, and Na<sub>3</sub>PO<sub>4</sub> solutions. The Setschenow salt effect parameters  $k_s = (1/m) \log(S^0/S)$  and  $k_{sx} = (1/m) \log(X^0/X)$ , where S is volume of gas at STP dissolved kg<sup>-1</sup> water and X is the gas mole fraction, are summarized in Table 1.

TABLE 1. Setschenow salt effect parameters for xenon dissolved in aqueous electrolyte solution.

Electrolyte	T/K	mol salt kg <sup>-1</sup> H <sub>2</sub> O	k <sub>s</sub>	k <sub>sx</sub>	Ref.
NaCl	273.15	0.76	0.182	0.197	2
		1.17	0.185	0.200	2
		2.68	0.175	0.190	2
	293.15	0.285	0.161	0.176	2
		1.32	0.161	0.176	2
		1.80	0.154	0.169	2
		0.155	0.237	0.252	3
	298.15	1.0	0.149	0.164	1
		0.155	0.172	0.187	3
	310.15	0.155	0.143	0.158	3
0.155		0.185	0.200	3	
Na <sub>3</sub> PO <sub>4</sub> *	298.15	0.066	0.499	--	3
		0.066	0.462	--	3
		0.066	0.368	--	3
		0.066	0.453	--	3
KI	298.15	1.0	0.113	0.128	1

\*Buffer solution, 0.066 mol Na<sub>3</sub>PO<sub>4</sub> dm<sup>-3</sup> solution. The Setschenow parameter is  $k_L = (1/m) \log(L^0/L)$ .

The Setschenow parameters from the data of Eucken and Hertzberg (2) and of Morrisson and Johnstone (1) appear to form a self-consistent set of values for aqueous NaCl solutions and they are recommended. The Setschenow salt effect parameters for aqueous NaCl solutions calculated from the data of Yeh and Peterson (3) appear high and erratic. This is partly due to the experimental difficulties in making accurate gas solubility measurements in water and dilute aqueous salt solutions and it may indicate the salt effect parameter is of greater magnitude in the dilute NaCl solution (0.155 molal) than in solutions of 1.0 molal and greater concentration. The Setschenow parameters for xenon in aqueous Na<sub>3</sub>PO<sub>4</sub> solution and aqueous KI solution are tentative.

## REFERENCES

1. Morrison, T.J.; Johnstone, N.B.B. J. Chem. Soc. 1955, 3655.
2. Eucken, A.; Hertzberg, G. Z. phys. Chem. 1950, 195, 1.
3. Yeh, S.-Y.; Peterson, R.E. J. Pharm. Sci. 1964, 53, 822.

Ladefoged and Anderson (4) report the solubility of xenon-133 in water and standard saline solution. The  $k_s$  value calculated from their data is 0.188 at 310.15 K. Isbister, Schofield and Torrance (5) report the solubility of xenon-133 in saline solution. The saline solution was not defined. The solubility value appears to be high and is not recommended.

4. Ladefoged, J.; Anderson, A. M. Phys. Med. Biol. 1967, 12, 353.
5. Isbister, W. H.; Schofield, P. F.; Torrance, H. B. Phys. Med. Biol. 1965, 10, 243.

<b>COMPONENTS:</b> 1. Xenon; Xe; 7440-63-3 2. Dioxosulfatouranium (Uranyl Sulfate); UO <sub>6</sub> S; 1314-64-3 3. Water; H <sub>2</sub> O; 7732-18-5				<b>ORIGINAL MEASUREMENTS:</b> Stephan, E. L., Hatfield, N. S., Peoples, A. S. and Pray, H. A. H., <i>Battelle Memorial Institute Report</i> <i>BMI-1067, 1956.</i>			
<b>VARIABLES:</b> Temperature, pressure, composition				<b>PREPARED BY:</b> C. L. Young			
<b>EXPERIMENTAL VALUES:</b>							
T/K	g Uranium per liter	$P^{\dagger}$ /bar	Solubility*	T/K	g Uranium per liter	$P^{\dagger}$ /bar	Solubility*
373.15	40	12.1	0.432	435.93	40	18.9	0.756
		12.4	0.443			19.6	0.79
		12.8	0.465			17.5	1.51
435.93	40	11.7	0.47	533.15	40	18.2	1.53
		12.0	0.505			18.5	1.63
		12.3	0.52			18.9	1.66
		18.2	0.735				
$P^{\dagger}$ partial pressure of xenon. * ml of xenon at S.T.P. per g of solution.							
<b>AUXILIARY INFORMATION</b>							
<b>METHOD/APPARATUS/PROCEDURE:</b> Static equilibrium apparatus. Gas and liquid equilibrated for 18 hours. Pressure measured with Bourdon gauge and temperature measured with thermocouple. Composition of liquid estimated by volumetric method. Details in source. Partial pressure estimated by subtracting vapor pressure from total pressure.				<b>SOURCE AND PURITY OF MATERIALS:</b> No details given.			
				<b>ESTIMATED ERROR:</b> $\delta T/K = \pm 0.6$ ; $\delta P/\text{bar} = \pm 0.3$ ; $\delta(\text{solubility}) = \pm 3\%$ (estimated by compiler).			
				<b>REFERENCES:</b>			

<b>COMPONENTS:</b> 1. Xenon; Xe; 7440-63-3 2. Water; H <sub>2</sub> O; 7732-18-5 3. Alkali Halides	<b>ORIGINAL MEASUREMENTS:</b> Morrison, T.J.; Johnstone, N.B.B.  <u>J. Chem. Soc.</u> 1955, 3655-3659.															
<b>VARIABLES:</b> T/K: 298.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> T.D. Kittredge H.L. Clever															
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: center;">T/K</th> <th style="text-align: center;"><math>k_s = (1/m) \log (S^0/S)</math></th> <th style="text-align: center;"><math>k_{sX} = (1/m) \log (X^0/X)</math></th> </tr> </thead> <tbody> <tr> <td colspan="3" style="text-align: center;">Sodium Chloride; NaCl; 7647-14-5</td> </tr> <tr> <td style="text-align: center;">298.15</td> <td style="text-align: center;">0.149</td> <td style="text-align: center;">0.164</td> </tr> <tr> <td colspan="3" style="text-align: center;">Potassium Iodide; KI; 7681-11-0</td> </tr> <tr> <td style="text-align: center;">298.15</td> <td style="text-align: center;">0.113</td> <td style="text-align: center;">0.128</td> </tr> </tbody> </table> <p>The values of the Setschenow salt effect parameter, <math>k_s</math>, were apparently determined from only two solubility measurements. They were the solubility of xenon in pure water, <math>S^0</math>, and the solubility of xenon in a near one equivalent of salt per kg of water solution, <math>S</math>. No solubility values are given in the paper. The <math>S^0/S</math> ratio was referenced to a solution containing one kg of water. The compiler calculated the salt effect parameter <math>k_{sX}</math> from the mole fraction solubility ratio <math>X^0/X</math>. The electrolytes were assumed to be 100 per cent dissociated and both cation and anion were used in the mole fraction calculation.</p>		T/K	$k_s = (1/m) \log (S^0/S)$	$k_{sX} = (1/m) \log (X^0/X)$	Sodium Chloride; NaCl; 7647-14-5			298.15	0.149	0.164	Potassium Iodide; KI; 7681-11-0			298.15	0.113	0.128
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<b>AUXILIARY INFORMATION</b>																
<b>METHOD:</b> Gas absorption in a flow system.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Xenon. British Oxygen Co. Ltd. 2. Water. No information given. 3. Electrolyte. No information given.															
<b>APPARATUS/PROCEDURE:</b> The previously degassed solvent flows in a thin film down an absorption spiral containing the gas plus solvent vapor at a total pressure of one atm. The volume of gas absorbed is measured in attached calibrated burets (1).	<b>ESTIMATED ERROR:</b> $\delta k_s = 0.010$  <b>REFERENCES:</b> 1. Morrison, T.J.; Billett, F. <u>J. Chem. Soc.</u> 1952, 3819.															

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<p>METHOD /APPARATUS/PROCEDURE:</p> <p>Gas absorption. The apparatus consists of a gas buret and an adsorption flask connected by a capillary tube. The whole apparatus is shaken. The capillary tube is a 2m-long glass helix. An amount of gas is measured at STP and placed in the gas buret. After shaking, the difference from the original amount of gas placed in the gas buret is determined.</p>	<p>SOURCE AND PURITY OF MATERIALS: Components. No information given.</p> <p>ESTIMATED ERROR: <math>\delta L/L = 0.01</math></p> <p>REFERENCES:</p>																														

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<b>METHOD / APPARATUS / PROCEDURE:</b> <p>Freshly boiled solution was introduced into 125 ml. absorption flask of solubility apparatus (1), then frozen and boiled under vacuum three times. Water-saturated gas was introduced and equilibrated (2) and weight of solution was determined.</p> <p>Thermodynamic constants were calculated from equations (3):</p> $\log S = A/T + B \log T - C$ $\Delta H^\circ = R(-2.3A + BT - T)$ $\Delta S^\circ = R(-B - B \ln T + 2.3C + \ln(0.082T) + 1)$	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Xenon. Matheson Co. 2. Water. Distilled from glass apparatus. 3. Sodium chloride. Analytical grade.																				
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<b>METHOD / APPARATUS / PROCEDURE:</b> Freshly boiled solution was introduced into 125 ml. absorption flask of solubility apparatus (1), then frozen and boiled under vacuum three times. Water-saturated gas was introduced and equilibrated (2) and weight of solution was determined.  Thermodynamic constants were calculated from equations (3):  $\log S = A/T + B \log T - C$ $\Delta H^{\circ} = R(-2.3A + BT - T)$ $\Delta S^{\circ} = R(-B - B \ln T + 2.3C + \ln(0.082T) + 1)$	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Xenon. Matheson Co. 2. Water. Distilled from glass apparatus. 3. Sodium phosphate. Analytical grade.  <b>ESTIMATED ERROR:</b> $\delta T/K = 0.05$ $\delta P/\text{mmHg} = 0.2$ $\delta L/L = 0.002$  <b>REFERENCES:</b> 1. Geffken, G. Z. Physik Chem. 1904, 49, 257. 2. Yeh, S.Y.; Peterson, R.E. J. Pharm. Sci. 1963, 52, 453-8. 3. Eley, E.E. Trans. Faraday Soc. 1939, 35, 1281.																				

<b>COMPONENTS:</b> 1. Xenon; Xe; 7440-63-3 2. Pentane; C <sub>5</sub> H <sub>12</sub> ; 109-66-0	<b>ORIGINAL MEASUREMENTS:</b> Makranczy, J.; Megyery-Balog, K.; Rusz, L.; Patyi, L.  <u>Hung. J. Ind. Chem.</u> 1976, <u>4</u> , 269-280.								
<b>VARIABLES:</b> T/K: 298.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> S.A. Johnson								
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<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Xenon; Xe; 7440-63-3</li> <li>Hexane; C<sub>6</sub>H<sub>14</sub>; 110-54-3</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Clever, H.L.</p> <p><u>J. Phys. Chem.</u> 1958, <u>62</u>, 375-376.</p>																																												
<p>VARIABLES:</p> <p>T/K: 289.15 - 316.25 P/kPa: 101.325 (1 atm)</p>	<p>PREPARED BY:</p> <p>C.E.Edelman A.L. Cramer</p>																																												
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<p>APPARATUS/PROCEDURE:</p> <p>The apparatus is a modification of that of Morrison and Billett (1). The modifications include the addition of a spiral storage for the solvent, a manometer for a constant reference pressure, and an extra buret for highly soluble gases. The solvent is degassed by a modification of the method of Baldwin and Daniel (2).</p>	<p>ESTIMATED ERROR:</p> <p><math>\delta T/K = 0.05</math>  <math>\delta P/\text{mmHg} = 3</math>  <math>\delta X_1/X_1 = 0.01</math></p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>Morrison, T.J.; Billett, F. <u>J. Chem. Soc.</u> 1948, 2033; <u>Ibid.</u> 1952, 3819.</li> <li>Baldwin, R.R.; Daniel, S.G. <u>J. Appl. Chem.</u> 1952, <u>2</u>, 161.</li> </ol>																																												



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COMPONENTS:	EVALUATOR:																								
1. Xenon; Xe; 7440-63-3	H. L. Clever Chemistry Department Emory University Atlanta, GA 30322 U.S.A.																								
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<b>CRITICAL EVALUATION:</b>																									
<p>Both Clever (1) and Dymond (2) measured the solubility of xenon in cyclohexane at four temperatures in the room temperature range. Dymond's data is more self-consistent than Clever's data. The smoothed data differs by 5.4 per cent at 288.15 K and 2.1 per cent at 308.15 K with Dymond's mole fraction solubilities greater than Clever's.</p>																									
<p>Dymond's four values and Clever's values at 307.60 and 316.25 K were combined in a linear regression of a Gibbs energy equation linear in temperature to obtain the recommended equation.</p>																									
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<p>APPARATUS/PROCEDURE:</p> <p>Dymond-Hildebrand apparatus (1) using an all-glass pumping system to spray slugs of degassed solvent into the gas. Amount of gas dissolved calculated from initial and final gas pressures.</p>	<p>ESTIMATED ERROR:</p> <p><math>\delta x_1 / x_1 = 0.01</math></p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>Dymond, J.; Hildebrand, J. H. <u>Ind. Eng. Chem. Fundam.</u> 1967, <u>6</u>, 130.</li> </ol>																				



<b>COMPONENTS:</b> 1. Xenon; Xe; 7440-63-3 2. Methylcyclohexane; C <sub>7</sub> H <sub>14</sub> ; 108-87-2	<b>ORIGINAL MEASUREMENTS:</b> Clever, H.L.; Saylor, J.H.; Gross, P.M.  J. <u>Phys. Chem.</u> 1958, <u>62</u> , 89-91.																																								
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<b>METHOD:</b> Volumetric. The apparatus (1) is a modification of that used by Morrison and Billett (2). Modifications include the addition of a spiral solvent storage tubing, a manometer for constant reference pressure, and an extra gas buret for highly soluble gases.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Xenon. Matheson Co., Inc. Both standard and research grades were used. 2. Methylcyclohexane. Eastman Kodak Co., white label. Dried over Na and distilled; corrected b.p. 100.95 to 100.97°, lit. b.p. 100.93°C.																																								
<b>APPARATUS/PROCEDURE:</b> (a) Degassing. 700 ml of solvent is shaken and evacuated while attached to a cold trap, until no bubbles are seen; solvent is then transferred through a 1 mm capillary tubing, released as a fine mist into a continuously evacuated flask. (b) Solvent is saturated with gas as it flows through 8 mm x 180 cm of tubing attached to a gas buret. Pressure is maintained at 1 atm as the gas is absorbed.	<b>ESTIMATED ERROR:</b> $\delta T/K = 0.05$ $\delta P/\text{mmHg} = 3$ $\delta x_1/x_1 = 0.03$  <b>REFERENCES:</b> 1. Clever, H.L.; Battino, R.; Saylor, J.H.; Gross, P.M. <u>J. Phys. Chem.</u> 1957, <u>61</u> , 1078. 2. Morrison, T.J.; Billett, F. <u>J. Chem. Soc.</u> 1948, 2033; <u>Ibid.</u> 1952, 3819.																																								

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<p>COMPONENTS:</p> <p>1. Xenon; Xe; 7440-63-3</p> <p>2. Methylbenzene (Toluene); C<sub>7</sub>H<sub>8</sub>; 108-88-3</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Saylor, J. H.; Battino, R.</p> <p>J. <u>Phys. Chem.</u> 1958, <u>62</u>, 1334-1337.</p>																														
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<p>METHOD / APPARATUS / PROCEDURE:</p> <p>The solvent was degassed by evacuating the space above it, shaking, and then passing it as a fine mist into another evacuated container. The degassed liquid was saturated as it passed as a thin film inside a glass helix which contained the solute gas plus solvent vapor at a total pressure of 1 atm (1,2). The volume of liquid and the volume of gas absorbed are determined in a system of burets.</p> <p>The smoothed data above are based on only two experimental points. They should be used with caution.</p> <p>Evaluator's Note: Steinberg, M.; Manowitz, B. <u>Ind. Eng. Chem.</u> 1959, <u>51</u>, 47 report an Absorption coefficient of 3.17 (mole fraction <math>1.41 \times 10^{-2}</math>) at 297.15 K for this system.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>1. Xenon. Linde Air Products Co.</p> <p>2. Toluene. Mallinckrodt. Reagent grade. Shaken over conc. H<sub>2</sub>SO<sub>4</sub>, water washed, dried over Drierite, distilled b.p. 110.40 - 110.60°C.</p> <p>ESTIMATED ERROR:</p> <p><math>\delta T/K = 0.03</math></p> <p><math>\delta P/\text{torr} = 1</math></p> <p><math>\delta X_1/X_1 = 0.005</math></p> <p>REFERENCES:</p> <p>1. Morrison, T. J.; Billett, F. <u>J. Chem. Soc.</u> 1948, 2033; <u>ibid</u>, 1952, 3819.</p> <p>2. Baldwin, R. R.; Daniel, S. G. <u>J. Appl. Chem.</u> 1952, <u>2</u>, 161.</p>																														

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<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="367 493 1039 1029"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^2</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Absorption Coefficient <math>\beta</math></th> </tr> </thead> <tbody> <tr> <td colspan="4" style="text-align: center;">Toluene; <math>C_7H_8</math>; 108-88-3</td> </tr> <tr> <td>297.15</td> <td>1.41</td> <td>3.00</td> <td>3.17</td> </tr> <tr> <td colspan="4" style="text-align: center;">1,4-Dimethylbenzene; <math>C_8H_{10}</math>; 106-42-3</td> </tr> <tr> <td>273.15</td> <td>1.67</td> <td>3.11</td> <td>3.28</td> </tr> <tr> <td>302.15</td> <td>1.55</td> <td>2.80</td> <td>2.95</td> </tr> <tr> <td colspan="4" style="text-align: center;">Dimethylbenzene Isomer Mixture; <math>C_8H_{10}</math>; 1330-20-7</td> </tr> <tr> <td>305.15</td> <td>0.743</td> <td>1.38</td> <td>1.46</td> </tr> <tr> <td colspan="4" style="text-align: center;">1,3,5-Trimethylbenzene (Mesitylene); <math>C_9H_{12}</math>; 108-67-8</td> </tr> <tr> <td>293.15</td> <td>1.45</td> <td>2.39</td> <td>2.52</td> </tr> </tbody> </table> <p>The authors define the absorption coefficient as the volume of gas, corrected to 288.15 K and 101.325 kPa, absorbed under a total system pressure of 101.325 kPa per unit volume of solvent at 288.15 K.</p> <p>The mole fraction solubilities and Bunsen coefficients were calculated by the compiler.</p>		T/K	Mol Fraction $X_1 \times 10^2$	Bunsen Coefficient $\alpha$	Absorption Coefficient $\beta$	Toluene; $C_7H_8$ ; 108-88-3				297.15	1.41	3.00	3.17	1,4-Dimethylbenzene; $C_8H_{10}$ ; 106-42-3				273.15	1.67	3.11	3.28	302.15	1.55	2.80	2.95	Dimethylbenzene Isomer Mixture; $C_8H_{10}$ ; 1330-20-7				305.15	0.743	1.38	1.46	1,3,5-Trimethylbenzene (Mesitylene); $C_9H_{12}$ ; 108-67-8				293.15	1.45	2.39	2.52
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<b>METHOD/APPARATUS/PROCEDURE:</b> The absorption coefficient at one atm xenon was measured by modified McDaniel method (1). The Henry's constant ( $K = (P/atm)/X_1$ ) at low concentration of xenon was measured by static and dynamic tracer techniques. The authors state that log (Absorption Coefficient vs 1/T is linear and gives an enthalpy of solution of $-3040 \text{ cal mol}^{-1}$ .	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Xenon. Matheson Co., Inc. Technical grade. 2. Amsco 123-15. American Mineral Spirits Co. No. 140. Paraffin 59.6 wt %, naphthene 27.3 wt %, aromatics 13.2 wt %.  <b>ESTIMATED ERROR:</b> $\delta K/K = 0.05 - 0.10$ (McDaniel method) $\delta K/K = 0.18$ (Tracer technique)  <b>REFERENCES:</b> 1. Furman, N.H. "Scott's Standard Methods of Chemical Analysis" Van Nostrand Co., NY 1939, 5th ed., Vol. II, p. 2587.																																							

<b>COMPONENTS:</b> 1. Xenon; Xe; 7440-63-3 2. 1-Propanol; C <sub>3</sub> H <sub>8</sub> O; 71-23-8	<b>ORIGINAL MEASUREMENTS:</b> Komarenko, V.G.; Manzhelii, V.G.  Ukr. Fiz. Zh. (Ukr. Ed.) 1968, 13, 387-391. Ukr. Phys. J. 1968, 13, 273-276.																																										
<b>VARIABLES:</b> T/K: 193.15 - 243.15 P/kPa: 26.664 (200 mmHg)	<b>PREPARED BY:</b> T.D. Kittredge																																										
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="431 486 921 746"> <thead> <tr> <th>T/K</th> <th>Mol Fraction P/mmHg 200 <math>X_1 \times 10^2</math></th> <th>Mol Fraction P/mmHg 760 <math>X_1 \times 10^2</math></th> </tr> </thead> <tbody> <tr><td>193.15</td><td>2.20</td><td>8.36</td></tr> <tr><td>203.15</td><td>1.648</td><td>6.262</td></tr> <tr><td>213.15</td><td>1.183</td><td>4.495</td></tr> <tr><td>223.15</td><td>0.862</td><td>3.28</td></tr> <tr><td>233.15</td><td>0.663</td><td>2.52</td></tr> <tr><td>243.15</td><td>0.515</td><td>1.96</td></tr> </tbody> </table> <p>Smoothed Data: <math>\ln X_1 = 188.924 - 262.126/(T/100) - 249.815 \ln (T/100) + 56.3087 (T/100)</math></p>		T/K	Mol Fraction P/mmHg 200 $X_1 \times 10^2$	Mol Fraction P/mmHg 760 $X_1 \times 10^2$	193.15	2.20	8.36	203.15	1.648	6.262	213.15	1.183	4.495	223.15	0.862	3.28	233.15	0.663	2.52	243.15	0.515	1.96																					
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<b>METHOD/APPARATUS/PROCEDURE:</b> <p>The solvent was degassed by vacuum. A thin layer of alcohol, cooled to 125-175 K, was kept for 20 hours in a vacuum maintained at 10<sup>-3</sup> mmHg.</p> <p>The degassed liquid was sealed under vacuum in an ampoule which was placed in the apparatus. The apparatus consisted of a manostat, a mercury compensator, and a solubility cell divided by a mercury seal. A gas pressure of 200 mmHg and the temperature were established. The foil ends of the ampoule were pierced. The gas dissolved as the liquid flowed through a series of small cups. The amount of gas dissolved was determined by the rise in mercury level in the compensator.</p> <p>Some measurements were made at 400 mmHg gas pressure. The results confirmed that Henry's law was obeyed.</p>	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Xenon. Source not given. Purity by chromatographic method was 99.85 per cent. 2. 1-Propanol. Purified and analyzed in the All-Union Sci. Res. Inst. for Single Crystals & High-Purity Substances. Purity 99.97 weight per cent.  <b>ESTIMATED ERROR:</b> $\delta T/K = 0.05$ $\delta P/\text{mmHg} = 0.01$ $\delta X_1/X_1 = 0.005$  <b>REFERENCES:</b>																																										

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Xenon; Xe; 7440-63-3</li> <li>Acetic Acid; <math>C_2H_4O_2</math> ; 64-19-7</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Steinberg, M.; Manowitz, B.</p> <p><u>Ind. Eng. Chem.</u> 1959, <u>51</u>, 47-50.</p>								
<p>VARIABLES:</p> <p>T/K: 301.15 P/kPa: 101.325 (1 atm)</p>	<p>PREPARED BY:</p> <p>H.L. Clever</p>								
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="302 502 978 632"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^2</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Absorption Coefficient <math>\beta</math></th> </tr> </thead> <tbody> <tr> <td>301.15</td> <td>0.258</td> <td>1.02</td> <td>1.08</td> </tr> </tbody> </table> <p>The authors define the Absorption Coefficient as the volume of gas, corrected to 288.15 K and 101.325 kPa, absorbed under a total system pressure of 101.325 kPa per unit volume of solvent at 288.15 K.</p> <p>The mole fraction solubility and Bunsen coefficient were calculated by the compiler.</p>		T/K	Mol Fraction $x_1 \times 10^2$	Bunsen Coefficient $\alpha$	Absorption Coefficient $\beta$	301.15	0.258	1.02	1.08
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<p>AUXILIARY INFORMATION</p>									
<p>METHOD/APPARATUS/PROCEDURE:</p> <p>Absorption coefficient determined by a modified McDaniel method (1).</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>Xenon. Matheson Co., Inc. Technical grade.</li> <li>Acetic acid. Source not given.</li> </ol> <p>ESTIMATED ERROR:</p> <p><math>\delta\beta/\beta = 0.05 - 0.10</math></p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>Furman, N.H. "Scott's Standard Methods of Chemical Analysis" Van Nostrand Co., NY 1939, 5th ed., Vol. II, p. 2587.</li> </ol>								

<b>COMPONENTS:</b> 1. Xenon; Xe; 7440-63-3  2. Undecafluoro (trifluoromethyl)-cyclohexane (Perfluoromethyl-cyclohexane); C <sub>7</sub> F <sub>14</sub> ; 355-02-2	<b>ORIGINAL MEASUREMENTS:</b> Clever, H.L.; Saylor, J.H.; Gross, P.M.  <u>J. Phys. Chem.</u> 1958, <u>62</u> , 89-91.																																								
<b>VARIABLES:</b> T/K: 289.15 - 316.25 Total P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b>  P.L. Long																																								
<b>EXPERIMENTAL VALUES:</b>  <table border="1" data-bbox="343 480 1022 666"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^2</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>289.15</td> <td>1.86</td> <td>2.20</td> <td>2.33</td> </tr> <tr> <td>303.15</td> <td>1.61</td> <td>1.86</td> <td>2.06</td> </tr> <tr> <td>316.25</td> <td>1.43</td> <td>1.62</td> <td>1.87</td> </tr> </tbody> </table> <p>Smoothed Data: <math>\Delta G^\circ/J \text{ mol}^{-1} = -RT \ln X_1 = -7375.1 + 58.643 T</math>            Std. Dev. <math>\Delta G^\circ = 3.9</math>, Coef. Corr. = 0.9999  <math>\Delta H^\circ/J \text{ mol}^{-1} = -7375.1</math>, <math>\Delta S^\circ/J \text{ K}^{-1} \text{ mol}^{-1} = -58.643</math></p> <table border="1" data-bbox="459 793 939 1068"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^2</math></th> <th><math>\Delta G^\circ/J \text{ mol}^{-1}</math></th> </tr> </thead> <tbody> <tr> <td>288.15</td> <td>1.88</td> <td>9,522.8</td> </tr> <tr> <td>293.15</td> <td>1.78</td> <td>9,816.0</td> </tr> <tr> <td>298.15</td> <td>1.69</td> <td>10,109</td> </tr> <tr> <td>303.15</td> <td>1.61</td> <td>10,402</td> </tr> <tr> <td>308.15</td> <td>1.54</td> <td>10,696</td> </tr> <tr> <td>313.15</td> <td>1.47</td> <td>10,989</td> </tr> <tr> <td>318.15</td> <td>1.40</td> <td>11,282</td> </tr> </tbody> </table> <p>The solubility values were adjusted to a partial pressure of xenon of 101.325 kPa (1 atm) by Henry's law.            The Bunsen coefficients were calculated by the compiler.</p>		T/K	Mol Fraction $X_1 \times 10^2$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	289.15	1.86	2.20	2.33	303.15	1.61	1.86	2.06	316.25	1.43	1.62	1.87	T/K	Mol Fraction $X_1 \times 10^2$	$\Delta G^\circ/J \text{ mol}^{-1}$	288.15	1.88	9,522.8	293.15	1.78	9,816.0	298.15	1.69	10,109	303.15	1.61	10,402	308.15	1.54	10,696	313.15	1.47	10,989	318.15	1.40	11,282
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<b>METHOD:</b> Volumetric. The apparatus (1) is a modification of that used by Morrison and Billett (2). Modifications include the addition of a spiral solvent storage tubing, a manometer for constant reference pressure, and an extra gas buret for highly soluble gases.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Xenon. Matheson Co., Inc. Both standard and research grades were used.  2. Perfluoromethylcyclohexane. du Pont FCS-326, shaken with concentrated H <sub>2</sub> SO <sub>4</sub> , washed, dried over Drierite and distilled. b.p. 75.95 to 76.05° at 753 mm., lit. b.p. 76.14 at 760 mm.																																								
<b>APPARATUS/PROCEDURE:</b> (a) Degassing. 700 ml of solvent is shaken and evacuated while attached to a cold trap, until no bubbles are seen; solvent is then transferred through a 1 mm capillary tubing, released as a fine mist into a continuously evacuated flask. (b) Solvent is saturated with gas as it flows through 8 mm x 180 cm of tubing attached to a gas buret. Pressure is maintained at 1 atm as the gas is absorbed.	<b>ESTIMATED ERROR:</b> $\delta T/K = 0.05$ $\delta P/\text{mmHg} = 3$ $\delta X_1/X_1 = 0.03$  <b>REFERENCES:</b> 1. Clever, H.L.; Battino, R.; Saylor, J.H.; Gross, P.M. <u>J. Phys. Chem.</u> 1957, <u>61</u> , 1078. 2. Morrison, T.J.; Billett, F. <u>J. Chem. Soc.</u> 1948, 2033; <u>ibid.</u> 1952, 3819.																																								



<b>COMPONENTS:</b> 1. Xenon; Xe; 7440-63-3 2. Dichlorodifluoromethane (Freon-12); CCl <sub>2</sub> F <sub>2</sub> ; 75-71-8		<b>ORIGINAL MEASUREMENTS:</b> Steinberg, M.; Manowitz, B.; Pruzansky, J. US AEC BNL-542 (T-140). Chem. Abstr. 1959, <u>53</u> , 21242g.			
<b>VARIABLES:</b> T/K: 196.15 - 273.15		<b>PREPARED BY:</b> H. L. Clever			
<b>EXPERIMENTAL VALUES:</b>					
T/K	Absorption Coefficient	Henry's Constant K/atm	Mol Fraction X <sub>1</sub> × 10 <sup>2</sup>	Bunsen Coefficient α	Ostwald Coefficient L
196.15	55.3	--	14.7	52.4	37.6
203.15	--	7.9	12.7	--	--
260.85	--	28.	3.6	--	--
273.15	7.4	37.	2.7	7.0	7.0
Smoothed Data: $\Delta G^{\circ}/J \text{ mol}^{-1} = -RT \ln X_1 = -9,778.5 + 65.508 T$ Std. Dev. $\Delta G^{\circ} = 87$ , Coef. Corr. = 0.9994 $\Delta H^{\circ}/J \text{ mol}^{-1} = -9,778.5$ , $\Delta S^{\circ}/J \text{ K}^{-1} \text{ mol}^{-1} = -65.508$					
T/K	Mol Fraction X <sub>1</sub> × 10 <sup>2</sup>	$\Delta G^{\circ}/J \text{ mol}^{-1}$			
193.15	16.7	2,874.4			
203.15	12.4	3,529.5			
213.15	9.43	4,184.6			
223.15	7.36	4,839.6			
233.15	5.87	5,494.7			
243.15	4.77	6,149.8			
253.15	3.94	6,804.9			
263.15	3.31	7,460.0			
273.15	2.81	8,115.0			
<b>AUXILIARY INFORMATION</b>					
<b>METHOD /APPARATUS/PROCEDURE:</b> Dynamic tracer technique (1). The Henry's constant is $K = (P/\text{atm})/X_1$ The Henry's constants are probably from data smoothed by the authors. The report is discussed further in a later paper (2).			<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Xenon. 2. Dichlorodifluoromethane.		
			<b>ESTIMATED ERROR:</b> $\delta X/X = 0.03 - 0.05$ (Compiler)		
			<b>REFERENCES:</b> 1. Steinberg, M.; Manowitz, B. Ind. Eng. Chem. 1959, <u>51</u> , 47. 2. Steinberg, M. US AEC TID-7593, 1959, 217. Chem. Abstr. 1961, <u>55</u> , 9083e.		

<b>COMPONENTS:</b> 1. Xenon; Xe; 7440-63-3  2. 1,1,2-Trichloro-1,2,2-trifluoroethane (Freon 113); C <sub>2</sub> Cl <sub>3</sub> F <sub>3</sub> ; 76-13-1	<b>ORIGINAL MEASUREMENTS:</b> Linford, R.G.; Hildebrand, J.H.  <u>Trans. Faraday Soc.</u> 1970, <u>66</u> , 577-581.																																							
<b>VARIABLES:</b> T/K: 284.37 - 298.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b>  P.L. Long																																							
<b>EXPERIMENTAL VALUES:</b>  <table border="1" data-bbox="341 491 1005 701"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^2</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr><td>284.37</td><td>2.568</td><td>5.03</td><td>5.24</td></tr> <tr><td>287.75</td><td>2.447</td><td>4.76</td><td>5.01</td></tr> <tr><td>290.40</td><td>2.362</td><td>4.36</td><td>4.64</td></tr> <tr><td>295.09</td><td>2.230</td><td>4.28</td><td>4.62</td></tr> <tr><td>298.15</td><td>2.149</td><td>4.11</td><td>4.49</td></tr> </tbody> </table> Smoothed Data: $\Delta G^\circ / \text{J mol}^{-1} = -RT \ln X_1 = -9060.7 + 62.327 T$ Std. Dev. $\Delta G^\circ = 3.9$ , Coef. Corr. = 0.9999 $\Delta H^\circ / \text{J mol}^{-1} = -9060.7$ , $\Delta S^\circ / \text{J K}^{-1} \text{ mol}^{-1} = -62.327$  <table border="1" data-bbox="458 834 932 1034"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^2</math></th> <th><math>\Delta G^\circ / \text{J mol}^{-1}</math></th> </tr> </thead> <tbody> <tr><td>283.15</td><td>2.605</td><td>8587.1</td></tr> <tr><td>288.15</td><td>2.437</td><td>8898.9</td></tr> <tr><td>293.15</td><td>2.285</td><td>9210.4</td></tr> <tr><td>298.15</td><td>2.147</td><td>9522.0</td></tr> </tbody> </table> The Bunsen and Ostwald coefficients were calculated by the compiler.		T/K	Mol Fraction $X_1 \times 10^2$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	284.37	2.568	5.03	5.24	287.75	2.447	4.76	5.01	290.40	2.362	4.36	4.64	295.09	2.230	4.28	4.62	298.15	2.149	4.11	4.49	T/K	Mol Fraction $X_1 \times 10^2$	$\Delta G^\circ / \text{J mol}^{-1}$	283.15	2.605	8587.1	288.15	2.437	8898.9	293.15	2.285	9210.4	298.15	2.147	9522.0
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<b>METHOD:</b> Saturation of liquid with gas at a partial pressure of gas equal to 1 atm.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Xenon. Source not given. Purest commercially obtainable, dried before use.  2. 1,1,2-Trichloro-1,2,2-trifluoroethane. Matheson, Coleman and Bell. Spectroquality.																																							
<b>APPARATUS/PROCEDURE:</b> Dymond-Hildebrand apparatus (1) which uses an all-glass pumping system to spray slugs of degassed solvent into the gas. The amount of gas dissolved is calculated from initial and final pressures.	<b>ESTIMATED ERROR:</b>  $\delta X_1 / X_1 = 0.005$ (Evaluator)  <b>REFERENCES:</b> 1. Dymond, J.H.; Hildebrand, J.H. <u>Ind. Eng. Chem. Fundam.</u> 1967, <u>6</u> , 130.																																							

<b>COMPONENTS:</b> 1. Xenon; Xe; 7440-63-3 2. Trichloromethane (Chloroform); CHCl <sub>3</sub> ; 67-66-3	<b>ORIGINAL MEASUREMENTS:</b> Yagi, M.; Kondo, K.  <u>Kakuriken Kenkyu Hokoku</u> 1969, 2(2), 153-154. Chem. Abstr. 1971, <u>75</u> , 54017c.								
<b>VARIABLES:</b> T/K: room temperature P/kPa: 1.333 - 49.329 (10 - 370 mmHg)	<b>PREPARED BY:</b>  H.L. Clever								
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<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Xenon; Xe; 7440-63-3</li> <li>Tetrachloromethane (Carbon Tetrachloride); CCl<sub>4</sub>; 56-23-5</li> </ol>	<p>ORIGINAL MEASUREMENTS: Yagi, M.; Kondo, K.</p> <p><u>Kakuriken Kenkyu Hokoku</u> 1969, 2(2), 153-154. Chem. Abstr. 1971, 75, 54017c.</p>						
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<p>VARIABLES:</p> <p>T/K: 288.65 - 328.15</p> <p>P/kPa: 101.325 (1 atm)</p>	<p>PREPARED BY:</p> <p>H.L. Clever, A.L. Cramer</p>																																																		
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="356 486 1049 682"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^2</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>288.65</td> <td>0.968</td> <td>1.972</td> <td>2.084</td> </tr> <tr> <td>298.15</td> <td>-</td> <td>-</td> <td>-</td> </tr> <tr> <td>313.15</td> <td>-</td> <td>-</td> <td>-</td> </tr> <tr> <td>328.15</td> <td>0.682</td> <td>1.338</td> <td>1.608</td> </tr> </tbody> </table> <p>Smoothed Data: <math>\Delta G^\circ/\text{J mol}^{-1} = -RT \ln X_1 = -6982.2 + 62.748 T</math></p> <p><math>\Delta H^\circ/\text{J mol}^{-1} = -6982.2</math>, <math>\Delta S^\circ/\text{J K}^{-1} \text{ mol}^{-1} = -62.748</math></p> <table border="1" data-bbox="459 793 932 1087"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^2</math></th> <th><math>\Delta G^\circ/\text{J mol}^{-1}</math></th> </tr> </thead> <tbody> <tr> <td>288.15</td> <td>0.973</td> <td>11,099</td> </tr> <tr> <td>293.15</td> <td>0.926</td> <td>11,412</td> </tr> <tr> <td>298.15</td> <td>0.882</td> <td>11,726</td> </tr> <tr> <td>303.15</td> <td>0.842</td> <td>12,040</td> </tr> <tr> <td>308.15</td> <td>0.805</td> <td>12,354</td> </tr> <tr> <td>313.15</td> <td>0.771</td> <td>12,667</td> </tr> <tr> <td>318.15</td> <td>0.739</td> <td>12,981</td> </tr> <tr> <td>323.15</td> <td>0.709</td> <td>13,295</td> </tr> <tr> <td>328.15</td> <td>0.682</td> <td>13,609</td> </tr> </tbody> </table> <p>Solubility values were adjusted to a partial pressure of xenon of 101.325 kPa (1 atm) by Henry's law. Bunsen coefficients were calculated by the compiler.</p>		T/K	Mol Fraction $X_1 \times 10^2$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	288.65	0.968	1.972	2.084	298.15	-	-	-	313.15	-	-	-	328.15	0.682	1.338	1.608	T/K	Mol Fraction $X_1 \times 10^2$	$\Delta G^\circ/\text{J mol}^{-1}$	288.15	0.973	11,099	293.15	0.926	11,412	298.15	0.882	11,726	303.15	0.842	12,040	308.15	0.805	12,354	313.15	0.771	12,667	318.15	0.739	12,981	323.15	0.709	13,295	328.15	0.682	13,609
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<p>METHOD /APPARATUS/PROCEDURE:</p> <p>The solvent was degassed by evacuating the space above it, shaking, and then passing it as a fine mist into another evacuated container. The degassed liquid was saturated as it passed as a thin film inside a glass helix which contained the solute gas plus solvent vapor at a total pressure of 1 atm (1,2). The volume of liquid and the volume of gas absorbed are determined in a system of burets.</p> <p>The smoothed data above are based on only two experimental points. They should be used with caution.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>1. Xenon. Linde Air Products Co.</p> <p>2. Iodobenzene. Eastman Kodak white label. Shaken with aq. Na<sub>2</sub>S<sub>2</sub>O<sub>3</sub>, dried over P<sub>4</sub>O<sub>10</sub>, distilled, b.p. 77.40 - 77.60°C (20 mmHg).</p> <p>ESTIMATED ERROR:</p> <p><math>\delta T/\text{K} = 0.03</math></p> <p><math>\delta P/\text{mmHg} = 1.0</math></p> <p><math>\delta X_1/X_1 = 0.005</math> (authors)</p> <p>REFERENCES:</p> <p>1. Morrison, T.J.; Billett, F. <u>J. Chem. Soc.</u> 1948, 2033.</p> <p>2. Clever, H.L.; Battino, R.; Saylor, J.H.; Gross, P. M. <u>J. Phys. Chem.</u> 1957, <u>61</u>, 1078.</p>																																																		



<p>COMPONENTS:</p> <p>1. Xenon; Xe; 7440-63-3  <sup>133</sup>Xe; 14932-42-4</p> <p>2. Carbon dioxide; CO<sub>2</sub>; 124-38-9</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Ackley, R.D.; Notz, K.J.  Oak Ridge Natl. Lab.  Oak Ridge, TN 37830</p> <p>ORNL-5122, October 1976  Aval. Nat'l. Tech. Infor. Service  Chem. Abstr. 1977, 86, 178229v.</p>																																												
<p>VARIABLES:</p> <p>T/K: 218.35 - 303.65</p>	<p>PREPARED BY:</p> <p>A.L. Cramer  H.L. Clever</p>																																												
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="297 498 971 830"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^2</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr><td>223.15</td><td>2.22</td><td>13.33</td><td>10.89</td></tr> <tr><td>233.15</td><td>1.95</td><td>11.26</td><td>9.61</td></tr> <tr><td>243.15</td><td>1.73</td><td>9.62</td><td>8.56</td></tr> <tr><td>253.15</td><td>1.53</td><td>8.15</td><td>7.55</td></tr> <tr><td>263.15</td><td>1.37</td><td>6.94</td><td>6.69</td></tr> <tr><td>273.15</td><td>1.23</td><td>5.88</td><td>5.88</td></tr> <tr><td>283.15</td><td>1.15</td><td>5.11</td><td>5.30</td></tr> <tr><td>293.15</td><td>1.12</td><td>4.43</td><td>4.75</td></tr> <tr><td>298.15</td><td>1.14</td><td>4.12</td><td>4.50</td></tr> <tr><td>303.15</td><td>1.17</td><td>3.69</td><td>4.10</td></tr> </tbody> </table> <p>The mole fraction solubility at a xenon partial pressure of 101.325 kPa (1 atm) was calculated by the compiler. The CO<sub>2</sub> density values were used from reference (1).</p> <p>A smoothed data fit with thermodynamic values for the transfer of one mole of xenon from the gas at 101.325 kPa to the hypothetical unit mole fraction xenon liquid is on the next page.</p>		T/K	Mol Fraction $x_1 \times 10^2$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	223.15	2.22	13.33	10.89	233.15	1.95	11.26	9.61	243.15	1.73	9.62	8.56	253.15	1.53	8.15	7.55	263.15	1.37	6.94	6.69	273.15	1.23	5.88	5.88	283.15	1.15	5.11	5.30	293.15	1.12	4.43	4.75	298.15	1.14	4.12	4.50	303.15	1.17	3.69	4.10
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<p>METHOD:</p> <p>Tracer technique (2). Corrected for 5.27 day half-life attenuation. Collimated counter with equilibrated gas-liquid samples. Xenon gas was a mixture of Xenon-133 and research grade Xe. The total pressure of the system was the equilibrium pressure of liquid CO<sub>2</sub> + the Xe pressure.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>1. Xenon. Cryogenic Rare Gas Labs. Ultra high purity grade. Xenon-133. Isotopes Div., ORNL.</p> <p>2. Carbon dioxide. Matheson Co., Inc. Research grade, 99.5 mol percent.</p>																																												
<p>APPARATUS/PROCEDURE:</p>	<p>ESTIMATED ERROR:</p> <p><math>\delta T/K = 0.2</math></p> <p>REFERENCES:</p> <p>1. Notz, K.J.; Meservey, A.B. ORNL-5121, June 1976.</p> <p>2. Notz, K.J.; Meservey, A.B.; Ackley, R.D. <u>Trans. Am. Nucl. Soc.</u> 1973, <u>17</u>, 318.</p>																																												

COMPONENTS:		ORIGINAL MEASUREMENTS:			
1. Xenon; Xe; 7440-63-3  <sup>133</sup> Xe; 14932-42-4		Ackley, R.D.; Notz, K.J.			
2. Carbon Dioxide; CO <sub>2</sub> ; 124-38-9		ORNL-5122, October 1976 Aval. Nat'l. Tech. Infor. Service			
VARIABLES:		PREPARED BY:			
T/K: 218.35 - 303.65		A.L. Cramer H.L. Clever			
EXPERIMENTAL VALUES:					
T/K	Mol Fraction X <sub>1</sub> x 10 <sup>2</sup>	ΔG <sup>o</sup> /kJmol <sup>-1</sup>	ΔH <sup>o</sup> /kJmol <sup>-1</sup>	ΔS <sup>o</sup> /JK <sup>-1</sup> mol <sup>-1</sup>	ΔCp <sup>o</sup> /JK <sup>-1</sup> mol <sup>-1</sup>
223.15	2.20	7.077	-3.795	-48.72	-215
233.15	1.98	7.606	-5.556	-56.45	-138
243.15	1.74	8.194	-6.547	-60.63	-60.7
253.15	1.52	8.808	-6.770	-61.53	+16.2
263.15	1.35	9.415	-6.222	-59.43	93.2
273.15	1.23	9.987	-4.907	-54.53	170
283.15	1.16	10.497	-2.821	-47.04	247
293.15	1.13	10.920	+0.033	-37.14	324
303.15	1.16	11.232	3.657	-24.99	401
<p>The smoothed data above was calculated from the linear regression of ln X<sub>1</sub> as a function of temperature according to the equation</p> $\ln X_1 = 206.368 - 283.363/(T/100) - 232.255 \ln (T/100) + 46.2585 (T/100)$					
AUXILIARY INFORMATION					
METHOD:			SOURCE AND PURITY OF MATERIALS:		
See preceding page			See preceding page		
APPARATUS/PROCEDURE:			ESTIMATED ERROR:		
			See preceding page		
			REFERENCES:		
			See preceding page.		

<b>COMPONENTS:</b> 1. Xenon; Xe; 7440-63-3 2. Carbon Disulfide; CS <sub>2</sub> ; 75-15-0	<b>ORIGINAL MEASUREMENTS:</b> Powell, R.J.  <u>J. Chem. Eng. Data</u> 1972, <u>17</u> , 302-304.
<b>VARIABLES:</b> T/K: 298.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> P.L. Long

**EXPERIMENTAL VALUES:**

T/K	Mol Fraction $x_1 \times 10^2$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	$R \frac{\Delta \log x_1}{\Delta \log T} = N$
298.15	1.042	3.89	4.25	-9.08

The author implies that solubility measurements were made between 273.15 and 308.15, but only the solubility at 298.15 was given in the paper. The slope  $R (\Delta \log x_1 / \Delta \log T)$  was given. The smoothed data below were calculated by the compiler from the slope in the form:

$$\log x_1 = \log (1.042 \times 10^{-2}) + (-9.08/R) \log (T/298.15)$$

with  $R = 1.9872 \text{ cal K}^{-1} \text{ mol}^{-1}$ .

Smoothed data:

T/K	Mol Fraction $x_1 \times 10^2$
273.15	1.555
278.15	1.431
283.15	1.319
288.15	1.218
293.15	1.126
298.15	1.042
303.15	0.9657

The Bunsen and Ostwald Coefficients were calculated by the compiler.

**AUXILIARY INFORMATION****METHOD / APPARATUS / PROCEDURE:**

Solvent is degassed by freezing and pumping, then boiling under reduced pressure. The Dymond and Hildebrand (1) apparatus, with all glass pumping system, is used to spray slugs of degassed solvent into the xenon. Amount of gas dissolved is calculated from the initial and final gas pressures.

**SOURCE AND PURITY OF MATERIALS:**

- Xenon. No source. Manufacturer's research grade, dried over CaCl<sub>2</sub> before use.
- Carbon disulfide. No source. Manufacturer's spectrochemical grade.

**ESTIMATED ERROR:**

$$\delta N / \text{cal K}^{-1} \text{ mol}^{-1} = 0.1$$

$$\delta x_1 / x_1 = 0.002$$

**REFERENCES:**

- Dymond, J.; Hildebrand, J.H. Ind. Eng. Chem. Fundam. 1967, 6, 130.

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Xenon; Xe; 7440-63-3</li> <li>Sulfinylbismethane (Dimethyl Sulfoxide); <math>C_2H_6OS</math> (<math>CH_3SOCH_3</math>); 67-68-5</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Dymond, J. H.</p> <p><u>J. Phys. Chem.</u> 1967, <u>71</u>, 1829-1831.</p>								
<p>VARIABLES:</p> <p>T/K: 298.15 P/kPa: 101.325 (1 atm)</p>	<p>PREPARED BY:</p> <p>M. E. Derrick</p>								
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="353 511 1075 638"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^2</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>0.170</td> <td>0.535</td> <td>0.584</td> </tr> </tbody> </table> <p>The Bunsen and Ostwald coefficients were calculated by the compiler.</p>		T/K	Mol Fraction $X_1 \times 10^2$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	298.15	0.170	0.535	0.584
T/K	Mol Fraction $X_1 \times 10^2$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L						
298.15	0.170	0.535	0.584						
<p>AUXILIARY INFORMATION</p>									
<p>METHOD/APPARATUS/PROCEDURE:</p> <p>The liquid is saturated with the gas at a gas partial pressure of 1 atm.</p> <p>The apparatus is that described by Dymond and Hildebrand (1). The apparatus uses an all-glass pumping system to spray slugs of degassed solvent into the gas. The amount of gas dissolved is calculated from the initial and final gas pressure.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>Xenon. Matheson Co., Dried.</li> <li>Dimethyl Sulfoxide. Matheson, Coleman, and Bell Co. Spectro-quality reagent, dried, and a fraction frozen out. Melting pt.: 18.37° C.</li> </ol> <p>ESTIMATED ERROR:</p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>Dymond, J.; Hildebrand, J. H. <u>Ind. Eng. Chem. Fundam.</u> 1967, <u>6</u>, 130.</li> </ol>								

<b>COMPONENTS:</b> 1. Xenon; Xe; 7440-63-3  2. 1,1,2,2,3,3,4,4,4-nonafluoro-N,N-bis(nonafluorobutyl)-1-butanamine (Perfluorotributylamine); (C <sub>4</sub> F <sub>9</sub> ) <sub>3</sub> N; 311-89-7	<b>ORIGINAL MEASUREMENTS:</b> Powell, R.J.  <u>J. Chem. Eng. Data</u> 1972, <u>17</u> , 302-304.																
<b>VARIABLES:</b> T/K: 298.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> P.L. Long																
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T/K	Mol Fraction $x_1 \times 10^2$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	$R \frac{\Delta \log x_1}{\Delta \log T} = N$													
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$\log x_1 = \log (2.152 \times 10^{-2}) + (-5.01/R) \log (T/298.15)$																	
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<p style="text-align: center;">AUXILIARY INFORMATION</p>																	
<b>METHOD/APPARATUS/PROCEDURE:</b> <p>Solvent is degassed by freezing and pumping, then boiling under reduced pressure. The Dymond and Hildebrand (1) apparatus, with all glass pumping system, is used to spray slugs of degassed solvent into the xenon. Amount of gas dissolved is calculated from the initial and final gas pressures.</p>	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Xenon. No source. Manufacturer's research grade, dried over CaCl <sub>2</sub> before use.  2. Perfluorotributylamine. Minnesota Mining & Mfg. Co. Column distilled, used portion with b.p. = 447.85 - 448.64K, & single peak GC.																
<b>ESTIMATED ERROR:</b> $\delta N / \text{cal K}^{-1} \text{ mol}^{-1} = 0.1$ $\delta x_1 / x_1 = 0.002$																	
<b>REFERENCES:</b> 1. Dymond, J.; Hildebrand, J.H. <u>Ind. Eng. Chem. Fundam.</u> 1967, <u>6</u> , 130.																	

COMPONENTS:		ORIGINAL MEASUREMENTS:			
1. Xenon; Xe; 7440-63-3		Steinberg, M.; Manowitz, B.; Pruzansky, J.			
2. Nitrous Oxide; N <sub>2</sub> O; 10024-97-2		US AEC BNL-542 (T-140). Chem. Abstr. 1959, <u>53</u> , 21242g.			
VARIABLES:		PREPARED BY:			
T/K: 193.15 - 243.65		H. L. Clever			
EXPERIMENTAL VALUES:					
T/K	Absorption Coefficient	Henry's Constant K/atm	Mol Fraction X <sub>1</sub> × 10 <sup>2</sup>	Bunsen Coefficient α	Ostwald Coefficient L
193.15	60.5	--	8.51	57.4	40.5 <sub>5</sub>
201.15	--	13.5	7.4	--	--
234.15	15.3	--	2.52	14.5	12.4
240.15	--	45	2.2	--	--
243.65	--	50	2.0	--	--
Smoothed Data: $\Delta G^{\circ}/J \text{ mol}^{-1} = -RT \ln X_1 = -11,702 + 80.501 T$					
Std. Dev. $\Delta G^{\circ} = 88.5$ , Coef. Corr. = 0.9989					
$\Delta H^{\circ}/J \text{ mol}^{-1} = -11,702$ , $\Delta S^{\circ}/J \text{ K}^{-1} \text{ mol}^{-1} = -80.501$					
T/K	Mol Fraction X <sub>1</sub> × 10 <sup>2</sup>	$\Delta G^{\circ}/J \text{ mol}^{-1}$			
193.15	9.12	3,845.9			
203.15	6.37	4,650.9			
213.15	4.60	5,455.9			
223.15	3.42	6,260.9			
233.15	2.61	7,065.9			
243.15	2.04	7,870.9			
AUXILIARY INFORMATION					
METHOD/APPARATUS/PROCEDURE:			SOURCE AND PURITY OF MATERIALS:		
Dynamic tracer technique (1).			1. Xenon.		
The Henry's constant is			2. Nitrous oxide.		
$K = (P/\text{atm})/X_1$					
The Henry's constants are probably from data smoothed by the authors.					
The report is discussed further in a later paper (2).					
			**ESTIMATED ERROR:		
			$\delta X/X = 0.03 - 0.05$ (Compiler)		
			REFERENCES:		
			1. Steinberg, M.; Manowitz, B. <u>Ind. Eng. Chem.</u> 1959, <u>51</u> , 47.		
			2. Steinberg, M. US AEC TID-7593, 1959, 217. <u>Chem. Abstr.</u> 1961, <u>55</u> , 9083e.		

<b>COMPONENTS:</b> 1. Xenon; Xe; 7440-63-3 2. Nitromethane; CH <sub>3</sub> NO <sub>2</sub> ; 75-52-5	<b>ORIGINAL MEASUREMENTS:</b>  Friedman, H.L.  J. Am. Chem. Soc. 1954, <u>76</u> , <u>3294-3297</u> .																		
<b>VARIABLES:</b> T/K: 298.00 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b>  P.L. Long																		
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="295 487 967 715"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td rowspan="3">298.00</td> <td></td> <td></td> <td>1.15</td> </tr> <tr> <td></td> <td></td> <td>1.11</td> </tr> <tr> <td></td> <td></td> <td>1.15</td> </tr> <tr> <td></td> <td>0.201</td> <td>1.04</td> <td>1.14 av.</td> </tr> </tbody> </table> <p data-bbox="77 735 1169 854">The author reports Ostwald coefficients measured at about 700 mmHg. The Bunsen coefficient and the mole fraction solubility at 101.325 kPa (1 atm) were calculated by the compiler with the assumptions that the gas is ideal, that Henry's law is obeyed and that the Ostwald coefficient is independent of pressure.</p>		T/K	Mol Fraction $x_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	298.00			1.15			1.11			1.15		0.201	1.04	1.14 av.
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<b>AUXILIARY INFORMATION</b>																			
<b>METHOD:</b> Gas absorption. The method was essentially that employed by Eucken and Herzberg (1). Modifications included a magnetic stirring device instead of shaking the saturation vessel, and balancing the gas pressure against a column of mercury with electrical contacts instead of balancing the gas pressure against the atmosphere.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Xenon. Air Reduction Co. Reagent grade, 99.8 per cent pure by mass spectroscopy. 2. Nitromethane. Source not given. Distilled, dried by filtering at 253 K.																		
<b>APPARATUS/PROCEDURE:</b> The solvent was degassed by vacuum. The procedure, repeated 5-10 times, was to alternate 5-15 s evacuation and rapid stirring to produce cavitation. In the solubility measurement, gas, pre-saturated with solvent vapor, was brought into contact with about 80 ml of solvent in the saturation vessel. Initial conditions were established by a time extrapolation. Solubility equilibrium was approached from both under- and supersaturation by varying the rate.	<b>ESTIMATED ERROR:</b> $\delta T/K = 0.05$ $\delta P/\text{mmHg} = 0.3$ $\delta L/L = 0.03$  <b>REFERENCES:</b> 1. Eucken, A.; Herzberg, G. <u>Z. Phys. Chem.</u> 1950, <u>195</u> , 1.																		

<b>COMPONENTS:</b> 1. Xenon; Xe; 7440-63-3 2. Benzenamine (Aniline); C <sub>6</sub> H <sub>7</sub> N; 62-53-3	<b>ORIGINAL MEASUREMENTS:</b> Steinberg, M.; Manowitz, B.  Ind. Eng. Chem. 1959, <u>51</u> , 47-51.								
<b>VARIABLES:</b> T/K: 303.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> H.L. Clever A.L. Cramer								
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="360 478 1022 595"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^2</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Absorption Coefficient <math>\beta</math></th> </tr> </thead> <tbody> <tr> <td>303.15</td> <td>0.173</td> <td>0.43</td> <td>0.45</td> </tr> </tbody> </table> <p>The authors define the Absorption coefficient as the volume of gas, corrected to 288.15 K and 101.325 kPa, absorbed under a total system pressure of 101.325 kPa per unit volume of solvent at 288.15 K.</p> <p>The mole fraction solubilities and Bunsen coefficients were calculated by the compiler.</p> <p>The solubility of xenon in benzenamine reported by von Antropoff at 303.15 K is about 9 per cent higher than the Steinberg and Manowitz value (see next page). There is not enough information to recommend one value over the other.</p>		T/K	Mol Fraction $X_1 \times 10^2$	Bunsen Coefficient $\alpha$	Absorption Coefficient $\beta$	303.15	0.173	0.43	0.45
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<b>AUXILIARY INFORMATION</b>									
<b>METHOD / APPARATUS / PROCEDURE:</b> Absorption coefficient determined by a modified McDaniel method (1).	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Xenon. Matheson Co., Inc. Technical grade. 2. Benzenamine. Source not given. Chemically pure grade.  <b>ESTIMATED ERROR:</b> $\delta\beta/\beta = 0.05 - 0.10$  <b>REFERENCES:</b> 1. Furman, N.H. "Scott's Standard Methods of Chemical Analysis" Van Nostrand Co., NY, 1939, 5th ed., Vol. II, p. 2587.								



<b>COMPONENTS:</b> 1. Xenon; Xe; 7440-63-3 2. Benzenamine (Aniline); C <sub>6</sub> H <sub>7</sub> N; 62-53-3			<b>ORIGINAL MEASUREMENTS:</b> von Antropoff, A.  Z. <u>Electrochem.</u> 1919, <u>25</u> , 269-308.			
<b>VARIABLES:</b> T/K: 283.15 - 323.15 P/kPa: 101.325 (1 atm)			<b>PREPARED BY:</b>			
<b>EXPERIMENTAL VALUES:</b>						
	T/K	Kuenen Coefficient S	Mol Fraction X <sub>1</sub> × 10 <sup>2</sup>	Bunsen Coefficient α	Ostwald Coefficient L	
	283.15	0.6687	0.277	0.689	0.714	
	293.15	0.5006	0.208	0.512	0.549	
	298.15	0.4758				
	298.15	0.4733	0.197	0.484	0.528	
	303.15	0.4546				
	303.15	0.4426	0.189	0.462	0.513	
	313.15	0.4336				
	313.15	0.4308	0.179	0.434	0.498	
	323.15	0.3892				
	323.15	0.4113	0.171	0.411	0.486	
<p>The Kuenen coefficient was measured at pressures varying from 518 to 632 mmHg and corrected to 760 mmHg by Henry's law by the author. The Bunsen, Ostwald and mole fraction solubilities were calculated by the compiler.</p> <p>Smoothed Data: The solubility value at 283.15 K was not used.  <math>\Delta G^\circ/J \text{ mol}^{-1} = -RT \ln X_1 = -4,957.1 + 68.381 T</math>            Std. Dev. <math>\Delta G^\circ = 28.9</math>, Coef. corr. = 0.9994  <math>\Delta H^\circ/J \text{ mol}^{-1} = -4,957.1</math>, <math>\Delta S^\circ/J \text{ K}^{-1} \text{ mol}^{-1} = -68.381</math></p>						
	T/K	Mol Fraction X <sub>1</sub> × 10 <sup>2</sup>	$\Delta G^\circ/J \text{ mol}^{-1}$	T/K	Mol Fraction X <sub>1</sub> × 10 <sup>2</sup>	$\Delta G^\circ/J \text{ mol}^{-1}$
	293.15	0.205	15,089	313.15	0.180	16,456
	298.15	0.198	15,431	318.15	0.175	16,798
	303.15	0.192	15,772	323.15	0.170	17,140
	308.15	0.186	16,114			
<b>AUXILIARY INFORMATION</b>						
<b>METHOD /APPARATUS/PROCEDURE:</b> Gas absorption. A modification of the apparatus of Estreicher. A calibrated buret connected to an absorption vessel by a flexible glass helix so the absorption vessel can be shaken. Solvent degassed by heat and vacuum (1).			<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Xenon. 2. Aniline was prepared from aniline sulfate. It was freshly distilled before use.			
			<b>ESTIMATED ERROR:</b> $\delta S/S = 0.03$			
			<b>REFERENCES:</b> 1. Estreicher, T. Z. <u>Phys. Chem.</u> 1899, <u>31</u> , 176.			

<b>COMPONENTS:</b> 1. Xenon; Xe; 7440-63-3 2. Nitrobenzene; C <sub>6</sub> H <sub>5</sub> NO <sub>2</sub> ; 98-95-3	<b>ORIGINAL MEASUREMENTS:</b> Saylor, J.H.; Battino, R.  J. Phys. Chem. 1953, <u>62</u> , 1334-1337.																																																		
<b>VARIABLES:</b> T/K: 288.25 - 328.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> H.L. Clever, A.L. Cramer																																																		
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<b>METHOD/APPARATUS/PROCEDURE:</b> <p>The solvent was degassed by evacuating the space above it, shaking, and then passing it as a fine mist into another evacuated container. The degassed liquid was saturated as it passed as a thin film inside a glass helix which contained the solute gas plus solvent vapor at a total pressure of 1 atm (1,2). The volume of liquid and the volume of gas absorbed are determined in a system of burets.</p> <p>The smoothed data above are based on only two experimental points. They should be used with caution.</p>	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Xenon. Linde Air Products Co. 2. Nitrobenzene. Eastman Kodak white label. Distilled from P <sub>4</sub> O <sub>10</sub> , b.p. 81.0 - 81.2°C (10 mmHg).  <b>ESTIMATED ERROR:</b> $\delta T/\text{K} = 0.03$ $\delta P/\text{mmHg} = 1.0$ $\delta X_1/X_1 = 0.005$ (authors)  <b>REFERENCES:</b> 1. Morrison, T.J.; Billett, F. J. Chem. Soc. 1948, 2033. 2. Clever, H.L.; Battino, R.; Saylor, J.H.; Gross, P.M. J. Phys. Chem. 1957, <u>61</u> , 1078.																																																		

<b>COMPONENTS:</b> 1. Xenon; Xe; 7440-63-3 2. Emulsions and Other Mixed Solvents	<b>ORIGINAL MEASUREMENTS:</b> Steinberg, M.; Manowitz, B.  <u>Ind. Eng. Chem.</u> 1959, <u>51</u> , 47-50.																						
<b>VARIABLES:</b> T/K: 292.15 - 305.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b>  P.L. Long																						
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="319 498 960 995"> <thead> <tr> <th>T/K</th> <th>Absorption Coefficient <math>\beta</math></th> </tr> </thead> <tbody> <tr> <td colspan="2" style="text-align: center;">Koppers Emulsion K-900 (50 wt % styrene - butadiene in water)</td> </tr> <tr> <td>305.15</td> <td>0.95</td> </tr> <tr> <td colspan="2" style="text-align: center;">Pine Oil</td> </tr> <tr> <td>292.15</td> <td>2.25</td> </tr> <tr> <td colspan="2" style="text-align: center;">Toluene; C<sub>7</sub>H<sub>8</sub>; 108-88-3</td> </tr> <tr> <td>297.15</td> <td>3.17</td> </tr> <tr> <td colspan="2" style="text-align: center;">Pine Oil (60 vol %) + Toluene (40 vol %)</td> </tr> <tr> <td>298.15</td> <td>2.55</td> </tr> <tr> <td colspan="2" style="text-align: center;">Ultrasene (80 wt % paraffin, 20 wt % naphthene)</td> </tr> <tr> <td>294.15</td> <td>3.53</td> </tr> </tbody> </table> <p>The authors define the Absorption Coefficient as the volume of gas, corrected to 288.15 K and 101.325 kPa, absorbed under a total system pressure of 101.325 kPa per unit volume of solvent at 288.15 K.</p>		T/K	Absorption Coefficient $\beta$	Koppers Emulsion K-900 (50 wt % styrene - butadiene in water)		305.15	0.95	Pine Oil		292.15	2.25	Toluene; C <sub>7</sub> H <sub>8</sub> ; 108-88-3		297.15	3.17	Pine Oil (60 vol %) + Toluene (40 vol %)		298.15	2.55	Ultrasene (80 wt % paraffin, 20 wt % naphthene)		294.15	3.53
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<b>METHOD/APPARATUS/PROCEDURE:</b> The absorption coefficients were determined by a modified McDaniel method (1). Dynamic tracer technique was used with the Ultrasene.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Xenon. Matheson Co., Inc. Technical pure grade. 2. Ultrasene. Atlantic Refining Co. No information given on other solvents.																						
	<b>ESTIMATED ERROR:</b>  $\delta\beta/\beta = 0.05 - 0.10$																						
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<b>COMPONENTS:</b> 1. Xenon; Xe; 7440-63-3 2. Silicone Oils and Related Fluids	<b>ORIGINAL MEASUREMENTS:</b> Steinberg, M.; Manowitz, B.  <u>Ind. Eng. Chem.</u> 1959, <u>51</u> , 47-50.																								
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<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: center; border-top: 1px solid black; border-bottom: 1px solid black;">T/K</th> <th style="text-align: center; border-top: 1px solid black; border-bottom: 1px solid black;">Absorption Coefficient <math>\beta</math></th> </tr> </thead> <tbody> <tr> <td colspan="2" style="text-align: center;">Dow Corning Silicone Oil 200 (Dimethylsiloxane, 10 centistoke)</td> </tr> <tr> <td style="text-align: center;">297.15</td> <td style="text-align: center;">1.50</td> </tr> <tr> <td style="text-align: center;">368.15</td> <td style="text-align: center;">0.17</td> </tr> <tr> <td colspan="2" style="text-align: center;">Dow Corning Silicone Oil 200 (Dimethylsiloxane, 1 centistoke)</td> </tr> <tr> <td style="text-align: center;">303.15</td> <td style="text-align: center;">2.45</td> </tr> <tr> <td colspan="2" style="text-align: center;">Dow Corning Silicone Oil 702 (contains diphenyl groups)</td> </tr> <tr> <td style="text-align: center;">300.15</td> <td style="text-align: center;">0.93</td> </tr> <tr> <td colspan="2" style="text-align: center;">Dow Corning Anti-Foam A (60 wt % silicone oil in water)</td> </tr> <tr> <td style="text-align: center;">301.15</td> <td style="text-align: center;">0.74</td> </tr> <tr> <td colspan="2" style="text-align: center;">Dowtherm A (Diphenyl-Diphenyl Oxide)</td> </tr> <tr> <td style="text-align: center;">301.15</td> <td style="text-align: center;">0.88</td> </tr> </tbody> </table> <p>The authors define the Absorption Coefficient as the volume of gas, corrected to 288.15 K and 101.325 kPa, absorbed under a total system pressure of 101.325 kPa per unit volume of solvent at 288.15 K.</p>		T/K	Absorption Coefficient $\beta$	Dow Corning Silicone Oil 200 (Dimethylsiloxane, 10 centistoke)		297.15	1.50	368.15	0.17	Dow Corning Silicone Oil 200 (Dimethylsiloxane, 1 centistoke)		303.15	2.45	Dow Corning Silicone Oil 702 (contains diphenyl groups)		300.15	0.93	Dow Corning Anti-Foam A (60 wt % silicone oil in water)		301.15	0.74	Dowtherm A (Diphenyl-Diphenyl Oxide)		301.15	0.88
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<b>AUXILIARY INFORMATION</b>																									
<b>METHOD/APPARATUS/PROCEDURE:</b> The absorption coefficient at one atmosphere of xenon was measured by a modified McDaniel method (1).	<b>SOURCE AND PURITY OF MATERIALS:</b> <ol style="list-style-type: none"> <li>1. Xenon. Matheson Co., Inc. Technical grade.</li> <li>2. Solvents. Dowtherm A from Dow Chemical Co. No statement about other solvents.</li> </ol> <b>ESTIMATED ERROR:</b>  $\delta\beta/\beta = 0.05 - 0.10$ <b>REFERENCES:</b> <ol style="list-style-type: none"> <li>1. Furman, N.H. "Scott's Standard Methods of Chemical Analysis" Van Nostrand Co., NY 1939, 5th ed., Vol. II, p. 2587.</li> </ol>																								

## COMPONENTS:

1. Xenon; Xe; 7440-63-3
2. Olive Oil

## EVALUATOR:

H. L. Clever  
 Chemistry Department  
 Emory University  
 Atlanta, GA 30322  
 U.S.A.

August 1978

## CRITICAL EVALUATION:

The solubility of xenon in olive oil was measured by Lawrence, Loomis, Tobias and Turpin (1) at 295.15 and 310.15 K, by Yeh and Peterson (2) at 298.15, 303.15, 310.15 and 318.15 K and at 310.15 K by Ladefoged and Anderson (3) and by Kitani (4).

The data were converted to a mole fraction solubility at a partial pressure of xenon of 101.325 kPa (1 atm) assuming that olive oil is 1,2,3-propanetriyl ester of Z-9-octadecenoic acid, or triolein, of molecular weight 885.46. The data from the four laboratories shows considerable scatter. Yeh and Peterson made direct volumetric measurements at atmospheric pressure. The other workers used radiochemical techniques at low xenon partial pressure in the presence of a carrier gas, which can be subject to greater errors than the volumetric method. The data of Yeh and Peterson are internally self-consistent. It was decided to accept the Yeh and Peterson data as tentative values of the xenon in olive oil solubility.

The Yeh and Peterson data were used in a linear regression of a Gibbs energy equation linear in temperature. The tentative values of the thermodynamic changes for the transfer of one mole of xenon from the gas at 101.325 kPa (1 atm) to the hypothetical unit mole fraction solution are

$$\Delta G^{\circ}/J \text{ mol}^{-1} = -RT \ln X_1 = -8,733.3 + 50.649 T$$

$$\text{Std. Dev.} = 4.9, \text{ Coef. Corr.} = 0.9999$$

$$\Delta H^{\circ}/J \text{ mol}^{-1} = -8,773.3, \Delta S^{\circ}/J \text{ K}^{-1} \text{ mol}^{-1} = -50.649$$

A table of tentative mole fraction solubility and Gibbs energy values as a function of temperature appears below.

TABLE 1. The solubility of xenon in olive oil. The tentative values of the mole fraction solubility at a xenon partial pressure of 101.325 kPa (1 atm) and the Gibbs energy change as a function of temperature.

T/K	Mol Fraction $X_1 \times 10^2$	$\Delta G^{\circ}/J \text{ mol}^{-1}$
293.15	8.14	6,114.5
295.15	7.94	6,215.8
298.15	7.66	6,367.8
303.15	7.23	6,621.0
308.15	6.83 <sub>5</sub>	6,874.3
310.15	6.69	6,975.6
313.15	6.47	7,127.5
318.15	6.14	7,380.8

Continued on next page.

## COMPONENTS:

1. Xenon; Xe; 7440-63-3
2. Olive Oil

## EVALUATOR:

H.L. Clever  
 Chemistry Department  
 Emory University  
 Atlanta, GA 30322  
 U.S.A.

August 1978

## CRITICAL EVALUATION:

Figure 1 shows the per cent deviation of all of the mole fraction solubility values from the smoothed data of Yeh and Peterson. Since olive oil is a natural product that may vary in composition and thus show variation in its solvent capacity it is not possible to classify any of the data as incorrect. Data sheets on all of the xenon in olive oil solubility reports are included.

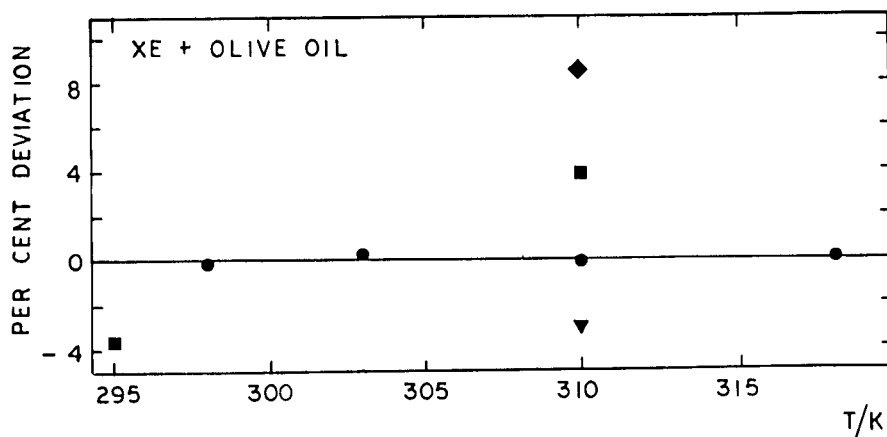


FIGURE 1. Solubility of xenon in olive oil. Per cent deviation from regression line for Yeh and Peterson's data.

▼ Ladefoged and Anderson, ● Yeh and Peterson,  
 ■ Lawrence, et al., and ◆ Kitani.

## REFERENCES

1. Lawrence, J.H.; Loomis, W.F.; Tobias, C.A., Turpin, F.H. J. Physiol. 1946, 105, 197.
2. Yeh, S.-Y.; Peterson, R.E. J. Pharm. Sci. 1963, 52, 453.
3. Ladefoged, J.; Anderson, A.M. Phys. Med. Biol. 1967, 12, 353.
4. Kitani, K. Scand. J. Clin. Lab. Invest. 1972, 29, 167.

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Xenon; Xe; 7440-63-3</li> <li>Olive oil</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Lawrence, J. H.; Loomis, W. F.; Tobias, C. A.; Turpin, F. H.</p> <p><u>J. Physiol.</u> 1946, <u>105</u>, 197-204.</p>												
<p>VARIABLES:</p> <p>T/K: 295.15 - 310.15</p>	<p>PREPARED BY:</p> <p>H. L. Clever A. L. Cramer</p>												
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="319 512 998 677"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^2</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>295.15</td> <td>7.65</td> <td>1.9</td> <td>2.0<sub>5</sub></td> </tr> <tr> <td>310.15</td> <td>6.95</td> <td>1.7</td> <td>1.9<sub>5</sub></td> </tr> </tbody> </table> <p>The mole fraction solubility and Ostwald coefficients were calculated by the compiler.</p> <p>The molecular weight of olive oil was taken to be 885 and the density was calculated from <math>\rho = 0.9152 - 0.000468t/^\circ\text{C}</math> (1) for the mole fraction calculation.</p> <p>See the evaluation sheet for the solubility in olive oil for more information.</p>		T/K	Mol Fraction $x_1 \times 10^2$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	295.15	7.65	1.9	2.0 <sub>5</sub>	310.15	6.95	1.7	1.9 <sub>5</sub>
T/K	Mol Fraction $x_1 \times 10^2$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L										
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310.15	6.95	1.7	1.9 <sub>5</sub>										
<p>AUXILIARY INFORMATION</p>													
<p>METHOD /APPARATUS/PROCEDURE:</p> <p>Radiochemical method. No details of the method given, but authors state they used an isotope of half life 34 days. Possibly the isotope was xenon-127.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>No information given.</p> <hr/> <p>ESTIMATED ERROR:</p> <p><math>\delta\alpha/\alpha = 0.05</math> (Compiler)</p> <hr/> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>Battino, R.; Evans, F.D.; Danforth, W. F. <u>J. Am. Oil Chem. Soc.</u> 1968, <u>45</u>, 830.</li> </ol>												

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Xenon; Xe; 7440-63-3</li> <li>Olive Oil</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Yeh, S.Y.; Peterson, R.E.</p> <p><u>J. Pharm. Sci.</u> 1963, <u>52</u>, 453-458.</p>																				
<p>VARIABLES:</p> <p>T/K: 298.15 - 318.15 P/kPa: 101.325 (1 atm)</p>	<p>PREPARED BY:</p> <p>H.L. Clever</p>																				
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="299 493 1081 697"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^2</math></th> <th>Bunsen Coefficient <math>\alpha \pm</math> Std. Dev.</th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>7.65</td> <td>1.8988 + 0.0014</td> <td>2.0725</td> </tr> <tr> <td>303.15</td> <td>7.25</td> <td>1.7857 + 0.0013</td> <td>1.9749</td> </tr> <tr> <td>310.15</td> <td>6.68</td> <td>1.6307 + 0.0014</td> <td>1.8532</td> </tr> <tr> <td>318.15</td> <td>6.14</td> <td>1.4839 + 0.0012</td> <td>1.7248</td> </tr> </tbody> </table> <p>The Bunsen coefficients are the average of three measurements. The Ostwald coefficients were fitted by the method of least squares to the equation <math>\log L = A/T + B</math> by the authors. The same line fitted olive oil and the fats. From the slope and intercept they obtained</p> $\Delta H^\circ = (-2273 \pm 80) \text{ cal mol}^{-1} \text{ and } \Delta S^\circ = (-6.4 \pm 0.2) \text{ cal K}^{-1} \text{ mol}^{-1}$ <p>The mole fractions were calculated by the compiler for a xenon partial pressure of 101.325 kPa (1 atm) assuming that olive oil has a molecular weight of 885.46 and a density of <math>\rho/g \text{ cm}^{-3} = 0.9152 - 4.68 \times 10^{-4}t/^\circ\text{C}</math> (2).</p> <p>See the evaluation of the xenon + olive oil system on pages 193 - 194 for the tentative thermodynamic changes of the solution process and the solubility values.</p> <p>The values of the thermodynamic changes above, which are based on the temperature coefficient of the Ostwald coefficient, are for the standard state change of transferring one mole of xenon from the gas phase at a concentration of one mole <math>\text{dm}^{-3}</math> to the solution at a concentration of one mole <math>\text{dm}^{-3}</math>. The values in the evaluation are for the standard state change of transferring one mole of xenon from the gas at 101.325 kPa (1 atm) to a hypothetical unit mole fraction solution.</p> <p style="text-align: center;">AUXILIARY INFORMATION</p>		T/K	Mol Fraction $X_1 \times 10^2$	Bunsen Coefficient $\alpha \pm$ Std. Dev.	Ostwald Coefficient L	298.15	7.65	1.8988 + 0.0014	2.0725	303.15	7.25	1.7857 + 0.0013	1.9749	310.15	6.68	1.6307 + 0.0014	1.8532	318.15	6.14	1.4839 + 0.0012	1.7248
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318.15	6.14	1.4839 + 0.0012	1.7248																		
<p>METHOD /APPARATUS/PROCEDURE:</p> <p>Oil was dried and degassed by stirring under vacuum at 80°C for about 12 hr. A 50 ml. sample was placed in an absorption flask attached to a Geffken gas buret (1). The oil was constantly stirred and equilibrated with increments of gas until no change was observed in a differential oil manometer for <math>\frac{1}{2}</math> hr. Difference between initial and final buret readings indicated amount of gas absorbed. Absorption at successively lower temperatures was determined. The authors also measured the viscosity and surface tension of the liquid.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>Xenon. Matheson Co. Research grade, maximum impurity 0.02 mol percent <math>\text{N}_2</math> and 0.05 mol percent Kr.</li> <li>Olive oil. Magnus, Mabee, and Raynard Co., U.S.P.</li> </ol>																				
	<p>ESTIMATED ERROR:</p> $\delta T/K = 0.05$ $\delta P/\text{mmHg} = 0.5$ $\delta \alpha/\alpha = 0.005$																				
	<p>REFERENCES:</p> <ol style="list-style-type: none"> <li>Geffken, G. <u>Z. Physik Chem.</u> 1904, <u>49</u>, 257.</li> <li>Battino, R.; Evans, F. D.; Danforth, W. F. <u>J. Am. Oil Chem. Soc.</u> 1968, <u>45</u>, 830.</li> </ol>																				



<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Xenon-133; <math>^{133}\text{Xe}</math>; 14932-42-4</li> <li>Olive Oil</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Ladefoged, J.; Andersen, A.M.</p> <p><u>Phys. Med. Biol.</u> 1967, <u>12</u>, 353-358.</p>										
<p>VARIABLES:</p> <p>T/K: 310.15</p>	<p>PREPARED BY:</p> <p>A.L. Cramer</p>										
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="198 498 1139 644"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^2</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L <math>\pm</math> Std Dev</th> <th>Number of Determinations</th> </tr> </thead> <tbody> <tr> <td>310.15</td> <td>6.48</td> <td>1.58</td> <td>1.79 <math>\pm</math> 0.04</td> <td>8</td> </tr> </tbody> </table> <p>The mole fraction solubility and Bunsen coefficient were calculated by the compiler.</p> <p>The molecular weight of olive oil was taken to be 885 and the density was calculated from <math>\rho = 0.9152 - 0.000468t/^\circ\text{C}</math> (1) for the mole fraction calculation.</p> <p>See the evaluation sheet for the solubility in olive oil for more information.</p>		T/K	Mol Fraction $x_1 \times 10^2$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L $\pm$ Std Dev	Number of Determinations	310.15	6.48	1.58	1.79 $\pm$ 0.04	8
T/K	Mol Fraction $x_1 \times 10^2$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L $\pm$ Std Dev	Number of Determinations							
310.15	6.48	1.58	1.79 $\pm$ 0.04	8							
<p>AUXILIARY INFORMATION</p>											
<p>METHOD /APPARATUS/PROCEDURE:</p> <p>The olive oil in small vials was equilibrated with a mixture of air and xenon-133 for 24 h at 310.15 K with continuous stirring. After equilibration, 0.1 ml samples were transferred by syringes to a 2 ml rubber-capped vial and counted in a scintillation counter to a statistical error below 1 per cent.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>Xenon-133. Radiochemical Centre, Amersham, UK. Impurities less than 2 per cent.</li> <li>Olive oil. Commercial Pharmacy. Met standards of Pharmacopia Nordeia and Pharmacopia Danica.</li> </ol> <p>ESTIMATED ERROR:</p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>Battino, R.; Evans, F.D. Danforth, W.F. <u>J. Am. Oil Chem. Soc.</u> 1968, <u>45</u>, 830.</li> </ol>										

<b>COMPONENTS:</b> 1. Xenon-133; $^{133}_{54}\text{Xe}$ ; 14932-42-4 2. Olive Oil	<b>ORIGINAL MEASUREMENTS:</b> Kitani, K.  Scand. J. Clin. Lab. Invest. 1972, <u>29</u> , 167-172.										
<b>VARIABLES:</b>  T/K: 310.15	<b>PREPARED BY:</b>  P. L. Long A. L. Cramer										
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="234 489 1171 622"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^2</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient <math>L \pm \text{Std Dev}</math></th> <th>Number of Determinations</th> </tr> </thead> <tbody> <tr> <td>310.15</td> <td>7.25</td> <td>1.658</td> <td>1.883 <math>\pm</math> 0.036</td> <td>9</td> </tr> </tbody> </table> <p>The mole fraction solubility and Bunsen coefficient were calculated by the compiler.</p> <p>The molecular weight of olive oil was taken to be 885, and the density (1) was calculated from <math>\rho = 0.9152 - 0.000468t/^\circ\text{C}</math> for the mole fraction calculation.</p> <p>See the evaluation sheet on olive oil for more information.</p>		T/K	Mol Fraction $X_1 \times 10^2$	Bunsen Coefficient $\alpha$	Ostwald Coefficient $L \pm \text{Std Dev}$	Number of Determinations	310.15	7.25	1.658	1.883 $\pm$ 0.036	9
T/K	Mol Fraction $X_1 \times 10^2$	Bunsen Coefficient $\alpha$	Ostwald Coefficient $L \pm \text{Std Dev}$	Number of Determinations							
310.15	7.25	1.658	1.883 $\pm$ 0.036	9							
<b>AUXILIARY INFORMATION</b>											
<b>METHOD /APPARATUS/PROCEDURE:</b>  Glass cuvettes were filled with the solvent. One-third was replaced by the radioactive gas and air. The sealed cuvette was rotated for two hours in a water bath at 37°C. The total pressure was adjusted to one atm by means of a thin needle. Samples from both the liquid and gas phase were counted by a scintillation detector and a Phillips pulse-height analyzer at the energy peak. Corrections for self absorption and scatter were made.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Xenon-133. Radiochemical Centre, Amersham, UK. 2. Olive oil. Commercial sample.										
<b>ESTIMATED ERROR:</b>  $\delta L/L = 0.02$											
<b>REFERENCES:</b> 1. Battino, R.; Evans, E.D.; Danforth, W.F. <u>J. Am. Oil Chem. Soc.</u> 1968, <u>45</u> , 830.											

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Xenon; Xe; 7440-63-3</li> <li>Biological systems</li> </ol>	<p>EVALUATOR:</p> <p>H. L. Clever Chemistry Department Emory University Atlanta, GA 30322 U.S.A.</p> <p>September 1978</p>
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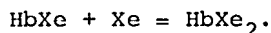
CRITICAL EVALUATION:

The solubility of xenon in biological fluids and tissues.

There are several factors that make it difficult to compare and evaluate the solubility of xenon in biological systems. First, the material from biological specimens may show a natural variation in properties which affects the solubility. Second, workers have used quite different experimental techniques to measure the solubility. Some have used classical volumetric methods with the xenon at a partial pressure near atmospheric pressure. Many have used radiochemical techniques either with natural xenon tagged with radioactive xenon at a total pressure near atmospheric or with a small unknown partial pressure of radioactive xenon. In neither of the radiochemical techniques is it necessary to know the total pressure to obtain an Ostwald coefficient. However, to compare the results of xenon solubility determinations by the volumetric method and by the radiochemical techniques one must assume the Ostwald coefficient is independent of pressure. This may not be true, especially if the gas associates with one or more components of the biological fluid. In these systems the solubility data are classed as tentative. Below are comments, which compare rather than evaluate, the solubility data in several types of biological systems.

Fat. Yeh and Peterson (1) found little difference between the solubility of xenon in olive oil and in human, rat, or dog fat. Conn (2) determined the distribution of xenon between water and dog fat. The distribution coefficient was converted to a gas-fat distribution coefficient on a weight basis, which if converted to a volume basis, assuming a density of  $0.9 \text{ g cm}^{-3}$  for fat, agrees with Yeh and Peterson's value.

Heme proteins. Hemoglobin and methemoglobin. Conn (2) showed that 5 to 12 weight percent solutions of human and dog hemoglobin and methemoglobin obey Henry's law at xenon partial pressures between 175 and 700 mmHg (23.33 - 93.33 kPa) at a temperature of 294.15 K. At a pressure of 700 mmHg (93.33 kPa) xenon, one mole of the protein associates with 1.9 mole of xenon, except the dog methemoglobin, which associates with 1.8 mole xenon. Schoenborn, Vogelhut and Featherstone (3) found 1.8 mole of xenon per mole of human hemoglobin at 293.15 K and a pressure of 760 mmHg (101.325 kPa). Yeh and Peterson (4) found 1.1 mole of xenon per mole of human hemoglobin at a temperature of 310.15 K and a xenon partial pressure of probably 720 mmHg (96.0 kPa). Schoenborn (5, 6) showed that Henry's law is obeyed between 0.5 and 1.5 atm (50.63 and 151.99 kPa) partial pressure xenon dissolved in a 5 per cent horse methemoglobin solution (solubility data not given) at temperatures between 273.15 and 313.15 K. Analysis of the solubility data showed about one mole of xenon bound per mole of protein at 313.15 K and nearly two moles bound at 273.15 K. The amount of xenon bound by reduced and oxyhemoglobin was the same within 5 percent as that bound by methemoglobin. X-ray diffraction analysis showed one xenon in the  $\alpha$  sub-unit and the other in the  $\beta$ -sub-unit of the methemoglobin (two of each site per molecule, for a total of four sites). Wishnia (7) used a radiochemical method with xenon-133 and showed that Henry's law is not obeyed by solutions of hemoglobin in 1.8 molar  $(\text{NH}_4)_2\text{SO}_4$  solution at 273.15 K (graph only). The curve was analyzed by a two step association of xenon and ferrihemoglobin.



He reported constants for the associations. Catchpool (8) reported on the solubility (graph) of xenon in a 0.5 per cent saline solution of human hemoglobin between 278.15 and 310.15 K at a xenon pressure of 1 atm (101.325 kPa). From his measurements he calculated 1.67 mole of xenon per mole of hemoglobin at 293.15 K and 1 atm (101.325 kPa) partial pressure

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Xenon; Xe; 7440-63-3</li> <li>Biological systems</li> </ol>	<p>EVALUATOR:</p> <p>H. L. Clever  Chemistry Department  Emory University  Atlanta, GA 30322  U.S.A.</p> <p>September 1978</p>
<p>CRITICAL EVALUATION:</p> <p>xenon gas. Meuhlbaecher, DeBon, and Featherstone (9) carried out experiments at 310.15 K in phosphate buffer solutions that showed that the solubility of xenon increases in the presence of bovine hemoglobin but not in the presence of either bovine gamma-globulin or bovine serum albumin.</p> <p>The experiments on human, dog, bovine and horse hemoglobin are consistent with a two site association between hemoglobin and xenon which increases as the temperature decreases. The x-ray evidence indicates there are two sites for each of the two associations.</p> <p>Myoglobin, metmyoglobin, cyanometmyoglobin. Schoenborn, Watson and Kendrew (10) equilibrated sperm whale metmyoglobin crystals with xenon at 2.5 atm (253.3 kPa) for 12 h. X-ray diffractions of the equilibrated crystal and normal material, analyzed by the difference Fourier method, showed that the xenon atom is bound to one specific site which is buried in the interior of the molecule. The xenon atom is nearly equidistant from the heme-linked histidine and a pyrrole ring of the heme group. Schoenborn and Nobbs (11) showed that the deoxymyoglobin crystal under similar conditions binds xenon to one specific site. Maestas and Ewing (12) showed that solutions of horse metmyoglobin do not obey Henry's law (graph) at 273.15 K and xenon partial pressures between 0.1 and 1.8 atm (10.133 - 182.385 kPa). The solubility curve was interpreted by a 1:1 association between metmyoglobin and xenon. However, Wishnia (7) interpreted his solubility measurements at 273.15 K in sperm whale myoglobin dissolved in either phosphate buffer (?) or <math>2 \text{ mol dm}^{-3} (\text{NH}_4)_2\text{SO}_4</math> by a two step association. Ewing and Maestas (13) measured the solubility of xenon in 10 per cent horse heart myoglobin, metmyoglobin and cyanometmyoglobin between xenon partial pressures of 0.5 to 5 atm (50.63 - 506.6 kPa) at temperatures of 293.15, 298.15, and 303.15 K. The solubility (data not given) did not obey Henry's law. The solubility data were interpreted as by a single association for the xenon-cyanometmyoglobin and a two step association for the xenon-myoglobin and xenon-metmyoglobin associations. Keys and Lumry (14) report experiments that show the binding of oxygen and xenon by sperm whale myoglobin are independent up to pressures of 2 atm (202.65 kPa) xenon, but that CO and xenon binding are not independent. The evidence of one site in the crystalline material and two sites in the material in solution for xenon may be explained either by differences in configuration of the material or by a difference in accessibility of the site in the crystal and in aqueous solution.</p> <p>Leghemoglobin. Leghemoglobin is a respiratory pigment found in the root nodules of most leguminous plants. Ewing and Ionescu (15) measured the solubility of xenon in 4-10 weight per cent solutions of the ferri- and ferro-leghemoglobin at 278.15, 288.15 and 298.15 K. The results (no solubility data presented) indicated a weak interaction between xenon and leghemoglobin solutions. However, the amount of xenon bound to the leghemoglobin is of the same order of magnitude as the experimental error and it was impossible to determine the stoichiometry of the interaction.</p> <p>Brain Matter. Conn (2) reported water/tissue distribution coefficients for dog gray and white brain matter. Yeh and Peterson (16) reported xenon solubility in a total beef brain homogenate. Both Isbister, Schofield and Torrance (17) and Veall and Mallett (18) report xenon solubility in human gray and white matter homogenate. The solubility coefficient of xenon in human white brain matter from the two laboratories (17, 18) agrees within one per cent. The solubility of xenon in gray brain matter is approximately half the value in white matter and the agreement of the two laboratories is 20 per cent, which is outside the standard error range of the two measurements. Conn's values for dog gray and white matter, when converted to a xenon gas/tissue ratio are much higher than the values for human brain matter. Conn used the solid tissue rather than a homogenate, and he froze the tissue in liquid nitrogen before counting the absorbed radioactive xenon. The difference in the experimental techniques makes a comparison of the results of uncertain value.</p>	

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Xenon; Xe; 7440-63-3</li> <li>Biological systems</li> </ol>	<p>EVALUATOR:</p> <p>H. L. Clever  Chemistry Department  Emory University  Atlanta, GA 30322  U.S.A.</p> <p>September 1978</p>
<p>CRITICAL EVALUATION:</p> <p>Albumin. Conn (2) found 1.1 mole xenon per mole of human albumin at 294 K and 700 mmHg (93.33 kPa) xenon pressure. Yeh and Peterson (16) measured the solubility of xenon in three concentrations of albumin at 1 atm (101.325 kPa) and temperatures of 298.15, 303.15, and 310.15 K. These results give 0.78, 0.56 and 0.46 mole xenon per mole of albumin at 101.325 kPa and temperatures of 298.15, 303.15 and 310.15 K respectively. Ladefoged and Anderson (19) made one set of measurements at 310.15 K which appears to agree with the Yeh and Peterson value at 310.15 K.</p> <p>Blood and blood components. The solubility of xenon in dog blood was studied by Conn (2). The solubility of xenon in human blood and blood components was studied by Yeh and Peterson (16), Anderson and Ladefoged (20), Ladefoged and Anderson (19), Isbister, Schofield and Torrance (17), Veall and Mallett (18) and Kitani (21). The data of Isbister <i>et al.</i>, Veall and Mallett, and Kitani agree within a 3.5 per cent range for the distribution of xenon between the gas phase and red blood cells.</p> <p>Tissues. Conn (2) studied dog tissues, Yeh and Peterson (16) studied rabbit leg muscle and Kitani and Winkler (21) studied human liver tissue of varying triglyceride content. Conn's results were for the solid tissue/water distribution, and they were converted to a tissue/gas distribution by us. Conn's 'solubility' values appear to be higher than the values determined by study of tissue homogenates.</p> <p>REFERENCES</p> <ol style="list-style-type: none"> <li>Yeh, S.Y.; Peterson, R.E. <u>J. Pharm. Sci.</u> 1963, <u>52</u>, 453.</li> <li>Conn, H.L. <u>J. Appl. Physiol.</u> 1961, <u>16</u>, 1065.</li> <li>Schoenborn, B.P.; Vogelhut, P.O.; Featherstone, R.M. <u>Pharmacologist</u> 1963, <u>5</u>, 264.</li> <li>Yeh, S.Y.; Peterson, R.E. <u>J. Appl. Physiol.</u> 1965, <u>20</u>, 1041.</li> <li>Schoenborn, B.P. <u>Nature</u> 1965, <u>208</u>, 760.</li> <li>Schoenborn, B.P. <u>Fed. Proc.</u> 1968, <u>27</u>, 888.</li> <li>Wishnia, A. <u>Biochem.</u> 1969, <u>8</u>, 5064.</li> <li>Catchpool, J.F. <u>Fed. Proc.</u> 1968, <u>27</u>, 884.</li> <li>Meuhlbaecher, C.; DeBon, F.L.; Featherstone, R.M. <u>Inst. Anesth. Clinics</u> 1963, <u>1</u>, 937.</li> <li>Schoenborn, B.P.; Watson, J.C.; Kendrew, J.C. <u>Nature</u> 1965, <u>207</u>, 28.</li> <li>Schoenborn, B.P.; Nobbs, C.L. <u>Mol. Pharmacol.</u> 1966, <u>2</u>, 491.</li> <li>Maestas, S.; Ewing, G.J. <u>Curr. Mod. Biol.</u> 1967, <u>1</u>, 148.</li> <li>Ewing, G.J.; Maestas, S. <u>J. Phys. Chem.</u> 1970, <u>74</u>, 2341.</li> <li>Keys, M.; Lumry, R. <u>Fed. Proc.</u> 1968, <u>27</u>, 895.</li> <li>Ewing, G.J.; Ionescu, L.G. <u>J. Phys. Chem.</u> 1972, <u>76</u>, 591.</li> <li>Yeh, S.-Y.; Peterson, R.E. <u>J. Appl. Physiol.</u> 1965, <u>20</u>, 1041.</li> <li>Isbister, W.J.; Schofield, P.F.; Torrance, H.B. <u>Phys. Med. Biol.</u> 1965, <u>10</u>, 243.</li> <li>Veall, N.; Mallett, B.L. <u>Phys. Med. Biol.</u> 1965, <u>10</u>, 375.</li> <li>Ladefoged, J.; Anderson, A.M. <u>Phys. Med. Biol.</u> 1967, <u>12</u>, 353.</li> <li>Kitani, K. <u>Scand. J. Clin. Lab. Invest.</u> 1972, <u>29</u>, 167.</li> <li>Kitani, K.; Winkler, K. <u>Scand. J. Clin. Lab. Invest.</u> 1972, <u>29</u>, 173.</li> </ol>	

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<p>VARIABLES:</p> <p>T/K: 310.15</p>	<p>PREPARED BY:</p> <p>A. L. Cramer</p>						
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COMPONENTS: 1. Xenon; $^{133}\text{Xe}$ ; 14932-42-4 2. Paraffin Oil 3. Lecithin	ORIGINAL MEASUREMENTS: Kitani, K.  <u>Scand. J. Clin. Lab. Invest.</u> <u>1972, 29, 167-172.</u>																								
VARIABLES: T/K: 310.15 P/kPa: 101.325 (1 atm)	PREPARED BY: P.L. Long A.L. Cramer																								
EXPERIMENTAL VALUES: <table border="1" data-bbox="312 486 1049 813"> <thead> <tr> <th>T/K</th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L <math>\pm</math> Std. Dev.</th> <th>Replications</th> </tr> </thead> <tbody> <tr> <td colspan="4" style="text-align: center;">Paraffin Oil</td> </tr> <tr> <td>310.15</td> <td>1.819</td> <td>2.065 <math>\pm</math> 0.043</td> <td>16</td> </tr> <tr> <td></td> <td>-</td> <td>2.079*</td> <td>-</td> </tr> <tr> <td colspan="4" style="text-align: center;">Lecithin</td> </tr> <tr> <td>310.15</td> <td>-</td> <td>1.477*</td> <td>-</td> </tr> </tbody> </table> <p>*Extrapolated values. See equation below.</p> <p>The Ostwald coefficient was independent of pressure.</p> <p>The solubility value for lecithin is a value extrapolated from the solubility of the gas in mixtures of paraffin oil and lecithin. The coefficient of solubility of the gas is linear in lecithin per cent (graph in paper). The equation for the straight line in the paper appears to be in error. The equation below was estimated from the graph by the compiler.</p> $L = 2.079 - (6.02 \times 10^{-3}) (\text{Lecithin w/v per cent})$		T/K	Bunsen Coefficient $\alpha$	Ostwald Coefficient L $\pm$ Std. Dev.	Replications	Paraffin Oil				310.15	1.819	2.065 $\pm$ 0.043	16		-	2.079*	-	Lecithin				310.15	-	1.477*	-
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METHOD/APPARATUS/PROCEDURE: A glass cuvette is filled with the liquid. One-third of the liquid is replaced with radioactive gas in air. The sealed cuvette is placed in a thermostated bath for 2 hours. The pressure is adjusted to 1 atm by means of a thin needle. The radioactive assay, corrected for self absorption and scatter, is made by a scintillation detector and a Philips pulse-height analyzer.	SOURCE AND PURITY OF MATERIALS: 1. Xenon. Radiochemical Centre, Amersham, England. 2. Paraffin oil. Commercial quality. 3. Egg lecithin. Purified twice with ether and acetone.  ESTIMATED ERROR: See standard deviation above.  REFERENCES:																								

<p>COMPONENTS:</p> <p>1. Xenon; Xe; 7440-63-3 Xenon-133; <math>^{133}\text{Xe}</math>; 14932-42-4 Xenon-135; <math>^{135}\text{Xe}</math>; 14995-63-1</p> <p>2. Dog Blood and Components</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Conn, H. L. <u>J. Appl. Physiol.</u> 1961, <u>16</u>, 1065-1070.</p>																																				
<p>VARIABLES:</p> <p>T/K: 294.15 Xe P/kPa: 1.867 - 21.332 (14-160 mmHg)</p>	<p>PREPARED BY:</p> <p>A. L. Cramer H. L. Clever</p>																																				
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="303 498 995 1059"> <thead> <tr> <th>T/K</th> <th>Xe (counts <math>\text{m}^{-1}</math>) <math>\text{g}^{-1}</math> Tissue</th> <th>Solubility* Coefficient S</th> </tr> <tr> <th></th> <th>Xe (counts <math>\text{m}^{-1}</math>) <math>\text{g}^{-1}</math> Water</th> <th></th> </tr> </thead> <tbody> <tr> <td colspan="3" style="text-align: center;">Water</td> </tr> <tr> <td>294.15</td> <td>1.00</td> <td>0.118**</td> </tr> <tr> <td colspan="3" style="text-align: center;">Plasma</td> </tr> <tr> <td>294.15</td> <td>1.45 <math>\pm</math> 0.05</td> <td>0.171</td> </tr> <tr> <td colspan="3" style="text-align: center;">Whole Blood (mean hemoglobin concentration 15 g 100 <math>\text{g}^{-1}</math> blood)</td> </tr> <tr> <td>294.15</td> <td>2.49 <math>\pm</math> 0.04</td> <td>0.294</td> </tr> <tr> <td colspan="3" style="text-align: center;">Erythrocytes (mean hemoglobin conc. 35 g 100 <math>\text{g}^{-1}</math> red blood cells)</td> </tr> <tr> <td>294.15</td> <td>3.75 <math>\pm</math> 0.06</td> <td>0.443</td> </tr> <tr> <td colspan="3" style="text-align: center;">Hemoglobin solution (mean hemoglobin conc. 35 g 100 <math>\text{g}^{-1}</math> solution)</td> </tr> <tr> <td>294.15</td> <td>2.83 <math>\pm</math> 0.05</td> <td>0.334</td> </tr> </tbody> </table> <p>*Calculated by the compiler. <math>\text{cm}^3</math> xenon at 1 atm and 294.15 K <math>\text{g}^{-1}</math> tissue. **<math>\text{cm}^3</math> Xe 1 atm and 294 K/g water. Calculated from data in critical evaluation of xenon in water.</p>		T/K	Xe (counts $\text{m}^{-1}$ ) $\text{g}^{-1}$ Tissue	Solubility* Coefficient S		Xe (counts $\text{m}^{-1}$ ) $\text{g}^{-1}$ Water		Water			294.15	1.00	0.118**	Plasma			294.15	1.45 $\pm$ 0.05	0.171	Whole Blood (mean hemoglobin concentration 15 g 100 $\text{g}^{-1}$ blood)			294.15	2.49 $\pm$ 0.04	0.294	Erythrocytes (mean hemoglobin conc. 35 g 100 $\text{g}^{-1}$ red blood cells)			294.15	3.75 $\pm$ 0.06	0.443	Hemoglobin solution (mean hemoglobin conc. 35 g 100 $\text{g}^{-1}$ solution)			294.15	2.83 $\pm$ 0.05	0.334
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<p>METHOD/APPARATUS/PROCEDURE:</p> <p>A one ml aliquot of each solution was placed in a 100 ml glass tonometer and equilibrated with the gas mixture for 2 hours at 294 K. Three-tenths ml of each sample was withdrawn anaerobically into a 1-ml syringe and the radioactivity was determined in a scintillation counter. Water under the same partial pressure xenon was counted for the tissue/water ratio.</p> <p>Some of the hemoglobin methemoglobin and albumin systems were determined by this method.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>1. Xenon. Air Reduction Sales. Specially purified. The gas was subjected to neutron bombardment in a nuclear reactor. Resultant xenon isotopes were mainly <math>^{133}\text{Xe}</math> and <math>^{135}\text{Xe}</math>.</p> <p>2. Dog Blood and Components.</p> <p>ESTIMATED ERROR:</p> <p>See standard error of mean for 36 experiments above.</p> <p>REFERENCES:</p>																																				

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<p>VARIABLES:</p> <p>T/K: 294.15 Xe P/kPa: 23.33 - 93.325 (175 - 700 mmHg)</p>	<p>PREPARED BY:</p> <p>A. L. Cramer H. L. Clever</p>																																												
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="333 493 1103 946"> <thead> <tr> <th>T/K</th> <th><math>\frac{\text{cm}^3 \text{Xe g}^{-1} \text{Protein}}{\text{cm}^3 \text{Xe g}^{-1} \text{Water}}</math></th> <th><math>\frac{\text{mol Xe}^*}{\text{mol Protein}}</math></th> <th>Solubility Coefficient S</th> </tr> </thead> <tbody> <tr> <td></td> <td colspan="3">Human Albumin</td> </tr> <tr> <td>294.15</td> <td>3.50 ± 0.3</td> <td>1.1</td> <td>0.413</td> </tr> <tr> <td></td> <td colspan="3">Human Hemoglobin</td> </tr> <tr> <td>294.15</td> <td>6.43 ± 0.4</td> <td>1.9</td> <td>0.759</td> </tr> <tr> <td></td> <td colspan="3">Human Methemoglobin</td> </tr> <tr> <td>294.15</td> <td>6.45 ± 0.4</td> <td>1.9</td> <td>0.761</td> </tr> <tr> <td></td> <td colspan="3">Dog Hemoglobin</td> </tr> <tr> <td>294.15</td> <td>6.24 ± 0.1</td> <td>1.9</td> <td>0.736</td> </tr> <tr> <td></td> <td colspan="3">Dog Methemoglobin</td> </tr> <tr> <td>294.15</td> <td>6.04 ± 0.4</td> <td>1.8</td> <td>0.713</td> </tr> </tbody> </table> <p>*calculated from experiments done at a xenon partial pressure of 700 mmHg.</p> <p>The solubility coefficient, S, was calculated by the compiler by multiplying the protein/water ratio by 0.118, which is the solubility coefficient of xenon g<sup>-1</sup> water at 294.15 K (See the critical evaluation of the solubility of xenon in water.)</p> <p>The hemoglobin and methemoglobin solutions were 5 to 12 weight percent.</p> <p>The xenon gas uptake by human and dog hemoglobin and methemoglobin obeys Henry's law.</p>		T/K	$\frac{\text{cm}^3 \text{Xe g}^{-1} \text{Protein}}{\text{cm}^3 \text{Xe g}^{-1} \text{Water}}$	$\frac{\text{mol Xe}^*}{\text{mol Protein}}$	Solubility Coefficient S		Human Albumin			294.15	3.50 ± 0.3	1.1	0.413		Human Hemoglobin			294.15	6.43 ± 0.4	1.9	0.759		Human Methemoglobin			294.15	6.45 ± 0.4	1.9	0.761		Dog Hemoglobin			294.15	6.24 ± 0.1	1.9	0.736		Dog Methemoglobin			294.15	6.04 ± 0.4	1.8	0.713
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<p>METHOD /APPARATUS/PROCEDURE:</p> <p>Blood was drawn and centrifuged. The red blood cells were washed repeatedly with saline to remove serum fats. Hemoglobin was obtained by hemolysing the red blood cells with distilled water, and precipitating stroma by centrifugation. The mid-portion of the supernatant fluid was withdrawn for testing and use. Only one peak was present in a starch block electrophoresis.</p> <p>Methemoglobin was obtained by oxidizing hemoglobin with excess potassium ferricyanide or sodium nitrite.</p> <p>One ml samples were drawn into a 5 ml syringe and filled with gas with a xenon partial pressure of 175 to 700 mmHg. The syringes were shaken 1-2 hours at 294 K. The gas phase was completely expelled and the solution radioactivity was determined in a scintillation counter. Water samples at the same xenon partial pressure were used to calculate the water/protein solubility ratio.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>Xenon. Air Reduction Sales. Specially purified. The gas was subjected to neutron bombardment in a nuclear reactor. Resultant xenon isotopes were mainly <math>^{133}\text{Xe}</math> and <math>^{135}\text{Xe}</math>.</li> <li>Albumin. Pentex Corp. Crystalline. albumin, 2-4% g. Hemoglobin, methemoglobin. See procedure.</li> </ol> <p>ESTIMATED ERROR:</p> <p>See standard error of mean above.</p> <p>REFERENCES:</p>																																												

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<p>VARIABLES:</p> <p>T/K: 293.15 Xe P/kPa: 101.325 (1 atm) pH: 7.0</p>	<p>PREPARED BY:  H. L. Clever</p>				
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<p>METHOD / APPARATUS / PROCEDURE:</p> <p>Standard PVT measurement. No experimental details in either this abstract of a meeting paper or a later publication (1).</p>	<p>SOURCE AND PURITY OF MATERIALS: No information given on any of the components.</p> <p>ESTIMATED ERROR:  Qualitative.</p> <p>REFERENCES: 1. Schoenborn, B.P.; Featherstone, R.M.; Vogelhut, P.O.; Süsskind, C. <u>Nature</u> 1964, <u>202</u>, 695.</p>				

<b>COMPONENTS:</b> 1. Xenon; Xe; 7440-63-3 2. Water; H <sub>2</sub> O; 7732-18-5 3. Sodium Phosphate Buffer 4. Bovine Blood Components	<b>ORIGINAL MEASUREMENTS:</b> Meuhlbaecher, C.; DeBon, F.L.; Featherstone, R.M.  Inst. Anesth. Clinics 1963, <u>1</u> , 937-952.														
<b>VARIABLES:</b>  T/K: 310.15	<b>PREPARED BY:</b>  H.L. Clever														
<b>EXPERIMENTAL VALUES:</b> The Bunsen coefficients were presented on large scale graphs. The xenon Bunsen coefficient in sodium phosphate buffer was about 0.083. Comments about the individual systems follow: <table border="1" data-bbox="203 566 1186 1123"> <thead> <tr> <th>T/K</th> <th>Comments</th> </tr> </thead> <tbody> <tr> <td></td> <td>Bovine Gamma-Globulin + Phosphate Buffer (pH 6.3-6.5, Ionic Strength 0.16)</td> </tr> <tr> <td>310.15</td> <td>No apparent change in the xenon Bunsen coefficient as bovine gamma-globulin was increased from 0-8 per cent.</td> </tr> <tr> <td></td> <td>Bovine Serum Albumin + Phosphate Buffer (pH 5.6-6.3, Ionic Strength 0.16)</td> </tr> <tr> <td>310.15</td> <td>No apparent change in the xenon Bunsen coefficient as the bovine serum albumin was increased from 0 to 10 per cent. At 20 per cent bovine serum albumin the Xenon Bunsen Coefficient appears to increase a little more than the 8 per cent uncertainty in the measurement.</td> </tr> <tr> <td></td> <td>Bovine Hemoglobin + Phosphate Buffer (pH 6.3-6.6, Ionic Strength 0.16)</td> </tr> <tr> <td>310.15</td> <td>A linear increase in the xenon Bunsen coefficient as the bovine hemoglobin was increased from 0 to 20 per cent. The 20 per cent solution absorbed 58 per cent more xenon than did the buffer solution.</td> </tr> </tbody> </table>		T/K	Comments		Bovine Gamma-Globulin + Phosphate Buffer (pH 6.3-6.5, Ionic Strength 0.16)	310.15	No apparent change in the xenon Bunsen coefficient as bovine gamma-globulin was increased from 0-8 per cent.		Bovine Serum Albumin + Phosphate Buffer (pH 5.6-6.3, Ionic Strength 0.16)	310.15	No apparent change in the xenon Bunsen coefficient as the bovine serum albumin was increased from 0 to 10 per cent. At 20 per cent bovine serum albumin the Xenon Bunsen Coefficient appears to increase a little more than the 8 per cent uncertainty in the measurement.		Bovine Hemoglobin + Phosphate Buffer (pH 6.3-6.6, Ionic Strength 0.16)	310.15	A linear increase in the xenon Bunsen coefficient as the bovine hemoglobin was increased from 0 to 20 per cent. The 20 per cent solution absorbed 58 per cent more xenon than did the buffer solution.
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<b>METHOD/APPARATUS/PROCEDURE:</b>  Gas chromatography	<b>SOURCE AND PURITY OF MATERIALS:</b>  No information  <b>ESTIMATED ERROR:</b>  $\delta\alpha/\alpha = 0.08$  <b>REFERENCES:</b>														

<b>COMPONENTS:</b> 1. Xenon; Xe; 7440-63-3 2. Water; H <sub>2</sub> O; 7732-18-5 3. Human Whole Blood and Blood Components	<b>ORIGINAL MEASUREMENTS:</b> Yeh, S-Y.; Peterson, R.E.  <u>J. Appl. Physiol.</u> 1965, <u>20</u> , 1041-1047.																												
<b>VARIABLES:</b> T/K: 310.15 Total P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> A.L. Cramer																												
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="212 522 1052 940"> <thead> <tr> <th>T/K</th> <th>Absorption Coefficient mean <math>\beta \pm</math> Std. Dev.</th> <th>Number of Determinations</th> <th>Absorption Coefficient <math>\text{g}^{-1}</math> Hemoglobin</th> </tr> </thead> <tbody> <tr> <td colspan="4">Hemoglobin Solution (7.63% hemoglobin, 92.35% water, 1.57 mg <math>\text{cm}^{-3}</math> lipid)</td> </tr> <tr> <td>310.15</td> <td>0.1046 <math>\pm</math> 0.0057</td> <td>3</td> <td>0.3918</td> </tr> <tr> <td colspan="4">Hemoglobin solution (15.39 hemoglobin, 84.60% water, 2.60 mg <math>\text{cm}^{-3}</math> lipid)</td> </tr> <tr> <td>310.15</td> <td>0.1241 <math>\pm</math> 0.0032</td> <td>4</td> <td>0.3469</td> </tr> <tr> <td colspan="4">Whole Blood (425 ml. whole blood + 120 ml. 1.32% sodium citrate solution)</td> </tr> <tr> <td>310.15</td> <td>0.1412 <math>\pm</math> 0.0044</td> <td>3</td> <td>-</td> </tr> </tbody> </table> <p data-bbox="64 960 1182 1069">*The authors give a weighted average of 0.3661 <math>\text{cm}^3</math> (STP) gas <math>\text{g}^{-1}</math> hemoglobin which is equivalent to 1.111 mole Xe mole<sup>-1</sup> hemoglobin (mol. wt. = 68,000). The values are for a partial pressure of xenon of (1-solution vapor pressure) atm. At one atm xenon the values would be about 6% higher.</p>		T/K	Absorption Coefficient mean $\beta \pm$ Std. Dev.	Number of Determinations	Absorption Coefficient $\text{g}^{-1}$ Hemoglobin	Hemoglobin Solution (7.63% hemoglobin, 92.35% water, 1.57 mg $\text{cm}^{-3}$ lipid)				310.15	0.1046 $\pm$ 0.0057	3	0.3918	Hemoglobin solution (15.39 hemoglobin, 84.60% water, 2.60 mg $\text{cm}^{-3}$ lipid)				310.15	0.1241 $\pm$ 0.0032	4	0.3469	Whole Blood (425 ml. whole blood + 120 ml. 1.32% sodium citrate solution)				310.15	0.1412 $\pm$ 0.0044	3	-
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<b>METHOD/APPARATUS/PROCEDURE:</b> In Yeh and Peterson (1) modification of Geffcken (2) apparatus, 45 ml. of liquid was frozen, evacuated, and melted repeatedly until no bubbles appeared in liquid under vacuum. Equilibration with gas and measurement of solubility followed (1).	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Xenon. The Matheson Co. Research grade, maximum impurity 0.02% nitrogen and 0.05% krypton. 2. Water. Distilled. 3. Human Blood. 425 ml. from a normal donor, mixed with 120 ml. 1.32% sodium citrate solution. Frozen and thawed to hemolyze red blood cells. 4. Hemoglobin. From centrifuged citrated human blood.																												
	<b>ESTIMATED ERROR:</b> $\delta T/K = 0.05$ $\delta P/\text{mmHg} = 0.2$ $\delta L/L = 0.0015$																												
	<b>REFERENCES:</b> 1. Yeh, S-Y.; Peterson, R.E. <u>J. Pharm. Sci.</u> 1963, <u>52</u> , 453. 2. Geffcken, G. <u>Z. Physik. Chem.</u> 1904, <u>49</u> , 257.																												

<b>COMPONENTS:</b> 1. Xenon-133; $^{133}_{54}\text{Xe}$ ; 14932-42-4 2. Human Blood	<b>ORIGINAL MEASUREMENTS:</b> Anderson, A.M.; Ladefoged, J.  <u>J. Pharm. Sci.</u> 1965, <u>54</u> , 1684-1685.
<b>VARIABLES:</b> T/K: 310.15 Hematocrit/%: 0 - 88	<b>PREPARED BY:</b> A.L. Cramer H.L. Clever
<b>EXPERIMENTAL VALUES:</b> A total of 64 determinations of the partition coefficient of xenon-133 between blood and water were carried out. Separate samples of water and of blood were equilibrated with the same air-radon-133 mixture in each experiment. The blood hematocrit varied from 0 to 88 weight per cent. The data was given in a graph and fitted by a linear regression to $\text{Partition Coefficient} = (1.02 \pm 0.02) + (0.0112 \pm 0.0004)(\text{wt } \% \text{ hematocrit})$ with an overall standard deviation of 0.08. The plasma/water partition coefficient is 1.02, and the erythrocyte/water partition coefficient is 2.14. A formula for the partition coefficient of tissue/blood as a function of hematocrit % was given. A plasma/gas and erythrocyte/gas partition coefficient may be obtained from the equation value by multiplying by 0.0834, the Ostwald solubility of xenon in water reported by the authors (see page 139). The erythrocyte/xenon gas Ostwald coefficient of 0.178 calculated from the information above is 12 - 15 per cent lower than values reported on pages 213 and 214, and 6 per cent lower than the authors value in a later report (see page 215). See also the data on page 218.	
<b>AUXILIARY INFORMATION</b>	
<b>METHOD/APPARATUS/PROCEDURE:</b> The samples in small vials were equilibrated with a mixture of air and xenon-133 for 24 h at 310 K. The samples were stirred continuously. After equilibration 0.1 ml samples were transferred anaerobically by syringes to a 2 ml. rubber-capped vial and counted in a scintillation counter to a statistical error below 1 per cent.  The hematocrit was varied by removal of plasma or erythrocytes from whole blood after centrifuging.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Xenon-133. The Radiochemical Centre, Amersham, England. Impurities (<2 per cent) were mainly xenon-133m with trace amounts of xenon-131 and krypton-85. 2. Blood. From voluntary donors.  <b>ESTIMATED ERROR:</b>  <b>REFERENCES:</b>



<b>COMPONENTS:</b> 1. Xenon-133; $^{133}_{54}\text{Xe}$ ; 14932-42-4 2. Saline and Blood Components	<b>ORIGINAL MEASUREMENTS:</b> Isbister, W. H.; Schofield, P. F.; Torrance, H. B. <u>Phys. Med. Biol.</u> 1965, <u>10</u> , 243-250.																					
<b>VARIABLES:</b>  T/K: 310.15	<b>PREPARED BY:</b>  A. L. Cramer H. L. Clever																					
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="352 500 927 819"> <thead> <tr> <th>T/K</th> <th>Ostwald Coefficient L <math>\pm</math> Std Error</th> <th>Number of Determinations</th> </tr> </thead> <tbody> <tr> <td colspan="3" style="text-align: center;">Saline (water)*</td> </tr> <tr> <td>310.15</td> <td>0.0926 <math>\pm</math> 0.0027</td> <td>7</td> </tr> <tr> <td colspan="3" style="text-align: center;">Plasma</td> </tr> <tr> <td>310.15</td> <td>0.1028 <math>\pm</math> 0.0008</td> <td>53</td> </tr> <tr> <td colspan="3" style="text-align: center;">Red Cells (Hematocrit 98%)</td> </tr> <tr> <td>310.15</td> <td>0.2020 <math>\pm</math> 0.0015</td> <td>2</td> </tr> </tbody> </table> <p>*The saline solution was not described. It may be the standard 0.9 weight percent solution of NaCl in water.</p>		T/K	Ostwald Coefficient L $\pm$ Std Error	Number of Determinations	Saline (water)*			310.15	0.0926 $\pm$ 0.0027	7	Plasma			310.15	0.1028 $\pm$ 0.0008	53	Red Cells (Hematocrit 98%)			310.15	0.2020 $\pm$ 0.0015	2
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<b>METHOD /APPARATUS/PROCEDURE:</b> <p>Two ml samples of blood were introduced into the sample tube, four ml of a concentrated xenon-133 air mixture were added to the tube which was then sealed. The tubes were shaken and equilibrated at 310 K for two hours. After equilibration the tubes were centrifuged at 310 K for 30 minutes at 3000 rpm. The three phases cells, plasma and gas were separately counted in a specially constructed lead collimator attached to a scintillation counter.</p>	<b>SOURCE AND PURITY OF MATERIALS:</b> <ol style="list-style-type: none"> <li>Xenon-133. No information given.</li> <li>Blood components. Fresh human blood containing a suitable amount of Sequestrene.</li> </ol> <b>ESTIMATED ERROR:</b>  See standard error of mean above.																					
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<p>COMPONENTS:</p> <p>1. Xenon-133; <math>^{133}_{54}\text{Xe}</math>; 14932-42-4</p> <p>2. Blood components</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Veall, N.; Mallett, B. L.</p> <p><u>Phys. Med. Biol.</u> 1965, <u>10</u>, 375-380.</p>																					
<p>VARIABLES:</p> <p>T/K: 310.15</p>	<p>PREPARED BY:</p> <p>A. L. Cramer H. L. Clever</p>																					
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="434 506 1000 825"> <thead> <tr> <th>T/K</th> <th>Solubility Coefficient <math>S \pm \text{Std Error}</math></th> <th>Number of Determinations</th> </tr> </thead> <tbody> <tr> <td colspan="3" style="text-align: center;">Water</td> </tr> <tr> <td>310.15</td> <td>0.0903 <math>\pm</math> 0.0005</td> <td>9</td> </tr> <tr> <td colspan="3" style="text-align: center;">Plasma</td> </tr> <tr> <td>310.15</td> <td>0.1025 <math>\pm</math> 0.0009</td> <td>12</td> </tr> <tr> <td colspan="3" style="text-align: center;">Red Cells</td> </tr> <tr> <td>310.15</td> <td>0.2100 <math>\pm</math> 0.0043</td> <td>12</td> </tr> </tbody> </table>		T/K	Solubility Coefficient $S \pm \text{Std Error}$	Number of Determinations	Water			310.15	0.0903 $\pm$ 0.0005	9	Plasma			310.15	0.1025 $\pm$ 0.0009	12	Red Cells			310.15	0.2100 $\pm$ 0.0043	12
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<p>METHOD / APPARATUS / PROCEDURE:</p> <p>Red cell measurements were made on blood samples of varying haematocrit. Plasma measurements were made on samples first haemolyzed by rapid freezing and thawing.</p> <p>Approximately 1 ml samples were added to sample tube; about 0.1 ml of air containing about 10 <math>\mu\text{C}</math> of xenon-133 was added and the tube sealed. Sample tubes were equilibrated either by leaving over night lying horizontally at 310 K or inverted every 2-3 minutes for several hours. The samples were briefly centrifuged to remove air bubbles from liquid and then gas and liquid phases counted.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>Xenon-133. No information given.</li> <li>Blood. Freshly drawn heparinized blood from normal people.</li> </ol> <p>ESTIMATED ERROR:</p> <p>See standard error of mean above.</p> <p><math>\delta T/K = 0.5</math> (Compiler)</p> <p>REFERENCES:</p>																					

<b>COMPONENTS:</b> 1. Xenon-133; $^{133}_{54}\text{Xe}$ ; 14932-42-4 2. Plasma and Erythrocytes	<b>ORIGINAL MEASUREMENTS:</b> Ladefoged, J.; Anderson, A.M.  <u>Phys. Med. Biol.</u> 1967, <u>12</u> , 353-358.																																								
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<b>METHOD/APPARATUS/PROCEDURE:</b> Blood from volunteer donors was heparinized and centrifuged 30 minutes at 1500 G. Samples were placed in small test tubes together with a sample of water in an air tight box containing 0.5 to 2 $\mu\text{Ci}$ xenon-133 in 100 ml of either air, nitrogen or oxygen. The system was stirred continuously at 310 K for 24 hours. After equilibration the samples were transferred into syringes, about 0.1 ml samples were counted in a scintillation counter and compared with water value. Authors calculated the Ostwald solubility coefficient in blood of 30, 40 and 50 percent hematocrit as 0.119, 0.129, and 0.139 respectively from the above values.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Xenon-133. Radiochemical Centre, Amersham, U.K. Two per cent impurity of $^{131}\text{Xe}$ and $^{85}\text{Kr}$ . Xenon. Dansk Ilt og Briut. 99.95 mol per cent. 2. Blood components. Volunteer donors.  <b>ESTIMATED ERROR:</b>  See standard deviations above.  <b>REFERENCES:</b> 1. Anderson, A.M.; Ladefoged, J. <u>J. Pharm. Sci.</u> 1965, <u>54</u> , 1684.																																								

COMPONENTS:		ORIGINAL MEASUREMENTS:			
1. Xenon; Xe; 7440-63-3		Yeh, S.-Y.; Peterson, R. E.			
2. Water; H <sub>2</sub> O; 7732-18-5		J. <u>Appl. Physiol.</u> 1965, <u>20</u> , 1041-1047			
3. Sodium Chloride; NaCl; 7647-14-5					
4. Human Albumin; 9048-46-8					
VARIABLES:		PREPARED BY:			
T/K: 298.15 - 310.15		A. L. Cramer			
P/kPa: 101.325 (1 atm)		H. L. Clever			
Albumin/wt %: 5.12 - 27.93					
EXPERIMENTAL VALUES:					
T/K	Albumin wt %	Mol Fraction X <sub>1</sub> x 10 <sup>2</sup>	Bunsen Coefficient α	Ostwald Coefficient L ± Std Dev	Number Determinations
298.15	5.12		0.0939	0.1025 ± 0.0028	4
303.15			0.0845	0.0938 ± 0.0025	3
310.15			0.0709	0.0805 ± 0.0008	2
298.15	15.34		0.1092	0.1192 ± 0.0028	3
303.15			0.0963	0.1069 ± 0.0047	3
310.15			0.0786	0.0892 ± 0.0020	3
298.15	27.93		0.1239	0.1352 ± 0.0070	4
303.15			0.1100	0.1221 ± 0.0046	4
310.15			0.0880	0.0999 ± 0.0087	4
298.15	100	42.26	0.2181	0.2382	
303.15			0.1761	0.1954	
310.15			0.1315	0.1493	
The Ostwald coefficients in 100 % human albumin were values extrapolated from the values at lower concentration by the authors. The Bunsen coefficients and mole fraction solubilities were calculated by the compiler. The authors used an albumin molecular weight of 69,000 and a density of 1.0 to calculate mole ratios of xenon to albumin of 0.732, 0.557, and 0.460 at the temperatures 298.15, 303.15, and 310.15 K respectively.					
AUXILIARY INFORMATION					
METHOD		SOURCE AND PURITY OF MATERIALS:			
A 45 cm <sup>3</sup> sample of albumin solution was frozen, evacuated, and melted repeatedly until no bubbles appeared in the liquid under vacuum in the Yeh and Peterson modification (1) of the Geffcken apparatus (2). Equilibration with gas and measurement of the solubility followed.		1. Xenon. The Matheson Co. Research grade, maximum impurity 0.02 % nitrogen and 0.05 % krypton.			
		2. Human serum albumin. Cutter Laboratories. A 25 % solution, stabilized with 0.02 M sodium caprylate and 0.02 M sodium acetyltryptophanate.			
		ESTIMATED ERROR: $\delta T/K = 0.05$ $\delta P/\text{mmHg} = 0.2$ $\delta L/L = 0.0015$			
		REFERENCES:			
		1. Yeh, S.-Y.; Peterson, R. E. <u>J. Pharm. Sci.</u> 1963, <u>52</u> , 453.			
		2. Geffcken, G. <u>Z. Phys. Chem.</u> 1904, <u>49</u> , 257.			

<b>COMPONENTS:</b> 1. Xenon-133; $^{133}_{54}\text{Xe}$ ; 14932-42-4 2. Water; $\text{H}_2\text{O}$ ; 7732-18-5 3. Sodium Chloride; $\text{NaCl}$ ; 7647-14-5, or Albumin	<b>ORIGINAL MEASUREMENTS:</b> Ladefoged, J.; Anderson, A. M.  <u>Phys. Med. Biol.</u> 1967, <u>12</u> , 353-358.																					
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<b>METHOD/APPARATUS/PROCEDURE:</b> <p>The technique described by Anderson and Ladefoged (1) was used. The materials were placed in small test tubes together with a sample of water in an air tight chamber. The chamber contained air and 0.5 to 2 <math>\mu\text{Ci}</math> of xenon-133. The samples were stirred continuously at 310.15 K for 24 hours. After equilibration the samples were transferred into syringes and samples of about 0.1 ml were counted in a scintillation counter. The Ostwald coefficients were calculated indirectly from the ratio of counts in water and the sample and the measured Ostwald coefficient in water. See the authors data sheet on <math>\text{Xe} + \text{H}_2\text{O}</math>.</p>	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Xenon-133. Radiochemical Centre, Amersham, U.K. Two per cent impurity of $^{131}\text{Xe}$ and $^{85}\text{Kr}$ . 2. Albumin. Statens Serum Institut. Cohn's fraction V, 97% albumin and 3% $\alpha$ and $\beta$ globulin. Heat treated 60°C for 10 hours.  <b>ESTIMATED ERROR:</b> See standard deviations above.  <b>REFERENCES:</b> 1. Anderson, A. M.; Ladefoged, J. <u>J. Pharm. Sci.</u> 1965, <u>54</u> , 1684.																					

<b>COMPONENTS:</b> 1. Xenon; $^{133}\text{Xe}$ ; 14932-42-4 2. Water, Saline Solution, Plasma, and Human Red Blood Cells	<b>ORIGINAL MEASUREMENTS:</b> Kitani, K.  <u>Scand. J. Clin. Lab. Invest.</u> <u>1972, 29, 167-172.</u>																																												
<b>VARIABLES:</b> T/K: 310.15 P/kPa: 101.325 (1 atm)	<b>PREPARED BY:</b> P.L. Long A.L. Cramer																																												
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<b>AUXILIARY INFORMATION</b>																																													
<b>METHOD/APPARATUS/PROCEDURE:</b> <p>A glass cuvette is filled with the liquid. One-third of the liquid is replaced with radioactive gas in air. The sealed cuvette is placed in a thermostated bath for 2 hours. The pressure is adjusted to 1 atm by means of a thin needle.</p> <p>The radioactive assay, corrected for self absorption and scatter, is made by a scintillation detector and a Philips pulse-height analyzer.</p>	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Xenon. Radiochemical Centre, Amersham, England. 2. Water and 0.9 per cent saline were prepared according to the criteria for purity in the Nordic Pharmacopeia. Heparinized blood from healthy donors was used.																																												
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<b>COMPONENTS:</b> 1. Xenon; Xe; 7440-63-3 2. Water; H <sub>2</sub> O; 7732-18-5 3. Sodium Chloride; NaCl; 7647-14-5 4. Methemoglobin	<b>ORIGINAL MEASUREMENTS:</b> Catchpool, J. F. <u>Fed. Proc.</u> 1968, <u>27</u> , 884 - 887.																
<b>VARIABLES:</b> T/K: 278.15 - 308.15 P/kPa: 80.93 - 92.66 (607 - 695 mmHg)	<b>PREPARED BY:</b> H. L. Clever																
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Henry's Constant K x 10<sup>-7</sup> (P<sub>1</sub>/mmHg)/(mol Xe/mol H<sub>2</sub>O)</th> </tr> </thead> <tbody> <tr><td style="text-align: center;">278.15</td><td style="text-align: center;">0.28</td></tr> <tr><td style="text-align: center;">283.15</td><td style="text-align: center;">0.34</td></tr> <tr><td style="text-align: center;">288.15</td><td style="text-align: center;">0.40</td></tr> <tr><td style="text-align: center;">293.15</td><td style="text-align: center;">0.45</td></tr> <tr><td style="text-align: center;">298.15</td><td style="text-align: center;">0.52</td></tr> <tr><td style="text-align: center;">303.15</td><td style="text-align: center;">0.60</td></tr> <tr><td style="text-align: center;">308.15</td><td style="text-align: center;">0.66</td></tr> </tbody> </table> <p>The values of Henry's constant were read from a graph in the original paper. There is an increase in the temperature coefficient of Henry's constant between temperatures of 293 and 303 K.</p> <p>The author calculated that at 293.15 K and a xenon partial pressure of 101.325 kPa (1 atm) 1.67 mole of xenon is combined with each mole of the methemoglobin. The result is based on a xenon Henry's constant of 0.88 x 10<sup>7</sup> in 0.5 per cent saline solution at 293.15 K.</p>		T/K	Henry's Constant K x 10 <sup>-7</sup> (P <sub>1</sub> /mmHg)/(mol Xe/mol H <sub>2</sub> O)	278.15	0.28	283.15	0.34	288.15	0.40	293.15	0.45	298.15	0.52	303.15	0.60	308.15	0.66
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<b>METHOD:</b> Volumetric apparatus with the gas pressure controlled by a quartz Bourdon tube, mirror-photocell, and a servomechanism. Measurements were made at all seven temperatures on one loading of the apparatus over a period of four days. Spectroscopic and density measurements before and after the experiment indicated no degradation of the sample. The sample was 0.00279 mole methemoglobin dm <sup>-3</sup> of 0.5 per cent saline solution.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Xenon. } No information. 2. Water. } 3. Sodium Chloride. } 4. Hemoglobin. Prepared from human type 0 Rh negative blood. Packed cells washed six times with 1 per cent saline. Lipids and cellular debris were dissolved in toluene.																
<b>ESTIMATED ERROR:</b> $\delta T/K = 0.005$ $\delta P/mmHg = 0.005$																	
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<b>COMPONENTS:</b> 1. Xenon; Xe; 7440-63-3 2. Water; H <sub>2</sub> O; 7732-18-5 3. Myoglobins	<b>ORIGINAL MEASUREMENTS:</b> Ewing, G. J.; Maestas, S.  <u>J. Phys. Chem.</u> 1970, <u>74</u> , 2341-2344.
<b>VARIABLES:</b> T/K: 293.15 - 303.15 Xe P/kPa: 50.663 - 491.426 (0.5 - 4.85 atm)	<b>PREPARED BY:</b>  H. L. Clever

**EXPERIMENTAL VALUES:**

T/K	Henry's Constant $K_H/\text{mmHg } x_1^{-1}$	$K/\text{m}^{-1}$	$K'/\text{m}^{-1}$
Water			
293.15	$0.85 \times 10^7$	-	-
298.15	$0.96 \times 10^7$	-	-
303.15	$1.13 \times 10^7$	-	-
Cyanometmyoglobin			
293.15	-	186	-
298.15	-	145	-
303.15	-	115	-
Metmyoglobin			
293.15	-	200	~8.2
298.15	-	146	~7.2
303.15	-	130	~2.3
Myoglobin			
293.15	-	109	2.3
298.15	-	94	2.6
303.15	-	85	0.5

The xenon solubility in the myoglobin solutions did not obey Henry's law. The xenon solubility data are presented graphically in the original paper.

**AUXILIARY INFORMATION****METHOD / APPARATUS / PROCEDURE:**

Manometric method. The amount of xenon absorbed by the solution was determined by measuring the initial pressure and the final pressure to obtain the pressure change,  $\Delta P$ , and applying the ideal gas law

$$\Delta n = \frac{(\Delta P)V}{RT}$$

To determine the amount of xenon absorbed by the hemoprotein, the amount of xenon calculated to dissolve in water at the temperature and equilibrium pressure of the experiment was subtracted from  $\Delta n$ . This quantity divided by the number of moles of myoglobin in the ~10 weight per cent solution (usually  $\sim 10^{-4}$  mol) yielded the amount of xenon dissolved per mole of myoglobin.

The xenon adsorptions in the hemoprotein solutions were presented graphically. No appreciable difference was noted in the results for buffered (phosphate buffer pH 8.1) and unbuffered (pH 6.95) metmyoglobin solutions.

**SOURCE AND PURITY OF MATERIALS:**

- Xenon. No information.
- Horse heart myoglobin. Calbiochem. The myoglobin was prepared by reduction of metmyoglobin by sodium dithionite. The cyanometmyoglobin was prepared from metmyoglobin by reaction with KCN and  $K_3Fe(CN)_6$  in a phosphate buffer solution.

**ESTIMATED ERROR:**

$$\begin{aligned} \delta T/K &= 0.1 \\ \delta K_H/\text{mmHg} &= 0.05 \text{ (Compiler)} \end{aligned}$$

The adsorptions were converted to association constants for the reactions

$$\text{Hp} + \text{Xe} = \text{HpXe} \quad K = \frac{m_{\text{HpXe}}}{m_{\text{Hp}} m_{\text{Xe}}}$$

$$\text{HpXe} + \text{Xe} = \text{HpXe}_2 \quad K' = \frac{m_{\text{HpXe}_2}}{m_{\text{HpXe}} m_{\text{Xe}}}$$

where  $m$  is mol kg<sup>-1</sup> H<sub>2</sub>O.



<p>COMPONENTS:</p> <p>1. Xenon; Xe; 7440-63-3 Xenon-133; <sup>133</sup>Xe; 14932-42-4 Xenon-135; <sup>135</sup>Xe; 14995-63-1</p> <p>2. Dog Tissues and Fat</p>	<p>ORIGINAL MEASUREMENTS: Conn, H. L. <u>J. Appl. Physiol.</u> 1961, <u>16</u>, 1065-1070.</p>																																																
<p>VARIABLES:</p> <p>T/K: 294.15 Xe P/kPa: 0.933 - 8.666 (7-65 mmHg)</p>	<p>PREPARED BY: A. L. Cramer H. L. Clever</p>																																																
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<p>METHOD /APPARATUS/PROCEDURE:</p> <p>Sample tissues weighing less than 100 mg and 1 mm or less in thickness were placed in individual cuvettes. They were equilibrated with a radioxenon-air mixture varying from 7 to 65 mmHg in several experiments. The tissues were allowed to equilibrate with the gas mixture for 1 to 8 hours. After equilibration the tissues were almost instantaneously removed from the container and plunged into a bath of liquid nitrogen. The Radioxenon concentration in the frozen samples was determined by counting the radioactivity of each in a well-type scintillation counter. The count was compared with the count in a liquid water sample equilibrated at the same xenon partial pressure.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>Xenon. Air Reduction Sales. Specially purified. The gas was subjected to neutron bombardment in a nuclear reactor. Resultant xenon isotopes were mainly <sup>133</sup>Xe and <sup>135</sup>Xe.</li> <li>Tissues. Taken within 10 minutes after sacrifice of the animal.</li> </ol> <p>ESTIMATED ERROR: See standard error of mean from 36 determinations above.</p> <p>REFERENCES:</p>																																																

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<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Xenon-133; <math>^{133}_{54}\text{Xe}</math>; 14932-42-4</li> <li>Human Liver Tissue</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Kitani, K.; Winkler, K.</p> <p><u>Scand. J. Clin. Lab. Invest.</u> 1972, <u>29</u>, 173-176.</p>
<p>VARIABLES:</p> <p>T/K: 310.15</p>	<p>PREPARED BY:</p> <p>A.L. Cramer</p>
<p>EXPERIMENTAL VALUES:</p> <p>Thirty three measurements of the solubility of xenon-133 were made in liver tissue with triglyceride content varying between 1 and 20 weight per cent. One measurement was made at 50 weight percent triglyceride. The results were given in a graph. The data fitted the regression equation</p> $L = 0.09524 + (0.016447) (\text{triglyceride wt } \%)$ <p>with a regression coefficient of 0.97.</p> <p>The triglyceride weight per cent was calculated as tripalmitin. The tissue solubility was corrected for the water added to the sample. Below a liver triglyceride content of 5 per cent the standard deviation was 0.7 per cent, at higher triglyceride content the standard error increases, and reaches a value of 5 per cent at 25 per cent triglyceride.</p> <p>Tripalmitin is Hexadecanoic acid, 1,2,3-propanetriyl ester; <math>\text{C}_{51}\text{H}_{98}\text{O}_6</math>; 555-44-2.</p>	
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<p>METHOD /APPARATUS/PROCEDURE:</p> <p>Five g of liver tissue was homogenized at 277 K for 15 m after addition of 5 cm<sup>3</sup> of water. A glass cuvette (1 x 1 x 10 cm) was 2/3 filled with the homogenate, and closed with a rubber stopper. The space above the homogenate was evacuated and filled with air containing xenon-133. The cuvette was rotated for 2 h in a water bath at 310 K. The radioactivity in the homogenate and in the air phase were determined by a scintillation counter placed in a thermostated box at 310 K (1).</p> <p>The triglyceride was determined enzymatically in chloroform-methanol extracts.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>Xenon-133. Radiochemical Centre. Amersham, U.K.</li> <li>Liver tissue. Autopsy material.</li> </ol> <p>ESTIMATED ERROR:</p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>Kitani, K. <u>Scand. J. Clin. Lab. Invest.</u> 1972, <u>29</u>, 167.</li> </ol>

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<p>COMPONENTS:</p> <p>1. Xenon-133; <math>^{133}_{54}\text{Xe}</math>; 14932-42-4</p> <p>2. Brain material.</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Isbister, W. H.; Schofield, P. F.; Torrance, H. B. <u>Phys. Med. Biol.</u> 1965, <u>10</u>, 243-250.</p>															
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<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="399 493 971 743"> <thead> <tr> <th>T/K</th> <th>Partition Coefficient S ± Std Error</th> <th>Number of Determinations</th> </tr> </thead> <tbody> <tr> <td colspan="3" style="text-align: center;">Brain Grey Matter</td> </tr> <tr> <td>310.15</td> <td>0.1466 ± 0.0052</td> <td>18</td> </tr> <tr> <td colspan="3" style="text-align: center;">Brain white Matter</td> </tr> <tr> <td>310.15</td> <td>0.2434 ± 0.0119</td> <td>11</td> </tr> </tbody> </table> <p>The authors calculated the partition coefficient of xenon-133 between blood and brain at varying haematocrit levels. See Table II of original paper.</p>		T/K	Partition Coefficient S ± Std Error	Number of Determinations	Brain Grey Matter			310.15	0.1466 ± 0.0052	18	Brain white Matter			310.15	0.2434 ± 0.0119	11
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<p>METHOD / APPARATUS / PROCEDURE:</p> <p>Know weights of grey and white matter were collected in glass containers under a known volume of saline. Fine homogenates of the material were prepared. Two ml. samples of the homogenate were introduced into the special counting tube and xenon-133 air mixture was added. Equilibration at 310 K was complete in two hours. The gas and homogenate phases were counted in a specially constructed lead collimator attached to a scintillation counter. The partition coefficient between gas and tissue was calculated from the gas homogenate partition coefficient by the formula of Kety <u>et al.</u></p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>Xenon-133. No information given.</li> <li>Brain material. Fresh adult human post-mortem material dissected and placed in glass container under saline solution.</li> </ol> <p>ESTIMATED ERROR:</p> <p>See standard error of mean above.</p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>Kety, S. S.; Harmel, M. H.; Broomell, H. T.; Rhode, C. B. <u>J. Biol. Chem.</u> 1948, <u>173</u>, 487.</li> </ol>															

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Radon-222; <math>^{222}_{86}\text{Rn}</math>; 14859-67-7</li> <li>Water; <math>\text{H}_2\text{O}</math>; 7732-18-5</li> </ol>	<p>EVALUATOR:</p> <p>Rubin Battino  Department of Chemistry  Wright State University  Dayton, Ohio, 45431 U.S.A.</p> <p>July 1978</p>
<p>CRITICAL EVALUATION:</p> <p>Radon solubilities are special because we are dealing with a naturally radioactive isotope with a half-life of 3.8 days. The usual technique for determining the solubility of radon is to equilibrate it in a carrier gas like air or nitrogen with the liquid (or solution) it is to be dissolved in. The radon partial pressure is about <math>10^{-4}</math> mm Hg (ca. 0.01 Pa). The solubility is then determined by measuring the radioactivity in the equilibrated gaseous phase and liquid phase. From this the Ostwald coefficient, <math>L</math>, is calculated at a given temperature according to</p> $L = \frac{\text{concentration of gas per unit volume of liquid phase}}{\text{concentration of gas per unit volume of gas phase}} \quad (1)$ <p>The Ostwald coefficient is normally defined as</p> $L = \frac{\text{volume of gas at its partial pressure and T/K}}{\text{volume of solvent used to absorb the gas at T/K}} \quad (2)$ <p>These two definitions are equal if there is no volume change on mixing or negligible volume change on mixing. For the radon partial gas pressure used in the experimental measurements, the latter is certainly the case. The mole fraction solubility at 101,325 Pa is then calculated via equation 3 with <math>P_1 = 101,325</math> Pa.</p> $x_1 = \left[ \frac{R(T/K)}{V_1^{\circ} L P_1} + 1 \right]^{-1} \quad (3)$ <p>where <math>R</math> is the gas constant and <math>V_1^{\circ}</math> is the molar volume of the solvent at <math>T/K</math>. The long extrapolation from 0.01 Pa to 101,325 Pa using Henry's law is questionable. However, by making this conversion we can treat the thermodynamic functions of all of the noble gases under the same standard state conditions. Boyle (1) did carry out a test of Henry's law by varying the <math>\text{Rn} + \text{Air}</math> pressure from <math>10^{-5}</math> mm Hg to <math>10^{-4}</math> mm Hg. The solubility (Ostwald Coefficient) at <math>14^{\circ}\text{C}</math> varied irregularly from 0.299 to 0.307 which was considered to be within experimental error.</p> <p>We used the data of three workers for smoothing. In fitting the equation those data points which differed from the smoothed curve by about two standard deviations or more were rejected and the data then re-fitted. The 40 points used for the final smoothing equation were obtained as follows (reference - number of data points used from that reference): 1-2; 2-6; 3-32. The fitting equation used was</p> $\ln x_1 = A + B/(T/100K) + C \ln (T/100K) \quad (4)$ <p>Using <math>T/K</math> as the variable rather than <math>T/100K</math> gives coefficients of approximately equal magnitude. The best fit for the 40 data points was</p> $\ln x_1 = -90.5481 + 130.026/(T/100K) + 35.0047 \ln (T/100K) \quad (5)$ <p>where <math>x_1</math> is the mole fraction solubility of radon at 101,325 Pa partial pressure of gas. The fit in <math>\ln x_1</math> gave a standard deviation of 1.02% taken at the middle of the temperature range. Table 1 gives smoothed values of the mole fraction solubility at 101,325 Pa partial pressure of gas and the Ostwald coefficient at 5K intervals.</p>	

<b>COMPONENTS:</b> 1. Radon-222; $^{222}_{86}\text{Rn}$ ; 14859-67-7 2. Water; $\text{H}_2\text{O}$ ; 7732-18-5	<b>EVALUATOR:</b> Ruben Battino Department of Chemistry Wright State University Dayton, Ohio, 45431 U.S.A.  July 1978
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**CRITICAL EVALUATION:**

TABLE 1. Smoothed values of radon solubility in water and thermodynamic functions<sup>a</sup> using equation 2. Mole fraction solubility at 101 325 Pa partial pressure of radon. Ostwald coefficient at equilibrium saturation pressure.

T/K	Mol Fraction $x_1 \times 10^4$	Ostwald Coefficient L	$\Delta\bar{G}_1^\circ/\text{KJmol}^{-1}$ <sup>b</sup>	$\Delta\bar{H}_1^\circ/\text{KJmol}^{-1}$	$\Delta\bar{S}_1^\circ/\text{JK}^{-1}\text{mol}^{-1}$
273.15	4.217	0.5249	17.65	-28.61	-169
278.15	3.382	0.4286	18.48	-27.15	-164
283.15	2.764	0.3565	19.29	-25.70	-159
288.15	2.299	0.3016	20.07	-24.24	-154
293.15	1.945	0.2593	20.83	-22.79	-149
298.15	1.671	0.2263	21.56	-21.33	-144
303.15	1.457	0.2003	22.27	-19.88	-139
308.15	1.288	0.1797	22.95	-18.42	-134
313.15	1.153	0.1632	23.61	-16.97	-130
318.15	1.046	0.1500	24.25	-15.51	-125
323.15	0.959	0.1395	24.86	-14.06	-120
328.15	0.889	0.1310	25.45	-12.60	-116
333.15	0.833	0.1243	26.02	-11.15	-112
338.15	0.788	0.1190	26.57	-9.69	-107
343.15	0.752	0.1149	27.09	-8.24	-103
348.15	0.724	0.1119	27.60	-6.78	-99
353.15	0.703	0.1099	28.08	-5.33	-95
358.15	0.688	0.1087	28.54	-3.87	-91
363.15	0.678	0.1082	28.98	-2.42	-86
368.15	0.673	0.1085	29.41	-0.96	-82
373.15	0.672	0.1095	29.81	0.49	-79

<sup>a</sup>  $\Delta\bar{C}_{p1}^\circ$  was independent of temperature and has a value of  $291 \text{ J K}^{-1} \text{ mol}^{-1}$ .

<sup>b</sup>  $\text{cal}_{\text{th}} = 4.184 \text{ joule}$

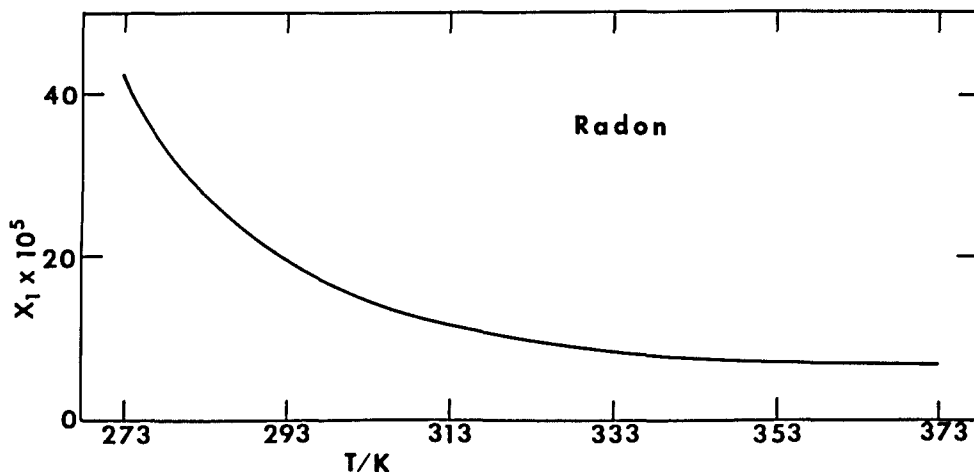


FIGURE 1. The mole fraction solubility of radon in water at a radon partial pressure of 101.325 kPa (1 atm).



<p>COMPONENTS:</p> <p>1. Radon-222; <math>^{222}_{86}\text{Rn}</math>; 14859-67-7</p> <p>2. Water; <math>\text{H}_2\text{O}</math>; 7732-18-5</p>	<p>EVALUATOR:</p> <p>Rubin Battino  Department of Chemistry  Wright State University  Dayton, Ohio, 45431 U.S.A.</p> <p>July 1978</p>
<p>CRITICAL EVALUATION:</p> <p>Table 1 also gives the thermodynamic functions <math>\Delta\bar{G}_1^\circ</math>, <math>\Delta\bar{H}_1^\circ</math>, <math>\Delta\bar{S}_1^\circ</math>, and <math>\Delta\bar{C}_{p1}^\circ</math> for the transfer of gas from the vapor phase at 101,325 Pa partial gas pressure to the (hypothetical) solution phase of unit mole fraction. These thermodynamic properties are calculated from the smoothing equation according to the following equations:</p> $\Delta\bar{G}_1^\circ = -\text{RAT} - 100\text{RB} - \text{RCT} \ln (T/100\text{K}) \quad (6)$ $\Delta\bar{S}_1^\circ = \text{RA} + \text{RC} \ln (T/100) + \text{RC} \quad (7)$ $\Delta\bar{H}_1^\circ = -100\text{RB} + \text{RCT} \quad (8)$ $\Delta\bar{C}_{p1}^\circ = \text{RC} \quad (9)$ <p>The results from three other workers was rejected for various reasons. The single point of Hofbauer's (4) was high by about 7%. Hofmann's seven values (5) were erratically high and low between 1 and 11%. Ramstedt's three measurements (6) were also high by about 2 to 4%. Although many references quote Valentiner (7), he used other people's data for his paper.</p> <p>Figure 1 shows the temperature dependence of the solubility of radon in water. The curve was obtained from the smoothing equation. There appears to be a minimum at about 363K for the Ostwald coefficient. The mole fraction solubility minimum is at 371.45 according to the fitted equation although there is no minimum evident over the temperature range of the experimental measurements.</p> <p><u>References</u></p> <ol style="list-style-type: none"> <li>Boyle, R. W. <u>Phil. Mag.</u> 1911, <u>22</u>, 840.</li> <li>Kofler, M. <u>Sitz. Akad. Wiss. Wien</u> 1912, <u>121</u>, 2169; <u>Monatsh.</u> 1913, <u>34</u>, 389.</li> <li>Szeparowicz, M. <u>Sitz. Akad. Wiss. Wien</u> 1920, <u>129</u>, 437.</li> <li>Hofbauer, G. <u>Sitz. Akad. Wiss. Wien</u> 1914, <u>123</u>, 2001.</li> <li>Hofmann, R. <u>Phys. Z.</u> 1905, <u>6</u>, 337.</li> <li>Ramstedt, E. <u>J. Phys. Radium</u> 1911, <u>8</u>, 253.</li> <li>Valentiner, S. <u>Z. Physik.</u> 1927, <u>42</u>, 253.</li> </ol>	

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<p>VARIABLES:</p> <p>T/K: 273.15 - 353.15</p>	<p>PREPARED BY:</p> <p>R. Battino</p>																								
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<b>VARIABLES:</b> T/K: 273.15 - 291.15	<b>PREPARED BY:</b> R. Battino												
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COMPONENTS:			ORIGINAL MEASUREMENTS:		
1. Radon-222; $^{222}_{86}\text{Rn}$ ; 14859-67-7			Szeparowicz, M.		
2. Water; $\text{H}_2\text{O}$ ; 7732-18-5			Sitz. Akad. Wiss. Wien. 1920, <u>129</u> , 437-454.		
VARIABLES:			PREPARED BY:		
T/K: 273.15 - 370.15			R. Battino		
EXPERIMENTAL VALUES:					
T/K	Mol Fraction $x_1 \times 10^4$	Ostwald Coefficient <sup>a</sup> L	T/K	Mol Fraction $x_1 \times 10^4$	Ostwald Coefficient L
273.15	4.122	0.513	323.15	0.969*	0.141
273.75	4.057	0.506	328.15	0.903*	0.133
274.15	3.987	0.498	334.15	0.822*	0.123
275.55	3.807*	0.478	338.15	0.794*	0.120
276.35	3.653*	0.460	340.65	0.757*	0.115
276.95	3.598	0.454	341.65	0.768*	0.117
277.15	3.556	0.449	347.15	0.739*	0.114
278.85	3.290*	0.418	349.15	0.710*	0.110
280.45	3.068*	0.392	350.55	0.708*	0.110
282.95	2.855	0.368	353.75	0.690*	0.108
284.85	2.590*	0.336	355.15	0.688*	0.108
285.95	2.473*	0.322	359.05	0.682*	0.108
289.15	2.204*	0.290	362.65	0.671*	0.107
290.65	2.163	0.286	363.65	0.669*	0.107
292.15	2.017*	0.268	364.15	0.687*	0.110
293.15	1.950*	0.260	365.15	0.674*	0.108
299.45	1.589*	0.216	366.35	0.666*	0.107
308.15	1.283*	0.179	368.05	0.676*	0.109
315.15	1.103*	0.157	368.95	0.712	0.115
317.75	1.088	0.156	369.15	0.687*	0.111
318.15	1.017	0.146	370.15	0.673*	0.109
<sup>a</sup> Ostwald coefficient. Since the original measurements were made in terms of radon concentrations in the gas and liquid phase, it is assumed that there is a negligible volume change on mixing.					
AUXILIARY INFORMATION					
METHOD/APPARATUS/PROCEDURE:			SOURCE AND PURITY OF MATERIALS:		
Radon in a carrier gas such as air is equilibrated with water and counts taken to determine the radon concentration in each phase and hence the Ostwald coefficient. The radon partial pressure is of the order of $10^{-4}$ mm Hg.			1. Radon -		
*solubility values which were used in the final smoothing equation for the recommended values given in the critical evaluation.			2. Water -		
The mole fraction solubility at 101.325 Pa partial pressure of radon was calculated by the compiler.			ESTIMATED ERROR:		
			REFERENCES:		

<b>COMPONENTS:</b> 1. Radon-222; $^{222}_{86}\text{Rn}$ ; 14859-67-7 2. Water-d <sub>2</sub> ; D <sub>2</sub> O; 7789-20-0	<b>ORIGINAL MEASUREMENTS:</b> Vdovenko, V. M.; Gurikov, Yu. V.; Legin, E. K. <u>Radiokhimiya</u> 1970, <u>12</u> , 670 - 673. <u>Soviet Radiochemistry</u> 1970, <u>12</u> , 631 - 633.																
<b>VARIABLES:</b>  T/K: 279.15 - 288.15	<b>PREPARED BY:</b>  H. L. Clever																
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="212 493 964 691"> <thead> <tr> <th>T/K</th> <th>Ratio <math>L_{\text{D}_2\text{O}}/L_{\text{H}_2\text{O}}</math></th> <th>Ostwald Coefficient <math>L_{\text{D}_2\text{O}}</math></th> <th>Mol Fraction 101.325 kPa Rn <math>X_1 \times 10^4</math></th> </tr> </thead> <tbody> <tr> <td>279.15</td> <td>1.09</td> <td>0.450</td> <td>3.57</td> </tr> <tr> <td>283.15</td> <td>1.08</td> <td>0.385</td> <td>3.00</td> </tr> <tr> <td>288.15</td> <td>1.07</td> <td>0.323</td> <td>2.48</td> </tr> </tbody> </table> <p>The authors reported only the ratio <math>L_{\text{D}_2\text{O}} / L_{\text{H}_2\text{O}}</math>.</p> <p>The compiler estimated the Ostwald coefficient and mole fraction. The Ostwald coefficient was obtained by multiplying the ratio times the Ostwald coefficient recommended in the critical evaluation for radon in H<sub>2</sub>O. For the mole fraction calculation it was assumed that the Ostwald coefficient was independent of pressure and that the gram mole volume of radon is 22,290 cm<sup>3</sup> at 273.15 K and 101.325 kPa.</p>		T/K	Ratio $L_{\text{D}_2\text{O}}/L_{\text{H}_2\text{O}}$	Ostwald Coefficient $L_{\text{D}_2\text{O}}$	Mol Fraction 101.325 kPa Rn $X_1 \times 10^4$	279.15	1.09	0.450	3.57	283.15	1.08	0.385	3.00	288.15	1.07	0.323	2.48
T/K	Ratio $L_{\text{D}_2\text{O}}/L_{\text{H}_2\text{O}}$	Ostwald Coefficient $L_{\text{D}_2\text{O}}$	Mol Fraction 101.325 kPa Rn $X_1 \times 10^4$														
279.15	1.09	0.450	3.57														
283.15	1.08	0.385	3.00														
288.15	1.07	0.323	2.48														
<b>AUXILIARY INFORMATION</b>																	
<b>METHOD:</b> <p>The distribution of radon between the aqueous and gas phase was measured. The vessel for the dissolution of radon was of thin-walled Plexiglass with a volume of about 100 cm<sup>3</sup>, divided into two portions by a 10 mm thick partition. The partition has three vertical openings. The vessel was filled with water to the partition. The upper part of the vessel contained radon + air at a low pressure. A magnetic stirrer causes the water to circulate up through two of the partition openings and back down through the center opening. It was established that gas/liquid equilibrium was reached in 20 minutes or less.</p> <p>After equilibrium was established, the gas phases was displaced by air, and the radon activity determined. Again equilibrium was established, the gas phase was displaced by air and the radon activity was determined. The distribution coefficient was calculated from the activities and gas and liquid volumes.</p>	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Radon-222. No information given. The compiler assumed Rn-222 was the isotope used since normally it is the most available. 2. Water. No information given.																
<b>ESTIMATED ERROR:</b>  $\delta T/K = 0.05$																	
<b>REFERENCES:</b>																	

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Radon-222; <math>^{222}_{86}\text{Rn}</math>; 14859-67-7</li> <li>Sea water</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Boyle, R.W.</p> <p><u>Phil. Mag.</u> 1911, <u>22</u>, 840-854.</p>				
<p>VARIABLES:</p> <p>T/K: 287.15</p>	<p>PREPARED BY:</p> <p>W. Gerrard May 1977</p>				
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="565 487 847 632"> <thead> <tr> <th>T/K</th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>287.15</td> <td>0.255</td> </tr> </tbody> </table> <p>Boyle defined the coefficient of solubility, <math>s</math>, as <math>(e_1/V_1)/(e_2/V_2)</math> where <math>e_1</math> is emanation in volume <math>V_1</math> of liquid, and <math>e_2</math> is emanation in volume <math>V_2</math> of gas. The partial pressure of radon is less than 0.1 kPa. The liquid is also saturated with carrier gas (air or another gas) at the prevailing pressure, originally about 101 kPa.</p> <p>The mole fraction solubility at 101.325 kPa (1 atm) was calculated by the compiler. It was assumed that the Ostwald coefficient was independent of pressure and that the gram-mole volume of radon is 22,290 cm<sup>3</sup> at 273.15 K and 101.325 kPa.</p>		T/K	Ostwald Coefficient L	287.15	0.255
T/K	Ostwald Coefficient L				
287.15	0.255				
<p>AUXILIARY INFORMATION</p>					
<p>METHOD:</p> <p>Radon-222 in a carrier gas (air, or other gas not specified) is shaken with a measured volume of liquid.</p> <p>Radioactivity is determined in the gas and liquid phases by gamma-ray electroscopes.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>Radon-222.</li> <li>Sea water. Specific gravity at 287.15 K is 1.022.</li> </ol>				
<p>APPARATUS/PROCEDURE:</p> <p>The sampling bulb and mixing bulb are connected by a three-way tap. For the measurement of radioactivity, the bulbs are separately placed near to the electroscopes. A diagram is given by Boyle.</p>	<p>ESTIMATED ERROR:</p> <p><math>\delta T/K = 0.2</math> <math>\delta L/L = 0.03</math></p> <p>REFERENCES:</p>				



<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Radon-222; <math>^{222}_{86}\text{Rn}</math>; 14859-67-7</li> <li>Sea water</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Kofler, M.</p> <p><u>Phys. Zeit.</u>, 1908, <u>9</u>, 6-8.</p>				
<p>VARIABLES:</p> <p>T/K: 291.15</p>	<p>PREPARED BY:</p> <p>W. Gerrard May 1977</p>				
<table border="1" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td style="text-align: center;">291.15</td> <td style="text-align: center;">0.165</td> </tr> </tbody> </table> <p>The absorption coefficient (Ostwald coefficient) is the ratio of the concentration of radon in the liquid phase and that in the gaseous phase (air and radon) at a partial pressure of radon less than 0.1 kPa.</p>		T/K	Ostwald Coefficient L	291.15	0.165
T/K	Ostwald Coefficient L				
291.15	0.165				
<p>AUXILIARY INFORMATION</p>					
<p>METHOD:</p> <p>Measurement of radioactivity in the liquid and gaseous phases. Described by Kofler (1,2), who gave a diagram.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>Radon. Not specified.</li> <li>Sea water. Specific gravity 1.028 at 291.15 K.</li> </ol>				
<p>APPARATUS/PROCEDURE:</p> <p>Two glass bulbs connected by a tap. Each bulb has also a separate tap. Radioactivity measured by an aluminum leaf electroscope.</p>	<p>ESTIMATED ERROR:</p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>Kofler, M. <u>Sitzungber. Akad. Wiss. Wien, Abt 2A, 1912, 121, 2169.</u></li> <li>Kofler, M. <u>Abt 2A, Monatsh., 1913, 34, 389.</u></li> </ol>				

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Radon-222; <math>^{222}_{86}\text{Rn}</math>; 14859-67-7</li> <li>Water; <math>\text{H}_2\text{O}</math>; 7732-18-5</li> <li>Electrolyte</li> </ol>	<p>EVALUATOR:</p> <p>H. L. Clever          Chemistry Department          Emory University          Atlanta, GA 30322          U.S.A.</p> <p>August 1978</p>																												
<p>CRITICAL EVALUATION:</p> <p>The solubility of radon in aqueous electrolyte solutions.</p> <p>The solubility of radon in aqueous electrolyte solution was measured by Kofler (1,2) who worked with radon-222, and by Hevesy (3) who worked with radon-219. Hevesy's results on two systems were only qualitative and of doubtful value (see p. ). Kofler determined the solubility of radon-222 in aqueous solutions of thirteen electrolytes. The <math>\text{NH}_4\text{NO}_3</math>, <math>\text{NaCl}</math> and <math>\text{Ba}(\text{NO}_3)_2</math> solutions were extensively studied as a function of temperature and electrolyte concentration. The other solutions were studied only at a temperature of 291.15 K.</p> <p>Kofler measured the solubility of radon-222 at a radon partial pressure of less than 0.1 kPa in the presence of air as a carrier gas at a pressure of about 100 kPa. Kofler reported the radon solubility, as the equivalent of an Ostwald coefficient, and the electrolyte solution density.</p> <p>In order to be able to compare the radon solubilities in electrolyte solutions with the other noble gases Kofler's data was converted into a Setschenow salt effect parameter. The solution density values were converted to molalities by the aid of the density data in The International Critical Tables (4). Kofler's (5) radon in water Ostwald coefficients were fitted to the equation</p> $\ln L^{\circ} = -82.0146 + 126.823/(T/100) + 34.7934 \ln (T/100)$ <p>to obtain <math>L^{\circ}</math> values at the various temperatures needed in the calculation. The Setschenow salt effect parameter was calculated as</p> $k_L = (1/m) \log (L^{\circ}/L)$ <p>where <math>m</math> is the mole salt <math>\text{kg}^{-1}</math> water (molality),  <math>L^{\circ}</math> is the Ostwald coefficient in water, and  <math>L</math> is the Ostwald coefficient in the electrolyte solution of molality <math>m</math>.</p> <p>The results of the calculation are given in Table 1.</p> <p>For the other noble gases the Setschenow salt effect parameter was calculated as <math>k_S = (1/m) \log (S^{\circ}/S)</math> and <math>k_{SX} = (1/m) \log (X^{\circ}/X)</math> where <math>S^{\circ}/S</math> is the gas solubility ratio with <math>S</math> in <math>\text{cm}^3</math> (STP) gas <math>\text{kg}^{-1}</math> water and <math>X^{\circ}/X</math> is the gas solubility ratio with <math>X</math> the mole fraction with respect to water and the electrolyte ions. The <math>k_L</math>, <math>k_S</math> and <math>k_{SX}</math> values for radon + water + sodium chloride at 291.15 K are compared below.</p> <table border="1" data-bbox="140 1580 1267 1779"> <tr> <td>Mol NaCl <math>\text{kg}^{-1}</math> water</td> <td>0.220</td> <td>0.542</td> <td>1.00</td> <td>2.59</td> <td>3.35</td> <td>6.20</td> </tr> <tr> <td><math>k_L</math></td> <td>0.313</td> <td>0.262</td> <td>0.235</td> <td>0.179</td> <td>0.167</td> <td>0.133</td> </tr> <tr> <td><math>k_S</math></td> <td>0.303</td> <td>0.253</td> <td>0.227</td> <td>0.171</td> <td>0.159</td> <td>0.124</td> </tr> <tr> <td><math>k_{SX}</math></td> <td>0.319</td> <td>0.269</td> <td>0.242</td> <td>0.186</td> <td>0.174</td> <td>0.138</td> </tr> </table> <p>The <math>k_L</math> and <math>k_{SX}</math> values are usually within 1-4 percent of each other. Thus the magnitude and trends in <math>k_L</math> shown in Table 1 are also representative of the <math>k_{SX}</math> values.</p>		Mol NaCl $\text{kg}^{-1}$ water	0.220	0.542	1.00	2.59	3.35	6.20	$k_L$	0.313	0.262	0.235	0.179	0.167	0.133	$k_S$	0.303	0.253	0.227	0.171	0.159	0.124	$k_{SX}$	0.319	0.269	0.242	0.186	0.174	0.138
Mol NaCl $\text{kg}^{-1}$ water	0.220	0.542	1.00	2.59	3.35	6.20																							
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COMPONENTS:		EVALUATOR:			
1. Radon-222; $^{222}_{86}\text{Rn}$ ; 14859-67-7		H. L. Clever Chemistry Department Emory University Atlanta, GA 30322 U. S. A.			
2. Water; $\text{H}_2\text{O}$ ; 7732-18-5					
3. Electrolyte		August 1978			
CRITICAL EVALUATION:					
TABLE 1. The Setschenow salt effect parameter of radon in aqueous salt solutions. $k_L = (1/m) \log (I^0/L)$ .					
Ammonium Nitrate; $\text{NH}_4\text{NO}_3$ ; 6484-52-2					
<u>T/K</u>	<u>mol salt kg<sup>-1</sup> water</u>				
	0.807	1.72	3.37	8.49	
273.35	0.138	0.100	0.084	0.066	
288.65	0.095	0.072	0.066	0.050	
309.95	-	0.047	0.038	0.034	
Ammonium Chloride; $\text{NH}_4\text{Cl}$ ; 12125-02-9					
<u>T/K</u>	<u>4.79 mol salt kg<sup>-1</sup> water</u>				
291.15	0.097				
Copper Sulfate; $\text{CuSO}_4$ ; 7758-98-7					
<u>T/K</u>	<u>mol salt kg<sup>-1</sup> water</u>				
	0.276	0.511	0.572	0.724	1.336
291.15	0.557	0.492	0.489	0.456	0.428
Silver nitrate; $\text{AgNO}_3$ ; 7761-88-8					
<u>T/K</u>	<u>1.43 mol salt kg<sup>-1</sup> water</u>				
291.15	0.115				
Zinc Sulfate; $\text{ZnSO}_4$ ; 7732-02-0					
<u>T/K</u>	<u>mol salt kg<sup>-1</sup> water</u>				
	1.30	2.45			
291.15	0.372	0.341			
Mercury (II) Chloride; $\text{HgCl}_2$ ; 7487-94-7					
<u>T/K</u>	<u>0.226 mol salt kg<sup>-1</sup> water</u>				
291.15	0.218				
Lead Nitrate; $\text{Pb}(\text{NO}_3)_2$ ; 10099-74-8					
<u>T/K</u>	<u>mol salt kg<sup>-1</sup> water</u>				
	0.889	1.081			
291.15	0.255	0.270			
Ferrous Sulfate; $\text{FeSO}_4$ ; 7720-78-7					
<u>T/K</u>	<u>1.58 mol salt kg<sup>-1</sup> water</u>				
291.15	0.341				
Barium Nitrate; $\text{Ba}(\text{NO}_3)_2$ ; 10022-31-8					
<u>T/K</u>	<u>mol salt kg<sup>-1</sup> water</u>				
	0.0346	0.0630	0.179	0.271	0.298
273.45	-	0.770	-	-	-
274.75	1.34	-	-	-	-
278.25	-	-	0.419	-	-
279.35	-	0.878	-	-	-
281.55	-	-	-	0.284	-
286.55	-	0.884	-	-	-
286.95	-	-	0.560	-	-
287.75	-	-	-	-	0.366
288.15	1.43	-	-	-	-
300.65	1.09	-	-	-	0.290
314.55	-	-	0.305	-	-

COMPONENTS:	EVALUATOR:
1. Radon-222; $^{222}_{86}\text{Rn}$ ; 14859-67-7	H. L. Clever
2. Water; $\text{H}_2\text{O}$ ; 7732-18-5	Chemistry Department
3. Electrolyte	Emory University
	Atlanta, GA 30322
	U.S.A.
	August 1978

## CRITICAL EVALUATION:

TABLE 1. The Setschenow salt effect parameter of radon in aqueous salt solution (continued).  $k_L = (1/m) \log (L^0/L)$ .

Sodium Chloride; $\text{NaCl}$ ; 7647-14-5										
T/K	mol salt $\text{kg}^{-1}$ water									
	0.220	0.245	0.542	1.00	1.87	2.59	2.80	3.35	4.05	6.65*
273.35	-	-	-	-	-	-	-	-	0.179	-
273.65	-	0.412	-	-	-	-	-	-	0.178	-
273.95	-	-	-	-	0.199	-	-	-	-	-
274.95	-	-	-	-	-	-	0.179	-	-	-
277.15	-	-	-	-	-	-	0.177	-	-	-
278.95	-	-	-	-	-	-	-	-	0.166	-
279.65	-	-	-	-	0.198	-	-	-	-	-
280.35	-	-	-	-	-	-	-	-	0.162	0.139
282.65	-	-	-	-	-	-	0.172	-	-	-
282.95	-	-	-	-	-	-	-	-	0.155	-
283.15	-	-	-	-	-	-	-	-	0.151	0.139
284.65	-	-	-	-	-	-	-	-	0.140	-
285.95	-	-	-	-	0.178	-	-	-	-	-
286.95	-	-	-	-	-	-	0.166	-	-	-
288.65	-	-	-	-	-	-	0.159	-	-	-
290.15	-	-	-	-	-	-	-	-	-	0.126
291.15	0.313	-	0.262	0.235	-	0.179	-	0.167	-	0.133**
297.35	-	-	-	-	-	-	0.172	-	-	-
298.35	-	-	-	-	-	-	-	-	0.140	-
298.85	-	-	-	-	-	-	0.163	-	-	-
305.35	-	-	-	-	-	-	-	-	0.130	-
323.65	-	-	-	-	-	-	-	-	0.113	-

Potassium Ferrocyanide; $\text{K}_4\text{Fe}(\text{CN})_6$ ; 13943-58-3	
T/K	0.490 mol salt $\text{kg}^{-1}$ water
291.15	0.895

Potassium Permanganate; $\text{KMnO}_4$ ; 7722-64-7	
T/K	0.380 mol salt $\text{kg}^{-1}$ water
291.15	0.419

Potassium Chloride; $\text{KCl}$ ; 7447-40-7					
T/K	mol salt $\text{kg}^{-1}$ water				
	0.641	1.032	1.62	2.42	4.63
291.15	0.274	0.228	0.200	0.161	0.143

\* molality greater than saturation of  $\text{NaCl}$  (?).\*\* value at 6.20 mol salt  $\text{kg}^{-1}$   $\text{H}_2\text{O}$ .

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>1. Radon-222; <math>^{222}_{86}\text{Rn}</math>; 14859-67-7</li> <li>2. Water; <math>\text{H}_2\text{O}</math>; 7732-18-5</li> <li>3. Electrolyte</li> </ol>	<p>EVALUATOR:</p> <p>H. L. Clever          Chemistry Department          Emory University          Atlanta, GA 30322          U.S.A.</p> <p>August 1978</p>
<p>CRITICAL EVALUATION:</p> <p>In general the magnitude of the salt effect parameter is greater for radon than the other noble gases for a given electrolyte concentration and temperature. The trends observed in the salt effect parameter in the radon + water + barium nitrate deserve special note. There is little accurate salt effect data at electrolyte concentrations below 0.1 molal. Kofler made measurements in 0.0346 and 0.0630 molal <math>\text{Ba}(\text{NO}_3)_2</math> that give a much larger value of the salt effect parameter than the values at higher concentration of <math>\text{Ba}(\text{NO}_3)_2</math>. Such a trend is hinted in other systems but the difficulty of making accurate measurements in the dilute salt solutions has caused the effect to be doubted. The salt effect in dilute salt solutions deserves more investigation.</p> <p>REFERENCES.</p> <ol style="list-style-type: none"> <li>1. Kofler, M. <u>Phys. Z.</u> 1908, <u>9</u>, 6.</li> <li>2. Kofler, M. <u>Sitzungsber. Akad. Wiss. Wien, Math. Naturwiss. Kl. Abt. 2A</u>, 1913, <u>122</u>, 1473.</li> <li>3. Hevesy, G. <u>Phys. Z.</u> 1911, <u>12</u>, 1214; <u>J. Phys. Chem.</u> 1912, <u>16</u>, 429.</li> <li>4. International Critical Tables, Washburn, E. W., Editor McGraw Hill Co. 1928, Vol. III.</li> <li>5. Kofler, M. <u>Sitzungsber. Akad. Wiss. Wien, Math. Naturwiss. Kl. Abt. 2A</u> 1912, <u>121</u>, 2169.</li> </ol>	

COMPONENTS: 1. Radon; $^{222}_{86}\text{Rn}$ ; 14859-67-7 2. Water; $\text{H}_2\text{O}$ ; 7732-18-5 3. Ammonium chloride; $\text{NH}_4\text{Cl}$ ; 12125-02-9	ORIGINAL MEASUREMENTS: Kofler, M.  <u>Physik. Z.</u> 1908, <u>9</u> , 6-8.												
VARIABLES: T/K: 291.15 Specific Gravity: 1.078	PREPARED BY: W. Gerrard												
EXPERIMENTAL VALUES: <table border="1" data-bbox="329 506 954 685" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">T/K</th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Specific Gravity</th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Ammonium Chloride mol kg<sup>-1</sup> H<sub>2</sub>O</th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td style="border-bottom: 1px solid black;">291.15</td> <td style="border-bottom: 1px solid black;">-</td> <td style="border-bottom: 1px solid black;">0.0</td> <td style="border-bottom: 1px solid black;">0.280</td> </tr> <tr> <td></td> <td style="border-bottom: 1px solid black;">1.078</td> <td style="border-bottom: 1px solid black;">4.79</td> <td style="border-bottom: 1px solid black;">0.096</td> </tr> </tbody> </table> <p>The solubility in water was interpolated from the author's data in reference (1).</p> <p>The ammonium chloride molality was calculated by the Editor from data taken from the International Critical Tables, Vol. III.</p> <p>The author reported his solubility values as an Absorption Coefficient = (Concentration of Rn in the liquid phase)/(Concentration in the gas phase). We have labelled it as an Ostwald coefficient. The solubility was measured at a radon partial pressure of less than 0.1 kPa at equilibrium. The liquid was also saturated with air as a carrier gas at a pressure of about 100 kPa.</p>		T/K	Specific Gravity	Ammonium Chloride mol kg <sup>-1</sup> H <sub>2</sub> O	Ostwald Coefficient L	291.15	-	0.0	0.280		1.078	4.79	0.096
T/K	Specific Gravity	Ammonium Chloride mol kg <sup>-1</sup> H <sub>2</sub> O	Ostwald Coefficient L										
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AUXILIARY INFORMATION													
METHOD: Measurement of radioactivity in the liquid and gaseous phases. Described by Kofler (1,2), who gave a diagram.	SOURCE AND PURITY OF MATERIALS: Not specified												
APPARATUS/PROCEDURE: The apparatus consisted of two glass bulbs connected by a tap. Each bulb had a separate tap. The assembly is shaken. Radioactivity is measured by an aluminum leaf electroscope.	ESTIMATED ERROR:  REFERENCES: 1. Kofler, M. <u>Sitzungsber. Akad. Wiss. Wien, Abt. 2A</u> 1912, <u>121</u> , 2169. 2. Kofler, M. <u>Monatsh.</u> 1913, <u>34</u> , 389.												

COMPONENTS: 1. Radon; $^{222}_{86}\text{Rn}$ ; 14859-67-7 2. Water; $\text{H}_2\text{O}$ ; 7732-18-5 3. Ammonium nitrate; $\text{NH}_4\text{NO}_3$ ; 6484-52-2		ORIGINAL MEASUREMENTS: Kofler, M.  <u>Sitzungsber. Akad. Wiss. Wien, Math.-Naturwiss. Kl. Abt. 2A 1913, 122, 1473 - 1479.</u>		
VARIABLES: T/K: 273.35 - 315.55 Specific Gravity: 1.024 - 1.180		PREPARED BY: W. Gerrard		
EXPERIMENTAL VALUES:				
$\text{NH}_4\text{Cl}$	T/K	Specific* Gravity	Ammonium Nitrate $\text{mol kg}^{-1} \text{H}_2\text{O}$	Ostwald Coefficient L
	273.35	-	0.0	0.532
	288.65			0.303
	309.95			0.176
	315.55			0.159
	273.35	1.024	0.807	0.412
	288.35			0.254
	302.75			0.177
	273.35	1.050	1.72	0.358
	288.65			0.228
	309.95			0.146
	315.55			(0.121?)
	273.45	1.090	3.37	0.278
	288.95			0.182
	307.55			0.131
	308.95			0.127
	275.75	1.180	8.49	0.147
	289.05			0.113
	309.45			0.090
*The specific gravities were measured at 291.15 except for the value 1.024 which was measured at 290.15 K.				
The Editor estimated the $\text{NH}_4\text{NO}_3$ molality from ICT density tables.				
AUXILIARY INFORMATION				
METHOD: Measurement of radioactivity in the liquid and gaseous phases. Described by Kofler (1,2), who gave a diagram.		SOURCE AND PURITY OF MATERIALS: Not specified		
APPARATUS/PROCEDURE: The apparatus consisted of two glass bulbs connected by a tap. Each bulb had a separate tap. The assembly is shaken. Radioactivity is measured by an aluminum leaf electroscope.		ESTIMATED ERROR:		
		REFERENCES: 1. Kofler, M. <u>Sitzungsber. Akad. Wiss. Wien, Abt. 2A 1912, 121, 2169.</u> 2. Kofler, M. <u>Monatsh. 1913, 34, 389.</u>		

<b>COMPONENTS:</b> 1. Radon; $^{222}_{86}\text{Rn}$ ; 14859-67-7 2. Water; $\text{H}_2\text{O}$ ; 7732-18-5 3. Copper Sulfate; $\text{CuSO}_4$ ; 7758-98-7	<b>ORIGINAL MEASUREMENTS:</b> Kofler, M.  <u>Physik. Z.</u> 1908, <u>9</u> , 6-8.																												
<b>VARIABLES:</b> T/K: 291.15 Specific Gravity: 1.042 - 1.193	<b>PREPARED BY:</b> W. Gerrard																												
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="344 493 979 761"> <thead> <tr> <th>T/K</th> <th>Specific Gravity</th> <th>Copper Sulfate mol kg<sup>-1</sup> H<sub>2</sub>O</th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>291.15</td> <td>-</td> <td>0.0</td> <td>0.280</td> </tr> <tr> <td></td> <td>1.042</td> <td>0.276</td> <td>0.194</td> </tr> <tr> <td></td> <td>1.0776</td> <td>0.511</td> <td>0.157</td> </tr> <tr> <td></td> <td>1.087</td> <td>0.572</td> <td>0.147</td> </tr> <tr> <td></td> <td>1.110</td> <td>0.724</td> <td>0.131</td> </tr> <tr> <td></td> <td>1.193</td> <td>1.336</td> <td>0.075</td> </tr> </tbody> </table> <p data-bbox="134 785 1144 830">The solubility in water was interpolated from the author's data from reference (1).</p> <p data-bbox="134 854 1157 900">The copper sulfate molalities were calculated by the Editor from data taken from the International Critical Tables, Vol. III.</p> <p data-bbox="134 924 1259 1043">The author reported his solubility values as an Absorption Coefficient = (Concentration of Rn in the liquid phase)/(Concentration in the gas phase). We have labelled it as an Ostwald coefficient. The solubility was measured at a radon partial pressure of less than 0.1 kPa at equilibrium. The liquid was also saturated with air as a carrier gas at a pressure of about 100 kPa.</p>		T/K	Specific Gravity	Copper Sulfate mol kg <sup>-1</sup> H <sub>2</sub> O	Ostwald Coefficient L	291.15	-	0.0	0.280		1.042	0.276	0.194		1.0776	0.511	0.157		1.087	0.572	0.147		1.110	0.724	0.131		1.193	1.336	0.075
T/K	Specific Gravity	Copper Sulfate mol kg <sup>-1</sup> H <sub>2</sub> O	Ostwald Coefficient L																										
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<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>1. Radon; <math>^{222}_{86}\text{Rn}</math>; 14859-67-7</li> <li>2. Water; <math>\text{H}_2\text{O}</math>; 7732-18-5</li> <li>3. Silver Nitrate; <math>\text{AgNO}_3</math>; 7761-88-8</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Kofler, M.</p> <p><u>Physik. Z.</u> 1908, <u>9</u>, 6-8.</p>												
<p>VARIABLES:</p> <p>T/K: 291.15</p> <p>Specific Gravity: 1.190</p>	<p>PREPARED BY:</p> <p>W. Gerrard</p>												
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="295 487 934 671"> <thead> <tr> <th>T/K</th> <th>Specific Gravity</th> <th>Silver nitrate <math>\text{mol kg}^{-1} \text{H}_2\text{O}</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>291.15</td> <td>-</td> <td>0.0</td> <td>0.280</td> </tr> <tr> <td></td> <td>1.190</td> <td>1.43</td> <td>0.192</td> </tr> </tbody> </table> <p>The solubility in water was interpolated from the author's data in reference (1).</p> <p>The silver nitrate molality was calculated by the Editor from data taken from the International Critical Tables, Vol. III.</p> <p>The author reported his solubility values as an Absorption Coefficient = (Concentration of Rn in the liquid phase)/(Concentration in the gas phase). We have labelled it as an Ostwald coefficient. The solubility was measured at a radon partial pressure of less than 0.1 kPa at equilibrium. The liquid was also saturated with air as a carrier gas at a pressure of about 100 kPa.</p>		T/K	Specific Gravity	Silver nitrate $\text{mol kg}^{-1} \text{H}_2\text{O}$	Ostwald Coefficient L	291.15	-	0.0	0.280		1.190	1.43	0.192
T/K	Specific Gravity	Silver nitrate $\text{mol kg}^{-1} \text{H}_2\text{O}$	Ostwald Coefficient L										
291.15	-	0.0	0.280										
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<p>APPARATUS/PROCEDURE:</p> <p>The apparatus consisted of two glass bulbs connected by a tap. Each bulb had a separate tap. The assembly is shaken. Radioactivity is measured by an aluminum leaf electroscope.</p>	<p>ESTIMATED ERROR:</p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>1. Kofler, M. <u>Sitzungsber. Akad. Wiss. Wien, Abt. 2A</u> 1912, <u>121</u>, 2169.</li> <li>2. Kofler, M. <u>Monatsh.</u> 1913, <u>34</u>, 389.</li> </ol>												

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Radon; <math>^{222}_{86}\text{Rn}</math>; 14859-67-7</li> <li>Water; <math>\text{H}_2\text{O}</math>; 7732-18-5</li> <li>Zinc Sulfate; <math>\text{ZnSO}_4</math>; 7732-02-0</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Kofler, M.</p> <p><u>Physik. Z.</u> 1908, <u>9</u>, 6-8.</p>																
<p>VARIABLES:</p> <p>T/K: 291.15</p> <p>Specific Gravity: 1.199-1.346</p>	<p>PREPARED BY:</p> <p>W. Gerrard</p>																
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="330 489 964 681"> <thead> <tr> <th>T/K</th> <th>Specific Gravity</th> <th>zinc sulfate <math>\text{mol kg}^{-1} \text{H}_2\text{O}</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>291.15</td> <td>-</td> <td>0.0</td> <td>0.280</td> </tr> <tr> <td></td> <td>1.199</td> <td>1.30</td> <td>0.092</td> </tr> <tr> <td></td> <td>1.346</td> <td>2.45</td> <td>0.041</td> </tr> </tbody> </table> <p>The solubility in water was interpolated from the author's data from reference (1).</p> <p>The zinc sulfate molalities were calculated by the Editor from data taken from the International Critical Tables, Vol. III.</p> <p>The author reported his solubility values as an Absorption Coefficient = (Concentration of Rn in the liquid phase)/(Concentration in the gas phase). We have labelled it as an Ostwald coefficient. The solubility was measured at a radon partial pressure of less than 0.1 kPa at equilibrium. The liquid was also saturated with air as a carrier gas at a pressure of about 100 kPa.</p>		T/K	Specific Gravity	zinc sulfate $\text{mol kg}^{-1} \text{H}_2\text{O}$	Ostwald Coefficient L	291.15	-	0.0	0.280		1.199	1.30	0.092		1.346	2.45	0.041
T/K	Specific Gravity	zinc sulfate $\text{mol kg}^{-1} \text{H}_2\text{O}$	Ostwald Coefficient L														
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<p>APPARATUS/PROCEDURE:</p> <p>The apparatus consisted of two glass bulbs connected by a tap. Each bulb had a separate tap. The assembly is shaken. Radioactivity is measured by an aluminum leaf electroscope.</p>	<p>ESTIMATED ERROR:</p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>Kofler, M. <u>Sitzungsber. Akad. Wiss. Wien, Abt. 2A</u> 1912, <u>121</u>, 2169.</li> <li>Kofler, M. <u>Monatsh.</u> 1913, <u>34</u>, 389.</li> </ol>																

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Radon; <math>^{222}_{86}\text{Rn}</math>; 14859-67-7</li> <li>Water; <math>\text{H}_2\text{O}</math>; 7732-18-5</li> <li>Mercury (II) Chloride; <math>\text{HgCl}_2</math>; 7487-94-7</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Kofler, M.</p> <p><u>Physik. Z.</u> 1908, <u>9</u>, 6-8.</p>												
<p>VARIABLES:</p> <p>T/K: 291.15</p> <p>Specific Gravity: 1.049</p>	<p>PREPARED BY:</p> <p>W. Gerrard</p>												
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="290 479 924 648"> <thead> <tr> <th>T/K</th> <th>Specific Gravity</th> <th>Mercury (II) Chloride mol kg<sup>-1</sup> H<sub>2</sub>O</th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>291.15</td> <td>-</td> <td>0.0</td> <td>0.280</td> </tr> <tr> <td></td> <td>1.049</td> <td>0.226</td> <td>0.250</td> </tr> </tbody> </table> <p>The solubility in water was interpolated from the author's data from reference (1).</p> <p>The mercury (II) chloride molality was calculated by the Editor from data taken from the International Critical Tables, Vol. III.</p> <p>The author reported his solubility values as an Absorption Coefficient = (Concentration of Rn in the liquid phase)/(Concentration in the gas phase). We have labelled it as an Ostwald coefficient. The solubility was measured at a radon partial pressure of less than 0.1 kPa at equilibrium. The liquid was also saturated with air as a carrier gas at a pressure of about 100 kPa.</p>		T/K	Specific Gravity	Mercury (II) Chloride mol kg <sup>-1</sup> H <sub>2</sub> O	Ostwald Coefficient L	291.15	-	0.0	0.280		1.049	0.226	0.250
T/K	Specific Gravity	Mercury (II) Chloride mol kg <sup>-1</sup> H <sub>2</sub> O	Ostwald Coefficient L										
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<p>AUXILIARY INFORMATION</p>													
<p>METHOD:</p> <p>Measurement of radioactivity in the liquid and gaseous phases. Described by Kofler (1,2), who gave a diagram.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>Not specified</p>												
<p>APPARATUS/PROCEDURE:</p> <p>The apparatus consisted of two glass bulbs connected by a tap. Each bulb had a separate tap. The assembly is shaken. Radioactivity is measured by an aluminum leaf electroscope.</p>	<p>ESTIMATED ERROR:</p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>Kofler, M. <u>Sitzungsber. Akad. Wiss. Wien, Abt. 2A</u> 1912, <u>121</u>, 2169.</li> <li>Kofler, M. <u>Monatsh.</u> 1913, <u>34</u>, 389.</li> </ol>												

<b>COMPONENTS:</b> 1. Radon; $^{222}_{86}\text{Rn}$ ; 14859-67-7 2. Water; $\text{H}_2\text{O}$ ; 7732-18-5 3. Lead Nitrate; $\text{Pb}(\text{NO}_3)_2$ ; 10099-74-8	<b>ORIGINAL MEASUREMENTS:</b> Kofler, M.  <u>Physik. Z.</u> 1908, <u>9</u> , 6-8																
<b>VARIABLES:</b> T/K: 291.15 Specific Gravity: 1.237 - 1.283	<b>PREPARED BY:</b> W. Gerrard																
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="381 498 1007 703"> <thead> <tr> <th>T/K</th> <th>Specific Gravity</th> <th>Lead nitrate mol kg<sup>-1</sup> H<sub>2</sub>O</th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>291.15</td> <td>-</td> <td>0.0</td> <td>0.280</td> </tr> <tr> <td></td> <td>1.237</td> <td>0.889</td> <td>0.166</td> </tr> <tr> <td></td> <td>1.283</td> <td>1.081</td> <td>0.143</td> </tr> </tbody> </table> <p>The solubility in water was interpolated from the author's data from reference (1).</p> <p>The lead nitrate molalities were calculated by the Editor from data taken from the International Critical Tables, Vol. III.</p> <p>The author reported his solubility values as an Absorption Coefficient = (Concentration of Rn in the liquid phase)/(Concentration in the gas phase). We have labelled it as an Ostwald coefficient. The solubility was measured at a radon partial pressure of less than 0.1 kPa at equilibrium. The liquid was also saturated with air as a carrier gas at a pressure of about 100 kPa.</p>		T/K	Specific Gravity	Lead nitrate mol kg <sup>-1</sup> H <sub>2</sub> O	Ostwald Coefficient L	291.15	-	0.0	0.280		1.237	0.889	0.166		1.283	1.081	0.143
T/K	Specific Gravity	Lead nitrate mol kg <sup>-1</sup> H <sub>2</sub> O	Ostwald Coefficient L														
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<b>COMPONENTS:</b> 1. Radon; $^{222}_{86}\text{Rn}$ ; 14859-67-7 2. Water; $\text{H}_2\text{O}$ ; 7732-18-5 3. Ferrous Sulfate; $\text{FeSO}_4$ ; 7720-78-7	<b>ORIGINAL MEASUREMENTS:</b> Kofler, M.  <u>Physik. Z.</u> 1908, <u>9</u> , 6-8.								
<b>VARIABLES:</b> T/K: 291.15 Specific Gravity: 1.226	<b>PREPARED BY:</b> W. Gerrard								
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="295 473 934 646"> <thead> <tr> <th>T/K</th> <th>Specific Gravity</th> <th>Ferrous Sulfate mol kg<sup>-1</sup> H<sub>2</sub>O</th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>291.15</td> <td>- 1.226</td> <td>0.0 1.58</td> <td>0.280 0.081</td> </tr> </tbody> </table> <p>The solubility in water was interpolated from the author's data from reference (1).</p> <p>The ferrous sulfate molality was calculated by the Editor from data taken from the International Critical Tables, Vol. III.</p> <p>The author reported his solubility values as an Absorption Coefficient = (Concentration of Rn in the liquid phase)/(Concentration in the gas phase). We have labelled it as an Ostwald coefficient. The solubility was measured at a radon partial pressure of less than 0.1 kPa at equilibrium. The liquid was also saturated with air as a carrier gas at a pressure of about 100 kPa.</p>		T/K	Specific Gravity	Ferrous Sulfate mol kg <sup>-1</sup> H <sub>2</sub> O	Ostwald Coefficient L	291.15	- 1.226	0.0 1.58	0.280 0.081
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291.15	- 1.226	0.0 1.58	0.280 0.081						
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<p>COMPONENTS:</p> <p>1. Radon; <math>^{222}_{86}\text{Rn}</math>; 14859-67-7</p> <p>2. Water; <math>\text{H}_2\text{O}</math>; 7732-18-5</p> <p>3. Barium Nitrate; <math>\text{Ba}(\text{NO}_3)_2</math>; 10022-31-8</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Kofler, M.</p> <p><u>Sitzungsber. Akad. Wiss. Wien, Math.-Naturwiss. Kl. Abt. 2A</u> 1913, <u>122</u>, 1473 - 1479.</p>																																																																																															
<p>VARIABLES:</p> <p>T/K: 273.45 - 314.55</p> <p>Specific Gravity: 1.006 - 1.0624</p>	<p>PREPARED BY:</p> <p>W. Gerrard</p>																																																																																															
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COMPONENTS: 1. Radon; $^{222}_{86}\text{Rn}$ ; 14859-67-7 2. Water; $\text{H}_2\text{O}$ ; 7732-18-5 3. Sodium Chloride; $\text{NaCl}$ ; 7647-14-5		ORIGINAL MEASUREMENTS: Kofler, M.  Sitzungsber. Akad. Wiss. Wien, <u>Math.-Naturwiss. Kl. Abt. 2A</u> 1913, <u>122</u> , 1473 - 1479.		
VARIABLES: T/K: 273.35 - 290.15  Specific Gravity: 1.008 - 1.215		PREPARED BY: W. Gerrard		
EXPERIMENTAL VALUES:				
NaCl	T/K	Specific* Gravity	Sodium Chloride $\text{mol kg}^{-1} \text{H}_2\text{O}$	Ostwald Coefficient L
	273.35	-	0.0	0.532
	273.65			0.526
	278.95			0.423
	280.35			0.403
	282.95			0.366
	284.65			0.345
	291.15			0.280
	298.35			0.229
	305.35			0.194
	323.65			0.140
	291.15	1.008	0.220	0.239
	273.65	1.009	0.245	0.417
	291.15	1.021	0.542	0.202
	291.15	1.039	1.00	0.163
	291.15	1.0392	1.01	0.163
	273.95	1.071	1.87	0.220
	279.65			0.176
	285.95			0.154
	291.15	1.096	2.59	0.096
*All specific gravity measurements were at 291.15 K except the value 1.145 which was at 289.15 K.				
AUXILIARY INFORMATION				
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<b>COMPONENTS:</b> 1. Radon; $^{222}_{86}\text{Rn}$ ; 14859-67-7 2. Water; $\text{H}_2\text{O}$ ; 7732-18-5 3. Tetrapotassium, (OC-6-11)-hexakis (cyano-C)-Ferrate (4-) (Potassium Ferrocyanide), $\text{K}_4\text{Fe}(\text{CN})_6$ ; 13943-58-3	<b>ORIGINAL MEASUREMENTS:</b> Kofler, M.  <u>Physik. Z.</u> 1908, <u>9</u> , 6-8.												
<b>VARIABLES:</b> T/K: 291.15 Specific Gravity: 1.107	<b>PREPARED BY:</b> W. Gerrard												
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	1.100	2.42	0.114																					
	1.175	4.63	0.061																					
<b>AUXILIARY INFORMATION</b>																								
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<b>COMPONENTS:</b> 1. Radon; $^{222}_{86}\text{Rn}$ ; 14859-67-7 2. Water; $\text{H}_2\text{O}$ ; 7732-18-5 3. Ethanol; $\text{C}_2\text{H}_5\text{OH}$ ; 64-17-5	<b>ORIGINAL MEASUREMENTS:</b> Kofler, M.  <u>Physik. Z.</u> 1908, <u>9</u> , 6-8.																												
<b>VARIABLES:</b> T/K: 291.15  Specific Gravity: 0.800 - 0.977	<b>PREPARED BY:</b> W. Gerrard																												
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="367 512 998 767"> <thead> <tr> <th>T/K</th> <th>Specific Gravity</th> <th>Ethanol Mol Fraction <math>X_3</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>291.15</td> <td>-</td> <td>0.0</td> <td>0.280</td> </tr> <tr> <td></td> <td>0.977</td> <td>0.061</td> <td>0.300</td> </tr> <tr> <td></td> <td>0.944</td> <td>0.182</td> <td>0.436</td> </tr> <tr> <td></td> <td>0.919</td> <td>0.268</td> <td>0.765</td> </tr> <tr> <td></td> <td>0.885</td> <td>0.403</td> <td>1.301</td> </tr> <tr> <td></td> <td>0.800</td> <td>0.928</td> <td>5.606</td> </tr> </tbody> </table> <p data-bbox="148 787 1136 836">The solubility in water was interpolated from the author' data from reference (1).</p> <p data-bbox="148 856 1277 906">The ethanol mole fractions were calculated by the Editor from data taken from the International Critical Tables, Vol. III.</p> <p data-bbox="148 926 1277 1049">The author reported his solubility values as an Absorption Coefficient = (Concentration of Rn in the liquid phase)/(Concentration in the gas phase). We have labelled it as an Ostwald coefficient. The solubility was measured at a radon partial pressure of less than 0.1 kPa at equilibrium. The liquid was also saturated with air as a carrier gas at a pressure of about 100 kPa.</p>		T/K	Specific Gravity	Ethanol Mol Fraction $X_3$	Ostwald Coefficient L	291.15	-	0.0	0.280		0.977	0.061	0.300		0.944	0.182	0.436		0.919	0.268	0.765		0.885	0.403	1.301		0.800	0.928	5.606
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<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Radon; <math>^{222}_{86}\text{Rn}</math>; 14859-67-7</li> <li>Water; <math>\text{H}_2\text{O}</math>; 7732-18-5</li> <li>Sucrose; <math>\text{C}_{12}\text{H}_{22}\text{O}_{11}</math>; 57-50-1</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Kofler, M.</p> <p><u>Physik. Z.</u> 1908, <u>9</u>, 6-8.</p>																
<p>VARIABLES:</p> <p>T/K: 291.15</p> <p>Specific Gravity: 1.082 - 1.214</p>	<p>PREPARED BY:</p> <p>W. Gerrard</p>																
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<b>COMPONENTS:</b> 1. Radon; $^{222}_{86}\text{Rn}$ ; 14859-67-7 2. Water; $\text{H}_2\text{O}$ ; 7732-18-5 3. Urea; $(\text{NH}_2)_2\text{CO}$ ; 57-13-6		<b>ORIGINAL MEASUREMENTS:</b> Kofler, M.  <u>Sitzungsber. Akad. Wiss. Wien, Math.-Naturwiss. Kl. Abt. 2A</u> 1913, <u>122</u> , 1473 - 1479.		
<b>VARIABLES:</b> T/K: 273.95 - 303.65 Specific Gravity: 1.004 - 1.070		<b>PREPARED BY:</b> W. Gerrard		
<b>EXPERIMENTAL VALUES:</b>				
Urea	T/K	Specific* Gravity	Urea mol kg <sup>-1</sup> H <sub>2</sub> O	Ostwald Coefficient L
	273.95	-	0.0	0.519
	278.65			0.429
	286.75			0.322
	298.75			0.227
	306.65			0.188
	289.55	1.004	0.336	0.270
	307.15			0.179
	276.75	1.012	0.862	0.412
	288.95			0.273
	306.65			0.181
	273.95	1.016	1.125	0.439
	288.35			0.273
	305.35			0.187
	273.95	1.029	2.095	0.418
	278.65			0.354
	286.75			0.278
	298.75			0.210
	306.65			0.174
	273.75	1.070	5.850	0.370
	287.95			0.255
	303.65			0.187
*All of the specific gravities were measured at 291.15 K except the value 1.016 which was measured at 290.15 K.				
<b>AUXILIARY INFORMATION</b>				
<b>METHOD:</b> Measurement of radioactivity in the liquid and gaseous phases. Described by Kofler (1,2), who gave a diagram.		<b>SOURCE AND PURITY OF MATERIALS:</b> Not specified		
		<b>DATA CLASS:</b>		
<b>APPARATUS/PROCEDURE:</b> The apparatus consisted of two glass bulbs connected by a tap. Each bulb had a separate tap. The assembly is shaken. Radioactivity is measured by an aluminum leaf electroscope.  The comments on water solubility, molality, and absorption coefficient on the other Kofler data sheets apply.		<b>ESTIMATED ERROR:</b>		
		<b>REFERENCES:</b> 1. Kofler, M. <u>Sitzungsber. Akad. Wiss. Wien, Abt. 2A</u> 1912, <u>121</u> , 2169. 2. Kofler, M. <u>Monatsh.</u> 1913, <u>34</u> , 389.		

<p>COMPONENTS:</p> <p>1. Radon; <math>^{222}_{86}\text{Rn}</math>; 14859-67-7</p> <p>2. Non-aqueous Liquids</p>	<p>EVALUATOR:</p> <p>William Gerrard Department of Chemistry The Polytechnic of North London Holloway, London N7 8DB U. K.</p> <p>May 1977</p>
<p>CRITICAL EVALUATION: PREAMBLE</p> <p>The determination of the solubility of radon in liquids is based on a technique so different from those used for other gases that a special explanation is required. In the gaseous phase, the concentration of radon is absolutely small, the partial pressure of radon being less than 0.1 kPa at equilibrium. Furthermore, it is present in a carrier gas (nitrogen or air), the initial pressure of the carrier gas being about 100 kPa. The liquid is therefore saturated with the carrier gas at the equilibrium partial pressure of that gas. The concentration of radon in the gaseous phase, and that in the liquid phase are separately determined by the measurement of gamma-ray emission by means of an electroscopes, a condenser, or a sodium iodide scintillation counter. Up to 1910, the electroscopes technique was primitive, and apparently not reliable. In 1911, Boyle (1) described the procedure of holding the vessel containing one of the phases near enough to the electroscopes to cause an effective ionization which could be compared with that produced by a standard amount of radium. Ramstedt (2) put the vessel into a condenser. Nussbaum and Hursh (3) however, used a sodium iodide scintillation counter.</p> <p>The primary results were presented as the equivalent of a ratio of concentrations: concentration in the liquid phase/concentration in the gaseous phase; and this ratio was called the "absorption coefficient." It was actually stated, or tacitly assumed, that Henry's law was "obeyed," and that this ratio was independent of pressure. The ratio of concentrations was assumed to be equal to the volume of radon absorbed by an equal volume of the liquid phase, i.e. in effect the Ostwald absorption coefficient; but with the implication that the partial pressure of radon was 101.325 kPa. Nussbaum and Hursh (3), for example, used nitrogen containing a concentration of radon equivalent to <math>1\mu\text{C per dm}^3</math> of nitrogen. The radioactivity was assayed by counting the gamma-rays emitted by the short-lived decay products in radioactive equilibrium with radon. The ratio: (net counts per min./<math>\text{cm}^3</math> of the original liquid)/(net counts per min./<math>\text{cm}^3</math> of gas) was called the Ostwald solubility coefficient, and given the symbol <math>\alpha'</math>. It must be emphasized that this ratio is pinned to a very small partial pressure of radon.</p> <p>For the comparison of solubilities on a molecular basis, the absorption coefficients in their primary form may not be used; they must be converted into mole ratios and mole fractions. The main purpose in doing this conversion is to check the primary data by means of the reference line procedure described by Gerrard (4), and to make easier the comparison of radon solubility values with the solubility values of other gases. The following statements indicate the basis of the conversion.</p> <ol style="list-style-type: none"> <li>1. The Ostwald coefficient is independent of pressure. In principle this is not valid; although deviations may be neglected in certain specific examples, they may not be in others.</li> <li>2. The gram-mole volume of radon is taken to be <math>22,290 \text{ cm}^3</math> at <math>273.15/\text{K}</math> and a pressure, <math>p_{\text{Rn}}</math>, of 101.325 kPa. The gram-mole volume for other temperatures is given by <math>22,290 \times T/273.15</math></li> <li>3. The density, <math>\rho_S</math>, of the liquid, S, is that for the temperature of observation of the primary data.</li> <li>4. The molecular weight of the liquid, S, is taken to be the simplest formula weight, e.g. <math>\text{C}_2\text{H}_5\text{OH}</math> (46.07) and <math>\text{CH}_3\text{CO}_2\text{H}</math> (60.05).</li> <li>5. The mole ratio is given by: (absorption coefficient/gram-mole volume) <math>\times (M_S/\rho_S)</math> where <math>M_S</math> is the molecular weight, and <math>\rho_S</math> is the density of S. The mole fraction <math>X_{\text{gas}}</math> obtained by (mole ratio)/(1 + mole ratio).</li> </ol>	





<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>1. Radon; <math>^{222}_{86}\text{Rn}</math>; 14859-67-7</li> <li>2. Non-aqueous Liquids</li> </ol>	<p>EVALUATOR:</p> <p>William Gerrard  Department of Chemistry  The Polytechnic of North London  Holloway, London N7 8DB  U. K.</p>
<p>CRITICAL EVALUATION:</p>	<p>REFERENCES</p> <ol style="list-style-type: none"> <li>1. Boyle, R.W. <u>Phil. Mag.</u> 1911, <u>22</u>, 840.</li> <li>2. Ramstedt, E. <u>Le Radium</u> 1911, <u>8</u>, 253.</li> <li>3. Nussbaum, E.; Hursh, J.B. <u>J. Phys. Chem.</u> 1958, <u>62</u>, 81.</li> <li>4. Gerrard, W. <u>Solubility of Gases and Liquids - A Graphic Approach</u>, Plenum, New York, 1976.</li> <li>5. Hofbauer, G. <u>Sitzungsber. Akad. Wiss. Wien, Abt. 2A</u>, 1914, <u>123</u> 2001.</li> <li>6. Lurie, A. Thesis, University of Grenoble, 1910.</li> <li>7. Traubenberg, H.F.R. <u>Phys. Z.</u> 1904, <u>5</u>, 130.</li> <li>8. Schulze, A. <u>Z. Phys. Chem.</u>, 1920, <u>95</u>, 257.</li> <li>9. Swinne, R. <u>Z. Phys. Chem.</u>, 1913, <u>84</u>, 348.</li> <li>10. Semenchenko, V.K. and Shakhparanov, M.I. <u>Zh. Fiz. Khim.</u>, 1948, <u>22</u>, 243.</li> <li>11. Szeparowicz, M. <u>Sitzungsber. Akad. Wiss. Wien Abt IIa</u>, 1920, <u>129</u>, 437.</li> <li>12. Gavrilova, E.N. <u>Trudy Vses. Nauch. Issles. Inst. Metro</u>, 1939, <u>26</u>, 39.</li> <li>13. Onum, N. <u>Bunseki Kagaku</u>, 1967, <u>16</u>, 274.</li> <li>14. Krestov, G.A. and Nedel'ko, B.E. <u>Tr. Ivanov. Khim. Tekhnol. Inst.</u>, 1972, <u>32</u>, 102.</li> </ol>

<b>COMPONENTS:</b> 1. Radon; $^{222}_{86}\text{Rn}$ ; 14859-67-7 2. Hexane; $\text{C}_6\text{H}_{14}$ ; 110-54-3	<b>ORIGINAL MEASUREMENTS:</b> Ramstedt, E.  <u>Le Radium</u> 1911, 8, 253 - 256.																														
<b>VARIABLES:</b> T/K: 255.15 - 291.15	<b>PREPARED BY:</b> W. Gerrard May 1977																														
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="436 493 979 648" style="margin: 10px auto;"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^2</math></th> <th>Ostwald Coefficient</th> </tr> </thead> <tbody> <tr> <td>255.15</td> <td>17.4</td> <td>35.2</td> </tr> <tr> <td>273.15</td> <td>11.8</td> <td>23.4</td> </tr> <tr> <td>291.15</td> <td>8.32</td> <td>16.56</td> </tr> </tbody> </table> <p>The Ostwald coefficient was measured at a radon partial pressure of less than 0.1 kPa at equilibrium. The radon was present in a carrier gas (air or nitrogen) at an initial pressure of about 101 kPa.</p> <p>The mole fraction solubility was calculated by the compiler. It was assumed that the Ostwald coefficient was independent of pressure and that the gram-mole volume of radon is 22,290 cm<sup>3</sup> at 273.15 K and 101.325 kPa.</p> <p>Smoothed Data: <math>\Delta G^\circ/\text{J mol}^{-1} = -RT \ln X_1 = -12,662 + 64.151 T</math>            Std. Dev. <math>\Delta G = 6</math>, Coef. Corr. = 0.9999  <math>\Delta H^\circ/\text{J mol}^{-1} = -12,662</math>, <math>\Delta S^\circ/\text{J K}^{-1}\text{mol}^{-1} = -64.151</math></p> <table border="1" data-bbox="467 978 1007 1168" style="margin: 10px auto;"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X \times 10^2</math></th> <th><math>\Delta G^\circ/\text{J mol}^{-1}</math></th> </tr> </thead> <tbody> <tr> <td>258.15</td> <td>16.3</td> <td>3,898.5</td> </tr> <tr> <td>268.15</td> <td>13.1</td> <td>4,540.0</td> </tr> <tr> <td>278.15</td> <td>10.6</td> <td>5,181.5</td> </tr> <tr> <td>288.15</td> <td>8.80</td> <td>5,823.0</td> </tr> <tr> <td>298.15</td> <td>7.37</td> <td>6,463.0</td> </tr> </tbody> </table> <p>The smoothed data fit was added by the Volume Editor.</p>		T/K	Mol Fraction $X_1 \times 10^2$	Ostwald Coefficient	255.15	17.4	35.2	273.15	11.8	23.4	291.15	8.32	16.56	T/K	Mol Fraction $X \times 10^2$	$\Delta G^\circ/\text{J mol}^{-1}$	258.15	16.3	3,898.5	268.15	13.1	4,540.0	278.15	10.6	5,181.5	288.15	8.80	5,823.0	298.15	7.37	6,463.0
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<b>APPARATUS/PROCEDURE:</b> Two tube connected by a wide tap. To determine concentration of radon, each tube is placed in a condenser.	<b>ESTIMATED ERROR:</b>  <b>REFERENCES:</b>																														

COMPONENTS: 1. Radon; $^{222}_{86}\text{Rn}$ ; 14859-67-7 2. Cyclohexane; $\text{C}_6\text{H}_{12}$ ; 110-82-7	ORIGINAL MEASUREMENTS: Ramstedt, E.  <u>Le Radium</u> 1911, <u>8</u> , 253-256.						
VARIABLES: T/K: 291.15	PREPARED BY:  W. Gerrard						
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291.15	7.59	18.04					
AUXILIARY INFORMATION							
METHOD: Measurement of radioactivity in the liquid and in the gaseous phase.	SOURCE AND PURITY OF MATERIALS: 1. Radon. 2. Cyclohexane. Dried and distilled, b.p. 80°C.						
APPARATUS/PROCEDURE:  Two tubes connected by a wide tap. To determine concentration of radon, each tube is placed in a condenser.	ESTIMATED ERROR:  REFERENCES:						

<p>COMPONENTS:</p> <p>1. Radon; <math>^{222}_{86}\text{Rn}</math>; 14859-67-7</p> <p>2. Benzene; <math>\text{C}_6\text{H}_6</math>; 71-43-2</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Ramstedt, E.</p> <p><u>Le Radium</u> 1911, <u>8</u>, 253-256.</p>																											
<p>VARIABLES:</p> <p>T/K: 276.15 - 291.15</p>	<p>PREPARED BY:</p> <p>W. Gerrard</p>																											
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## CRITICAL EVALUATION:

The solubility of radon-222 in methylbenzene is reported by four laboratories. Hofman (1) reports radon solubilities at 194.15 and 293.15 K, Lurie (2) at 293.15 K, Boyle (3) at 287.15 K and Ramstedt (4) at 255.15, 273.15 and 291.15 K.

The Hofman value at 194.15 K should be used with caution. If the Ostwald coefficient at 194.15 K and an approximate radon pressure of 0.1 kPa has the same value at 101.325 kPa the mole fraction solubility is 0.258 at 101.325 kPa radon pressure. However, the normal boiling point of radon is 211.4 K and thus the mole fraction solubility must, in effect, be unity at 194.15 K and 101.325 kPa.

The Hofman and the Lurie Ostwald coefficients at 293.15 K agree well but appear to be too small.

The Ostwald coefficient values of Ramstedt are probably the best available, but they are classed as tentative. The Ramstedt data, smoothed by a linear regression of a Gibbs energy equation linear in temperature, are 3.3 per cent higher than the Boyle value at 287.15 K and about 8 per cent higher than the Hofman and the Lurie values at 293.15 K.

The tentative values of the thermodynamic properties of solution for the transfer of one mole of radon from the gas at 101.325 kPa to the hypothetical unit mole fraction solution are

$$\Delta G^\circ/\text{J mol}^{-1} = -RT \ln X_1 = -12,673 + 67.505 T$$

$$\text{Std. Dev. } \Delta G^\circ = 2.8, \text{ Coef. corr.} = 0.9999$$

$$\Delta H^\circ/\text{J mol}^{-1} = -12,673, \Delta S^\circ/\text{J K}^{-1} \text{ mol}^{-1} = -67.505$$

A table of tentative mole fraction solubility and Gibbs energy values as a function of temperature appears on the Ramstedt data sheet, and below.

## REFERENCES

- Hofman, R. Phys. Z. 1905, 6, 339.
- Lurie, A. Thesis 1910, University of Grenoble.
- Boyle, R. W. Phil. Mag. 1911, 22, 840.
- Ramstedt, E. Le Radium 1911, 8, 253.

TABLE 1. The solubility of radon-222 in methylbenzene. The tentative mole fraction solubility of radon at a partial pressure of 101.325 kPa (1 atm), and the Gibbs energy change as a function of temperature.

T/K	Mol Fraction $X_1 \times 10^2$	$\Delta G^\circ/\text{J mol}^{-1}$
258.15	10.92	4,752.5
263.15	9.76	5,090.0
268.15	8.76	5,427.5
273.15	7.90	5,765.1
278.15	7.14	6,102.6
283.15	6.49	6,440.1
288.15	5.91	6,777.6
293.15	5.40	7,116.1
298.15	4.95	7,453.6

<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Radon-222; <math>^{222}_{86}\text{Rn}</math>; 14859-67-7</li> <li>Methylbenzene (Toluene); <math>\text{C}_7\text{H}_8</math>;</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Hofmann, R.</p> <p><u>Phys. Z.</u> 1905, <u>6</u>, 339-340.</p>						
<p>VARIABLES:</p> <p>T/K: 194.15 - 293.15</p>	<p>PREPARED BY:</p> <p>W. Gerrard</p>						
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="587 479 867 632"> <thead> <tr> <th>T/K</th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>194.15</td> <td>66.69</td> </tr> <tr> <td>293.15</td> <td>11.79</td> </tr> </tbody> </table> <p>The author reported an Absorption coefficient which appears equivalent to the Ostwald coefficient. The coefficient was measured at a radon-222 partial pressure of less than 0.1 kPa at equilibrium. The radon was present in a carrier gas (air or nitrogen) at an initial pressure of about 101 kPa.</p>		T/K	Ostwald Coefficient L	194.15	66.69	293.15	11.79
T/K	Ostwald Coefficient L						
194.15	66.69						
293.15	11.79						
<p>AUXILIARY INFORMATION</p>							
<p>METHOD:</p> <p>Determination of concentration of radon in the gas and liquid phases by means of radioactivity.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>No specific information.</p>						
<p>APPARATUS/PROCEDURE:</p> <p>Electroscope, and glass containers for measurement of radioactivity.</p>	<p>ESTIMATED ERROR:</p> <p>Of doubtful accuracy because of the primitive electroscope technique.</p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>Trautenberg, H.F.R. <u>Phys. Z.</u> 1904, <u>5</u>, 130.</li> </ol>						

<b>COMPONENTS:</b> 1. Radon-222; $^{222}_{86}\text{Rn}$ ; 14859-67-7 2. Methylbenzene (Toluene); $\text{C}_7\text{H}_8$ ; 108-88-3	<b>ORIGINAL MEASUREMENTS:</b> Lurie, A. Thesis University of Grenoble, 1910 Microfilm available. See also Tables annuelles de constantes et donnees numeriques de chimie, de physique et de technologie 1913 (for 1911), 2, 401.						
<b>VARIABLES:</b>  T/K: 293.15	<b>PREPARED BY:</b> W. Gerrard						
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="413 465 897 588" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">T/K</th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Mol Fraction <math>x_1 \times 10^2</math></th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td style="border-bottom: 1px solid black;">293.15</td> <td style="border-bottom: 1px solid black;">4.97</td> <td style="border-bottom: 1px solid black;">11.76</td> </tr> </tbody> </table> <p data-bbox="95 608 1159 703">The author reported a coefficient of absorption, <math>\alpha</math>, which appears to have the same meaning as the ratio of concentrations: concentration of radon in the liquid/concentration of radon in the gas. The coefficient of absorption has been labelled as the Ostwald coefficient.</p> <p data-bbox="95 727 1159 801">The coefficient of absorption was measured at a radon partial pressure of less than 0.1 kPa at equilibrium. The radon was present in a carrier gas (air or nitrogen) at an initial pressure of about 101 kPa.</p> <p data-bbox="95 825 1186 920">The mole fraction solubility at 101.325 kPa was calculated by the compiler. It was assumed that the Ostwald coefficient was independent of pressure and that the gram-mole volume of radon is 22,290 <math>\text{cm}^3</math> at 273.15 K and 101.325 kPa.</p>		T/K	Mol Fraction $x_1 \times 10^2$	Ostwald Coefficient L	293.15	4.97	11.76
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<p>VARIABLES:</p> <p>T/K: 287.15</p>	<p>PREPARED BY:</p> <p>W. Gerrard</p>						
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<p>METHOD:</p> <p>Radon-222 in a carrier gas (air, or other gas not specified) is shaken with a measured volume of liquid.</p> <p>Radioactivity is determined in the gas and liquid phases by gamma-ray electroscope.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>Radon-222</li> <li>Methylbenzene (Toluene).</li> </ol>						
<p>APPARATUS/PROCEDURE:</p> <p>The sampling bulb and mixing bulb are connected by a three-way tap. For the measurement of radioactivity, the bulbs are separately placed near to the electroscope. A diagram is given by Boyle.</p>	<p>ESTIMATED ERROR:</p> <p><math>\delta T/K = 0.2</math>  <math>\delta L/L = 0.03</math></p> <p>REFERENCES:</p>						



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<b>METHOD /APPARATUS/PROCEDURE:</b> The concentration of radon in the gas and liquid phases determined by measurements of radioactivity. An aluminum foil electroscopes was used to measure the radioactivity. Diagrams given by Lurie.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Radon 2. Dimethylbenzene. Purity of liquid not specified. Mixture of isomers. 1,3-Dimethylbenzene 40 - 48%, 1,2-dimethylbenzene 20 - 24%, 1,4-dimethylbenzene 16 - 20%, and ethylbenzene 10 - 15%.  <b>ESTIMATED ERROR:</b>  <b>REFERENCES:</b>																					

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<p>VARIABLES:</p> <p>T/K: 276.95 - 302.75</p>	<p>PREPARED BY:</p> <p>W. Gerrard</p>																														
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="477 493 961 638"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^2</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>276.95</td> <td>1.32</td> <td>7.43</td> </tr> <tr> <td>289.35</td> <td>0.980</td> <td>5.71</td> </tr> <tr> <td>302.75</td> <td></td> <td>(5.37)*</td> </tr> </tbody> </table> <p>*Operational defect.</p> <p>The author reported a coefficient of solubility, <math>\alpha'</math>, based on the radon concentration ratio in the liquid and gaseous phases at equilibrium by radioactivity. The coefficient of solubility is labelled an Ostwald coefficient above. It was measured at a radon partial pressure of probably less than 0.1 kPa at equilibrium. The liquid was also saturated with air as a carrier gas at an initial pressure of about 100 kPa.</p> <p>The mole fraction solubility was calculated by the compiler. It was assumed that the Ostwald coefficient was independent of pressure and that the gram-mole volume of radon is 22,290 <math>\text{cm}^3</math> at 273.15 K and 101.325 kPa.</p> <p>Smoothed Data: <math>\Delta G^\circ/\text{J mol}^{-1} = -RT \ln X_1 = -16,003 + 93.764 T</math>  <math>\Delta H^\circ/\text{J mol}^{-1} = -16,003</math>, <math>\Delta S^\circ/\text{J K}^{-1} \text{ mol}^{-1} = -93.764</math></p> <table border="1" data-bbox="491 980 975 1178"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^2</math></th> <th><math>\Delta G^\circ/\text{J mol}^{-1}</math></th> </tr> </thead> <tbody> <tr> <td>273.15</td> <td>1.45</td> <td>9,608</td> </tr> <tr> <td>278.15</td> <td>1.28</td> <td>10,077</td> </tr> <tr> <td>283.15</td> <td>1.13</td> <td>10,546</td> </tr> <tr> <td>288.15</td> <td>1.01</td> <td>11,014</td> </tr> <tr> <td>293.15</td> <td>0.90</td> <td>11,484</td> </tr> </tbody> </table> <p>The smoothed data fit was added by the Volume Editor.</p>		T/K	Mol Fraction $X_1 \times 10^2$	Ostwald Coefficient L	276.95	1.32	7.43	289.35	0.980	5.71	302.75		(5.37)*	T/K	Mol Fraction $X_1 \times 10^2$	$\Delta G^\circ/\text{J mol}^{-1}$	273.15	1.45	9,608	278.15	1.28	10,077	283.15	1.13	10,546	288.15	1.01	11,014	293.15	0.90	11,484
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## COMPONENTS:

1. Radon-222;  $^{222}_{86}\text{Rn}$ ; 14859-67-7
2. Ethanol;  $\text{C}_2\text{H}_6\text{O}$ ; 64-17-5

## EVALUATOR:

H. L. Clever  
 Chemistry Department  
 Emory University  
 Atlanta, GA 30322  
 U.S.A.

August 1978

## CRITICAL EVALUATION:

Four laboratories report the solubility of radon-222 in ethanol. Trautenberg (1) reports a solubility relative to water at room temperature, Boyle (2) reports an Ostwald coefficient at 287.15 K, Ramstedt (3) reports Ostwald coefficients at 255.15, 273.15 and 291.15 K, and Hofbauer (4) reports four Ostwald coefficients between 275.15 and 310.95 K.

In the experience of the evaluator both Boyle's and Ramstedt's data are usually more reliable than Hofbauer's data. For the radon + ethanol system Hofbauer's solubility values are a consistent 15.0 to 16.5 percent higher than Ramstedt's values over the temperature range of common measurement of 273.15 to 298.15 K. For this system Boyle's single value agrees better with the Hofbauer data than the Ramstedt data. Although the evidence is conflicting, the evaluator prefers the Ramstedt data.

The tentative values of the thermodynamic changes for the transfer of one mole of radon from the gas at 101.325 kPa (1 atm) to the hypothetical unit mole fraction solution are the values from the Ramstedt data:

$$\Delta G^{\circ}/\text{J mol}^{-1} = -RT \ln X_1 = -11,900 + 75.819 T$$

$$\text{Std. Dev. } \Delta G^{\circ} = 12.9, \text{ Coef. Corr.} = 0.9998$$

$$\Delta H^{\circ}/\text{J mol}^{-1} = -11,900, \Delta S^{\circ}/\text{J K}^{-1} \text{ mol}^{-1} = -75.819$$

A table of tentative mole fraction solubility and Gibbs energy values as a function of temperature at 5 degree interval between 258.15 and 298.15 K appears on the radon + ethanol data sheet of Ramstedt, and below.

## REFERENCES

1. Trautenberg, H. F. R. Phys. Z. 1904, 5, 130.
2. Boyle, R. W. Phil. Mag. 1911, 22, 840.
3. Ramstedt, E. Le Radium 1911, 8, 253.
4. Hofbauer, G. Sitzungsber. Akad. Wiss. Wien. Math. Naturwiss. Kl. Abt. 2A 1914, 123, 2001.

TABLE 1. The solubility of radon-222 in ethanol. The tentative mole fraction solubility of radon at a partial pressure of 101.325 kPa (1 atm), and the Gibbs energy change on solution as a function of temperature.

T/K	Mol Fraction $X_1 \times 10^2$	$\Delta G^{\circ}/\text{J mol}^{-1}$
258.15	2.80	7,673.0
263.15	2.52	8,052.1
268.15	2.28	8,431.2
273.15	2.07	8,810.3
278.15	1.88	9,189.4
283.15	1.72	9,568.4
288.15	1.57	9,947.5
293.15	1.44	10,326
298.15	1.33	10,705

<b>COMPONENTS:</b> 1. Radon-222; $^{222}_{86}\text{Rn}$ ; 14859-67-7 2. Ethanol; $\text{C}_2\text{H}_6\text{O}$ ; 64-17-5	<b>ORIGINAL MEASUREMENTS:</b> Traubenberg, H.F.R. Phys. Z. 1904, <u>5</u> , 130 - 134.						
<b>VARIABLES:</b>	<b>PREPARED BY:</b> W. Gerrard						
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<b>AUXILIARY INFORMATION</b>							
<b>METHOD:</b> Measurement of radioactivity.	<b>SOURCE AND PURITY OF MATERIALS:</b> Not stated.						
<b>APPARATUS/PROCEDURE:</b> Electroscope for measurement of radioactivity.	<b>ESTIMATED ERROR:</b> Traubenberg's values appear to be low when compared with values reported by other workers. <b>REFERENCES:</b>						

<b>COMPONENTS:</b> 1. Radon-222; $^{222}_{86}\text{Rn}$ ; 14859-67-7 2. Ethanol; $\text{C}_2\text{H}_6\text{O}$ ; 64-17-5	<b>ORIGINAL MEASUREMENTS:</b> Boyle, R. W.  <u>Phil. Mag.</u> 1911, <u>22</u> , 840- 854.						
<b>VARIABLES:</b> T/K: 287.15	<b>PREPARED BY:</b> W. Gerrard						
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<b>AUXILIARY INFORMATION</b>							
<b>METHOD:</b> Radon-222 in a carrier gas (air, or other gas not specified) is shaken with a measured volume of liquid.  Radioactivity is determined in the gas and liquid phases by gamma-ray electroscope.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Radon-222. 2. Ethanol. Density at 287.15 K is 0.796 $\text{g cm}^{-3}$ .						
<b>APPARATUS/PROCEDURE:</b> The sampling bulb and mixing bulb are connected by a three-way tap. For the measurement of radioactivity, the bulbs are separately placed near to the electroscope. A diagram is given by Boyle.	<b>ESTIMATED ERROR:</b> $\delta T/K = 0.2$ $\delta L/L = 0.03$  <b>REFERENCES:</b>						

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<p>VARIABLES:</p> <p>T/K: 286.75 - 303.35</p>	<p>PREPARED BY:</p> <p>W. Gerrard</p>									
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<p>METHOD/APPARATUS/PROCEDURE:</p> <p>The concentration of radon in the gas and liquid phases determined by measurements of radioactivity. An aluminum foil electroscope was used to measure the radioactivity. Diagrams given by Lurie.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>Radon.</li> <li>1-Pentanol (Amyl Alcohol). Purity of liquid not specified.</li> </ol> <p>ESTIMATED ERROR:</p> <p>REFERENCES:</p>						



<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Radon-222; <math>^{222}_{86}\text{Rn}</math>; 14859-67-7</li> <li>1-Pentanol (Amyl Alcohol); <math>\text{C}_6\text{H}_{12}\text{O}</math>; 71-41-0</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Boyle, R.W.</p> <p><u>Phil. Mag.</u> 1911, <u>22</u>, 840-854.</p>						
<p>VARIABLES:</p> <p>T/K: 287.15</p>	<p>PREPARED BY:</p> <p>W. Gerrard</p>						
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="459 485 946 610"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^2</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>287.15</td> <td>4.11</td> <td>9.31</td> </tr> </tbody> </table> <p>Boyle defined the coefficient of solubility, <math>s</math>, as <math>(e_1/V_1)/(e_2/V_2)</math> where <math>e_1</math> is emanation in volume <math>V_1</math> of liquid, and <math>e_2</math> is emanation in volume <math>V_2</math> of gas. The partial pressure of radon is less than 0.1 kPa. The liquid is also saturated with carrier gas (air or another gas) at the prevailing pressure, originally about 101 kPa.</p> <p>The mole fraction solubility at 101.325 kPa (1 atm) was calculated by the compiler. It was assumed that the Ostwald coefficient was independent of pressure and that the gram-mole volume of radon is 22,290 <math>\text{cm}^3</math> at 273.15 K and 101.325 kPa.</p>		T/K	Mol Fraction $X_1 \times 10^2$	Ostwald Coefficient L	287.15	4.11	9.31
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<p>AUXILIARY INFORMATION</p>							
<p>METHOD:</p> <p>Radon-222 in a carrier gas (air, or other gas not specified) is shaken with a measured volume of liquid.</p> <p>Radioactivity is determined in the gas and liquid phases by gamma-ray electroscope.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <ol style="list-style-type: none"> <li>Radon-222.</li> <li>1-Pentanol (Amyl Alcohol).</li> </ol>						
<p>APPARATUS/PROCEDURE:</p> <p>The sampling bulb and mixing bulb are connected by a three-way tap. For the measurement of radioactivity, the bulbs are separately placed near to the electroscope. A diagram is given by Boyle.</p>	<p>ESTIMATED ERROR:</p> <p><math>\delta T/K = 0.2</math> <math>\delta L/L = 0.03</math></p> <p>REFERENCES:</p>						

COMPONENTS: 1. Radon; $^{222}_{86}\text{Rn}$ ; 14859-67-7 2. 1,2,3-Propanetriol (Glycerol); $\text{C}_3\text{H}_8\text{O}_3$ ; 56-81-5	ORIGINAL MEASUREMENTS: Ramstedt, E.  <u>Le Radium</u> 1911, <u>8</u> , 253-256.						
VARIABLES: T/K: 291.15	PREPARED BY:  W. Gerrard						
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<b>COMPONENTS:</b> 1. Radon-222; $^{222}_{86}\text{Rn}$ ; 14859-67-7 2. 1,2,3-Propanetriol (Glycerol); $\text{C}_3\text{H}_8\text{O}_3$ ; 56-81-5	<b>ORIGINAL MEASUREMENTS:</b> Lurie, A. Thesis University of Grenoble, 1910 Microfilm available. See also Tables annuelles de constantes et donnees numeriques de chimie, de physique et de technologie 1913 (for 1911), 2, 401.										
<b>VARIABLES:</b> T/K: 276.15 - 323.15	<b>PREPARED BY:</b> W. Gerrard May 1977										
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="557 485 837 677" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">T/K</th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>276.15</td> <td>2.87</td> </tr> <tr> <td>291.15</td> <td>1.7</td> </tr> <tr> <td>303.15</td> <td>0.6</td> </tr> <tr> <td style="border-bottom: 1px solid black;">323.15</td> <td style="border-bottom: 1px solid black;">0.09</td> </tr> </tbody> </table> <p>The author reported a coefficient of absorption, <math>\alpha</math>, which appears to have the same meaning as the ratio of concentrations: concentration of radon in the liquid/concentration of radon in the gas. The coefficient of absorption has been labelled as the Ostwald coefficient.</p> <p>The coefficient of absorption was measured at a radon partial pressure of less than 0.1 kPa at equilibrium. The radon was present in a carrier gas (air or nitrogen) at an initial pressure of about 101 kPa.</p>		T/K	Ostwald Coefficient L	276.15	2.87	291.15	1.7	303.15	0.6	323.15	0.09
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<b>COMPONENTS:</b> 1. Radon; $^{222}_{86}\text{Rn}$ ; 14859-67-7 2. Formic Acid; $\text{CH}_2\text{O}_2$ ; 64-18-6	<b>ORIGINAL MEASUREMENTS:</b> Nussbaum, E.; Hursh, J. B.  J. Phys. Chem. 1958, 62, 81 - 84.																																	
<b>VARIABLES:</b> T/K: 298.15 - ,323.15	<b>PREPARED BY:</b> W. Gerrard																																	
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<b>METHOD:</b> The concentration of radon was determined by measurement of radioactivity in sample withdrawn from the liquid and from the gas phases. The procedure was stated to be similar in principle to that of Boyle (1).	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Radon. 2. Formic acid. Eastman Chemical Co. Highest grade.																																	
<b>APPARATUS/PROCEDURE:</b> A cylindrical glass vessel with a stopcock at each end. The gamma-rays emitted were estimated by a sodium iodide scintillation counter.	<b>ESTIMATED ERROR:</b>  <b>REFERENCES:</b> 1. Boyle, R. W. Phil. Mag. 1911, 22, 840.																																	

## COMPONENTS:

1. Radon-222;  $^{222}_{86}\text{Rn}$ ; 14859-67-7
2. Acetic Acid;  $\text{C}_2\text{H}_4\text{O}_2$ ; 64-19-7

## EVALUATOR:

H. L. Clever  
Chemistry Department  
Emory University  
Atlanta, GA 30322  
U.S.A.

August 1978

## CRITICAL EVALUATION:

Hofbauer (1) reported four values of the solubility of radon-222 in acetic acid between 290.65 and 300.25 K, and Nussbaum and Hursh (2) reported three values between 298.15 and 323.15 K. The two smoothed data sets differ by 9-10 percent over the five degree range of common measurement, with the Hofbauer data having the higher values.

The agreement between the two data sets is marginal but within reason, when one considers the 0.1 kPa pressure of the gas in the measurement and the adjustment to the 101.325 kPa pressure for the mole fraction calculation. The two data sets were combined with a weight of 1 to Hofbauer data and a weight of 2 to the Nussbaum and Hursh data in a linear regression of a Gibbs energy equation linear in temperature. The result gives the tentative values for the transfer of one mole of radon from the gas at a partial pressure of 101.325 kPa to the hypothetical unit mole fraction solution of

$$\Delta G^\circ/\text{J mol}^{-1} = -RT \ln X_1 = -12,805 + 80.750 T$$

$$\text{Std. Dev. } \Delta G^\circ = 121, \text{ Coef. corr.} = 0.9916$$

$$\Delta H^\circ/\text{J mol}^{-1} = -12,805, \Delta S^\circ/\text{J K}^{-1} \text{ mol}^{-1} = -80.750$$

The tentative solubility and Gibbs energy values as a function of temperature are in Table 1.

TABLE 1. The solubility of radon-222 in acetic acid. Tentative values of the mole fraction solubility at 101.325 kPa and the Gibbs energy changes as a function of temperature.

T/K	Mol Fraction $X_1 \times 10^2$	$\Delta G^\circ/\text{J mol}^{-1}$
288.15	1.270*	10,462
293.15	1.160*	10,866
298.15	1.060*	11,270
303.15	0.974	11,674
308.15	0.897	12,077
313.15	0.828	12,481
318.15	0.767	12,885
323.15	0.711	13,289

\*Rounded to the nearest  $0.005 \times 10^{-2}$ .

## REFERENCES.

1. Hofbauer, G. Sitzugsber. Akad. Wiss. Wien, Math. Naturwiss. Kl. Abt. 2A 1914, 123, 2001.
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## COMPONENTS:

1. Radon-222;  ${}^{222}_{86}\text{Rn}$ ; 14859-67-7
2. Propanoic Acid;  $\text{C}_3\text{H}_6\text{O}_2$ ; 79-09-4

## EVALUATOR:

H. L. Clever  
 Department of Chemistry  
 Emory University  
 Atlanta, GA 30322  
 U.S.A.

August 1978

## CRITICAL EVALUATION:

Hofbauer (1) reported values of the radon-222 solubility in propanoic acid at temperatures of 293.85 and 302.85 K, and Nussbaum and Hursh (2) reported three values between temperatures of 298.15 and 323.15 K.

The two data sets show more scatter than the same two laboratory's results for acetic acid. It is likely that the increase in solubility shown by the Nussbaum and Hursh data between temperatures of 310.15 and 323.15 K is in error. The 323.15 K solubility value was not used in the linear regression described below.

The two data sets were combined on a one to one weight bases in a linear regression of a Gibbs energy equation linear in temperature. The result gives the tentative values for the thermodynamic changes for the transfer of one mole of radon from the gas at a partial pressure of 101.325 kPa to the hypothetical unit mole fraction solution of

$$\Delta G^\circ/\text{J mol}^{-1} = -RT \ln X_1 = -15,919 + 85.697 T$$

$$\text{Std. Dev. } \Delta G^\circ = 159.7, \text{ Coef. corr.} = 0.9661$$

$$\Delta H^\circ/\text{J mol}^{-1} = -15,919, \Delta S^\circ/\text{J K}^{-1} \text{ mol}^{-1} = -85.697$$

The tentative solubility and Gibbs energy values as a function of temperature are in Table 1.

TABLE 1. The solubility of radon-222 in propanoic acid. Tentative values of the mole fraction solubility at 101.325 kPa partial pressure radon and the Gibbs energy change as a function of temperature.

T/K	Mol Fraction $X_1 \times 10^2$	$\Delta G^\circ/\text{J mol}^{-1}$
293.15	2.29	9,203.1
298.15	2.05	9,631.6
303.15	1.85	10,060
308.15	1.67	10,489
313.15	1.51	10,917
318.15	1.37	11,346
323.15	1.25	11,774

## REFERENCES.

1. Hofbauer, G. Sitzungsber. Akad. Wiss. Wien, Math. Naturwiss. Kl. Abt. 2A 1914, 123, 2001.
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<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>1. Radon; <math>^{222}_{86}\text{Rn}</math>; 14859-67-7</li> <li>2. 2-Methyl Propanoic Acid; <math>\text{C}_4\text{H}_8\text{O}_2</math>; 79-31-2</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Hofbauer, G.</p> <p><u>Sitzungsber. Akad. Wiss. Wien, Math. Naturwiss. Kl. Abt. 2A 1914, 123, 2001.</u></p>						
<p>VARIABLES:</p> <p>T/K: 293.05</p>	<p>PREPARED BY:</p> <p>W. Gerrard</p>						
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<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Radon; <math>^{222}_{86}\text{Rn}</math>; 14859-67-7</li> <li>Butanoic Acid; <math>\text{C}_4\text{H}_8\text{O}_2</math>; 107-92-6</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Hofbauer, G.</p> <p><u>Sitzungsber. Akad. Wiss. Wien, Math. Naturwiss. Kl. Abt. 2A 1914, 123, 2001.</u></p>						
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323.15	3.38	6.33																																
T/K	Mol Fraction $X_1 \times 10^2$	$\Delta G^\circ/\text{J mol}^{-1}$																																
298.15	4.80	7526.7																																
303.15	4.44	7848.1																																
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<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Radon; <math>^{222}_{86}\text{Rn}</math>; 14859-67-7</li> <li>Octanoic Acid, <math>\text{C}_8\text{H}_{16}\text{O}_2</math>; 124-07-2</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Nussbaum, E.; Hursh, J. B.</p> <p><u>J. Phys. Chem.</u> 1958, <u>62</u>, 81 - 84.</p>																																	
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<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Radon; <math>^{222}_{86}\text{Rn}</math>; 14859-67-7</li> <li>Decanoic Acid; <math>\text{C}_{10}\text{H}_{20}\text{O}_2</math>; 334-48-5</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Nussbaum, E.; Hursh, J. B.</p> <p><u>J. Phys. Chem.</u> 1958, <u>62</u>, 81 - 84.</p>						
<p>VARIABLES:</p> <p>T/K: 310.15</p>	<p>PREPARED BY:</p> <p>W. Gerrard</p>						
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<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Radon; <math>^{222}_{86}\text{Rn}</math>; 14859-67-7</li> <li>Undecanoic Acid; <math>\text{C}_{11}\text{H}_{22}\text{O}_2</math>; 112-37-8</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Nussbaum, E.; Hursh, J. B.</p> <p><u>J. Phys. Chem.</u> 1958, <u>62</u>, 81-84.</p>						
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<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Radon; <math>^{222}_{86}\text{Rn}</math>; 14859-67-7</li> <li>(Z)-9-Octadecenoic Acid (Oleic Acid); <math>\text{C}_{18}\text{H}_{34}\text{O}_2</math>; 112-80-1</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Nussbaum, E.; Hursh, J. B.</p> <p><i>J. Phys. Chem.</i> 1958, <u>62</u>, 81 - 84.</p>																																	
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<b>COMPONENTS:</b> 1. Radon; $^{222}_{86}\text{Rn}$ ; 14859-67-7 2. Acetic Acid Ethyl Ester (Ethyl Acetate); $\text{C}_4\text{H}_8\text{O}_2$ ; 141-78-6	<b>ORIGINAL MEASUREMENTS:</b> Ramstedt, E.  <u>Le Radium</u> 1911, <u>8</u> , 253-256.																																										
<b>VARIABLES:</b> T/K: 255.15 - 291.15	<b>PREPARED BY:</b> W. Gerrard																																										
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<b>APPARATUS/PROCEDURE:</b> Two tubes connected by a wide tap. To determine concentration of radon, each tube is placed in a condenser.	<b>ESTIMATED ERROR:</b>  <b>REFERENCES:</b>																																										

<b>COMPONENTS:</b> 1. Radon-222; $^{222}_{86}\text{Rn}$ ; 14859-67-7 2. Acetic Acid Pentyl Ester (Amyl Acetate); $\text{C}_7\text{H}_{14}\text{O}_2$ ; 628-63-7	<b>ORIGINAL MEASUREMENTS:</b> Lurie, A. Thesis University of Grenoble, 1910 Microfilm available. See also Tables annuelles de constantes et donnees numeriques de chemie, de physique et de technologie 1913 (for 1911), 2, 401.																		
<b>VARIABLES:</b> T/K: 253.15 - 343.15	<b>PREPARED BY:</b> W. Gerrard																		
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<b>METHOD /APPARATUS/PROCEDURE:</b> The concentration of radon in the gas and liquid phases determined by measurements of radioactivity. An aluminum foil electroscope was used to measure the radioactivity. Diagrams given by Lurie.	<b>SOURCE AND PURITY OF MATERIALS:</b> 1. Radon-222. 2. Acetic Acid Pentyl Ester (Amyl Acetate). Purity of liquid not specified.																		
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<b>COMPONENTS:</b> 1. Radon; $^{222}_{86}\text{Rn}$ ; 14859-67-7 2. 1,2,3-Propanetriol, Triacetate (Triacetin); $\text{C}_9\text{H}_{14}\text{O}_6$ ; 102-76-1	<b>ORIGINAL MEASUREMENTS:</b> Nussbaum, E.; Hursh, J. B.  <u>J. Phys. Chem.</u> 1958, <u>62</u> , 81 - 84.																								
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<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Radon; <math>^{222}_{86}\text{Rn}</math>; 14859-67-7</li> <li>Octanoic acid; 1,2,3-propanetriyl ester (Trioctanoin); <math>\text{C}_{27}\text{H}_{50}\text{O}_6</math>; 538-23-8</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Nussbaum, E.; Hursh, J. B.</p> <p><u>J. Phys. Chem.</u> 1958, <u>62</u>, 81 - 84.</p>																																	
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<p>APPARATUS/PROCEDURE:</p> <p>Two tubes connected by a wide tap. To determine concentration of radon, each tube is placed in a condenser.</p> <p>The mole fraction solubilities calculated above are for a radon partial pressure of 101.325 kPa.</p>	<p>ESTIMATED ERROR:</p> <p>REFERENCES:</p>																														

<b>COMPONENTS:</b> 1. Radon-222; $^{222}_{86}\text{Rn}$ ; 14859-67-7 2. Nitrobenzene; $\text{C}_6\text{H}_5\text{NO}_2$ ; 98-95-3	<b>ORIGINAL MEASUREMENTS:</b> Trautenberg, H.F.R.  <u>Phys. Z.</u> 1904, <u>5</u> , 130 - 134.						
<b>VARIABLES:</b>	<b>PREPARED BY:</b>  W. Gerrard						
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="302 511 1013 645" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Ratio compared with water*</th> <th style="text-align: center;">Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td style="text-align: center;">"Room temperature"</td> <td style="text-align: center;">18.06</td> <td style="text-align: center;">5.42</td> </tr> </tbody> </table> <p style="margin-left: 40px;">*water was taken as 0.3</p> <p>The author reported his solubility value as an absorption coefficient based on the concentration ratio of radon in the gas and in the liquid phases. It has been labelled as an Ostwald coefficient above. The solubility was measured at a radon partial pressure of less than 0.1 kPa. The liquid was also saturated with air as a carrier gas at a pressure of about 100 kPa.</p>		T/K	Ratio compared with water*	Ostwald Coefficient L	"Room temperature"	18.06	5.42
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<b>METHOD:</b> Measurement of radioactivity.	<b>SOURCE AND PURITY OF MATERIALS:</b> Not stated.						
<b>APPARATUS/PROCEDURE:</b>  Electroscope for the measurement of radioactivity.	<b>ESTIMATED ERROR:</b> Trautenberg's values appear to be low when compared with values reported by other workers.						
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<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>1. Radon-222; <math>^{222}_{86}\text{Rn}</math>; 14859-67-7</li> <li>2. Petroleum Products</li> </ol>	<p>EVALUATOR:</p> <p>William Gerrard  Department of Chemistry  The Polytechnic of North London  Holloway, London N7 8DB  U.K.</p> <p>May 1977</p>
<p>CRITICAL EVALUATION:</p> <p>Petroleum.</p> <p>There are three reports of the solubility of radon-222 in petroleum. Hofman's (1) values were based on a primitive electroscopic technique and are of doubtful accuracy. Lurie (2) cited Hofman's values and gave his own as being in approximate agreement. Trautenberg's (3) value appears to be much too small.</p> <p>Paraffin oil.</p> <p>There are three reports of the solubility of radon-222 in paraffin oil. Two of the reports give the temperature as only "room temperature." Schrod't's (4) value is too large and Trautenberg's (3) value is too small. Ramstedt's (5) values of the radon Ostwald coefficient at 273.15 and 291.15 K are classed as tentative.</p> <p>Petroleum ether.</p> <p>Trautenberg's (3) value is too small.</p> <p>REFERENCES.</p> <ol style="list-style-type: none"> <li>1. Hofman, R. <u>Phys. Z.</u> 1905, <u>6</u>, 339.</li> <li>2. Lurie, A. Thesis 1910, University of Grenoble.</li> <li>3. Trautenberg, H. F. R. <u>Phys. Z.</u> 1904, <u>5</u>, 130.</li> <li>4. Schrod't, O. <u>Roentgenpraxis (Leipzig)</u> 1938, <u>10</u>, 743.</li> <li>5. Ramstedt, E. <u>Le Radium</u> 1911, <u>8</u>, 253.</li> </ol>	

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<b>VARIABLES:</b>  T/K: 255.15 - 333.15	<b>PREPARED BY:</b> W. Gerrard												
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<p>APPARATUS/PROCEDURE:</p> <p>Electroscope, and glass containers for measurement of radioactivity.</p>	<p>ESTIMATED ERROR:</p> <p>Of doubtful accuracy because of the primitive electroscope technique.</p> <p>REFERENCES:</p> <p>1. Trautenberg, H.F.R. <u>Phys. Z.</u> 1904, <u>5</u>, 130.</p>												



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<p>VARIABLES:</p> <p>T/K: 273.15 - 291.15</p>	<p>PREPARED BY:</p> <p>W. Gerrard</p>						
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<p>VARIABLES:</p> <p>T/K: 252.15 - 338.15</p>	<p>PREPARED BY:</p> <p>W. Gerrard May 1977</p>																					
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<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Radon-222; <math>^{222}_{86}\text{Rn}</math>; 14859-67-7</li> <li>Olive Oil</li> </ol>	<p>EVALUATOR:</p> <p>William Gerrard  Department of Chemistry  The Polytechnic of North London  Holloway, London N7 8DB  U.K.</p> <p>May 1977</p>												
<p>CRITICAL EVALUATION:</p> <p>Lurie (1) reports Ostwald coefficients for radon-222 in olive oil at temperatures of 273.15, 288.15, 313.15 and 333.15 K. Both Strasburger (2) and Schrodtt (3) report a "room temperature" Ostwald coefficient which agrees with the Lurie 288.15 K value. Nussbaum and Hursh (4) report Ostwald coefficients at 298.15 and 310.15 K which are about one-third the Lurie values, and may be taken as reliable.</p> <p>The mole fraction solubility of radon-222 in olive oil was calculated assuming that olive oil is 1,2,3-propanetriyl ester of (Z)-9-octadecenoic acid, or triolein, of molecular weight 885.46. The Nussbaum and Hursh solubility values are preferred.</p> <p>The tentative values of the thermodynamic properties of solution for the transfer of one mole of radon from the gas at 101.325 kPa (1 atm) to the hypothetical unit mole fraction solution are</p> $\Delta G^{\circ}/J \text{ mol}^{-1} = -RT \ln X_1 = -11.914 + 51.962 T$ $\Delta H^{\circ}/J \text{ mol}^{-1} = -11.914, \Delta S^{\circ}/J \text{ K}^{-1} \text{ mol}^{-1} = -51.962$ <p>A table of tentative mole fraction solubility and Gibbs energy values as a function of temperature appears on the radon + olive oil data sheet of Nussbaum and Hursh, and in Table 1 below.</p> <p>Lawrence, Loomis, Tobias and Turpin (5) cite Bunsen coefficients for radon-222 in olive oil which they attribute to Lurie and state to be given in the International Critical Tables (6). The values are 0.01 times the values reported by Lurie. They are not found in the International Critical Tables, but they are in Seidell and Linke (7) which cite no other of Lurie's data. The radon in olive oil data cited in these references (5,7) are in error and should not be used.</p> <p>REFERENCES.</p> <ol style="list-style-type: none"> <li>Lurie, A. Thesis 1910, University of Grenoble.</li> <li>Strasburger, J. <u>Deut. Med. Wochsehr.</u> 1923, <u>49</u>, 1459.</li> <li>Schrodtt, O. <u>Roentgenpraxis (Leipzig)</u> 1938, <u>10</u>, 743.</li> <li>Nussbaum, E.; Hursh, J. B. <u>J. Phys. Chem.</u> 1958, <u>62</u>, 81.</li> <li>Lawrence, J. H.; Loomis, W. F.; Tobias, C. A.; Turpin, F. H. <u>J. Physiol.</u> 1946, <u>105</u>, 197.</li> <li>Washburn, E. W. Editor, International Critical Tables, McGraw Hill Co., New York 1928.</li> <li>Seidell, A.; Linke, W. F. Solubilities of Inorganic and Organic Compounds, American Chemical Society, 1958, 1965.</li> </ol> <p>TABLE 1. The solubility of radon-222 in olive oil. Tentative values of the mole fraction solubility at a radon partial pressure of 101.325 kPa and the Gibbs energy change as a function of temperature.</p> <table border="1" data-bbox="420 1753 979 1937"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^2</math></th> <th><math>\Delta G^{\circ}/J \text{ mol}^{-1}</math></th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>23.6</td> <td>3,578.7</td> </tr> <tr> <td>303.15</td> <td>21.8</td> <td>3,838.5</td> </tr> <tr> <td>308.15</td> <td>20.2</td> <td>4,098.3</td> </tr> </tbody> </table>		T/K	Mol Fraction $X_1 \times 10^2$	$\Delta G^{\circ}/J \text{ mol}^{-1}$	298.15	23.6	3,578.7	303.15	21.8	3,838.5	308.15	20.2	4,098.3
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<b>COMPONENTS:</b> 1. Radon-222; $^{222}_{86}\text{Rn}$ ; 14859-67-7 2. Fats and Oils for Ointment Base.	<b>ORIGINAL MEASUREMENTS:</b> Schrodtt, O.  <u>Roentgenpraxis (Leipzig) 1938, 10, 743.</u>																						
<b>VARIABLES:</b>  T/K: "Room temperature" (?)	<b>PREPARED BY:</b> W. Gerrard																						
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<b>APPARATUS/PROCEDURE:</b>  Glass bulbs and electroscope. Diagrams given by Schrodtt.	<b>ESTIMATED ERROR:</b>																						
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<p>COMPONENTS:</p> <ol style="list-style-type: none"> <li>Radon-222; <math>^{222}_{86}\text{Rn}</math>; 14859-67-7</li> <li>Colza oil</li> </ol>	<p>ORIGINAL MEASUREMENTS:</p> <p>Lurie, A. Thesis University of Grenoble, 1910 Microfilm available. See also Tables annuelles de constantes et donnees numeriques de chimie, de physique et de technologie 1913 (for 1911), <u>2</u>, 401.</p>														
<p>VARIABLES:</p> <p>T/K: 270.15 - 473.15</p>	<p>PREPARED BY:</p> <p>W. Gerrard</p>														
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<p>VARIABLES:</p> <p>T/K: 310.15</p>	<p>PREPARED BY:</p> <p>W. Gerrard</p>
<p>EXPERIMENTAL VALUES:</p> <p>Knaffle-Lenz reported that at 310.15 K the absorption coefficient for blood is 0.42 times that for water.</p>	
<p>AUXILIARY INFORMATION</p>	
<p>METHOD:</p>	<p>SOURCE AND PURITY OF MATERIALS:</p>
<p>APPARATUS/PROCEDURE:</p>	<p>ESTIMATED ERROR:</p>
	<p>REFERENCES:</p>

<p>COMPONENTS:</p> <p>1. Radon-222; <math>^{222}_{86}\text{Rn}</math>; 14859-67-7</p> <p>2. Egg Lecithin</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Tasca, M.</p> <p><u>Radiol. Med. (Milan) 1940, 27, 401.</u></p>
<p>VARIABLES:</p>	<p>PREPARED BY:</p> <p>W. Gerrard</p>
<p>EXPERIMENTAL VALUES:</p> <p>Tasca reported the the "quantity" of radon retained by egg lecithin is 40 time that retained by an equal volume of water, at a temperature which was not clearly stated, but could have been room temperature.</p> <p>Nussbaum and Hursh (1) cite Tasca and express this solubility as the Ostwald coefficient, 6.4 at 310.15 K, presumably obtained from <math>40 \times 0.16</math>, where 0.16 is the radon Ostwald coefficient in water at 310.15 K.</p>	
<p>AUXILIARY INFORMATION</p>	
<p>METHOD:</p>	<p>SOURCE AND PURITY OF MATERIALS:</p>
<p>APPARATUS/PROCEDURE:</p>	<p>ESTIMATED ERROR:</p> <p>REFERENCES:</p> <p>1. Nussbaum, E.; Hursh, J. B. <u>J. Phys. Chem. 1958, 62, 81.</u></p>

<p>COMPONENTS:</p> <ol style="list-style-type: none"><li>1. Radon-219 (Actinium Emanation); <math>^{219}_{86}\text{Rn}</math>; 14835-02-0</li><li>2. Liquids</li></ol>	<p>EVALUATOR:</p> <p>William Gerrard Department of Chemistry The Polytechnic of North London Holloway, London N7 8DB United Kingdom</p>
<p>CRITICAL EVALUATION:</p> <p>The half life of radon-219 (actinon) is only 3.92 seconds. The mean values of the partition coefficient show a variation from 5 to 10 % (one is 20 %) from the observed maximum. The partition coefficient for the non-aqueous liquid, or the aqueous solution, was given as that compared with water, taken to be 2. The evaluator contends that it is much more reliable to take the observed radon-222 values as those for radon-219 (actinon).</p> <p>Hevesy's (1,2) results for the solubility of radon-219 in various liquids are on the following data sheets.</p> <ol style="list-style-type: none"><li>1. Hevesy, G. <u>Phys. Z.</u> 1911, <u>12</u>, 1214.</li><li>2. Hevesy, G. <u>J. Phys. Chem.</u> 1912, <u>16</u>, 429.</li></ol>	

<b>COMPONENTS:</b> 1. Radon-219 (Actinium Emanation); $^{219}_{86}\text{Rn}$ ; 14835-02-0 2. Water; $\text{H}_2\text{O}$ ; 7732-18-5 3. Electrolytes	<b>ORIGINAL MEASUREMENTS:</b> Hevesy, G.  Phys. Z. 1911, <u>12</u> , 1214 J. Phys. Chem. 1912, <u>16</u> , 429-453.												
<b>VARIABLES:</b> T/K: "Ordinary Temperatures"	<b>PREPARED BY:</b> W. Gerrard												
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<b>AUXILIARY INFORMATION</b>													
<b>METHOD:</b> Dried air was passed over a radon-219 preparation, and then through a column of liquid in which part was absorbed, and the remainder passed to the ionization chamber of an electroscope.	<b>SOURCE AND PURITY OF MATERIALS:</b>  No details.												
<b>APPARATUS/PROCEDURE:</b> Assembly for the "dynamical flow method" as distinct from the shaking method. Radioactivity was measured. The partial pressure of radon-219 was extremely small.	<b>ESTIMATED ERROR:</b> $\delta L/L = 0.05 - 0.10$  <b>REFERENCES:</b>												



<b>COMPONENTS:</b> 1. Radon-219 (Actinium Emanation); $^{219}_{86}\text{Rn}$ ; 14835-02-0 2. Hydrocarbons	<b>ORIGINAL MEASUREMENTS:</b> Hevesy, G.  <u>Phys. Z.</u> 1911, <u>12</u> , 1214 <u>J. Phys. Chem.</u> 1912, <u>16</u> , 429-453.												
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<p>CRITICAL EVALUATION:</p> <p>The half life of radon-220 (thoron), <math>^{220}_{86}\text{Rn}</math>, is 54.5 seconds. Therefore the reported absorption coefficients must be accepted with caution. Boyle (1) used a streaming method (diagram given in the original paper) and placed the following liquids in the order of increasing solutivity: but did not give actual values: <math>\text{CuSO}_4</math> (aqueous) &lt; <math>\text{CaCl}_2</math> (aqueous) &lt; water &lt; <math>\text{H}_2\text{SO}_4</math> &lt; alcohol &lt; petroleum; "the same as for radon (radon-222)."</p> <p>Klaus (2) reported the solubility of radon-220 in water and petroleum (see the following two data sheets).</p> <p>The evaluator contends that it is much more reliable to take the observed values for radon-222 as the values for radon-220 (thoron).</p> <p>References: 1. Boyle, R.W., <u>Le Radium</u>, 1910, <u>7</u>, 200. See also  Boyle, R.W., <u>Bull. Macdonald Physics Bldg.</u>, 1910, <u>1</u>, 52.</p> <p>2. Klaus, A. <u>Phys. Z.</u> 1905, <u>6</u>, 820.</p>	

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<p>APPARATUS/PROCEDURE:</p> <p>Gas cylinder, 500 cm<sup>3</sup>. Absorption vessel, 1.25 dm<sup>3</sup>, which is shaken. Author gave a diagram.</p>	<p>ESTIMATED ERROR:</p> <p>REFERENCES:</p>				

<b>COMPONENTS:</b> 1. Radon-220 (Thorium Emanation); $^{220}_{86}\text{Rn}$ ; 22481-88-7 2. Petroleum	<b>ORIGINAL MEASUREMENTS:</b> Klaus, A.  <u>Phys. Zeit.</u> , 1905, <u>6</u> , 820.				
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## SYSTEM INDEX

Underlined page numbers refer to the evaluation text and those not underlined to the compiled tables for that system. The compounds are listed in the order as in the Chemical Abstract indexes, for example toluene is listed as benzene, methyl- and dimethylsulfoxide is listed as methane, sulfinylbis-.

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